

# **Studies on Some Novel Methods of Synthesis and Sintering of Nanocrystalline Ceramics**

*By*

**SANJAY KUMAR. D**

(Enrolment No: CHEM 02 2011 04 001)

**Indira Gandhi Centre for Atomic Research, Kalpakkam**

*A Thesis Submitted to the  
Board of Studies in Chemical Sciences  
In partial fulfillment of requirements  
For the Degree of*

**DOCTOR OF PHILOSOPHY**

*of*

**HOMI BHABHA NATIONAL INSTITUTE**



**July, 2017**



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## **DECLARATION**

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**Sanjay Kumar. D**

## List of Publications

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### Journal

#### a. Published

1. Bulk synthesis of nanocrystalline urania powders by citrate gel-combustion method  
**D. Sanjay Kumar**, K. Ananthasivan, R. Venkata Krishnan, S. Amirthapandian, Arup Dasgupta, J. Nucl. Mater. 468 (2016) 178-193.
2. Studies on the synthesis of nanocrystalline  $Y_2O_3$  and  $ThO_2$  through volume combustion and their sintering  
**D. Sanjay Kumar**, K. Ananthasivan, R. Venkata Krishnan, S. Amirthapandian, Arup Dasgupta, J. Nucl. Mater. 479 (2016) 585-592.
3. A novel gel combustion procedure for the preparation of foam and porous pellets of  $UO_2$   
**D. Sanjay Kumar**, K. Ananthasivan, R. Venkata Krishnan, Arup Dasgupta, J. Nucl. Mater. 483 (2017) 199-204.
4. Synthesis of monoclinic and cubic (metastable) nanocrystalline  $HfO_2$  through the nitrate fusion technique  
**D. Sanjay Kumar**, K. Ananthasivan, R. Venkata Krishnan, S. Amirthapandian, T. R. Ravindran, S. Balakrishnan, Ceram. Int. 43 (2017) 12623-12632.
5. Citrate gel-combustion synthesis and sintering of nanocrystalline  $ThO_2$  powders  
**D. Sanjay Kumar**, K. Ananthasivan, S. Amirthapandian, Arup Dasgupta, G. Jogeswara Rao, J. Nucl. Mater. 497 (2017) 16-29.
6. Reaction mechanism and kinetic analysis of citrate gel-combustion synthesis of nanocrystalline urania  
**D. Sanjay Kumar**, K. Ananthasivan, R. Venkata Krishnan, Abhiram Senapathi, J. Therm. Anal. Calorim. 2017 (DOI: 10.1007/s10973-017-6695-4).

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1. Nitrate fusion synthesis and two-step sintering of nanocrystalline yttria stabilized hafnia powders

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2. Low Temperature Two-Step Sintering of nanocrystalline  $\text{UO}_2$

**D. Sanjay Kumar**, K. Ananthasivan, Arup Dasgupta, J. Nucl. Mater. **2018**.

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1. Gel-Combustion Synthesis of Nanocrystalline Cerium Oxide and Its Powder Characteristics

S. Balakrishnan, **D. Sanjay Kumar**, K. Ananthasivan, T. Indian I. Metals **2015**, 68 S243-S252.

2. High pressure Raman spectroscopic studies on nanocrystalline  $\text{ThO}_2$ ,

K. Kamali, K. Ananthasivan, T. R. Ravindran, **D. Sanjay Kumar**, J. Nucl. Mater. 493 (2017) 77-83.

3. High pressure studies on Thorium-Praseodymium mixed oxides,

K. A. Irshad, **D. Sanjay Kumar**, **G. Paneerselvam**, K. Ananthasivan, N. V. Chandra Shekar, S. Kalavathi, J. Nucl. Mater. 498 (2018) 221-226.

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1. TEM study of nanocrystalline  $\text{UO}_2$  prepared by gel-combustion method,

**D. Sanjay Kumar**, K. Ananthasivan, S. Balakrishnan, Amrita Pandian, Arup Dasgupta, K. Nagarajan, International Conference on Electron Microscopy and XXXIV Annual Meeting of the Electron Microscope Society of India (EMSI-2013), SINP, Kolkata, India, July 2013.

2. Citrate gel-combustion synthesis of nanocrystalline cerium oxide  
S. Balakrishnan, **D. Sanjay Kumar**, K. Ananthasivan, International Symposium for Research Scholars on Metallurgy, Materials Science and Engineering (ISRS 2014), IIT-M, Chennai, India, December 2014.
3. Carbon coated urania foam (CCUF)  
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4. Stabilization of the cubic structure in nanocrystalline (nc)  $\text{HfO}_2$   
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5. Low Temperature Two-Steps Sintering (LTTSS) - An Innovative Method for Consolidating Porous  $\text{UO}_2$  Pellets  
**D. Sanjay Kumar**, K. Ananthasivan, Abhiram Senapati, R. Venkata Krishnan, Chemistry in nuclear technology (CHEMNUT-2015), IGCAR, Kalpakkam, India, July 2015.
6. Microstructural investigations of nanocrystalline yttria stabilized hafnia prepared by nitrate fusion technique  
**D. Sanjay Kumar**, K. Ananthasivan, S. Amirthapandian, Arup Dasgupta, International Conference on Electron Microscopy and XXXVII Annual Meeting of the Electron Microscope Society of India (EMSI-2016), IIT-BHU, Varanasi, India, June 2016.
7. TEM investigation of nanocrystalline  $\text{ThO}_2$  prepared by citrate gel-combustion  
**D. Sanjay Kumar**, K. Ananthasivan, S. Amirthapandian, Arup Dasgupta, International Conference on Electron Microscopy and XXXVII Annual Meeting of the Electron Microscope Society of India (EMSI-2016), IIT-BHU, Varanasi, India, June 2016.





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## Synopsis

Nuclear energy plays an important role in meeting the energy demand of the world without the release of CO/CO<sub>2</sub> to the environment<sup>1</sup>. In the Indian context, the increase in energy demand vis-a-vis the non-availability of sufficient alternate conventional sources of energy have necessitated the nuclear energy to play a key role in meeting the energy demand<sup>2</sup>. International nuclear communities have taken initiatives to resolve the problems related to the efficient utilization of fuels, the management and minimization of radiotoxic waste, economics, recycling, non-proliferation and transmutation of minor actinides (Am, Np and Cm). Oxide fuels with enhanced performance characteristics are being developed to be deployed in the Generation IV reactors<sup>3</sup>. They are pertinent in the Indian context as well. The class of advanced materials developed for such applications are broadly known as “nuclear materials”. In this work, an effort has been made to synthesize and characterize some “advanced nuclear materials” pertinent to fission reactors. Recent research on nano nuclear materials reveals that nanocrystalline (nc) fission reactor fuels exhibit superior properties (both physical and chemical) as compared to their microcrystalline counterparts<sup>45</sup>. Hence, R&D on these materials are useful and relevant to nuclear technology.

Nc-Y<sub>2</sub>O<sub>3</sub>, nc-HfO<sub>2</sub> and nc-yttria stabilized hafnia (YSH) are used extensively in high temperature applications. HfO<sub>2</sub> and YSH (both pure and doped with aliovalent cations) find application in the nuclear industry owing to their low thermal expansion coefficient, structural stability and chemical inertness even at high temperature<sup>6</sup>. Since, Y<sub>2</sub>O<sub>3</sub>, HfO<sub>2</sub> and YSH are thermodynamically compatible with molten uranium at temperatures above 1400 K; crucibles made out of HfO<sub>2</sub> and YSH would be useful for applications involving containment of molten U.

Current challenges in the preparation of nano nuclear materials include scaling-up the preparation of nc powders (about 100g), optimizing their consolidation parameters and choice of an advanced sintering method. In view of the above two novel techniques, viz., citrate gel-combustion (nc-urania, nc-thoria and nc-yttria) and salt melt synthesis (nc-HfO<sub>2</sub> and nc-YSH) have been investigated in this study for synthesizing nc nuclear materials in bulk. The systematic dependence of the reaction as well as the properties of these (nc-urania and nc-thoria) powders on the composition of the combustion mixture [R = fuel to nitrate (mole ratio)] was investigated. It was demonstrated for the first time that “volume combustion reaction (VCR)”

takes place in citrate gels containing thorium nitrate, yttrium nitrate and uranyl nitrate with citric acid at an R value of 0.125, 0.17 and 0.25 respectively. Reaction mechanism pertaining to citrate gel-combustion and salt melt synthesis (SMS) was also investigated. It was demonstrated for the first time that nc-HfO<sub>2</sub> powders (30 g) i.e. either the thermodynamically stable monoclinic phase or the metastable cubic phase could be synthesized by tailoring the nitrite to nitrate mole ratio ( $\Phi$ ) in eutectic mixtures containing the nitrates of potassium and sodium along with NaNO<sub>2</sub>. Similarly, bulk quantities of monodisperse nc-YSH (30 g) powders were also prepared for the first time by using SMS at a temperature as low as 673 K. The powder properties, compaction pressure and mode of sintering of nanocrystalline materials play an important role in the fabrication of dense monoliths. Hence, all these powders were characterized by different techniques. Further, it is difficult to sinter nc materials to dense monoliths with uniform microstructure and submicron grains due to significant grain coarsening. Hence, these powders were sintered by different methods viz., conventional sintering (CS), two-step sintering (TSS) and Spark Plasma Sintering (SPS). The utility of two-step sintering proposed by Chu et al.<sup>7</sup> (TSS<sub>C</sub>) and Chen and Wang<sup>8</sup> (TSS<sub>CW</sub>) was also investigated. Both the synthesis and sintering procedures were optimized to obtain dense small sintered crucibles made out of nc-HfO<sub>2</sub> and nc-YSH. Further, the utility of these small crucibles for holding molten U (compatibility test) was also investigated. An attempt has been made to prepare fine grained sintered bodies from nc-Y<sub>2</sub>O<sub>3</sub>, nc-HfO<sub>2</sub> and nc-YSH powders by using SPS as well.

Direct oxide reduction (DOR)<sup>9</sup> of metal oxide to metal is an attractive alternative compared to the conventional pyrometallurgical process for the production of uranium. In the DOR process, open porosity plays a key role in the complete reduction of uranium, necessitating a porous sintered body an important prerequisite. In this context, a novel gel based procedure was devised for the first time to obtain a dense UO<sub>2</sub> foam and porous UO<sub>2</sub> pellets. The procedure was optimized by controlling various parameters viz., fuel (sucrose / citric acid) to nitrate content, carbon residue, compaction pressure and mode of sintering.

## **Chapter 1 – Introduction**

Chapter 1 presents a brief introduction highlighting the importance of nuclear energy and India's three stage nuclear power programme. The importance of high burn-up structure observed in the irradiated fuel has also been brought out. Nano nuclear materials, their preparation, properties

and their potential applications in the nuclear power industry are also discussed. Different conventional and advanced methods used in their consolidation and sintering are discussed in detail. Advanced sintering techniques which are used to densify nanocrystalline powders without grain coarsening are discussed.

## **Chapter 2 – Experimental**

Chapter 2 describes the details pertaining to the starting materials, experimental procedure and details of instrumental analyses. This chapter explains in detail about the different synthetic procedures adopted for the scaled-up synthesis of nc urania,  $\text{ThO}_2$ ,  $\text{Y}_2\text{O}_3$ ,  $\text{HfO}_2$  and YSH powders. Chapter 2 also explains a novel gel-combustion procedure used in the preparation of foam and porous pellets of  $\text{UO}_2$ . Methods of characterization of powders, green pellets, sintered pellets, foam and porous pellets are described in this chapter. Methods used in the microstructural investigation of these powders [scanning electron microscopy (SEM) and transmission electron microscopy (TEM) coupled with electron energy loss spectroscopy (EELS)] are presented in detail. Thermal methods of analysis used to elucidate the plausible mechanism of the gel-combustion reaction and SMS by using differential scanning calorimetry (DSC), simultaneous thermogravimetry and differential thermal analysis coupled with mass spectrometry (TG-DTA-MS) are also described in detail. The green pellets made out of the powders derived in this study were sintered by using three different methods viz., CS and TSS ( $\text{TSS}_\text{C}$  and  $\text{TSS}_\text{CW}$ ). This chapter also describes the details pertaining to the SPS investigations on  $\text{Y}_2\text{O}_3$ ,  $\text{HfO}_2$  and YSH powders. Experiments carried out to find out the critical compaction pressure have also been described. Details of the experiments performed to ascertain the compatibility of sintered  $\text{HfO}_2$  and YSH cups with molten U have also been detailed in this chapter. The procedure used in the preparation of samples for microstructural investigations have also been described.

## **Chapter 3 – Synthesis, Characterization and Sintering of Nanocrystalline Urania**

Chapter 3 deals with the bulk synthesis (60 g) of nanocrystalline (nc) free flowing urania powders with crystallite size ranging from 38-252 nm for the first time. A systematic study of the influence of the fuel (citric acid) to nitrate ratio (R) on the characteristics of the powders has also been carried out. Mixtures with an “R” value 0.25 exhibited a vigorous auto-ignition reaction (VCR). This reaction was investigated with DSC and in-situ TG-DTA-MS. SEM investigation of

some of these powders revealed the presence of agglomerates with irregular exfoliated morphology, while analysis of their TEM images confirmed nanocrystallinity. EELS of some calcined ( $\alpha$ - $\text{U}_3\text{O}_8$ ) and hydrogen reduced ( $\text{UO}_2$ ) powders, testified the covalent nature of the U-O bond. The reaction mechanism and kinetic parameters pertaining to citrate gel-combustion synthesis of nc-urania were determined. All powders were consolidated at different compaction pressures and were sintered (CS and TSS). The extent of sintering in all sintered products was determined by measuring their sintered density, porosity and shrinkage characteristics. A maximum sintered density of  $98.0 \pm 0.4$  % theoretical density (T.D) was obtained in this study. Selected samples of sintered specimens were characterized by using XRD and SEM to determine the constituent phases and the influence of the powder characteristics on their microstructure sizes of pores and grains and the final sintered density. The sintered pellets comprised sintered grains with grain size ranging from 1 – 15  $\mu\text{m}$ .

#### **Chapter 4 – Preparation of $\text{UO}_2$ foam and porous pellets of $\text{UO}_2$**

Chapter 4 reports the first time preparation of  $\text{UO}_2$  foam (sucrose gel-combustion) and porous pellets of  $\text{UO}_2$  (citrate gel-combustion). The final products possessed a high matrix density and interconnected porosity. The utility of TSS (1073 K, 30 min and 1473 K, 4 h) for obtaining these porous bodies was also demonstrated for the first time. The foams and pellets possessed meso and macro pores. Sucrose to nitrate mole ratio of 2.4 was best suited for obtaining urania foam with good handling strength. The porous pellets were found to be more suitable for the end application for they had lesser carbon residue and a higher overall density. A citric acid to nitrate mole ratio of 0.25 and a compaction pressure of 180 MPa were found to be optimal for obtaining a pellet with 40 % porosity.

#### **Chapter 5 – Synthesis, Characterization and Sintering of Nanocrystalline Thoria**

Chapter 5 deals with the bulk synthesis (60 g) of nc free flowing  $\text{ThO}_2$  powders. These investigations helped to establish the influence of R on the characteristics of the final product. It was also demonstrated that VCR occurs at a fuel (citric acid) to oxidant (nitrate) ratio close to that demanded by the stoichiometry (0.125) in mixtures containing  $\text{Th}^{4+}$ . The extent of sintering in all sintered products ( $R = 0$  to 0.50) was determined by measuring their sintered density, porosity and shrinkage characteristics. In this study, it was observed that TSS led to the formation of highly sintered products compared to CS.  $\text{ThO}_2$  with a maximum sintered density of



$98.8 \pm 0.3$  % T.D could be obtained by using TSS. The sintered density of  $\text{ThO}_2$  reported in this study is the highest among the values reported so far, for the pellets made from nc- $\text{ThO}_2$  derived through citrate gel-combustion. The sintered pellets comprised faceted sintered grains with a uniform size distribution with grain size ranging between 6 – 15  $\mu\text{m}$ . It was also demonstrated that the two-step heating restricts “runaway” sintering and yields products with controlled microstructure.

## **Chapter 6 – Synthesis, Conventional Sintering and SPS of Nanocrystalline Ytria**

Chapter 6 describes the experiments on the VCR in the citrate gels containing the  $\text{Y}(\text{NO}_3)_3$ . It was also demonstrated that volume combustion occurs at a fuel (citric acid) to oxidant (nitrate) ratio close to that demanded by the stoichiometry in mixtures containing  $\text{Y}^{3+}$ . These powders were pelletized at various compaction pressures ranging from 60-353 MPa. Green pellets were subjected to both CS as well as TSS. It was demonstrated that sintered  $\text{Y}_2\text{O}_3$  pellets with a density as high as  $98.9 \pm 0.1$  % T. D. could be produced by using the TSS method at a final temperature as low as 1673 K (grain size < 3  $\mu\text{m}$ ). The sintered density of  $\text{Y}_2\text{O}_3$  reported in this study is the highest among the values reported so far, for the pellets made from nc- $\text{Y}_2\text{O}_3$  derived through citrate gel-combustion method. Selected samples of powders and monoliths were also characterized by using SEM investigation. The sintered pellets comprised faceted sintered grains with a uniform size distribution. It was also demonstrated that the two-step heating yields products with controlled microstructure. SPS of these samples had also been carried out. A maximum sintered density of  $99.3 \pm 0.2$  % T.D was obtained by using SPS with grain size ranging from 6 – 12  $\mu\text{m}$ . However, further optimization of experimental parameters is required in order to obtain nanograined  $\text{Y}_2\text{O}_3$  pellets by using SPS.

## **Chapter 7 – Synthesis, Characterization and Sintering of Nanocrystalline $\text{HfO}_2$ and YSH powders by SMS**

Chapter 7 demonstrates for the first time that nc- $\text{HfO}_2$  powders (30 g) i.e. either the thermodynamically stable monoclinic phase or the metastable cubic phase could be synthesized by tailoring the nitrite to nitrate mole ratio ( $\Phi$ ) in eutectic mixtures containing the nitrates of potassium and sodium along with  $\text{NaNO}_2$ . In addition, nc-YSH powders (30 g) were synthesized for the first time through salt melt synthesis. TEM reaffirmed the values of crystallite size estimated through XRD investigations as well as the constituent phases. Raman spectroscopy

also confirmed the phases present. It was demonstrated that the SMS could be used as a simple method for producing bulk quantities of these nc powders. All “as prepared” powders were compacted at different pressures (60 to 353 MPa) and were sintered by using three different sintering methods viz., CS, TSS and SPS. The sintered products were characterized for their phase (XRD) and microstructure by using SEM. Elemental mapping confirmed the homogeneous distribution of yttrium in YSH. Maximum sintered densities of (TSS)  $97.2 \pm 0.4$  % T.D and  $98.2 \pm 0.3$  % T.D were obtained for  $\text{HfO}_2$  and YSH powders respectively. SPS technique was used for the preparation of sintered pellets and the characteristics of the sintered products were compared with that of the products obtained by CS. SEM investigation revealed that the grain size varies from 1 - 3  $\mu\text{m}$  ( $\text{HfO}_2$  derived by using TSS) and 5 - 12  $\mu\text{m}$  (YSH derived by using TSS). By using SPS, a maximum sintered density of  $98.8 \pm 0.1$  % T.D and  $97.3 \pm 0.6$  % T.D. were obtained for  $\text{HfO}_2$  and YSH powders respectively. SEM investigation revealed that the grain sizes were varying from 5 - 25  $\mu\text{m}$  (both  $\text{HfO}_2$  and YSH derived by using SPS). Selected powders of  $\text{HfO}_2$  and YSH were used in the fabrication of cups and the compatibility of these cups with molten U at 1410 K was tested. These investigations revealed that these could be used for U metal melting since the cups were compatible with molten U at 1410 K. These results are consolidated and are discussed in detail in this chapter.

## Chapter 8 – Summary and conclusions

The highlights of this dissertation and conclusions of the studies carried out in understanding the bulk scale synthesis and sintering of nanocrystalline ceramic powders are summarized in chapter 8. The key findings of the thesis are highlighted as follows:

1. nc-ceramic powders of about 60 g ( $\text{UO}_2$ ,  $\text{ThO}_2$ ,  $\text{Y}_2\text{O}_3$ ) and 30 g ( $\text{HfO}_2$  and YSH) were successfully prepared by using both (aqueous) citrate gel-combustion method and (non-aqueous) salt melt synthesis;
2. The systematic dependence of the reaction as well as the properties of these (nc-urania and nc-thoria) powders on the composition of the combustion mixture (R) was investigated;
3. Variation in lattice strain in the nc-powders derived through citrate gel-combustion and their correlation with the X-ray crystallite size is being reported for the first time;

4. It was demonstrated for the first time that volume combustion reaction (VCR) takes place in citrate gels containing thorium nitrate, yttrium nitrate and uranyl nitrate with citric acid at an R value of 0.125, 0.17 and 0.25 respectively;
5. Porous  $\text{UO}_2$  (both foam and sintered pellets) were prepared by using gel-combustion (sucrose and citric acid gels) method;
6. Salt melt synthesis (SMS) and a modified SMS were formulated to synthesize nanocrystalline m- $\text{HfO}_2$ , c- $\text{HfO}_2$  and YSH powders in bulk, with near uni-modal size distribution of grains;
7. For the first time TEM and EELS investigations were carried out on the products obtained through volume combustion reaction (nc- $\text{UO}_2$ , nc- $\text{ThO}_2$  and nc- $\text{Y}_2\text{O}_3$ ) and SMS [nc- $\text{HfO}_2$  (both the monoclinic and cubic phases) and nc-YSH];
8. The utility of TSS in obtaining a final product with high density and uniform microstructure was investigated
9. For the first time shrinkage anisotropic factor ( $\alpha$ ) was estimated to understand the importance of obtaining dense monoliths with uniform shrinkage and
10. SPS of nc- $\text{Y}_2\text{O}_3$  (VCR), nc- $\text{HfO}_2$  (SMS) and nc-YSH (SMS) was carried out for the first time to prepare dense monoliths (99 % T.D).

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## **List of Abbreviations**

a	Acoustic mode
“A”	As prepared powders
ADS	Accelerator Driven System
AFCI	Advanced Fuel Cycle Initiative
AHWR	Advanced Heavy Water Reactor
ADU	Ammonium diuranate
AISI	American Iron and Steel Institute
AR	Analytical reagent
ASTM	American Society for Testing and Materials
AUC	Ammonium uranyl carbonate
BARC	Bhabha Atomic Research Centre
<i>c</i>	Cubic
“C”	Calcined powders
CCD	Charge Coupled Device
CGC	Citrate gel-combustion
Comm	Commercial powder
CP	Compaction pressure
CS	Conventional Sintering
CVD	Chemical Vapor Deposition
D	Direct denitration
DBP	DiButyl Phthalate
DC	Direct current
DOR	Direct Oxide Reduction
DSC	Differential Scanning Calorimetry
DTA	Differential Thermal Analysis
DTG	Derivative thermo-gravimetric
DTGS	Deuterated Triglycine Sulfate
EDS	Energy dispersive X-ray spectroscopy
EELS	Electron Energy Loss Spectroscopy
EGA	Evolved gas analysis
FAS	Ferrous ammonium sulphate
FBR	Fast Breeder Reactor
FBTR	Fast Breeder Test Reactor

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FE-SEM	Field Emission Scanning Electron Microscope
FFT	Fast Fourier Transform
GIF	Generation IV International Forum
GIXRD	Grazing Incidence X-ray Diffraction
GWd/tHM	Giga Watt days/metric ton of heavy metal
HBS	High Burn-up structure
HBRP	High Burn-up Rim Project
HCHCr	High Carbon - High Chromium
HEBM	High energy ball milling
HP	Hot Pressing
HRTEM	High Resolution Transmission Electron Microscopy
HW	Hall-Williamson method
IAEA	International Atomic Energy Agency
ICP-MS	Inductively Coupled Plasma – Mass Spectrometer
IFFT	Inverse Fast Fourier Transform
IGCAR	Indira Gandhi Centre for Atomic Research
IMF	Inert Matrix Fuel
INPRO	International Project on Innovative Nuclear Reactors and Fuel Cycles
IP	Isostatic Pressing
IR	Infrared mode
IREL	Indian Rare Earths Limited
JCPDS	Joint Committee on Powder Diffraction Standards
KAS	Kissinger-Akahira-Sunose
<i>m</i>	monoclinic
<i>M</i>	Molarity
MA	Minor Actinides
MOX	Mixed Oxide
MPa	Mega Pascal
MS	Mass Spectrometry
<i>N</i>	Normality
Nc/nc	Nanocrystalline
NFC	Nuclear Fuel Complex
NIST	National Institute of Standards and Technology
Ox de	Oxalate decomposition
<i>P</i>	Porous agent (Vol %)
P&T	Partition and Transmutation

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PCS	Photon Correlation Spectroscopy
PFBR	Prototype Fast Breeder Reactor
PHWR	Pressurized Heavy Water Reactor
PIR	Photochemically induced reaction
P <sub>o</sub> SD	Pore size distribution / Distribution of pores
ppm	Parts per million
PSD	Particle size distribution / Distribution of particles
PTFE	Polytetrafluoroethylene
<i>R</i>	Raman mode
R	Fuel (citric acid / sucrose) to Nitrate (in mole ratio)
RC	Carbon residue
RCS	Rate Controlled Sintering
Re-Ox	Reduction-Oxidation
RF	Radio Frequency
RO	Re-oxidized
<i>S</i>	External gelation sol-gel technique
SAED	Selected Area Electron Diffraction
Sc	Scherrer method
SEM	Scanning Electron Microscopy
SMS	Salt Melt Synthesis
SPS / FAST	Spark plasma Sintering / Field-Assisted Sintering Technology
SRM	Standard Reference Material
SSA	Specific Surface Area
STEM	Scanning transmission electron microscopy
TBP	TriButyl Phosphate
T.D	Theoretical density
TEM	Transmission Electron Microscopy
TG	Thermogravimetry
TG-DTA-MS	Thermogravimetry-Differential Thermal Analysis coupled with Mass Spectrometry
Thde	Thermal decomposition
Th-Ox	Thorium oxalate
TSS	Two-step Sintering
TSS <sub>C</sub>	Two-step Sintering proposed by Chu
TSS <sub>CW</sub>	Two-step Sintering proposed by Chen and Wang
TWh	Terawatt hours
UV-VIS-NIR	Ultraviolet-visible-near infrared

VCR	Volume combustion reaction
XCS	X-ray crystallite size
XRD	X-ray Diffraction
YSH	Yttria Stabilized Hafnia
2-D	Two dimension



## List of Symbols

$K$	Temperature dependent constant
$K$	Crystallite shape factor
$\rho$	Relative density
$G$	Grain size
$n$	Exponent that depends on the type of diffusion mechanism
$D_l$	Lattice diffusion coefficients
$D_{gb}$	Grain boundary diffusion coefficients
$\Omega$	Atomic volume
$\gamma_{sv}$	Surface particle / pore interfacial energy
$T$	Temperature
$\delta_{gb}$	Width of the grain boundary
$T_m$	Melting Point of that substance expressed in Kelvin
$k$	Boltzmann constant
$F(\rho)$	Unspecified function of density ( $\rho$ )
$D$	Grain boundary diffusivity
$\rho_B$	Bulk density
$\rho_G$	Green density
$\rho_S$	Sintered density
$S/N$	Signal to Noise ratio
$V_m$	Volume fraction of monoclinic phase
$I$	Integrated intensity of the X-ray diffraction lines
$\lambda$	X-ray Wavelength
$\varepsilon$	Strain distribution within the material
$\beta$	Full width at half maxima in radians / Heating rate
$\alpha$	Degree of conversion / Shrinkage anisotropy factor
$R$	Gas constant
$f(\alpha)$	Conversion function
$A$	Pre-exponential factor
$T_P$	Peak temperature
$E_a$	Activation energy
$g(\alpha)$	Integral form of $f(\alpha)$

$g$	Geometrical density
$\Psi$	Dihedral angle
$\gamma_{gb}$	Grain boundary energy
$N$	Number of grains surrounding the pores
$N_c$	Critical coordination number
$\Delta S$	Relative shrinkage parameter
$B$	Branching ratio
$K_{Eq}$	Equilibrium constant

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# **Chapter 1**

## **Introduction**

Nuclear energy is one of the best alternatives that could help us meet the growing energy demands with zero green house gas emission [1-3]. Although issues related to waste disposal are still a concern [3-5], it is the only available large-scale alternative that could be a major provider of green energy. However, as of now, the global share of nuclear power is rather meager [India (3 %) – 32 TWh] in comparison with coal, natural gas and hydropower [6]. In order to enhance the share of nuclear power in the global power production novel strategies are necessary [5, 7]. Some of the new strategies include minimization of the radiotoxic burden and destruction of the “long-lived” radiotoxic waste [5, 7]. In this context advanced nuclear fuels and advanced structural materials are particularly important [8-12]. India is aiming to meet 25 % of her power demand through the nuclear means by 2050 [6]. International agencies [International Atomic Energy Agency (IAEA) and Generation IV International Forum (GIF)] have also started programs viz., International Project on Innovative Nuclear Reactors and Fuel Cycles (INPRO) and Advanced Fuel Cycle Initiative (AFCI) [8, 13-15], that aim at coordinating the research and development to deploy innovative nuclear fission reactors (Generation IV reactors) with special emphasis to address certain challenges. These challenges are, efficient utilization of fuels, economics, safety, reliability, minimizing radiological toxic waste and partitioning and transmutation (P&T) of long lived radioactive elements in the nuclear waste (minor actinides (MA)) [5, 15].

India’s nuclear energy programme was initiated by Homi Bhabha about sixty years ago keeping in view the limited uranium and surplus thorium reserves of this nation [3, 16]. India has

adopted the well-known three stage nuclear programme with closed fuel cycle reprocessing in order to utilize nuclear fuels completely and to reprocess the spent nuclear fuel<sup>1</sup> (nuclear waste management) [3, 16-18]. The first stage is primarily based on the Pressurized Heavy Water Reactors (PHWRs) which use natural uranium and heavy water as moderator<sup>2</sup> and coolant<sup>3</sup> [3, 16]. With the successful operation of Fast Breeder Test Reactor (FBTR) and the experience gained, the country has embarked on to the second stage programme based on Sodium cooled Fast Breeder Reactor (FBR) [3, 19]. One such Prototype Fast Breeder Reactor (PFBR) being built at Kalpakkam envisages the use of U, Pu mixed oxide (MOX) (with  $\approx 21\text{wt}\%$  and  $\approx 28\text{wt}\%$  Pu) as fuel [3, 20]. Thorium ( $^{232}\text{Th}$ ) which is present around the core<sup>4</sup> in this reactor (blanket material) would be transmuted into  $^{233}\text{U}$ , which will fuel the reactors in the third stage [3, 17, 18]. India has also designed an Advanced Heavy Water Reactor (AHWR) which would use mixed oxide (MOX) fuels comprising solid solutions of the oxides of  $^{233}\text{U}$  &  $^{232}\text{Th}$  or  $^{233}\text{U}$  &  $^{239}\text{Pu}$  [3, 21, 22]. AHWR would help shorten the period of thorium utilization [3, 21, 22]. India has also initiated a programme on Accelerator Driven Subcritical System (ADS) [3] to burn long lived minor actinides and to generate fissile  $^{233}\text{U}$  from thorium. The third stage would involve generation of  $^{233}\text{U}$  from  $^{232}\text{Th}$  in PHWRs [3, 17, 18, 21, 22].

The fission reactors mentioned above, deploy a variety of special materials which are collectively called as nuclear materials [23]. In general the term “nuclear materials” include fuel,

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<sup>1</sup> Nuclear fuel reprocessing / reprocess the spent nuclear fuel - The process by which spent fuel is separated into waste material for disposal and into material such as uranium and plutonium to be reused as fuel [<http://www.srsro.org/>].

<sup>2</sup> Moderator - Material used in a nuclear reactor to decelerate neutrons from the high velocities at which they are released. Neutrons lose velocity by scattering collisions with nuclei of the moderator. A good moderator has high scattering cross section, low atomic weight, and low neutron-absorption cross section [9].

<sup>3</sup> Coolant - Any fluid circulated through the core of a reactor to extract heat liberated in the fission process [<https://nucleus.iaea.org/>].

<sup>4</sup> Core - The central portion of a nuclear reactor, which contains the fuel assemblies, moderator, neutron poisons, control rods, and support structures. The reactor core is where fission takes place [[www.nrc.gov](http://www.nrc.gov)].

clad<sup>5</sup>, coolant, moderator, reflector<sup>6</sup>, control rod<sup>7</sup>, shielding material<sup>8</sup>, thermal insulation material and the structural materials<sup>9</sup> [9]. These materials are often subjected to an extremely harsh environment viz., intense radiation, prolonged exposure to coolant, thermal and mechanical stresses [8, 9]. Hence, investigations on the synthesis, characterization and fabrication of nuclear materials are pertinent to nuclear technology which aims at power production at an economically viable cost.

## 1.1 Nuclear fuels

The most common physical form of a nuclear fuel is “sintered cylindrical pellet” [9]. Less common forms include rod [9], microspheres [9, 19] and plates [19]. Nuclear fuels could be broadly classified into metallic (alloys containing U / Pu), ceramic (oxides, nitrides and carbides) and dispersion fuels [9].

As highlighted in the foregoing section, UO<sub>2</sub>, PuO<sub>2</sub>, ThO<sub>2</sub> and mixed oxides of U,Th or U,Pu (MOX) are important driver fuels<sup>10</sup> for fission nuclear reactors [3, 9, 17-19, 21, 22, 24]. Sintered UO<sub>2</sub> is most widely used in the nuclear power reactor because of its high melting point, compatibility with the cladding materials (stainless steel and zircaloy<sup>11</sup>) and chemical stability

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<sup>5</sup> Clad - Tightly bound (usually metallic) casing directly surrounding the nuclear fuel which protects it against a chemically active ambience (cooling water) and prevents the escape of fission products into the cooling water [www.euronuclear.org].

<sup>6</sup> Reflectors - Layer of material surrounding the core of a nuclear reactor that serves to deflect escaping neutrons and return mainly to the core [9].

<sup>7</sup> Control rods - Device containing material with a high neutron absorption cross section that is used to govern the fission rate of a nuclear reactor by absorbing excess neutrons [9].

<sup>8</sup> Shielding materials - A mass of material surrounding a source of radiation that reduces radiation intensity, for the purposes of protection of equipment, material or personnel. Dense concrete, several metres thick, is used for shielding [https://nucleus.iaea.org].

<sup>9</sup> Structural materials - The materials used to encase the fuel in fuel rods, to hold fuel rods together in fuel assemblies, and to hold fuel assemblies in place, materials used in control rods and core monitoring instruments and their supporting structures are all considered as structural materials [www.iaea.org].

<sup>10</sup> Driver fuel - Fissionable material that has been enriched to a composition that will support a self-sustaining fission chain reaction when used to fuel a nuclear reactor, thereby producing energy (usually in the form of heat or useful radiation) for use in other processes., e.g., <sup>233</sup>U, <sup>235</sup>U, <sup>239</sup>Pu (and higher odd isotopes) [www.nrc.gov].

<sup>11</sup> Zircaloy - Zirconium alloy used as a tube to contain uranium oxide fuel pellets in a fuel rod (part of a reactor fuel assembly) [https://infocis.iaea.org].

towards water and well established fabrication technology [9]. The oxide fuels are fabricated through conventional powder metallurgical processes [9, 17-19, 24]. The fuels used in almost all the commercial oxide fuelled reactors are produced by this process [9, 17, 18, 24].

## **1.2 Advanced fuels – oxides, carbides and nitrides**

Nuclear fuels which incorporate the concept of recycling, incineration of minor actinides, higher breeding ratio<sup>12</sup> (in turn short doubling time<sup>13</sup>) for waste minimization, higher power density and higher fuel reliability are generally termed as “advanced actinide fuels” [25, 26]. These fuels have significant advantages over the conventional fuels but are yet to be commercialized. Similarly “advanced fuel fabrication method” refers to a method that is advantageous over the conventional methods but is yet to be commercially deployed.

Table 1.1 enlists an intercomparison of the thermo-physical properties of some of the advanced fuel forms vis-à-vis that of the conventional oxide fuel [19].

The preparation of advanced oxide fuel forms containing <sup>233</sup>U, <sup>239</sup>Pu and Minor Actinides (MA) which call for improvised “advanced techniques” owing to the higher radiotoxicity of the latter is a typical example that necessitates the deployment of alternate fuel fabrication techniques [5, 10, 12-14, 18-20, 25]. Nitride, carbide and metallic fuels are considered as “advanced fuels” for they possess better thermo-physical and thermo-chemical properties as compared to the mixed oxide (Table 1.1) [19, 26].

The sol-gel method is considered as an ideal alternative “advanced method” for the fabrication of oxide fuels because it is dust free, easy to remotize and is a cost-effective technique [18, 24]. This process was successfully implemented for the preparation of sintered

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<sup>12</sup> Breeding ratio - The ratio of fissile material obtained to spent fissile material after the use of a fuel mixture of fissile and fertile material in a reactor [www.euronuclear.org].

<sup>13</sup> Doubling time - The time during which the fissile material input of a breeding reactor doubles. Depending on the breeding reactor concept, doubling times of 8 to 20 years result [www.euronuclear.org].

microspheres of different size fractions of  $\text{UO}_2$ ,  $\text{ThO}_2$ , mixed metal oxides (MOX) of U & Pu or U & Th and  $(\text{U, MA})\text{O}_2$  [18, 24].

Carbide fuel was considered as an advanced fuel for Fast Reactors [3, 19]. However, due to difficulties in fabrication, reprocessing and economics, the carbide fuel technology did not take off [19, 24]. Even though the Fast Breeder Test Reactor (FBTR) at Kalpakkam, India uses a plutonium rich mixed uranium and plutonium carbide fuel, PFBR, the commercial fast reactor being commissioned at Kalpakkam, would use only the MOX fuel [3, 19, 24].

**Table 1.1 Comparison of some characteristics of the fuels used in Fast Reactor [19]**

		Oxide fuel	Carbide fuels	Nitride fuels	Metallic fuels
		$\text{U}_{0.8}\text{Pu}_{0.2}\text{O}_2$	$\text{U}_{0.8}\text{Pu}_{0.2}\text{C}$	$\text{U}_{0.8}\text{Pu}_{0.2}\text{N}$	$\text{U-19Pu-10Zr}$
<b>T.D (<math>\text{g cm}^{-3}</math>)</b>		11.04	13.58	14.32	15.73
<b><math>T_m</math> (K)</b>		3083	2750	3070	1330
<b>Crystal structure (Space group)</b>		Fluorite (Fm3m)	NaCl (Fm3m)	NaCl (Fm3m)	Multi-phase
<b>Breeding ratio</b>		1.1	1.2-1.3	1.2-1.3	1.4-1.5
<b>Swelling</b>		Moderate	High	High	High
<b>Handling atmosphere</b>		Air	Inert gas	Inert gas	Inert gas
<b>Dissolution and amenability to reprocessing</b>		Demonstrated for industrial scale for aqueous and pilot scale for pyro reprocessing	Difficult-yet to be demonstrated industrially	Easy but risk of $\text{C}^{14}$ in waste management	Pyro - reprocessing demonstrated on pilot scale
<b>Fabrication/irradiation experience</b>		Good	Limited	Very little	limited
<b>Thermal conductivity (<math>\text{W m}^{-1} \text{ } ^\circ\text{K}</math>)</b>	1000 K	2.6	18.8	15.8	40
	2000 K	2.4	21.2	20.1	-
<b>Compatibility with</b>	Clad	Average	Carburization	Good	Low melting eutectics
	Coolant	Average	Good	Good	Good

$T_m$  – Melting point and  $T.D$  – Theoretical density

### 1.3 “In-reactor” behavior of nuclear fuels

During its life in a reactor the nuclear fuel would undergo substantial physical, microstructural and chemical changes apart from radiation induced changes [19]. In order to improve the economics of the nuclear power production it is desirable to extract the maximum possible power from a given fuel. This necessitates a longer residence time or “burn-up”<sup>14</sup> of the fuel [8, 15, 27-29]. Increasing the fuel burn-up in the reactor would require the development and testing of advanced fuels and structural materials that would withstand the extended operation [8, 15]. Recently, Idaho National Laboratory had established a facility for the testing of advanced fuels and materials [15]. The investigations carried out in this facility would throw light on fuel performance, economics, safety and reliability [15]. Several countries including India are regularly monitoring and updating their tests for enhancing the performance of fuels and materials for the current and future advanced reactors [15].

#### 1.3.1 High Burn-up Structure/phase (HBS)

Studies carried out in the past on LWR (oxide) fuels with a burn-up of about 60 GWd/tHM revealed that this fuel had undergone significant restructuring<sup>15</sup>, comprised pores and a fine grained microstructure at its rim [27, 30, 31]. This feature was initially termed as the “rim structure” and later it was called as the “high burn-up structure” (HBS) [27, 30, 31]. Studies carried out earlier in the 1950-60s by Barney and Wemple [32] and Belle [33] were the first investigations on HBS. However, the significance of HBS was not known at that time and hence it was not investigated in detail [27]. But in the late 1990s, the HBS was rediscovered in

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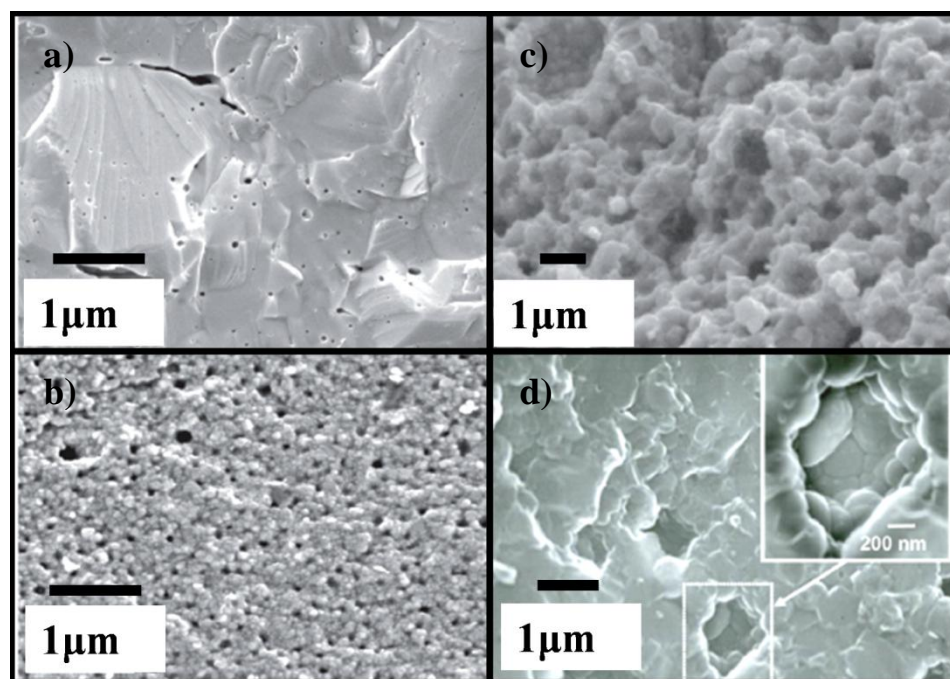
<sup>14</sup> Burn-up - Measure of the number of fissionable atoms that have undergone fission. It is usually expressed as the atomic percent of the total uranium atoms that have fissioned in the fuel, as megawatt-days of energy generated per ton of uranium, or as gigajoules of energy per kg of uranium. Other definitions include fissions/cc or atomic percent of fissions per total atoms present in the fuel [9].

<sup>15</sup> Restructuring – The increase in the local burn-up of the nuclear fuels leads to the formation of cracks followed by self healing and eventually redistribution of actinides and porosity in the fuels. Thus the fuel yields a new morphology. These processes are collectively termed as restructuring of the fuel [27].

“modern reactor fuels” and for the past two decades, research is being carried out world over [for e.g. High Burn-up Rim Project - HBRP] in order to understand the formation mechanisms, properties and significance of HBS [27]. It is now surmised that the HBS is formed due to the capture of epithermal neutrons with energies matching the resonance absorption cross-section of  $^{238}\text{U}$  leading to  $^{239}\text{Pu}$  build-up at the “rim” of the fuel [27, 30]. Further, it was observed that the Pu content at the rim of the  $\text{UO}_2$  fuel is 2 to 3 times higher than that of the average Pu content in the fuel at an average burn-up of 60 GWd/tHM [27, 29]. Unlike the fresh fuel which possesses microcrystalline  $\text{UO}_2$  grains with a size of about 10  $\mu\text{m}$ , HBS was found to contain grains with size ranging from 100-300 nm (grain subdivision  $\approx 10^4$  times) [27, 30]. Further, it was found that it contains closed intergranular macropores with a porosity fraction of about 20 % (Fig. 1.1) [27, 29]. Significant amount of fission gases were entrapped in these closed pores [29, 31]. Microstructural analysis of HBS revealed that the restructured fuels were devoid of any defects [27, 30] and a thin section of HBS at the rim of the fuel extends to the inner region of the fuel pellet with increasing burn-up [27, 30]. It was found that the fuel with the average burn-up of about 60 GWd/tHM comprised HBS of about 8 % of the fuel volume [1]. HBS is not only observed in  $\text{UO}_2$  fuel and U-Mo alloy fuel but also in other fuels viz., MOX, carbide and nitride fuels used in the FBRs [27, 30]. Lozano et al. [34] had identified two types of grains in the HBS viz., polyhedral (bulk of HBS) and round (around pores and open surface) grains.

Studies on HBS revealed that it possesses the following advantageous features, i) retention of 90% of fission gases in the closed pores, ii) lack of enhanced fission gas release, iii) improved thermal conductivity, iv) increased fracture toughness and plasticity and v) stability towards radiation and elimination of defects by itself (self healing mechanism) [27, 31]. All these properties are most suitable for achieving higher burn-up. Further, recent investigations on HBS

analogue materials (partially stabilized zirconia doped with 4 mol% yttria by Spino et al. [31] revealed that nanocrystalline (nc)  $\text{UO}_2$  is a potential candidate material to be used in reactors which aim at a higher burn-up as well as in inert matrix fuels (IMF)<sup>16</sup> [27, 30].



*Figure 1.1 Scanning Electron Microscopy micrographs showing fuel fracture surfaces: (a) unirradiated  $\text{UO}_2$  fuel; the pores visible in the as-fabricated fuel structure are removed in-pile during the early stage of irradiation by fuel densification processes, (b) Fuel with local burn-up of  $\sim 75$  GWd/tHM showing the typical HBS morphology (HBRP [27]), (c) High magnification SEM fracture surface micrograph of LWR  $\text{UO}_2$  fuel with a local burn-up of around 160 GWd/tHM. The image shows in detail the morphology of HBS, characterized by sub-micron grains and micron-sized intergranular pores and (d) High magnification scanning electron microscopy image of 75 GWd/tHM  $\text{UO}_2$  showing HBS morphology. Polyhedral sub-grains are present in the bulk while round sub-grains (see inset) occur mainly around pores and open surfaces (HBRP) (Figure reproduced from [27])*

The mechanism leading to the formation of HBS is not understood completely due to the interplay of many complex factors. However, various researchers had tried to explain this

<sup>16</sup> Inert matrix fuels – IMF is a type of nuclear reactor fuel that consists of a neutron-transparent matrix and a fissile phase that is either dissolved in the matrix or incorporated as macroscopic inclusions. The matrix plays a crucial role of diluting the fissile phase to the volumetric concentrations required by reactor control considerations, the same role  $^{238}\text{U}$  played in conventional low enriched uranium (LEU) or MOX fuel. The key difference is that replacing fertile  $^{238}\text{U}$  with a neutron-transparent matrix eliminates plutonium breeding as a result of neutron capture [IAEA TECDOC 1516].



phenomenon by using different theories and models [27]. Some of these theories pertaining to the mechanism of HBS formation need to be modified as the recent findings indicate conflicting results [27]. Hence, several novel experiments are being devised for a better understanding of the HBS [35, 36]. Also new models / theories are being developed with these new results [27]. Many researchers are of the view that the formation of small grains could possibly be due to either recrystallization (formation of a subgrain which ultimately grow into recrystallized nanograins) or polygonization (formation of micro-domain of an over structure of the  $\text{UO}_2$  which results in planar defects) [27, 29, 30]. Recent investigations provide enormous evidence pointing towards the polygonization mechanism [27]. *Thus investigations on nc- $\text{UO}_2$  have become very pertinent to advanced nuclear fuel forms.*

#### **1.4 Foam and porous pellets**

In addition to the above application nanostructured oxide foams and porous pellets also are relevant to advanced metal production viz., the direct oxide reduction (DOR) process. Uranium metal is a starting material for the preparation of uranium bearing alloys that are candidate fuels for the Fast Reactors. Usually the preparation of metallic uranium is accomplished by the reduction of its fluoride through the expensive fluoro-metallothermic process. Recent research carried out at the University of Cambridge has brought about a paradigm shift in the reduction of metal oxides [37]. This research group has reduced  $\text{TiO}_2$  to Ti through a novel direct electrochemical reduction called DOR process [37]. This process is an attractive alternative to the expensive conventional metallothermy. Plutonium is presently being recovered from the spent nuclear fuel through aqueous nuclear fuel reprocessing technology [18]. Production of metallic Pu through direct electrochemical reduction coupled with reprocessing would serve as an attractive alternative method for the production of Pu metal.

This “advanced” DOR method is particularly advantageous because it is cost effective and less cumbersome than the “conventional bomb reduction”<sup>17</sup>.

In view of the above, a research program on DOR is currently being pursued in some countries (including India), world over [38, 39]. Although, this method involves many process variables, percolation of the molten salt (into the  $\text{MO}_2$  / pre-form used for the reduction) is one of the principal prerequisites that determine the complete conversion of the oxide to the metal. The oxide “pre-form” used in the reduction needs to have a high matrix density in order to have a good electrical conductivity vis-à-vis high porosity to facilitate complete reduction of the oxide. Hence, preparation of porous  $\text{UO}_2$  bodies (either foam or a pellet) is necessary. Recently, a patent which describes a novel method for the fabrication of porous pellets has been registered [40]. In this study, we had investigated the possibility of producing both porous urania and urania foam through two different techniques, appropriate precursors.

The third application which warrants the use of nanocrystalline oxide ceramics in nuclear technology is the fabrication of chemically inert crucibles to be used in melting metallic U or alloys bearing U and Pu. This application encompasses both thermodynamic investigations as well as fuel fabrication [41, 42].

### **1.5 Crucibles for uranium melting**

Experimental determination of the properties of U and its alloys, viz., self diffusion, melting, electrical resistivity and magnetic susceptibility are relevant to nuclear technology [43]. Data on the solidus temperature<sup>18</sup> of uranium bearing alloys serve as useful inputs for nuclear

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<sup>17</sup> Conventional bomb reduction - Ames process or bomb reduction is a process by which high pure uranium is prepared. It involves the heating of mixtures of uranium halides and magnesium powder.

<sup>18</sup> Solidus temperature - It is the highest temperature up to which an alloy / solid solution could be heated without melting.

fuel design [41]. Liquid uranium bearing alloys are highly oxyphilic and have to be held at high temperatures in ceramic containers without any chemical interaction with the latter [43-45].

The use of many inert ceramic crucibles have been reported in the literature [41, 43-45]. These include crucibles made out of MgO [43, 45], Al<sub>2</sub>O<sub>3</sub> [43, 44], UO<sub>2</sub> [43], BeO [43, 45], ThO<sub>2</sub> [41], yttria stabilized zirconia (YSZ) [41, 43] and graphite [43].

From a simple Ellingham diagram analysis, it is evident that both Y<sub>2</sub>O<sub>3</sub> and HfO<sub>2</sub> are very stable in presence of molten U [42, 46, 47]. Hence crucibles made out of HfO<sub>2</sub> or Y<sub>2</sub>O<sub>3</sub> are best suited for this application.

Reactions with impurities including those introduced through the additives (binders) used while making crucibles could contaminate the molten uranium [43]. Therefore, it is desirable to use binderless process for the production of crucibles for uranium melting. Hence, we undertook investigations on the fabrication of high density crucibles out of HfO<sub>2</sub> [P2<sub>1</sub>/c (14)] and Y<sub>2</sub>O<sub>3</sub> [Ia-3 (206)]. HfO<sub>2</sub> undergoes a phase transformation from the monoclinic [P2<sub>1</sub>/c (14)] to quadratic<sup>19</sup> (P4<sub>2</sub>/nmc) phase at 1973 K and the quadratic phase transforms into the cubic phase (Fm3m) at 2873 K [47, 48]. Monoclinic hafnia is less dense compared to the quadratic phase and hence thermal cycling of hafnia is accompanied by a volume expansion (+3.4%) [48]. This results in cracking of the sintered (1973 K) hafnia products [47-49]. Hence, yttria stabilized hafnia was prepared and crucibles were made out of the same. In view of their high sinterability nc powders were chosen for fabricating the crucibles.

## 1.6 Preparation of nanocrystalline (nc) oxides

Nanocrystalline materials possess superior material properties as compared to their microcrystalline counterparts [50]. The challenges in the fabrication of crucibles from nc

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<sup>19</sup> Quadratic (P4<sub>2</sub>/nmc) phase - Alternate name for tetragonal crystal system.

powders include preparation of nc materials in bulk quantities, optimizing the powder processing and consolidation parameters as well as choosing a suitable sintering technique [51-55].

There are many methods reported in the literature that could be used to synthesize nanocrystalline ceramics which include chemical vapor deposition (CVD) [56], pyrolysis [57], precipitation [52], sol-gel [52] and high-energy ball milling (HEBM) [51, 52]. However, some of these methods have their own limitations. Among these, the precipitation synthesis is most commonly used, in the preparation of nanocrystalline oxides in bulk quantities [52, 58].

In the precipitation method two or more reactants are mixed together (in an aqueous / non-aqueous solution) to precipitate the precursor. Subsequently the product is separated by filtration [52, 58]. The liquid solvent residue in the precipitate is removed by a suitable “post-processing” [52]. The product thus obtained is decomposed to yield the desired product. This method yields a homogeneous product [52, 58]. Typical examples include the preparation of ThO<sub>2</sub> powders from thorium oxalate [59] and BeO from Be(OH)<sub>2</sub> [60].

### **1.6.1 Challenges involved in the preparation of nanocrystalline materials**

The primary challenge in the synthesis of nanocrystalline powders is the amenability of a given method to scale-up and its ability to control both the size and size distribution of particles, surface contamination and degree of agglomeration [52, 55, 61, 62]. CVD and chemical pyrolysis produce powders with a high degree of agglomeration with particle size over a wide range [52, 61]. In general, precipitation synthesis is carried out in aqueous media and in the subsequent stages moisture is removed by drying [55, 58, 62]. During drying hard agglomerates could be formed [52, 55, 62]. Some authors [52, 55, 62] had used dispersants during the synthesis or had washed the precipitates with an organic solvent and removed the latter subsequently by evaporation / decomposition at a higher temperature [55, 63]. In most cases, this

heat treatment leads to localized densification and formation of harder agglomerates leading to heterogeneous density distribution in the green compacts [52, 55, 63]. This could lead to differential densification while these are sintered later [52, 55, 64]. Often these powders require high compaction pressures (to break the hard agglomerates) and very high temperature for sintering, if a dense product is to be obtained by consolidation [52, 55, 62]. On the other hand, gel based methods are promising alternatives for the preparation of nanopowders with control over both particle size and the distribution of sizes [52, 55]. HEBM has been used for grain refinement and for the preparation of novel nanomaterials which includes metastable phases [52, 65]. However, mechanical attrition generally leads to contamination and yields powders with a wide size distribution of particles [52].

Monoliths made out of nc materials densify at a faster rate (enhanced diffusion kinetics) at the surface than at the interior of the sample [54, 55, 62, 66]. In agglomerated powders, densification is strongly dependent on the agglomerate size rather than the crystallite size because of larger pores (both inter and intra agglomerate) [54, 55]. These larger pores are much stable and lead to a lower densification rate [54, 55, 62, 66]. Hence, control of agglomeration is a key parameter in the preparation of nc powders.

### **1.6.2 Advanced preparation techniques for the bulk preparation of nanocrystalline powders**

Among the methods that are cited in the literature for the synthesis of nc materials only a few are useful for scale-up [52]. Presence of undesirable impurities, generation of a large volume of liquid waste and economic viability are the main factors that decide the scalability of a given method [52].

The precipitation method could be modified (for a scale-up) by adding surfactants / capping agents [67] or by changing the experimental conditions (e.g. high P [68], high T [58], and hydrothermal method [69]). Further, different post-processing techniques (e.g. freeze drying [70] and azeotropic distillation [71]) could be used for treating the powders or precipitates. Ananthasivan et al. [72] have prepared nc-ThO<sub>2</sub> powders by “oxalate ultrasonic deagglomeration” method.

Complex and uniform nanocrystals could also be prepared by carrying out the synthesis in non-aqueous media [73, 74]. Several mechanisms had been proposed for the non-aqueous synthesis of nanocrystals but the role played by solvent and surfactant in defining the specific structure of nanocrystals is yet to be completely understood [75]. Typically, a mixture containing a definite proportion oleic acid, oleyl amine, organic solvent and precursor salt are used in some procedures. This mixture is heated in a stream of an inert gas in an enclosed polytetrafluoroethylene (PTFE) vessel [75, 76]. UO<sub>2</sub>, ThO<sub>2</sub> and mixed oxides of U and Th of monodisperse nanocrystals have been successfully prepared by using this non-aqueous method [74].

### **1.6.3 Gel-Combustion Synthesis**

Yet another promising advanced method for the preparation of nc-ceramic (UO<sub>2</sub>, ThO<sub>2</sub> and Y<sub>2</sub>O<sub>3</sub>) powders is the combustion synthesis [77, 78]. Combustion synthesis involves the thermal decomposition of a mixture containing an oxidant and a reducing agent (fuel). Based on the physical state of the reactants this technique is further subdivided into solid state combustion synthesis and solution-combustion synthesis [79]. The latter is being widely used in the preparation of nc-oxide materials as it is simple, economical, fast and amenable to scale-up [80]. This method involves the thermal decomposition of a homogeneous aqueous gel containing a

metal nitrate (oxidant) and an organic ligand (fuel: citric acid, urea, glycine, hydrazine, etc.) [79]. It is established that the composition of the combustion mixture ( $R$  = fuel to nitrate mole ratio) influences the characteristics of the final product [78]. Among the fuels citric acid is preferred for it produces moderate reactions and leaves behind lesser carbon residue in the product [81].

So far no reports are available in the literature pertaining to the citrate gel-combustion synthesis of nc-UO<sub>2</sub> powders while synthesis of nc-ThO<sub>2</sub> [78], solid solution of urania-thoria [82] and yttria [83] have been reported. Purohit et al. [84] have prepared nc-ThO<sub>2</sub> by using glycine gel combustion. These authors have carried out combustion synthesis with both fuel lean and fuel rich mixtures. However, they [84] did not investigate the systematic dependence of  $R$  on the characteristics of the final product. Chandramouli et al. [78] have used both urea and citric acid for the preparation of the nc-ThO<sub>2</sub>, and also studied the influence of different modes of heating (hot plate and microwave) on the characteristics of the final product. So far, no report has been published in which the influence of fuel to nitrate mole ratio, in the fuel lean region ( $R = 0 - 0.31$ ) on the citrate gel-combustion synthesis of nc-ThO<sub>2</sub> powders has been studied. Several authors had reported the preparation of nc-Y<sub>2</sub>O<sub>3</sub> by using gel-combustion method [83, 85, 86]. However, no reports have so far been made on the preparation of nc-Y<sub>2</sub>O<sub>3</sub>, nc-UO<sub>2</sub> and nc-ThO<sub>2</sub> powders through “volume combustion reaction”<sup>20</sup> of citrate gels. Hence, we investigated these citrate gels of specific composition, in this study.

#### 1.6.4 Salt Melt Synthesis (SMS)

The SMS is a non-aqueous molten salt technique that is very useful for the preparation of nc-oxides. The SMS involves the decomposition of a precursor [ $M(NO_3)_x$  or  $MCl_x$  or  $M(SO_4)_x$ ]

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<sup>20</sup> Volume combustion reaction (VCR) – It is a kind of solution combustion synthesis wherein the entire reactive solution or gels is preheated uniformly to the boiling point of the solvent and held at this temperature for certain period until the mixture self propagates (exothermic) itself in the form of combustion wave. This mode is also called volume combustion mode [A. Verma et al. Chem. Rev. 116 (3) (2016) 14493-14586].

in a pool of molten metal nitrate [87-89]. The reaction between the precursor and molten salt could be viewed as an acid-base reaction (Lux-Flood concept [90]) wherein a base ( $\text{NO}_3^-$ ) donates its oxide ion to an acid ( $\text{M}^{n+}$ ). Extensive work has been carried out on SMS by Kerridge et al. [91] and Durand et al. [92]. These authors were able to prepare metastable nanocrystalline ceramics (t-ZrO<sub>2</sub>, c-ZrO<sub>2</sub> and  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>) by using SMS [91, 92].

Recent reports on the salt melt synthesis [88, 89] explain in detail about the preparation of metastable materials with different structures by tuning either one or more experimental parameters. The latter include varying the composition of the eutectic mixture, its basicity, reaction conditions (closed or open), heating rate, soaking temperature and duration of reaction [88, 89]. The SMS could be used to prepare nanocrystalline materials in bulk and is particularly suitable for the preparation of nc-HfO<sub>2</sub> and nc-YSH. However, nc-HfO<sub>2</sub> and nc-YSH has not so far been prepared in bulk quantities by using this method. Hence, we investigated the preparation of nc-HfO<sub>2</sub> and nc-YSH on a 30 g scale by using this method.

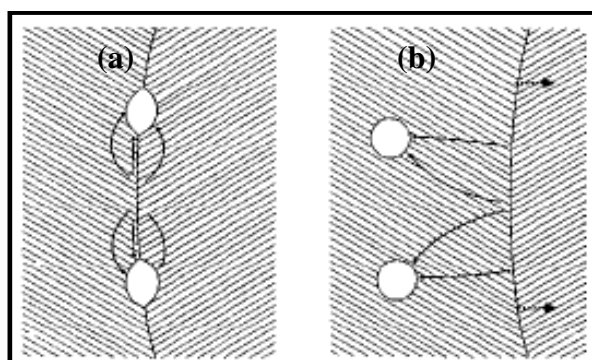
### **1.7 Sintering of nanocrystalline powders**

Sintering is a thermal treatment for bonding particles into a coherent, predominately solid structure via mass transport events that often occur at the atomic scale. The bonding leads to improved strength and lower system energy [93]. The main driving forces for sintering are curvature of the particle surface, and (or) an externally applied pressure and a chemical reaction [93, 94]. The phenomenon of sintering in microcrystalline powders is well studied and many treatises are available on the same [62]. However, the sintering of nc powders are not fully understood [55, 62, 66]. Sintering in a real system involves many complex variables and many theories and models were developed in the past (scaling law, numerical simulations, analytical models, topological models, statistical models and phenomenological equations) to analyze the



densification process [62, 94]. In general, these theoretical approaches indicate that the densification of nanocrystalline powders is affected significantly by the following variables viz., high SSA, agglomeration of particles, size distribution of particles, particle packing in green compacts, pores, heating schedule, sintering atmosphere and other process variables [52, 54, 55, 62]. Although, these factors affect the microcrystalline materials as well, the magnitude of their impact is more pronounced in the former [54]. Sintering of nc powders are greatly affected by their green density ( $\rho_G$ ) and the compaction process as well [52, 55, 62]. It is observed that the nc powders do not yield green bodies with a high density due to the restricted sliding and rearrangement of particles during compaction owing to the presence of large interparticle frictional resistance [52, 54, 94]. In addition nc ceramic powders are prone to get agglomerated due to the presence of weak van der Waals force of attraction viz., Keesom forces, Debye induction forces and London dispersion forces [62].

During sintering, densification occurs due to grain boundary diffusion (grain boundaries to the pores) [62, 94]. Therefore increase in grain size would increase the diffusional path which in turn results in suppression of the densification rate (Fig 1.2) [94].



*Figure 1.2 (a) Densification mechanisms for porosity attached to a grain boundary. The arrows indicate paths for atom diffusion and (b) Densification mechanisms for porosity separated from a grain boundary. The solid arrows indicate paths for atom diffusion, and the dashed arrows indicate the direction of boundary migration [94]*

The relation between densification rate and the size of the grain boundary [63] is given by eqn. (1.1).

$$\frac{1}{\rho} \frac{d\rho}{dt} = \frac{K}{G^n} \quad (1.1)$$

where K is a temperature dependent constant,  $\rho$  is relative density, G is the grain size, n is an exponent that depends on the type of diffusion mechanism that prevails [ $n = 3$  for lattice diffusion from the surface and 4 grain boundary diffusion].

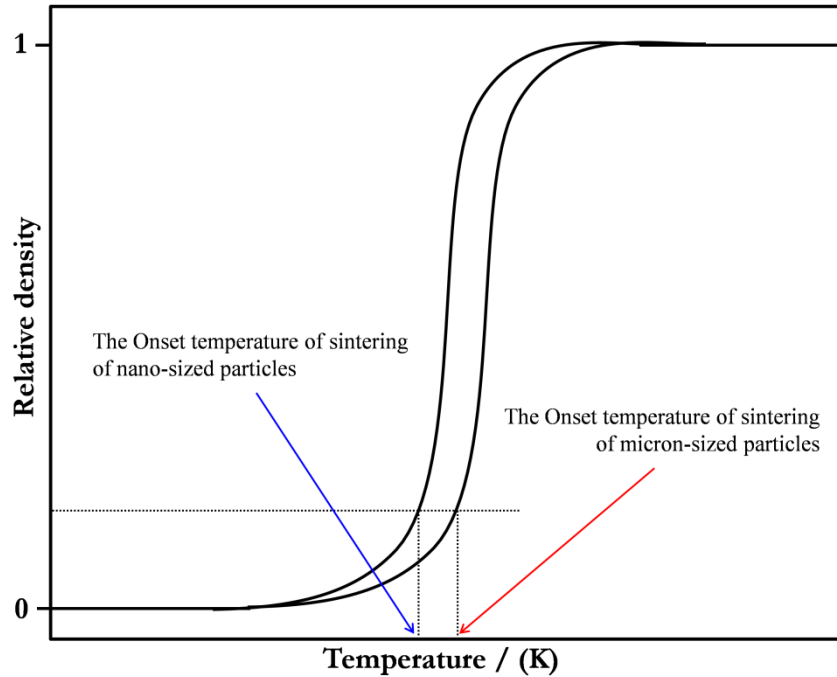


Figure 1.3 Schematic diagram illustrating different onset temperatures of sintering of nano- and micro-meter sized particles based on the model proposed by Fang [54]

Thus, to obtain highly dense monoliths it is necessary that the powder should contain small particles with unimodal size distribution and that the sintering is carried out in a controlled environment with normal grain growth [52, 53, 55, 62, 66]. The latter is a thermally activated microstructure evolution process wherein curvature driven grain rotation and grain boundary migration occurs [95]. In general, microcrystalline materials exhibit normal grain growth [95]. However, in some instances abnormal grain growth could occur due to the faster mobility of

atoms at the grain boundary [95]. It is observed that the materials that comprise impurities and defects at the interface, as well as nc materials exhibits abnormal grain growth [95]. From the foregoing it is evident that considerable attention must be given during all the processing steps in the sintering of nc materials.

Herring's scaling law predicts that the sintering rate in a nc material could be as much as twelve orders higher than that of its microcrystalline counterpart [62]. Nanoparticles bear a high concentration of defects and unsatiated valence at their surface [66]. Therefore the mobility of atoms on the surface of such a particle is higher compared to that of the atoms at its interior [66]. Thus, the temperature at which sintering starts in a nc material is lower as compared to its microcrystalline counterpart (Fig.1.3) [54, 66].

Fang and Wang [54] have termed the “onset sintering temperature” as “rapid densification stage” due to the lack of demarcation between the coarsening and the densification processes. Further, these authors had also reported that due to the large surface to volume ratio prevailing in nc materials, surface premelting could also result in rapid densification [54]. Recent experimental investigation on laser heating of nc-UO<sub>2</sub> [96] had revealed that the nanostructured UO<sub>2</sub> compacts had melted at a lower temperature  $2790 \pm 60$  K as compared to microcrystalline UO<sub>2</sub> ( $3120 \pm 30$  K) [97]. Rahaman [94] had reported that the reduction in particle size increases the diffusion rate which in turn increases the densification rate (eqns. 1.2-1.3):

$$\text{Lattice diffusion} = \frac{1}{\rho} \frac{d\rho}{dt} \approx \frac{10D_l\gamma_{sv}\Omega}{\rho G^3 kT} \quad (1.2)$$

$$\text{Grain boundary diffusion} = \frac{1}{\rho} \frac{d\rho}{dt} \approx \frac{4}{3} \frac{D_{gb}\gamma_{sv}\Omega\delta_{gb}}{\rho(1-\rho)^3 G^4 kT} \quad (1.3)$$

where,  $\rho$  is relative density,  $D_l$  and  $D_{gb}$  are lattice and grain boundary diffusion coefficients,  $k$  is the Boltzmann constant,  $T$  is temperature,  $\delta_{gb}$  is the width of the grain boundary,  $\gamma_{sv}$  is the

specific energy of the solid-vapor interface and  $\Omega$  is the atomic volume. Groza [61] had reported that the depression in sintering onset temperature for nc materials is in the range of  $0.2 T_m$  to  $0.3 T_m$  (where,  $T_m$  = melting point of that substance expressed in Kelvin) while in microcrystalline materials it is in the range of  $0.5 T_m$  to  $0.8 T_m$ .

Recent studies [52, 55, 62] had revealed that nanopowders comprising smaller aggregates and narrow unimodal size distribution of particles undergo homogeneous particle packing which in turn results in small pores with a narrow size distribution during sintering. Thus, homogeneous particle packing leads to uniform densification and yields a final product with controlled microstructure [55, 62, 94]. Further, the densification rate is higher when nc powders with a narrow unimodal size distribution of particles are used [55, 66].

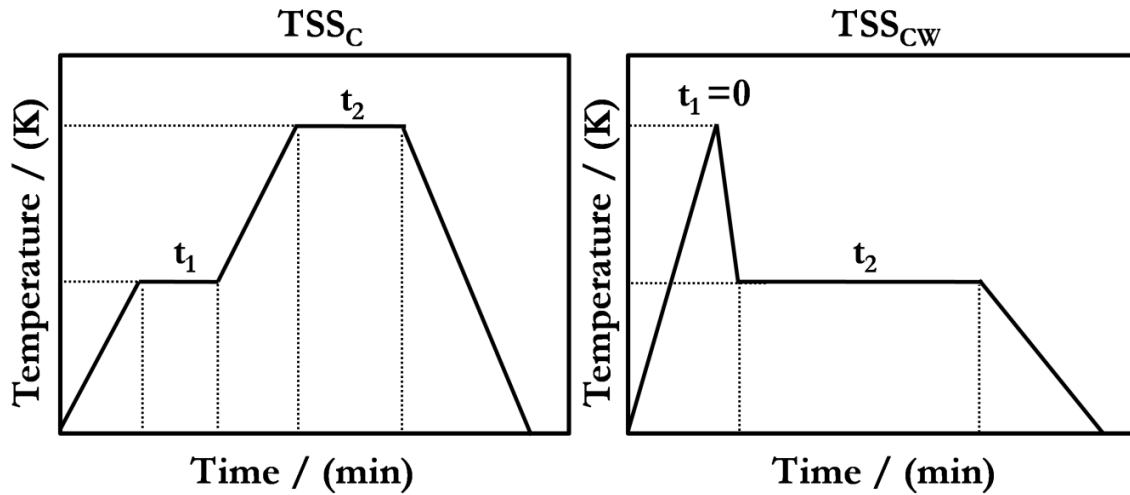
## **1.8 Advanced sintering methods**

Several studies were carried out pertaining to microstructure refinement by optimizing the sintering curve profile which includes Rate Controlled Sintering (RCS) [98], Two-Step Sintering (TSS) [99-102] and Spark Plasma Sintering (SPS) [103-105]. In RCS, the relationship between the densification and grain growth rate is obtained which in turn helps to identify the soaking temperature and duration of sintering for obtaining dense ceramics [101].

### **1.8.1 Two-step sintering (TSS) method proposed by Chu [102]**

Chu et al. [102] had devised a novel two-step procedure ( $TSS_C$ ) to sinter powders with wide size distribution of particles to high density. In this method [101, 102], the green compacts are subjected to “pre-heat treatment” at a low temperature ( $T_1$ ) followed by high temperature sintering ( $T_2$ ) [ $T_1 < T_2$ ] (Fig. 1.4). Chu et al. [102] had successfully sintered conventional alumina ( $Al_2O_3$ ) and magnesia ( $MgO$ ) powders to a very high density and uniform microstructure (grain refinement) by using  $TSS_C$ . These authors [102] claim that “pre-heat

treatment” eliminates fine particles by Ostwald ripening and delays the onset of abnormal grain growth, thus preventing differential densification. Thus,  $TSS_C$  method devised by Chu et al. [102] is a promising one to obtain a dense ceramic body with uniform microstructure and smaller grain sizes.



**Figure 1.4** Illustrative representation of the  $TSS_C$  and  $TSS_{CW}$  sintering plots as illustrated by Loh et al. [101] (where  $TSS_C$  and  $TSS_{CW}$  denotes two-step sintering methods proposed by Chu [102] and Chen and Wang [99])

### 1.8.2 Two-step sintering (TSS) method proposed by Chen and Wang [99]

Another TSS method devised by Chen and Wang [99] is the most widely used sintering technique to obtain dense ceramic body with controlled microstructure from an nc powder. This ( $TSS_{CW}$ ) proposed by Chen and Wang [99] limits “runaway” sintering and yields a product with uniform grain size. In this method the sample is taken to a very high temperature [ $T_1$ ] for a short duration (critical density:  $\rho \geq 75\%$  T.D) and then cooled and held at a lower temperature [ $T_2$ ], for a longer duration ( $T_1 > T_2$ ). Chen and Wang [99] had reported that during the first step in the  $TSS_{CW}$  the compact should attain a relative density of about 75 % in order to obtain unstable pores (Fig. 1.4). While in the second stage the grain growth is suppressed and the densification occurs with a frozen microstructure and a slower kinetics.

It is well known that the sintering phenomenon of real materials could not be explained by using models as it were built on various assumptions (for instance: uniform shape and size). However, it is reported that the diffusion kinetics of “two-step sintered” products could be estimated by measuring their normalized densification rate (final product) and comparing it with Herring’s dimensional theory [99]. The normalized densification rate ( $dp/pdt$ , where  $p$  is relative density and  $t$  is time) is given as (eqn. 1.4):

$$\frac{dp}{pdt} = F(p) \left( \frac{\gamma\Omega}{GkT} \right) \left( \frac{\delta D}{G^3} \right) \quad (1.4)$$

where,  $F(p)$  is a unspecified function of density ( $p$ ) which is independent of the grain size,  $\gamma$  is the surface energy,  $\Omega$  is the atomic volume,  $G$  is the grain size,  $\delta$  is the grain boundary thickness,  $k$  is the Boltzmann constant and  $D$  is grain boundary diffusivity. It is also reported that densification without grain growth requires not only suppression of grain boundary migration but also retention of active grain boundary diffusion [100]. Grain boundary migration and grain boundary diffusion are activation controlled processes [100]. The activation energy of the former is higher than that of the latter [100]. Hence grain boundary migration is suppressed at lower temperatures. It is now being perceived that in the TSS<sub>CW</sub> higher T<sub>1</sub> temperature is required for bringing about a different sintering mechanism below and above a critical density [100]. Particle coarsening and repacking are possible mechanisms for densification below this critical density [54, 106]. Otherwise pores would grow as predicted by the Kingery and Francois theory [107]. Particle coarsening takes place at a lower temperature itself since the activation energy for surface diffusion is lower than that of grain boundary diffusion [54, 106]. However, particle repacking would require a higher energy [106]. Hence a higher T<sub>1</sub> is employed [106]. Once the critical density is achieved grain boundary diffusion alone is sufficient for densification at T<sub>2</sub>. However, T<sub>2</sub> should not be too low to weaken the diffusion process [106].

### 1.8.3 Field-Assisted Sintering Technology / Spark plasma sintering (FAST/SPS)

The field-assisted sintering technique or Spark Plasma Sintering is a technique which involves consolidation of the powders or green compacts under the simultaneous action of a low-voltage, pulsed direct current (DC) and mechanical pressure [103]. Though it is similar to hot pressing (HP) wherein the powders or green pellet is sintered under the action of a thermal and mechanical stress, it differs from HP in the mode of heating (heat production and its transmission through the material) [103-105]. In HP, the heating element indirectly heats the punch, die and the powder through radiation, conduction and convection [104]. The passage of electric current through the heating element produces heat (Joule heating or ohmic heating or resistive heating) and the power of heat generated depends on current and resistance of the heating element [103, 104]. Further, the heating rate depends exclusively on the heat transfer modes (radiation, conduction and convection) [104]. However, in SPS the electric current and heat (Joule heat) are passed directly through the punches. The electric current density is of the order  $> 10 \text{ kA cm}^{-2}$  and the heating rate of the powder could reach  $10^6 \text{ K s}^{-1}$  [104]. Further details about this technique and the experimental conditions (electric effects, thermal effects, mechanical effects and sintering atmosphere) which would affect the final densification are explained in ref. [103]. This method is particularly useful for producing oxides with high density and very small grain size ( $< 1 \mu\text{m}$ ) [62, 103, 108].

Sintering data pertaining to SPS of nc-HfO<sub>2</sub>, nc-YSH and Y<sub>2</sub>O<sub>3</sub> are rather limited. Tyrpekl et al. [109] had prepared YSH (Hf<sub>0.85</sub>Y<sub>0.15</sub>O<sub>2-x</sub>) by employing the external gelation method and the derived beads were sintered by using SPS (57 MPa; 1873 K; 5 min). Further, no reports have been published so far on the SPS of nc-HfO<sub>2</sub> powders. Bu et al. [110] had sintered ball milled YSH powders by using both the conventional and SPS techniques (100 MPa; 1923 K;

3 min). Chapter 6 and Chapter 7 elaborate in detail about the SPS studies carried out by various authors on nc-Y<sub>2</sub>O<sub>3</sub> and HfO<sub>2</sub> (microcrystalline) and YSH powders. Hence, in this study we carried out the preliminary investigations on the SPS of nc-Y<sub>2</sub>O<sub>3</sub>, nc-HfO<sub>2</sub> and YSH. Further, the SPS studies of volume combustion derived nc-Y<sub>2</sub>O<sub>3</sub> powders and SMS derived nc-HfO<sub>2</sub> and YSH powders reported in this study are first of its kind.



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## Chapter 2

### Experimental

*In this chapter details pertaining to the chemicals, reagents and materials that have been used in this study and the experimental procedures and instruments that had been used for characterizing the powders, green pellets and sintered products are also presented.*

#### 2.1 Chemicals

Uranium oxide powders and thorium nitrate of nuclear grade purity were supplied by M/s. Indian Rare Earths Limited (IREL) and Nuclear Fuel Complex (NFC), India respectively. Uranium metal of 99.9 % pure was supplied by BARC, Mumbai. Nitric acid, phosphoric acid, sulphuric acid and hydrofluoric acid of AR grade were procured from M/s. Merck, India. Ferroin indicator (0.025 M) and citric acid of AR grade (>99.5 %) were obtained from Loba Chime Pvt. Ltd. India. Ferrous ammonium sulphate (AR grade) was procured from M/s. Merck, India. Hafnium (IV) chloride (99.9% pure) and yttrium nitrate hexahydrate (99.9% pure) were procured from M/s. Otto Chemie Pvt. Ltd. India.  $\text{KNO}_3$  (GR 99.5 %) and  $\text{NaNO}_3$  (GR 99.5 %) were obtained from M/s. Merck Specialties Pvt. Ltd, India. Propan-2-ol and silver nitrate (AR grade) were received from M/s. Merck, India. Dibutyl phthalate (DBP 99 % pure) was supplied by M/s. Ranbaxy Fine Chemicals Ltd, India.

#### 2.2 Scaled-up synthesis of nanocrystalline oxide powders

Nanocrystalline powders of urania, thoria and yttria were prepared on a 60 g scale by using citrate gel-combustion method. Hafnia and yttria stabilized hafnia (YSH) were prepared on a 30 g scale by using the SMS.

## 2.2.1 Preparation of nanocrystalline powders by gel-combustion method

### 2.2.1.1 Preparation of uranyl nitrate

Urania powder was converted quantitatively into  $U_3O_8$  powders by heating in air at 773 K for 4 h. An appropriate amount of this powder was taken and dissolved in concentrated nitric acid (12 M). This solution was heated on a hot plate to dryness to obtain uranyl nitrate crystals, which were dissolved subsequently in distilled water. The amount of nitrate present in this solution was quantitatively determined by titrimetry [1]. For this estimation, a known quantity of uranyl nitrate solution was taken along with 25 mL of 0.2 N ferrous ammonium sulphate (FAS), acidified with 10 mL of (12.2 M) HCl and 25 mL  $H_2SO_4$  (18.4 M) and titrated against  $K_2Cr_2O_7$  (0.1 N) by using ferroin indicator under ice cold condition. The exact amount of fuel (citric acid or sucrose) required for carrying out the combustion reaction with a particular value of fuel to nitrate mole ratio (R) was calculated from the estimated value of the concentration of nitrate.

### 2.2.1.2 Preparation of yttrium nitrate and thorium nitrate

Yttrium nitrate solution was prepared by dissolving preheated (473 K, 2 h)  $Y_2O_3$  in 12 M nitric acid by warming it on a hot plate. In a typical experiment, yttrium nitrate / thorium nitrate solution was prepared by dissolving an appropriate quantity of the metal nitrate in a minimum quantity of distilled water. The nitrate content of this solution was estimated by using titrimetry [1] (Section 2.2.1.1).

### 2.2.1.3 Citrate gel-combustion synthesis of nc-urania, nc-thoria and nc-yttria powders

In a typical gel-combustion synthesis (urania, thoria and yttria), desired quantities of the fuel and oxidant were dissolved in a minimum quantity of demineralized water and warmed on a hot plate. R values chosen for the preparation of nc-urania, nc-thoria and nc-yttria powders are presented in Table 2.1.



**Table 2.1 R values of the mixtures employed in citrate gel-combustion experiments**

S. No.	Materials	Index			Value of R & index “XX”								
		A	C	H									
1	nc-urania	U <sub>C</sub> XXA	U <sub>C</sub> XXC	U <sub>C</sub> XXH	R	0	0.05	0.10	0.25	0.50	0.75	0.90	1.00
					XX	0	05	10	25	50	75	90	100
2	nc-thoria	T <sub>C</sub> XXA	T <sub>C</sub> XXC	-	R	0	0.05	0.125	0.17	0.25	0.50		
					XX	0	05	12.5	17	25	50		
3	nc-yttria	Y <sub>C</sub> XXA	Y <sub>C</sub> XXC	-	R	0.17							
					XX	17							

The combustion mixture was gelated on a hot plate. Upon prolonged heating the gel got dehydrated and auto ignition ensued leaving behind a carboneous residue. These powders were named as “as prepared” powders (A). These powders were calcined in air in a furnace fitted with SiC heating element at 1073 K for 4 h to remove the residual carbon. The powders thus derived were named as the “calcined” powders (C).

“Calcined” urania powders were subsequently reduced to UO<sub>2</sub> in a flowing stream of hydrogen (flow rate = 400 mL min<sup>-1</sup>) at a pressure of 49 to 98 kPa in a custom made furnace equipped with inconel sample holders at 1123 K for 5 h 30 min. The powders thus derived were named as “hydrogen reduced” powders (H). The indices used to denote the different “combustion derived” samples are presented in Table 2.1

### 2.2.2 SMS of nc-Hafnia and nc-YSH

Fine grained nc-hafnia and nc-YSH were prepared in bulk quantities (30 g) by using SMS. In a typical experiment an appropriate quantity of the eutectic salt mixture (NaNO<sub>3</sub>-KNO<sub>3</sub>) was mixed with either HfCl<sub>4</sub> and NaNO<sub>2</sub> (for preparing nc-HfO<sub>2</sub> powders) or Y(NO<sub>3</sub>)<sub>3</sub>.6H<sub>2</sub>O and HfCl<sub>4</sub> (for synthesizing nc-yttria stabilized hafnia powders). The weight ratio of metal salts to that of the eutectic mixture was maintained at 1:4. This reaction mixture was transferred into a

180 mm long one end closed quartz reaction tube, which in turn was placed into a quartz muffle tube (400 mm long, 100 mm outer diameter, 2.5 mm thick) [Fig. 2.1].

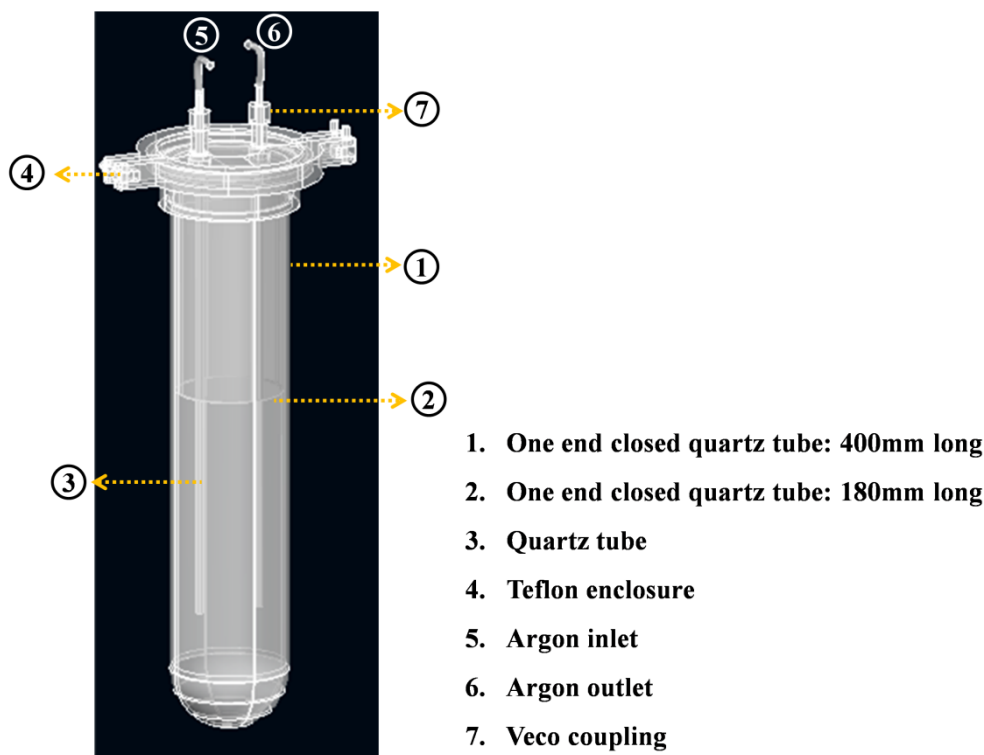


Figure 2.1 A schematic of the experimental set-up used in the SMS of nc-HfO<sub>2</sub> and nc-YSH

The entire assembly was lowered into a pit type nichrome wire wound resistance furnace (M/s. High Temp Ind, Kochi, India). The mouth of this muffle tube was covered with a lid fabricated out of poly tetra fluoro ethylene (PTFE) that had provisions for purging argon through the reaction mass. The reaction mixture was heated under an argon flow of 250 mL min<sup>-1</sup> at 673 K, for an hour and then cooled. Subsequently the whole assembly was cooled to room temperature. The contents were discharged from the reaction tube and treated with demineralized water, upon which the chlorides and nitrates dissolved leaving behind an insoluble oxide residue. Washing was repeated many times and the supernatant liquid was tested for chloride residue. The washing was stopped when the supernatant liquid did not yield either turbidity or a white precipitate upon treating with a few drops of AgNO<sub>3</sub> solution (0.1 wt/vol %). The powders thus

obtained were washed and were dispersed in propan-2-ol and ultrasonicated for 1 h at 323 K. Subsequently, this suspension was subjected to vacuum filtration to obtain the product. The oxide residue was dried in an oven at 393 K in air for 5 h and stored in an air tight container for further processing. The preparation of nc-HfO<sub>2</sub> powder was carried out with five different salt mixtures that contained nitrite to nitrate in the mole ratio ( $\Phi$ ) of 0, 0.05, 0.11, 0.32 and 0.82 respectively (Flow sheet-Fig. 2.2). The details pertaining to the nomenclature used to denote the mixtures and products are given in Table 2.2.

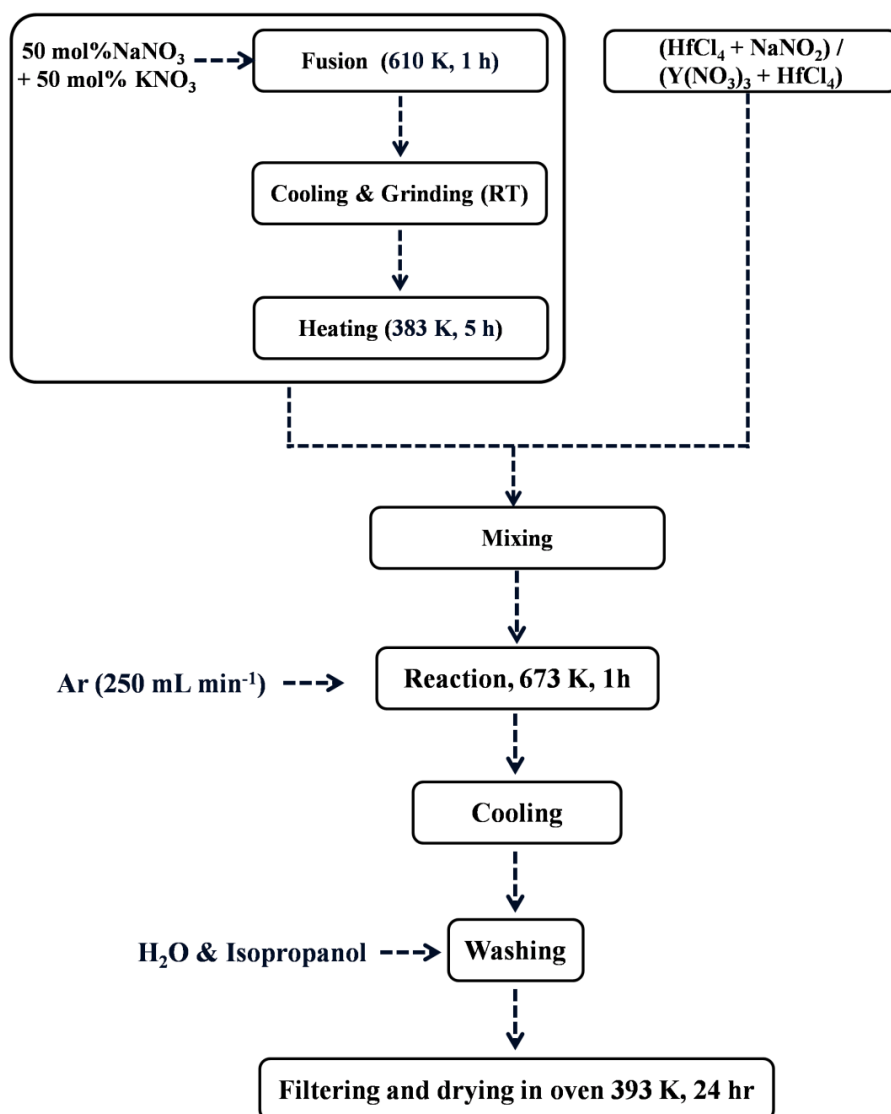


Figure 2.2 Flow sheet for the preparation of nc-HfO<sub>2</sub> / nc-YSH through SMS

**Table 2.2  $\Phi$  values of the mixtures and indices of powders derived in SMS**

S. No.	Materials	Index	Value					
1	nc-HfO <sub>2</sub>	HfYD	$\Phi$	0	0.055	0.11	0.32	0.82
			Y	0	5.5	11	32	82
2	nc-YSH	xxYSH	(mol% of Y)	6	10	14	20	30
			xx	6	10	14	20	30

where  $D$  – dried powders and  $Y = \Phi * 100$

### 2.3 Preparation of porous UO<sub>2</sub>

Porous UO<sub>2</sub> bodies (either foam or a pellet) were prepared by two different methods. UO<sub>2</sub> foam was prepared through the ignition of a gel made from sucrose and uranyl nitrate while the porous pellets were prepared from a nc powder derived through the citrate gel combustion of uranyl nitrate.

#### 2.3.1 Novel gel-combustion process for the preparation of porous UO<sub>2</sub> pellets

In the preparation of porous UO<sub>2</sub> pellets a procedure similar to that employed in the preparation of UO<sub>2</sub> powders (Section 2.2.1) was used, except that the calcination and hydrogen reduction steps were excluded. The “as prepared” powders ( $R = 0.25$  and  $1.0$ ) were consolidated at different pressures viz., 60, 120, 180, 243, 280, 317 and 353 MPa.

#### 2.3.2 Novel gel-combustion process for the preparation of UO<sub>2</sub> foam

In a typical experiment the exact quantity of sucrose required to carry out the reaction with a predetermined sucrose to nitrate mole ratio ( $R$ ) was calculated. This mixture containing sucrose and uranyl nitrate held in a polytetrafluoroethylene (PTFE) beaker (200 mL) was heated on a hot plate to form a dark viscous resin and subsequently the urania xerogel. These xerogel was heated at 393 K for 24 h in an oven. The product thus obtained was then cut into pieces of definite shapes.

## 2.4 Thermal analysis of gel-combustion reaction, salt melt reaction and products

### 2.4.1 Differential Scanning Calorimetry (DSC)

Heat flux differential scanning calorimetry (DSC) supplied by M/s. Mettler Toledo GmbH, Switzerland (model DSC821e/700) was used to determine the quantity of the heat liberated during the combustion reaction. For the DSC experiment, citrate gels containing thorium ( $R = 0.50$ ) and uranyl ions ( $R = 0.25$ ) were prepared, dried and loaded in a Pt pan of 70  $\mu\text{L}$  capacity and heated at  $10\text{ K min}^{-1}$  in flowing high purity  $\text{O}_2$  ( $50\text{ mL min}^{-1}$ ). At first, the sample was heated to 378 K and held at this temperature for about 10 min and subsequently cooled to room temperature in flowing  $\text{O}_2$ . Without altering the rates of heating and gas flow, the mixture was heated again from room temperature to 973 K. The details of the experimental procedure adopted for carrying out the calibration of the DSC instrument for the measurement of temperature, heating rate and heat flow are described elsewhere [2]. DSC experiments (similar to those described earlier) were also carried out with gels containing uranyl nitrate and citric acid ( $R = 0.25$ ) at different heating rates viz., 5, 10, 15 and  $20\text{ K min}^{-1}$  to elucidate the kinetics and mechanism of citrate gel-combustion reaction.

In the mixtures used for SMS, in order to ascertain the eutectic reaction temperature ( $\text{NaNO}_3\text{-KNO}_3$ ), about 3 mg of the eutectic salt mixture was loaded in a Pt pan (70  $\mu\text{L}$ ) and heated at a rate of  $10\text{ K min}^{-1}$  under flowing high purity Ar gas (flow rate =  $50\text{ mL min}^{-1}$ ) in the temperature range 298 K to 973 K.

### 2.4.2 Thermogravimetry-Differential Thermal Analysis coupled with Mass Spectrometry (TG-DTA-MS)

The thermal decomposition of the gel containing uranyl nitrate and citric acid was investigated with the help of simultaneous thermogravimetry (TG) coupled with differential

thermal analysis (DTA) and mass spectrometry (MS). A TG-DTA-MS system SETSYS Evolution 16/18, supplied by M/s Setaram, France was used for this purpose.

Simultaneous thermogravimetry (TG) and differential thermal analysis (DTA) coupled with mass spectrometry (MS) analysis of gel containing thorium nitrate and citric acid as well as mixtures of  $\text{KNO}_3$  and  $\text{NaNO}_3$  (with and without  $\text{NaNO}_2$ ) were carried out by using TG-DTA-MS (STA 449 - F3 Jupiter Model) supplied by Netzsch, Germany.

## **2.5 Characterization of the powders**

### **2.5.1 Measurement of bulk density ( $\rho_B$ ) of the powders**

An electronic balance supplied by M/s. Scaltec, GmbH, Germany was used to estimate the bulk density of all the powders. Bulk densities of all the powders were measured from the weight of the powder that filled up to the rim of a cuvette of known volume (5 mL). The average values of five measurements are reported here.

### **2.5.2 Determination of size distribution of particles in the nc-powders**

A particle size analyzer (laser light scattering, Mastersizer, M/s. Malvern, Worcestershire, UK) was used to measure the size distribution of particles. This equipment was calibrated with alumina standards supplied by NIST, USA. A suspension of the desired sample in demineralised water prepared by stirring was used to determine the particle size distribution (PSD). An appropriate quantity of sample was dispersed into the holder containing millipore water with stirring (2500 rpm). Average of ten measurements is reported. The size distribution of particles was deconvoluted using Origin<sup>®</sup> 6.1 software (OriginLab Corporation, USA).

### **2.5.3 Measurement of specific surface area (SSA) of the powders**

Specific surface area (SSA) of all the powders was determined by using Thermo Scientific Surfer gas adsorption porosimeter (Thermo Fisher Scientific S.p.A, Milan, Italy). Blank analyses

as well as calibration were carried out before analyses with the help of powder standards obtained from NIST. The powders were heated (degassed) at 393 K to remove surface adsorbed moisture and gases and were subsequently evacuated at a pressure of 0.1 Pa for 5 h by using a rotary pump (Pfeiffer-Model Duo1.6, Germany).

#### **2.5.4 Determination of carbon residue (RC) of particles in the nc powders**

Carbon residue present in all these samples was determined by using a carbon analyzer (Eltra CS 800, Germany). Mixtures containing about 200 mg of the samples and 1500 mg of tungsten were taken in an alumina crucible and heated in an induction furnace under flowing O<sub>2</sub>. The CO<sub>2</sub> evolved was quantitatively measured by using an IR detector.

#### **2.5.5 Determination of size and distribution of pores (P<sub>o</sub>SD)**

##### **a) Mercury porosimetry**

Analyses of the distribution of sizes of the pores (10 nm to 50 µm) present in the powders were carried out by using Pascal 140 and 440 mercury porosimeters (Thermo Fisher Scientific S.p.A, Milan, Italy) at an operating pressure range of 0.1 to 400 kPa and 0.1 to 400 MPa respectively. Blank analyses as well as calibration were carried out before analyzing the sample in the mercury porosimeter experiments by using alumina standards (SRM 1918) obtained from NIST.

##### **b) Gas adsorption**

Analyses of size distribution of pores (< 50 nm) present in the powders were also carried out by using Thermo Scientific Surfer gas adsorption porosimeter (Thermo Fisher Scientific S.p.A, Milan, Italy). Calibration was carried out by using powder standards obtained from NIST. Evaporation of the liquid N<sub>2</sub> condensate from the pores are related to the pore diameter. By using

Kelvin equation the pore diameter were derived from the volume of the gas desorbed (evaporated) from the pore.

### **c) Liquid immersion**

Open and closed porosity in all the sintered pellets and cups were determined by employing ASTM C1039-85 procedure. DBP was used as the pycnometric liquid. Average of five different measurements is reported here. This method involved measuring the volume of the open pores from the volume of the liquid entrapped in them. The volume of closed pores was obtained by difference from the total and open porosity.

### **2.5.6 Spectroscopic analysis of starting materials, gels and powders**

Uranyl nitrate and thorium nitrate samples were analyzed for impurity by using an Inductively Coupled Plasma – Mass Spectrometer (ICP-MS) [ELAN 250, M/s. Perkin Elmer, Canada]. ICP-OES measurements were carried out with Ultima C, HORIBA, Jobin Yvon, Longjumeau, France. This instrument was calibrated by measuring standard solutions of metals certified by National Institute of Standards and Technology (NIST).

Nitrate solutions were mixed with 4 M HNO<sub>3</sub> and equilibrated along with a drop of HF and tributyl phosphate (TBP) solution (30% TBP in dodecane). This process was repeated three times to remove uranium / thorium ions from the solution [3]. The aqueous solution thus obtained was diluted and subjected to ICPMS and ICPOES analysis.

The FTIR spectrum was recorded by using MB 100 FT-IR spectrometer (BOMEM, Canada). To obtain a good signal to noise (S/N) ratio, the samples were scanned for at least 8 times. This spectrometer has a resolution of 1 cm<sup>-1</sup> and operated in the region of 4000-400 cm<sup>-1</sup>. This instrument is equipped with deuterated triglycine sulfate (DTGS) detector. Calibration was carried out by using salicylic acid standard supplied by NIST.



UV-VIS-NIR spectrophotometer supplied by Shimadzu with model no. UV-3600 was used for spectrophotometric analysis. This instrument was equipped with three detectors, consisting of photomultiplier tubes for the ultraviolet and visible regions and InGaAs and cooled PbS detectors for near infrared region. The wavelength range of 200-1000 nm with double monochromator and rectangular cuvette made up of fused silica with an optical path length of 10 mm were used for measuring the absorbance of the metal complexes.

Micro Raman spectrometer supplied by M/s. Renishaw, (UK, model Invia) was used to record the Raman spectra. A laser excitation source of 514.5 nm was directed through a 10  $\mu$ m pinhole and was focused by using a microscope on to the sample (a few mg) which is placed on transparent slide. A charge coupled device was used as the detector. Raman shift in the wave numbers was calibrated by using 520.5 nm Raman line from a Si single crystal.

## **2.6 Preparation of pellets and cups**

A semi automatic double action (biaxial) hydraulic powder compacting press (Model No. 027) supplied by M/s. Sri Yugantak Engineers, Bangalore, India was used for compaction. Top punch, die and bottom punches made up of AISI D3 tool steel lined with tungsten carbide were used. These tools were cleaned with acetone before every compaction. To investigate the influence of the compaction pressures (CP) and to elucidate the critical compaction pressure each powder was compacted into green pellets (10 mm diameter) at different compaction pressures (CP) viz., 60, 120, 180, 220, 243, 280, 317 and 353 MPa.

Ceramic cups were compacted by using a double action hydraulic press which was supplied by M/s. Bemco hydraulics Ltd., Belgaum, India. The plungers were made out of high carbon - high chromium (HCHCr) steel while the die was made with tungsten carbide encased in

tool steel. The green cups were of the following dimensions; outer diameter x inner diameter x height = 10 mm x 6 mm x 5 mm.

## **2.7 Sintering of nanocrystalline green bodies**

### **2.7.1 Conventional Sintering (CS)**

The CS method involved sintering the green pellet at an isothermal temperature for 4h. The samples nc-UO<sub>2</sub>, nc-ThO<sub>2</sub>, nc-Y<sub>2</sub>O<sub>3</sub>, nc-HfO<sub>2</sub> and nc-YSH were sintered by using this procedure. The temperature and procedure used along with the indices of the specimens are given in Table 2.3. All the urania samples were sintered under flowing Ar+8%H<sub>2</sub> (500 mL min<sup>-1</sup>) while rest of the samples were sintered in air in a furnace equipped with MoSi<sub>2</sub> heating elements (M/s. Carbolite UK).

### **2.7.2 Two-step sintering (TSS)**

Two different two-step sintering (TSS) routines were used. TSS<sub>C</sub> method involved heating the sample at a lower temperature viz., 1073 K and then at a higher temperature 1473 or 1673 K for about 4 h. This method was used to sinter nc-UO<sub>2</sub> powders, nc-U<sub>3</sub>O<sub>8</sub> powders and foam. The details pertaining to the sintering routine and nomenclature are given in Table 2.3.

In the second TSS<sub>CW</sub> method the samples were held at a higher temperature 1873 K (held at this temperature for 30 min) and cooled to a lower temperature (either 1773 K or 1673 K) at 10 K min<sup>-1</sup> and held at the latter for about 4 h. This procedure was used in the sintering of nc-ThO<sub>2</sub>, nc-Y<sub>2</sub>O<sub>3</sub>, nc-HfO<sub>2</sub> and nc-YSH. The details pertaining to these sintering routines are presented in Table 2.3 along with the indices used for denoting different products.

**Table 2.3 Nomenclature used for indexing the sintered monoliths**

Sample	Form	Sintering method		Sintering schedule	Atm	Sample index	
Urania	UO <sub>2</sub>	Pellet	Conventional sintering (CS)	1673 K; 4 h; 5 K min <sup>-1</sup>	Ar+8% H <sub>2</sub>	U <sub>C</sub> XXS <sub>C</sub>	
			Two-step sintering (TSS <sub>1</sub> )	1473 K; 4 h; 3 K min <sup>-1</sup>		U <sub>C</sub> XXS <sub>1</sub>	
			Two-step sintering (TSS <sub>2</sub> )	<b>Step 1:</b> 1073 K; 2 h; 5 K min <sup>-1</sup> <b>Step 2:</b> 1673 K; 4 h; 3 K min <sup>-1</sup>		U <sub>C</sub> XXS <sub>2</sub>	
	UO <sub>2</sub> U <sub>3</sub> O <sub>8</sub>	Foam Pellet	Two-step sintering (TSS <sub>3</sub> )	<b>Step 1:</b> 1073 K; 30 min; 5 K min <sup>-1</sup> <b>Step 2:</b> 1473 K; 4 h; 5 K min <sup>-1</sup>		USXXXXS U <sub>C</sub> XXA-CP	
Thoria	ThO <sub>2</sub>	Pellet	Conventional sintering	Single step 1 (CS <sub>1</sub> ) Single step 2 (CS <sub>2</sub> )	Air	T <sub>C</sub> 13S <sub>CS1</sub> T <sub>C</sub> 13S <sub>CS2</sub>	
			Two-step sintering	Two-step sintering (TSS <sub>1</sub> )		<b>Step 1:</b> 1873 K; 30 min; 5 K min <sup>-1</sup> <b>Step 2:</b> 1673 K; 4 h; 5 K min <sup>-1</sup>	T <sub>C</sub> 13S <sub>1</sub>
			Two-step sintering	Two-step sintering (TSS <sub>2</sub> )		<b>Step 1:</b> 1873 K; 30 min; 5 K min <sup>-1</sup> <b>Step 2:</b> 1773 K; 4 h; 5 K min <sup>-1</sup>	T <sub>C</sub> XXS <sub>2</sub>
Yttria	Y <sub>2</sub> O <sub>3</sub>	Pellet	Conventional sintering	Single step 1 (CS <sup>Y</sup> <sub>1</sub> ) Single step 2 (CS <sup>Y</sup> <sub>2</sub> )	Air	Y <sub>C</sub> 13S <sub>CS1</sub> Y <sub>C</sub> 13S <sub>CS2</sub>	
			Two-step sintering	Two-step sintering (TSS <sup>Y</sup> <sub>1</sub> )		<b>Step 1:</b> 1873 K; 30 min; 5 K min <sup>-1</sup> <b>Step 2:</b> 1673 K; 4 h; 5 K min <sup>-1</sup>	Y <sub>C</sub> 13S <sub>1</sub>
			Two-step sintering	Two-step sintering (TSS <sup>Y</sup> <sub>2</sub> )		<b>Step 1:</b> 1873 K; 30 min; 5 K min <sup>-1</sup> <b>Step 2:</b> 1773 K; 4 h; 5 K min <sup>-1</sup>	Y <sub>C</sub> XXS <sub>2</sub>
Hafnia	HfO <sub>2</sub>	Pellet	Conventional sintering	Single step 1 (CS <sub>1</sub> ) Single step 2 (CS <sub>2</sub> ) Single step 3 (CS <sub>3</sub> )	Air	HfYD <sub>CS1</sub> HfYD <sub>CS2</sub> HfYD <sub>CS3</sub>	
			Two-step sintering	Two-step sintering (TSS <sub>1</sub> )		<b>Step 1:</b> 1873 K; 1 h; 3 K min <sup>-1</sup> <b>Step 2:</b> 1673 K; 1 h; 3 K min <sup>-1</sup>	HfYDS <sub>1</sub>
			Two-step sintering	Two-step sintering (TSS <sub>2</sub> )		<b>Step 1:</b> 1873 K; 30 min; 3 K min <sup>-1</sup> <b>Step 2:</b> 1773 K; 4 h; 3 K min <sup>-1</sup>	HfYDS <sub>2</sub>
Yttria stabilized hafnia	YSH	Pellet	Conventional sintering	Single step 1 (CS <sub>1</sub> ) Single step 2 (CS <sub>2</sub> ) Single step 3 (CS <sub>3</sub> )	Air	xxYSH <sub>CS1</sub> xxYSH <sub>CS2</sub> xxYSH <sub>CS3</sub>	
			Two-step sintering	Two-step sintering (TSS <sub>1</sub> )		<b>Step 1:</b> 1873 K; 1 h; 3 K min <sup>-1</sup> <b>Step 2:</b> 1673 K; 1 h; 3 K min <sup>-1</sup>	xxYSHS <sub>1</sub>
			Two-step sintering	Two-step sintering (TSS <sub>2</sub> )		<b>Step 1:</b> 1873 K; 30 min; 3 K min <sup>-1</sup> <b>Step 2:</b> 1773 K; 4 h; 3 K min <sup>-1</sup>	xxYSHS <sub>2</sub>

U<sub>C</sub>, T<sub>C</sub> and Y<sub>C</sub> indicate citrate gel-combustion derived urania, thoria and yttria powders respectively; Atm – atmosphere; XX denotes R value in %; CS-conventional sintering; Y = Φ\*100 and xx – mole fraction of yttrium (in %). Sintering schedule denotes soaking temperature, duration of soaking & heating/cooling rate.

## **2.8 Spark plasma sintering (SPS)**

Spark Plasma Sintering (SPS) studies of nc powders were carried out using Dr. Sinter Spark Plasma unit (Model SPS-625, SPS Syntex Inc., Japan). Monoliths of  $\text{HfO}_2$ , YSH and  $\text{Y}_2\text{O}_3$  were made by using uniaxial pressing under vacuum ( $\approx 0.133$  Pa). The die and punches were made of high density graphite (HDG) material. The dimension of the die and plungers were as follows: inner diameter - 10 mm, outer diameter - 30 mm, height - 40 mm and a centre pin hole - 0.50 mm. Before filling the HDG die with nanocrystalline powders; the inner surface of HDG die was covered with a graphite foil of thickness 0.15 mm. The graphite foil helps to facilitate the easy removal of sintered monoliths. To minimize the radiative heat losses at high temperatures, the die was covered with graphite felt (except the central pin hole). K type thermocouple was used to measure temperature till 873 K. An optical pyrometer was used to measure temperature beyond 873 K and it was focused on to a pin hole on the periphery of the graphite die. SPS compacts had a thickness and diameter of about 2.0 mm and 9.5 mm respectively. The applied voltage, current, temperature and pressure were recorded by the instrumentation provided in the equipment. A compaction pressure (CP) of 50 MPa was applied from the start of the experiment, till the end. The compacts were heated to 1873 K and soaked at this temperature for 7 min with a heating rate of either  $50 \text{ K min}^{-1}$  ( $\text{HfO}_2$ ) or  $100 \text{ K min}^{-1}$  ( $\text{Y}_2\text{O}_3$  and YSH). The sintering experiment comprising die and plunger were cooled naturally to room temperature to remove monoliths from the graphite die.

## **2.9 X-ray diffraction analysis of powders and pellets**

Phases present in the powder samples were identified by using X-ray diffraction (XRD) by using X'pert MPD system supplied by Philips, The Netherlands ( $\text{Cu K}_\alpha$  radiation ( $\lambda = 1.541 \text{ \AA}$ )), equipped with a graphite monochromator and a scintillation detector. Calibration

was carried out by using silicon and alumina standards supplied by NIST, USA. All the powder samples were used as such without any further processing, whereas the sintered pellets were grounded to a fine powder by using a mortar and pestle.

Spark Plasma sintered pellets were characterized by using Bruker X-ray diffractometer of grazing incidence X-ray diffraction (GIXRD), (Model: D8-Discover): Cu  $K_\alpha$  radiation of wavelength 1.5418 Å was used. The incident angle in the GIXRD measurements was kept as 0.3° which could probe upto a depth of 184 nm. The collection angle was increased in steps of 0.05° from 25° to 95°.

By considering the multiplicity factor and linear absorption coefficient, the volume fraction of monoclinic hafnia phase in YSH was derived by making use of eqn. (2.1) [4].

$$V_m = \frac{(1.6031 * I_m(11\bar{1}))}{1.6031 * I_m(11\bar{1}) + I_c(111)} \quad (2.1)$$

Where,  $I_m(11\bar{1})$  and  $I_c(111)$  represent the integrated intensity of the X-ray diffraction lines of the monoclinic ( $11\bar{1}$ ) and cubic (111) phases respectively.

The size of the crystallites in all these samples was estimated from the width of peaks in the X-ray diffraction (XRD) patterns [5]. All XRD patterns that are presented in this work represent raw data and the peaks obtained were well resolved. Crystallite sizes of all these samples were calculated by using both the Scherrer formula ( $Sc$ ) [eqn. 2.2] and the Hall-Williamson (HW) plots (eqn. 2.3), while the lattice strain was derived from the latter [5].

$$Sc_{XCS} = \frac{K\lambda}{\beta \cos \theta} \quad (2.2)$$

$$\beta \cos \theta = \frac{K\lambda}{HW_{XCS}} + 4\varepsilon \sin \theta \quad (2.3)$$

Where,  $\lambda$  is the X-ray wavelength (Cu- $K_\alpha$ ),  $K$  is crystallite shape factor,  $\beta$  is the full width at half maxima in radians,  $\theta$  is Bragg angle and  $\varepsilon$  is strain distribution within the material.

## **2.10 Measurement of green density ( $\rho_G$ ), radial and axial shrinkage and sintered density ( $\rho_S$ )**

Relative  $\rho_G$  of the pellets were obtained from their weight and volume. Average of the values obtained in five such measurements is reported. Radial and axial shrinkage were obtained by measuring the dimension of green and sintered pellets. Their dimensions were measured by using a digital screw gauge (accuracy of  $\pm 0.001$  mm) supplied by Mitutoyo, Japan. Density of the sintered pellets was measured at room temperature by using Archimedes method (ASTM: B962-13) [6], in which, dibutyl phthalate ((DBP)\*; density -  $1.056 \text{ g cm}^{-3}$  (293 K)) was used as the immersion liquid. The mean of the values obtained in five measurements is reported here.

## **2.11 Microstructural characterization**

### **2.11.1 Scanning Electron Microscopy (SEM) and Energy Dispersive X-ray Spectroscopy (EDS) of powders and pellets**

For carrying out the SEM analyses, a few milligrams of the powder was dispersed on to the carbon tape. The morphological analysis of these samples was carried out by using a Field Emission Scanning Electron Microscope (FE-SEM, Model-Helios NanoLab 600i), (FEG Quanta, Philips, The Netherlands). Pieces of a sintered pellet were polished and thermally etched at the corresponding sintering temperature. These were placed on a carbon tape and were coated with gold.

### **2.11.2 Transmission Electron Microscopy (TEM) and Electron Energy Loss Spectroscopy (EELS)**

For the TEM analyses, a few milligram of the powder under investigation was suspended in propan-2-ol and deagglomerated by ultrasonication. A few drops of this solution were then

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\* Generally it is preferable to use a liquid with low surface tension low vapor pressure. DBP is inert, has low vapor pressure and has a surface tension compared with water.

dropped on to a holey carbon grid. TEM investigations were carried out in a LIBRA 200FE (Carl Zeiss) high resolution TEM operated at 200 kV equipped with energy dispersive X-ray spectroscopy (EDS) analysis, scanning transmission electron microscopy (STEM) and an in-column energy filter.

Both SEM and TEM images were analyzed by using CaRine v3.1<sup>®</sup> software.

## **2.12 Studies on the compatibility of molten uranium with crucibles made out of HfO<sub>2</sub> and YSH**

Sintered hafnia and YSH crucibles were used to investigate the compatibility of these crucibles with the molten uranium. Experiments pertaining to these investigations were carried out by using a custom made “spot technique” instrumentation. The construction of this equipment and the principle behind the experiment are explained in detail in ref. [7-9]. Prior to the experiment, these crucibles together with the Knudsen cell in which they were held were degassed under high vacuum ( $2.7 \times 10^{-7}$  mbar) for about 1 h by radio frequency (RF) induction heating at 1773 K (Fig. 2.3).

In a typical experiment, pieces of uranium were taken in a degassed sintered hafnia or YSH crucible. This crucible along with the Knudsen cell and its susceptor were heated by electromagnetic induction (RF) under vacuum ( $2.7 \times 10^{-7}$  mbar). The Knudsen cell orifice was viewed by using a long distance optical microscope (QM1, M/s. Questar, Inc. USA). Temperature at which a spot is observed (fusion) was measured by focusing the black body hole (at the bottom of the Knudsen cell) on to a two color pyrometer (M78, M/s. Micron, USA). The corresponding video image of the sample surface was viewed through the Knudsen cell orifice by using a long distance optical microscope, fitted with a charge coupled device (CCD) camera

(WAT 207 A, M/s. Watec Co. Ltd., Japan). After the experiment these crucibles were recovered and were subjected to microstructural investigations by using SEM.

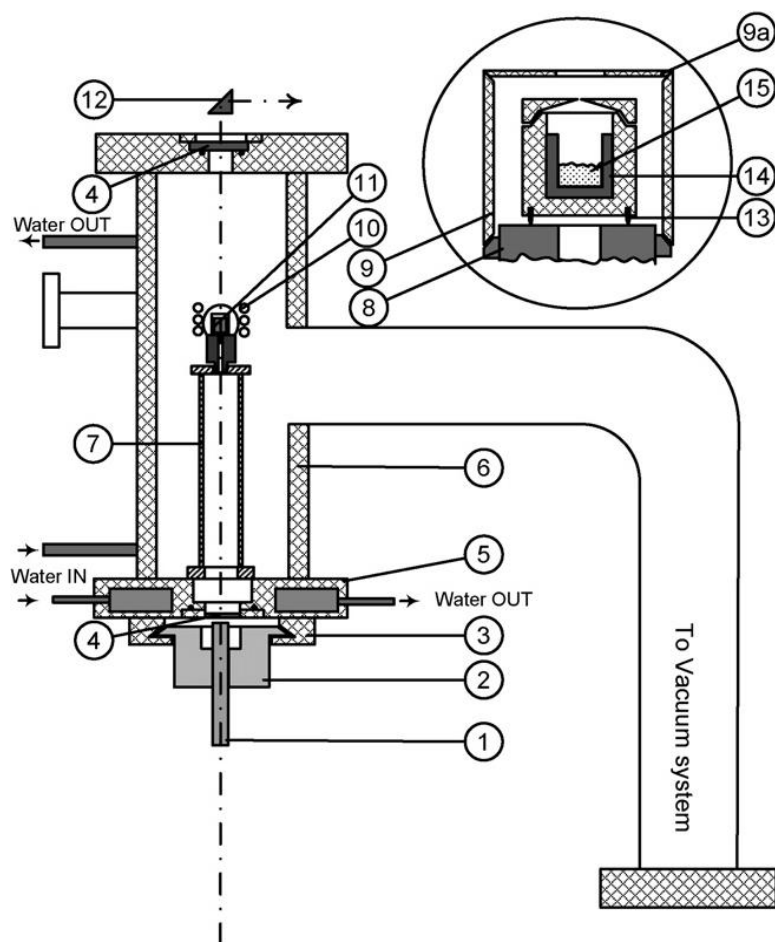


Figure 2.3 Schematic showing the experimental system used for the spot experiments: 1) IR two color pyrometer; 2) fixture for pyrometer; 3) optical rail; 4) quartz optical window; 5) bottom flange; 6) vacuum chamber; 7) sample support assembly; 8) molybdenum table; 9 & 9a ) radiation shield; 10) RF coil; 11) Knudsen cell; 12) quartz prism; 13) tungsten legs; 14) crucible; 15) sample (Adopted from [9])



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## Chapter 3

# Synthesis, Characterization and Sintering of Nanocrystalline Urania

*This chapter explains in detail about the investigations carried out on bulk synthesis of nc-UO<sub>2</sub> by using citrate gel-combustion method. An attempt was made to evaluate the mechanism and the kinetic parameters of the “volume combustion reaction” of an initial mixture with a citric acid to nitrate mole ratio (R) of 0.25. The utility of “two-step sintering” of nc-UO<sub>2</sub> powders was also investigated. The shrinkage, distribution of porosity as well as the microstructure of the sintered pellets were also studied.*

### 3.1 Purity of the starting materials

The starting materials used in the preparation of the combustion mixtures were devoid of impurities that would significantly alter the characteristics of the gel-combustion derived powders as testified by the ICP-MS analysis of the starting urania powders (Table 3.1).

### 3.2 Gel-combustion synthesis

The gel-combustion synthesis [1-6] involves blending together an oxidizing agent (metal nitrate) and an organic complexing agent in a definite proportion to form a homogenous aqueous solution, followed by gelation and combustion. In this study, the composition of the combustion mixture was found to influence the properties of the product (Table 3.2). No attempt has been made, however, to measure the reaction temperatures as well as the heat of the reaction since these reactions were carried out in an open glass bowl and not in a thermally isolated environment. “Volume combustion” a vigorous reaction that involved sudden expulsion of gases

**Table 3.1 Impurity analysis by ICPMS**

Elements	Ni	Zn	Mo	Ba	Al	Mg	Ca	V	Cr	Mn	Fe	Cu	Ce	La	Sm	Eu	Gd	Dy	C
Conc. of impurities /ppm	8	2	9	<1	<1	<1	<1	<1	7	8	45	<1	1	6	<1	<1	28	<1	<100

**Table 3.2 Characteristics of the urania powder synthesized by “gel-combustion”**

Sample	Mole ratio	Color of the sample			$\rho_g$ (Mg m <sup>-3</sup> )			RC (ppm)			SSA (m <sup>2</sup> g <sup>-1</sup> )			O/U		
	$\frac{N_{CA}}{N_{NO_3^-}}$															
		A	C	H	A	C	H	A	C	H	A	C	H	C	H	H <sub>a</sub>
U	0	Y	Bl	Br	2.39	2.15	2.68	110	114	92	7	5	6	2.62 ± 0.05	2.02 ± 0.04	2.06 ± 0.04
U <sub>C</sub> 5.5	0.055	Or	Bl	Br	1.01	0.88	1.22	563	185	109	5	5	5	2.67 ± 0.02	2.06 ± 0.03	2.09 ± 0.03
U <sub>C</sub> 10	0.100	Ol	Ol	LBr	0.18	0.26	0.44	417	158	116	7	7	7	2.68 ± 0.04	2.06 ± 0.04	2.12 ± 0.04
U <sub>C</sub> 25	0.249	LOl	LOl	Ol	0.06	0.09	1.61	660	447	156	18	8	10	2.74 ± 0.07	2.15 ± 0.05	2.13 ± 0.04
U <sub>C</sub> 50	0.499	DGy	Bl	Re	1.79	1.59	3.73	877	631	229	6	5	6	2.74 ± 0.06	2.10 ± 0.06	2.14 ± 0.05
U <sub>C</sub> 75	0.750	DGy	Gy	Re	1.29	1.25	2.63	1270	552	274	6	5	6	2.75 ± 0.08	2.04 ± 0.03	2.12 ± 0.03
U <sub>C</sub> 90	0.899	DGy	Gy	Gy	1.18	1.11	2.42	1163	552	296	6	5	5	2.69 ± 0.02	2.12 ± 0.06	2.20 ± 0.02
U <sub>C</sub> 100	0.994	DGy	DGy	Bl	1.28	1.15	2.27	1004	698	310	6	5	5	2.73 ± 0.06	2.05 ± 0.02	2.19 ± 0.02

*Y=Yellow; Bl - Black; Br/LBr – Brown/Light Brown; Gy/DGy - Grey/Dark Grey; Ol/LOl - Olive/Light Olive; Or - Orange; Re - Dark Red; CA - Citric acid; A, C & H = “As-prepared”, Calcined & Hydrogen reduced powders; O/U – mole ratio of oxygen to uranium; H<sub>a</sub> - O/U of H after 52 days*

that yields a very voluminous product was observed in the mixtures with R values of 0.10 and 0.25, whereas all the other gels decomposed through a reaction at a moderate pace followed by auto ignition with attendant smoldering.

### 3.3 IR spectroscopy of the precursor and products

The FTIR spectra of citric acid, uranyl nitrate and the products derived from a mixture with an R value of unity (“A”, “C” and “H” powders) are depicted in Fig. 3.1. The absorption minima observed in these specimens are enlisted in Table 3.3 are comparable to the standard spectra cited in Refs. [7-9].

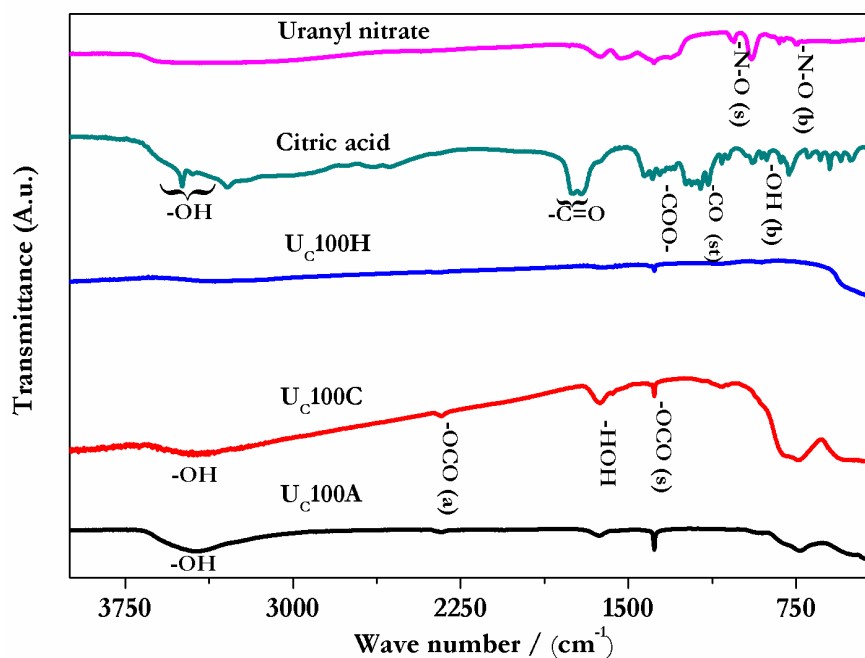


Figure 3.1 FTIR spectra of precursors and products [*s*-symmetric, *a*-asymmetric, *st*-stretching and *b*-bending]

Table 3.3 Absorption minima of starting materials and products

Functional group	Wave number (cm <sup>-1</sup> )
O-H	3300 - 3500 cm <sup>-1</sup> (s); 1419 cm <sup>-1</sup> (b)
C-O	1706 cm <sup>-1</sup> (st)
COO <sup>-</sup>	1384 cm <sup>-1</sup> (st)
N-O	1021 cm <sup>-1</sup> (st); 813 cm <sup>-1</sup> (rocking); 740 - 750 cm <sup>-1</sup> (s.b) and 710 cm <sup>-1</sup> (a. b)

*st* – stretching, *b* – bending; *s.b* and *a.b* symmetric and asymmetric bending

The IR spectra pertaining to the sample U<sub>C</sub>100A was devoid of the absorption signatures pertaining to citric acid and uranyl nitrate indicating that the reaction has proceeded to completion. In the spectra of the powder U<sub>C</sub>100H, the intensities observed were the lowest, possibly due to the complete removal of the organic precursor and nitrates. The bands pertaining to O=C=O and O-H observed in the powders U<sub>C</sub>100A and U<sub>C</sub>100C could be ascribed to the presence of adsorbed CO<sub>2</sub> and moisture. However, since a quantitative determination of the constituent moieties was not attempted, inter comparison of these spectra would not be appropriate. The IR spectra, in general, suggest that the reaction has proceeded up to completion.

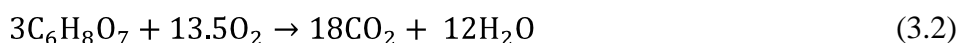
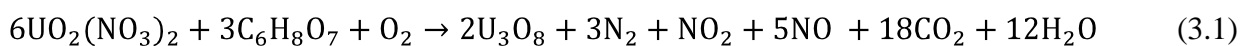
### **3.4 Thermal analysis**

#### **3.4.1 Analysis by using TG-DTA-MS**

The results obtained in the TG-DTA-MS investigation of the pyrolysis of a gel prepared from a mixture with an R value of 0.25, are presented in Fig. 3.2 and Fig. 3.3. Two distinct weight loss regions were observed in the TG curve. The first step in the TG curve reveals a weight loss due to simultaneous reactions (slope change). In order to reaffirm this observation, the first TG curve was differentiated (DTG). The DTG curve, further confirmed that the TG curve could be resolved into two distinct peaks revealing that the simultaneous reaction did take place (inset in Fig. 3.2). This could be due to the dehydration of citric acid to form aconitic acid [10]. These two steps could therefore be attributed to the direct participation of citric acid in the combustion reaction as well as the participation of its dehydrated moiety (aconitic acid) [10]. A minor weight loss was observed (Fig. 3.2) at 625 K and at 830 K which may be due to the oxidation of trace amounts of carbon present in the sample. This is further substantiated by the mass spectrometric data of the gases evolved during combustion reaction (Fig. 3.3). Three

exothermic peaks were observed in the DTA with onset temperatures at 430 K, 535 K and 625 K (Fig. 3.2).

The mass spectrometric analysis of the gases evolved at various stages from the sample is shown in Fig. 3.3. As seen in the figure (Fig. 3.3) the gases evolved corresponding to the first step of the mass loss are H<sub>2</sub>O, N<sub>2</sub>, CO<sub>2</sub>, NO and NO<sub>2</sub>. The gases evolved in the second step are H<sub>2</sub>O, CO<sub>2</sub> and CO. The mass spectrometric, DTA and TG analyses suggest that the following reactions (eqns. 3.1-3.2) probably take place during the gel-combustion synthesis.



The reaction pertaining to the first exothermic peak given in eqn. 3.1 corresponds to the overall reaction. The second exothermic peak could therefore be attributed to the decomposition of residual unreacted fuel (citric acid) [eqn. 3.2]. This is also substantiated by the fact that the evolution of N<sub>2</sub> [11] which is a typical product of the combustion reaction [12, 13].

The third exothermic peak was observed at the 625 K. The weight loss (<1 wt %) observed at temperatures above 625 K is due to the oxidation of residual carbon present in the sample. The EGA analysis (Fig. 3.3) does show the evolution of CO<sub>2</sub> at temperatures above 625 K. Since the heat of the combustion of trace amounts of carbon would be quite low, it is reasonable to assign the third exothermic peak to the crystallization of uranium oxide (U<sub>3</sub>O<sub>8</sub>). The minor mass loss at 830 K corroborates well with the evolution of CO<sub>2</sub> at 830 K. The XRD patterns of nc-U<sub>3</sub>O<sub>8</sub> phase (both “A” and “C”) are shown in Fig. 3.7. These analyses were carried out on samples retrieved immediately after the completion of combustion reaction (around 673 K) as well as beyond the latter (973 K).

**Table 3.4 XCS of urania powders**

Sample	A			C			H		
	Sc (nm)	HW (nm)	Strain $\times 10^{-3}$	Sc (nm)	HW (nm)	Strain $\times 10^{-3}$	Sc (nm)	HW (nm)	Strain $\times 10^{-3}$
U	-	-	-	48	283	1.58	42	146	1.45
U <sub>C</sub> 5.5	14	-	-	45	252	1.69	40	113	1.36
U <sub>C</sub> 10	13	23	4.96	41	50	0.36	39	79	1.06
U <sub>C</sub> 25	20	32	2.75	36	38	0.10	32	47	0.77
U <sub>C</sub> 50	19	24	1.75	35	58	0.97	33	54	0.98
U <sub>C</sub> 75	18	24	1.42	34	69	1.34	35	85	1.39
U <sub>C</sub> 90	20	51	4.23	38	87	1.32	29	71	1.66
U <sub>C</sub> 100	24	90	4.63	38	98	1.61	27	45	1.22

**Table 3.5 PSD and total pore volume of urania powders**

Sample	Particle size distribution (vol %)										
	10 vol. % of sample has size less than (μm)			50 vol. % of sample has size less than (μm)			90 vol. % of sample has size less than (μm)			Total pore volume (mm <sup>3</sup> g <sup>-1</sup> )	
	A	C	H	A	C	H	A	C	H	C	H
U	2	6	5	11	56	13	179	662	63	226	269
U <sub>C</sub> 5.5	6	10	7	42	53	33	229	246	141	433	521
U <sub>C</sub> 10	7	4	5	62	32	32	270	162	131	699	1116
U <sub>C</sub> 25	5	3	11	27	14	61	108	56	220	1549	4787
U <sub>C</sub> 50	2	4	3	24	28	21	411	304	371	320	281
U <sub>C</sub> 75	2	3	3	26	33	27	192	254	150	405	403
U <sub>C</sub> 90	2	3	3	29	31	35	196	245	149	434	381
U <sub>C</sub> 100	2	4	3	38	48	20	166	230	97	414	414

Both “A” and “C” samples revealed the presence of nc-U<sub>3</sub>O<sub>8</sub> phase. However, the XRD peaks of the latter were more prominent and well resolved due to significant grain coarsening. The XCS computed by using the HW method for the sample is 24 nm at 673 K (Table 3.4). The



nc- $\text{U}_3\text{O}_8$  when heated in air at 1073 K for 4 h yielded the product with a higher crystallite size of 58 nm. The XRD patterns of nc- $\text{U}_3\text{O}_8$  (both “A” and “C”) are shown in Fig. 3.7.

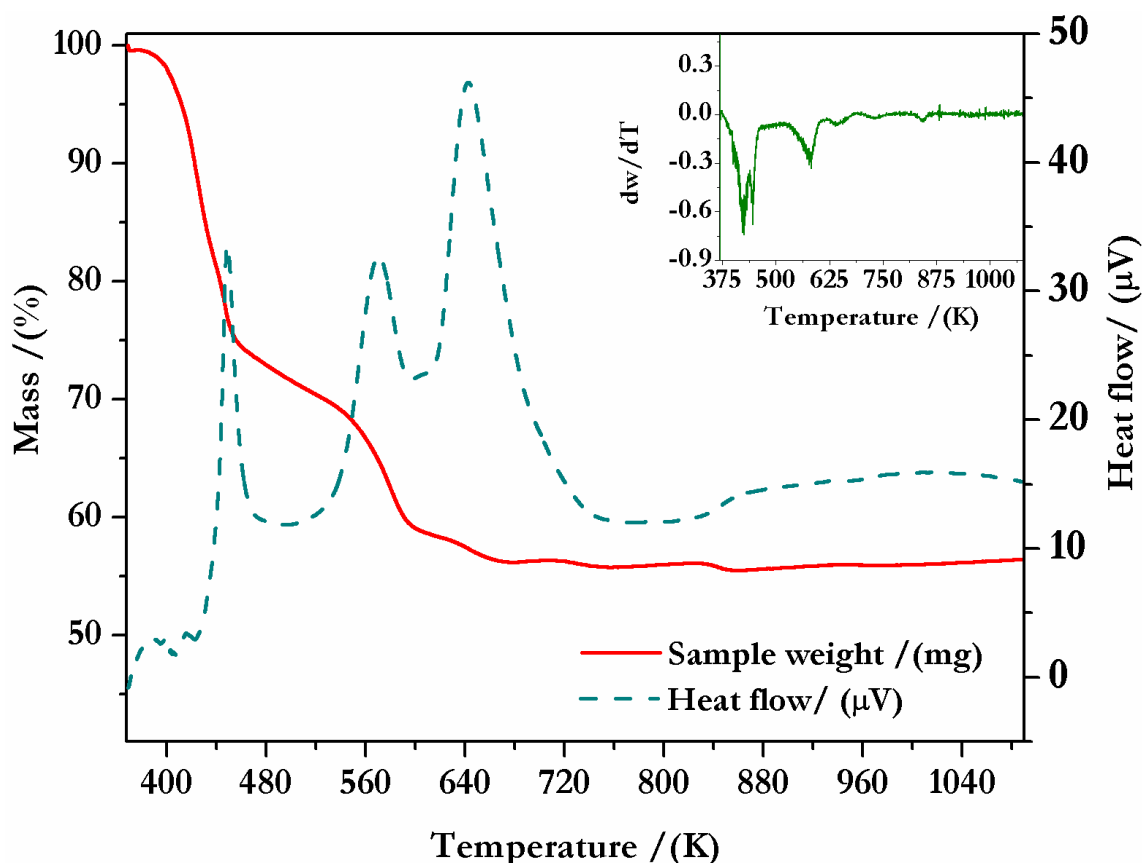


Figure 3.2 TG-DTA curve pertaining to the combustion reaction at a heating rate of  $10 \text{ K min}^{-1}$  in  $\text{O}_2$  (inset shows the differential weight with respect to temperature)

### 3.4.2 Analysis by using DSC

The sample gel contains considerable amounts of adsorbed moisture. In order to avoid the thermal artifact due to the evaporation of the adsorbed moisture and to determine the quantum of heat evolved during the course of the reaction, the specimen gels were preheated before carrying out the actual experiments at 373 K for 30 min in  $\text{O}_2$  atmosphere inside the DSC sample cell (Inset Fig. 3.4). The sample was cooled to room temperature and then again heated from 298 - 973 K.

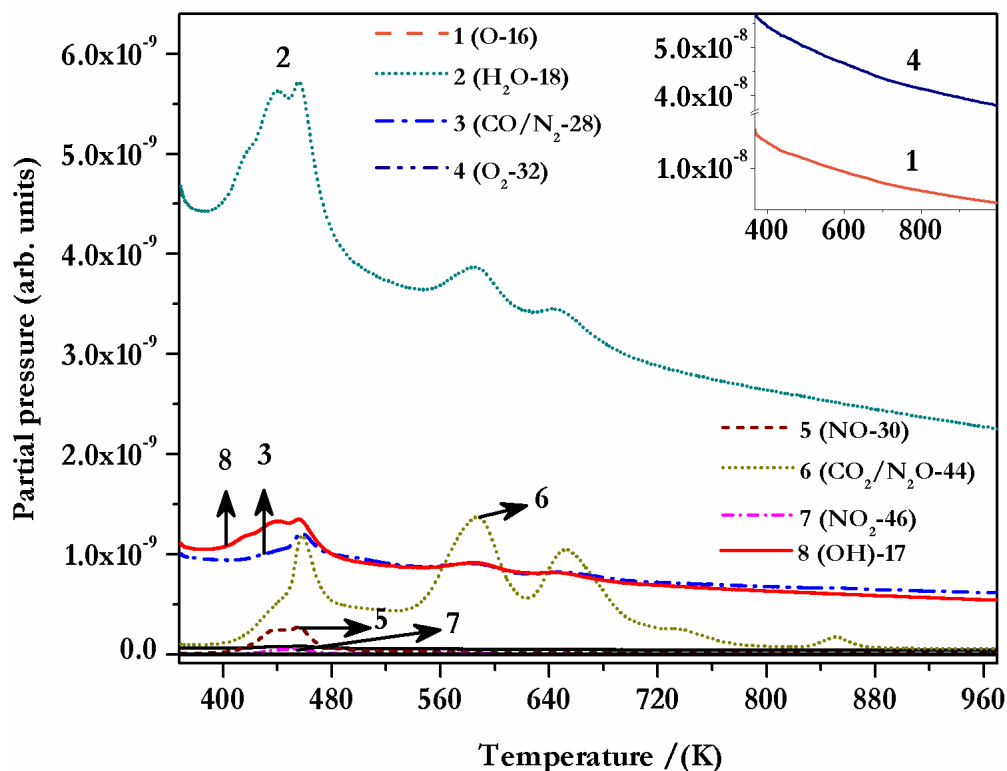


Figure 3.3 Mass spectrometric analysis of evolved gases during the citrate gel-combustion synthesis of nc- $U_3O_8$

The samples were subjected to different linear heating rates viz., 5, 10, 15 and 20 K min<sup>-1</sup>. A heat flow rate curve obtained as a function of temperature at different heating rates is shown in Fig. 3.4. Similar to the DTA analysis, three exothermic peaks were observed. The onset temperature of these peaks is in good agreement with that obtained by using DTA. DSC curves also revealed that the peaks shift with the heating rate while the area under the curve differs significantly with the heating rate.

The optimum calcination temperature was chosen with the help of the results obtained in the thermogravimetric analysis of the  $U_{C100A}$  powders. The thermal analysis revealed that the weight of this sample remained nearly constant at temperatures beyond 1050 K. Hence the calcination was carried out at 1073 K in order to remove the carbon residue present in the “as prepared” powders.

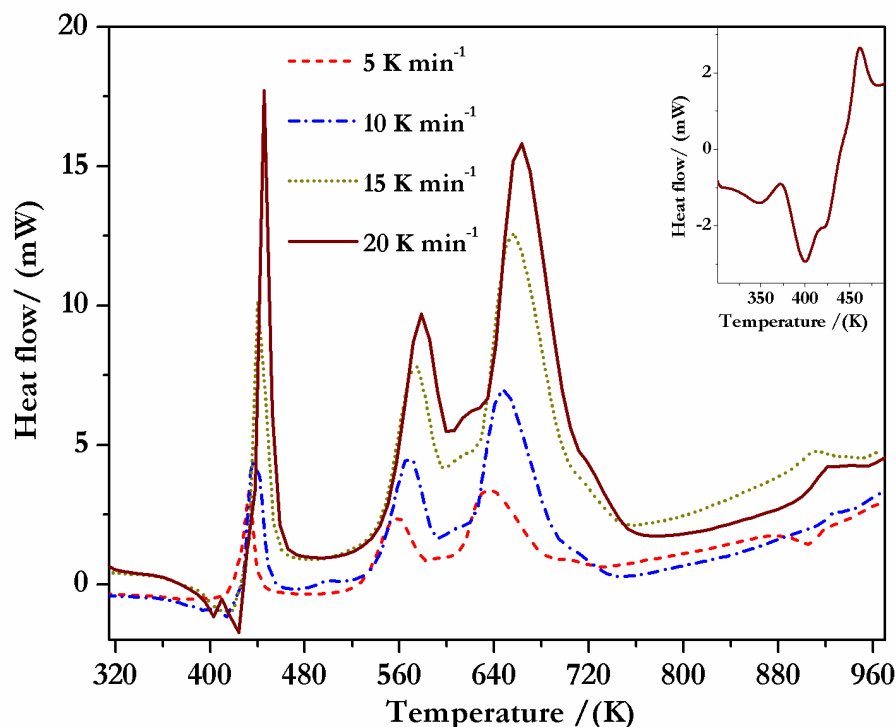


Figure 3.4 DSC curves pertaining to the combustion reaction at various heating rates in  $O_2$  atmosphere (Inset: DSC curve pertaining to dehydration)

### 3.5 Characterization of the powders

#### 3.5.1 Particle size distribution (PSD) and Bulk density ( $\rho_B$ )

The packing density of a powder depends on the size distribution of its constituent particles, mode of their packing, their flowability and shape. All these factors are directly linked to the powder preparation method [14, 15]. The same is true for the powders derived through combustion synthesis. Earlier, Anthonysamy et al. [16] showed that the mode of heating (microwave and hot plate) affected the PSD for urania-thoria solid solution prepared by using the citrate gel-combustion method and they have also reported that the difference in size distribution affected the sinterability of the final product. The properties of the powders prepared through citrate gel-combustion would depend strongly on the fuel to nitrate ratio [17]. These include their  $\rho_B$ , SSA,  $P_{O_2}$ SD and sinterability. The PSD in the “A”, “C” and “H” powders are presented in

Table 3.5 and in Fig. 3.5. In this Fig. 3.5 the thick solid line represents the experimentally observed size distribution of particles whereas the thin solid lines depict the deconvoluted size distribution derived from the former. The integral areas in percentage are given in the legend. The distribution of sizes among these particles was found to be in the range of 0.5 - 1000  $\mu\text{m}$ . The size distribution histograms were deconvoluted in order to delineate the contribution pertaining to different size fractions. The “A” and “C” powders exhibited mono and poly modal size distributions while the hydrogen reduced powders revealed only poly modal size distribution. The product  $\text{U}_{\text{C}}25\text{A}$  possessed a unimodal distribution.  $\text{U}_{\text{C}}25\text{C}$  and  $\text{U}_{\text{C}}25\text{H}$  comprised a bimodal distribution of particles.

The bulk densities as well as the PSD in these powders (A, C and H) exhibited a systematic dependence on the value of R (Fig. 3.6a). In all these powders the number of different size fractions had a bearing on their  $\rho_{\text{B}}$  and the following trend was discernible  $\rho_{\text{B (tetra)}} > \rho_{\text{B (tri)}} > \rho_{\text{B (bi)}} > \rho_{\text{B (uni)}}$ . The variation in the  $\rho_{\text{B}}$  of the “A” powders exhibited the following trend:

$$\rho_{\text{B (tetra/tri)}}^{\text{U00A}} > \rho_{\text{B (tri)}}^{\text{U}_{\text{C}}50\text{A}} > \rho_{\text{B (tri/bi)}}^{\text{U}_{\text{C}}75\text{A}} \approx \rho_{\text{B (tri/bi)}}^{\text{U}_{\text{C}}100\text{A}} > \rho_{\text{B (tri)}}^{\text{U}_{\text{C}}90\text{A}} > \rho_{\text{B (tri/bi)}}^{\text{U}_{\text{C}}5.5\text{A}} > \rho_{\text{B (bi)}}^{\text{U}_{\text{C}}10\text{A}} > \rho_{\text{B (uni)}}^{\text{U}_{\text{C}}25\text{A}}$$

In the above expression the type of distribution is indicated within the parenthesis. Powders with polymodal distribution of particulates exhibited higher bulk densities. More the number of size fractions higher was the value of the  $\rho_{\text{B}}$ . Among the powders,  $\text{U}_{\text{C}}25\text{A}$  was found to have the minimum bulk density, while U00A exhibited the highest  $\rho_{\text{B}}$ . This is evidently due to the better packing arising from appropriate distribution of size fractions i.e., when all the three size fractions are significantly populated, the  $\rho_{\text{B}}$  tends to be high. However in those powders that had a relatively less populated third size fraction the  $\rho_{\text{B}}$  was low. In powders with a bimodal distribution of particles the  $\rho_{\text{B}}$  was positively correlated with the quantities of the coarser

fraction, indicating that in these powders the relative population of the heavier particles determined the former. U<sub>C</sub>25A exhibited only a flat uni-modal distribution which spanned over a wide range of sizes and was found to possess the lowest  $\rho_B$ . The  $\rho_B$  and PSD in “calcined” urania powders followed the trend:

$$\rho_{B(\text{tri})}^{U00C} > \rho_{B(\text{tri})}^{U_{C50}C} > \rho_{B(\text{tri})}^{U_{C75}C} > \rho_{B(\text{tri/bi})}^{U_{C100}C} > \rho_{B(\text{bi})}^{U_{C90}C} > \rho_{B(\text{bi})}^{U_{C5.5}C} > \rho_{B(\text{bi})}^{U_{C10}C} > \rho_{B(\text{bi/uni})}^{U_{C25}C}$$

Calcined powders with tri, bi and uni modal distributions were found to possess the highest, intermediate and lowest  $\rho_B$  respectively. The  $\rho_B$  of the powders with a tri modal distribution, increased with the relative proportion of the fines. This could be ascribed to better packing of the particles facilitated by the percolation of fines into the interspaces of the larger particles. Thus the variation in  $\rho_B$  indicated in the above expression pertaining to the calcined powder and in Fig. (3.6a) could be substantiated.

“Calcined” powders with a bimodal distribution were found to possess a lower  $\rho_B$  than those with a tri modal distribution of particles. Unlike in the latter the bulk densities of the former bore an inverse correlation with the relative fraction of the fines. Possibly a higher fraction of the coarser agglomerates is necessary to compensate the relatively poorer packing in these powders as compared to their counterparts with three different size fractions. It is interesting to note that the pattern of PSD in a given calcined powder closely resembled that of its precursor. This suggests that these powders did not undergo significant self attrition during calcination and subsequent handling.

The  $\rho_B$  of “hydrogen reduced” UO<sub>2</sub> powders followed the trend:

$$\rho_{B(\text{tetra})}^{U_{C50}H} > \rho_{B(\text{tetra/tri})}^{U00H} \approx \rho_{B(\text{tri/bi})}^{U_{C75}H} > \rho_{B(\text{tri})}^{U_{C90}H} > \rho_{B(\text{tri})}^{U_{C100}H} > \rho_{B(\text{tri/bi})}^{U_{C25}H} > \rho_{B(\text{tri/bi})}^{U_{C5.5}H} > \rho_{B(\text{bi})}^{U_{C10}H}$$

From Fig. 3.5 it is evident that none of these powders exhibited uni modal distribution of sizes. This is due to the formation of multiple size fractions during the conversion of  $U_3O_8$  to  $UO_2$ .  $U_C50H$  was found to exhibit a tetra modal distribution and the highest  $\rho_B$ .  $U_C10H$  comprised a larger coarser fraction and the least  $\rho_B$ .  $U00H$  was found to have the largest fraction of particles with an average size of 100  $\mu m$  and much smaller fractions of the terminal sizes. Among the powders which exhibited a tri or tetra modal distribution of sizes those with the higher fraction of fines exhibited a higher value of  $\rho_B$ .

The bulk densities of hydrogen reduced powders were highest while that of the “as prepared” precursors were the least and that of the calcined powders were intermediate. Powders obtained from the mixture with an R value of 0.25 possessed the lowest  $\rho_B$  among the “A” and “C” powders. It is appropriate to compare the bulk densities of the powders obtained in the present study with those of the powders prepared through well established conventional processes cited in the literature (Table 3.6).

It is evident that  $UO_2$  powders with the lowest  $\rho_B$  could be produced by employing citrate combustion mixtures with R values 0.10 and 0.25 (Table 3.2). These are the lowest  $\rho_B$  values reported so far, for  $UO_2$ . All the other powders synthesized in this study exhibited values of  $\rho_B$  that were comparable to those pertaining to the powders obtained by the ADU [18], AUC [18], dry ADU [19] and the atomization method [20]. Both, the exothermicity as well as the rate of the combustion depend upon the composition of the combustion mixture (R). The variation in the powder properties substantiates the fact that the combustion reaction is vigorous for mixtures with an R value of 0.25. Hence, these highly porous powders exhibit the lowest  $\rho_B$ .

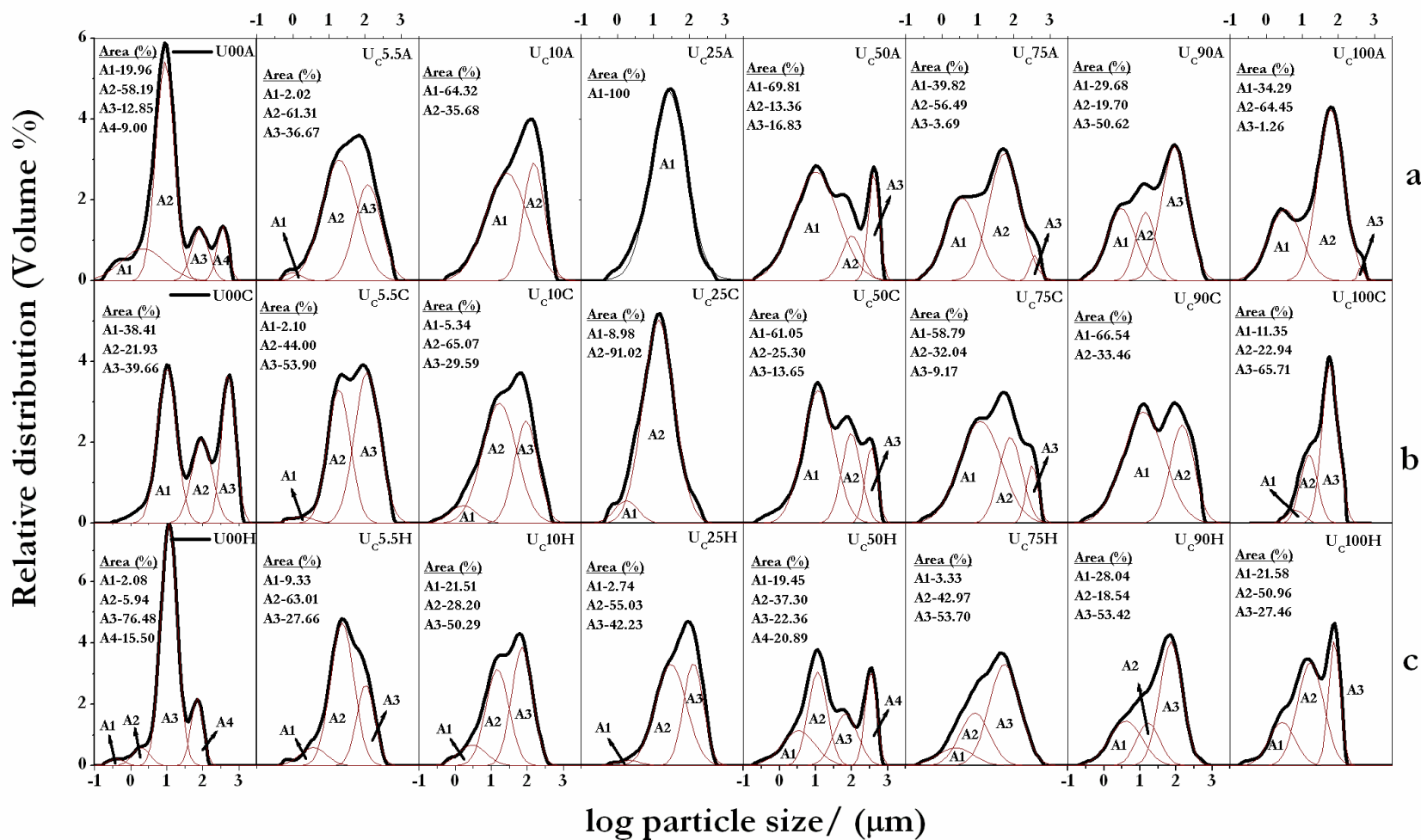


Figure 3.5 Distribution of sizes among particles in the “A”, “C” and “H” urania powders (Thick solid lines – experimental curve, thin solid line – deconvoluted curves)

### **3.5.2. Specific surface area (SSA)**

The dependence of SSA of the urania powders on the value of R is presented in Fig. 3.6b. From these data it is evident that the SSA of the “A” ( $SSA_A$ ), “calcined” ( $SSA_C$ ) and “H” ( $SSA_H$ ) powders follow the trend:  $SSA_A > SSA_H > SSA_C$ .

$U_{C25A}$  was found to have the highest SSA which decreased upon calcination, probably due to grain coarsening, as evidenced by a concomitant increase in the XCS. Hydrogen reduction of  $U_{C25C}$  yielded  $U_{C25H}$  with an enhanced SSA due to crumbling of the  $U_3O_8$  particles. The powder  $U_{C25A}$  was found to be extremely reactive and underwent oxidation under ambient conditions and developed yellow patches on its surface upon prolonged exposure to air. XRD analysis suggested that these were streaks of  $UO_3$ . The surface oxidation is possibly accentuated by the nano pores (Fig 3.15a). While  $U_{C25A}$  and  $U_{C25H}$  were found to have significantly higher values of SSA compared to the rest of the powders, the values of SSA of all the other powders were comparable.

From Table 3.2 and Table 3.6 it is evident that the SSA of urania powders derived through citrate gel combustion method was moderate and comparable with those pertaining to the powders derived through ADU [18], dry ADU [19] and AUC [18] processes. The final product (hydrogen reduced powders) had a SSA ranging from 4.98 - 9.68  $m^2 g^{-1}$ .

### **3.5.3. Residual carbon**

Table 3.2 depicts the variation in the quantity of carbon residue in the powders with the value of R. The data presented in Table 3.2 confirms that the quantity of carbon residue increases with R and decreases upon calcination and hydrogen reduction. The decrease in the quantity of carbon (residue) upon calcination is due to oxidation whereas during hydrogen reduction the



residual carbon gets converted into hydrocarbons. The quantity of carbon residue varies between 100 and 700 ppm and 90 and 300 ppm in the “C” and “H” powders respectively.

**Table 3.6 Comparison of  $\rho_B$ , SSA and XCS of urania powders reported values in the literature**

References	Method	$\rho_B$ (Mg m <sup>-3</sup> )	SSA (m <sup>2</sup> g <sup>-1</sup> )	XCS (nm)
[18]	AUC	2.08 - 2.24	4.29 – 6.66	-
	ADU	1.02	6.04	-
[19]	modified dry ADU	1.63 - 2.22	2.16 – 3.7	-
[20]	Atomization of uranyl nitrate	0.58 - 1.49	2.30 – 4.90	-
[21]	ADU	1.77 - 1.92	7.24 – 35.39	-
[22, 23]	AUC	-	0.50 – 5.96	-
[24]	AUC	-	4.70 – 14	10 – 100 (using SSA)
[25]	reoxidised U <sub>3</sub> O <sub>8</sub>	-	0.66 – 1.20	-
[26, 27]	ADU	-	1.1 – 6.2	15 – 32
[28]	Electrochemical method	-	10.3	4 – 6 (Sc)
[29]	Hydrothermal	-	28 (porous U <sub>3</sub> O <sub>8</sub> )	80 - 100
			10.0 (U <sub>3</sub> O <sub>8</sub> )	
[30]	ADU	1.5 – 1.8	5.82 – 10.4	-
[31]	Radiation chemical synthesis	-	60 – 70	22-35 (PCS) 9 (using SSA)
[32]	Hydrothermal (UO <sub>2</sub> )	-	-	30 – 250 (Sc)
	Hydrothermal (U <sub>3</sub> O <sub>8</sub> )	-	-	44.1 – 51.1 (Sc)
[33]	Electrochemically reduced	-	-	3 (Sc)
	673 K	-	-	-
[34]	873 K 1h	-	-	9 (Sc)
	873 K 2h	-	-	11 (Sc)
	973 K 1h	-	-	20 (Sc)
	1073 K 1h	-	-	52 (Sc)
	A	0.06 - 2.39	5-18	23-90 (HW)
This study	C	0.09 - 2.15	5-8	38-283 (HW)
	H	0.44 - 3.73	5-10	45-146 (HW)

AUC - Ammonium uranyl carbonate; ADU - Ammonium diuranate-; PCS – photon correlation spectroscopy; and Ox de – oxalate decomposition

Y.W. Lee and M.S. Yang [18] produced urania powders by both ADU and AUC process with a residual carbon content of 110 ppm and 160 ppm respectively. The quantity of carbon residue found in the powders obtained in this study is comparable to those reported in ref. [18]. The residual carbon could assist presintering of the agglomerates as well as could influence O/U in these powders.

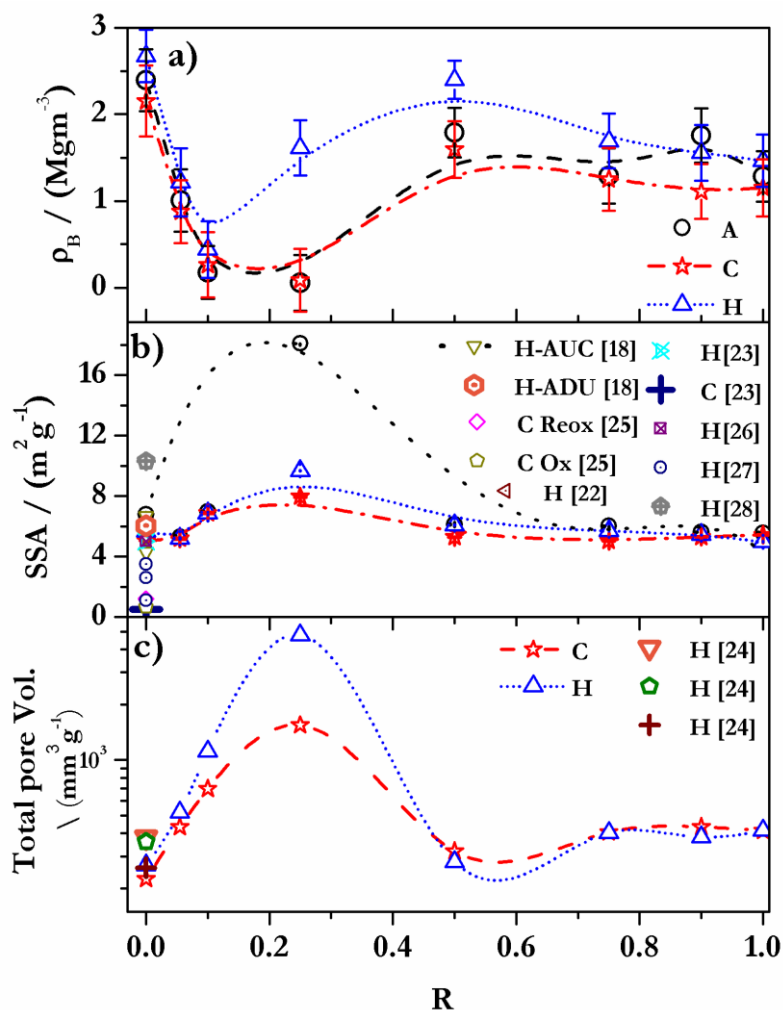


Figure 3.6 Dependence of (a)  $\rho_B$  of the powders; (b) SSA of the powders and (c) total pore volume on the value of  $R$  in, “C”  $U_3O_8$  and “H”  $UO_2$  powders

### 3.5.4. Phase characterization and XCS

XRD analyses of the urania powders synthesized in this study revealed that the “A” and “C” powders comprised  $U_3O_8$  phase (JCPDS: 00-047-1493 & 00-031-1424) while the reduced

“H” powders consisted of the fluorite phase (JCPDS: 00-041-1422) (Fig. 3.7). These results are summarized in Table 3.4. The urania powders obtained through denitration without the addition of citric acid (U00A) were amorphous (Fig. 3.7). This product upon calcination yielded a  $\text{U}_3\text{O}_8$  powder with a higher XCS. Subsequent reduction of this powder yielded  $\text{UO}_2$  with a lower crystallite size. Except U00A and  $\text{U}_{\text{C}5.5\text{A}}$ , all the other “as prepared” powders comprised essentially  $\text{U}_3\text{O}_8$  (Fig. 3.7). The constituent phases found in  $\text{U}_{\text{C}25\text{A}}$  were  $\text{UO}_2$ ,  $\text{UO}_3$  and  $\text{U}_3\text{O}_8$  (major quantity). This powder was derived through volume combustion.

A limited supply of oxygen during the combustion reaction could have resulted in the formation of  $\text{UO}_2$  along with  $\text{U}_3\text{O}_8$ . Later on these nc-phases would have got converted into  $\text{UO}_3$  through oxidation in air. Air calcination of these powders resulted in their complete transformation into orthorhombic  $\text{U}_3\text{O}_8$  phase as identified by the XRD pattern presented in Fig. 3.7. Subsequent hydrogen reduction of these powders yielded  $\text{UO}_2$ .

The estimates of XCS obtained by using the Sc formula were significantly different than those derived from the HW plots. All the “A” powders were found to be nc (XCS < 100 nm) and comprised smaller crystallites than the “C” powders. Both the XCS and the lattice strain of all the powders (A, C and H) exhibited a systematic dependence on the value of R (Fig. 3.8a and 3.8d). This variation is correlated with the rate of the combustion reaction. A faster rate led to a smaller XCS. Mixtures with R values between 0.25 and 0.75 yielded “A” powders with lower XCS than the rest of the mixtures. The powder  $\text{U}_{\text{C}25\text{A}}$  was distinctly different from the rest, in that it possessed the lowest XCS among all. “A” powders upon calcination and hydrogen reduction yielded “C” and “H” powders with enhanced XCS.

The combustion reaction is a self propagating and fast reaction (as evidenced by DSC) and does not allow enough time for the growth of the crystallites. This is the primary reason

because of which the combustion synthesis yields nc powders. The dispersion of the mixture by the gaseous products further accentuates the reduction in the size of these crystallites.

In order to understand the trends in the variation of XCS observed in the powders synthesized in the present study as well as to compare the present observations with those reported in the literature (for both microcrystalline and nanocrystalline), the results reported by other workers are cited here (Table 3.6). V. Tyrpekl [34] reported the presence of carbonate residue and complete removal of carbon necessitated calcination at 1073 K. All the above methods cited in refs [28, 31-33] have been employed for producing only a few mg of nc-UO<sub>2</sub>. Further, these processes as well as the citrate gel-combustion would require further optimization trials before they could be gainfully deployed for the production of nc-UO<sub>2</sub> in significant bulk quantities.

The results obtained in the present investigations show that the citrate gel-combustion is an easy method for the synthesis of nc-UO<sub>2</sub>. The XCS (HW) of the product was found to vary from 45 - 113 nm for UO<sub>2</sub> and 38 - 252 nm for U<sub>3</sub>O<sub>8</sub>. These values compare well with those obtained in recently reported advanced methods [28, 31-34].

Upon storage the dioxide powders picked up oxygen from the ambience and got converted in to an oxide that was hyperstoichiometric with respect to oxygen ( $O/U > 2.00$ ). There appeared to be a minor, yet noticeable variation in the oxygen stoichiometry of the freshly reduced powders (Fig. 3.9). In general the extent of hyperstoichiometry seems to depend on the relative fraction of fines in a given powder. However, this correlation defies a simple reasoning. The complex interplay of distribution of porosity and particle size as well as the specific surface area seem to determine the relative ease with which these powders would pick up oxygen when stored under identical conditions.

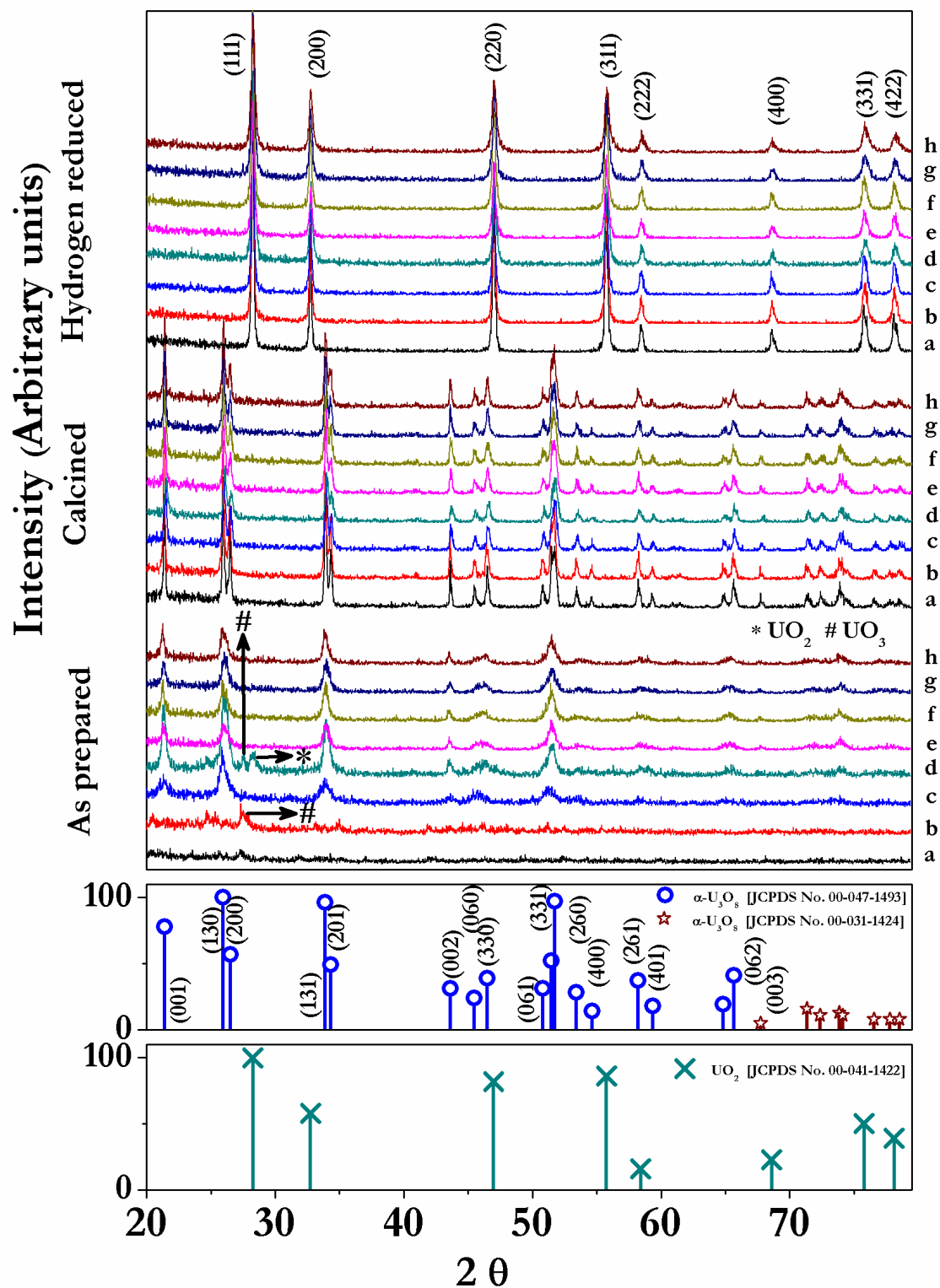


Figure 3.7 XRD of the “ $\text{U}_c\text{XXA}$ ”, “ $\text{U}_c\text{XXC}$ ”, “ $\text{U}_c\text{XXH}$ ” urania powders (Where  $XX = R$  value in %) 0, b) 5.5, c) 10, d) 25, e) 50, f) 75, g) 90 and h) 100

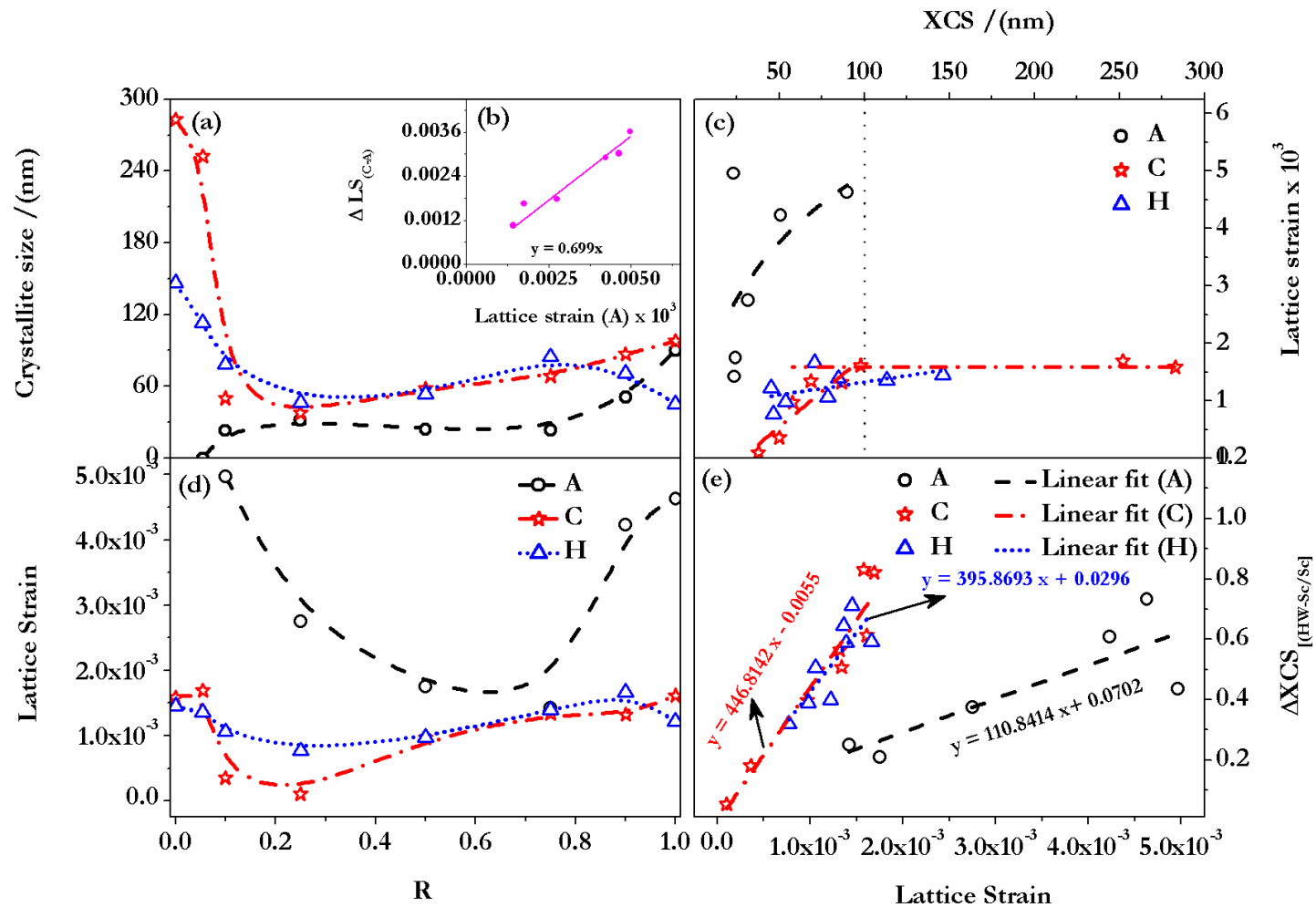


Figure 3.8 (a) Variation of sizes of crystallites in the powders on R ratio by HW's method; (b) Dependence of difference in lattice strain between "C" and "A" powders with the lattice strain of "A" powders; (c) Variation of lattice strain with XCS; (d) Variation of lattice strain in crystallites with ratio R and (e) Variation of relative difference in XCS with the lattice strain

In order to ascertain the variation in the lattice parameter with the oxygen to uranium ratio (O/U) in the hydrogen reduced  $\text{UO}_2$  powders, their O/U was measured by quantitatively estimating the concentrations of  $\text{U}^{4+}$  and  $\text{U}^{6+}$  in the oxide by using a spectroscopic technique [35]. The lattice parameter was computed from the X-ray diffractograms. From the data presented in Fig. 3.9. It is evident that the lattice parameter decreases with a rise in the value of oxygen to metal ratio (O/U) as expected, and has a linear dependence on the O/U ratio in  $\text{UO}_{2+x}$  [36].

Thus it is evident that the urania powders obtained through citrate gel-combustion (except  $\text{U}_{\text{C}25\text{H}}$  and  $\text{U}_{\text{C}10\text{H}}$ ) get stabilized after initial surface oxidation and that the hydrogen reduction yields a nearly stoichiometric product.

The dimensionless lattice strain obtained from the HW treatment [37] of the XRD data revealed many interesting aspects (Fig. 3.8b – 3.8e). The lattice strain in the “A” powders had a parabolic dependence on the value of R with a minimum at an R value of 0.50. Lattice strain in the “C” and “H” powders were much lower than that found in “A” and did not have a strong dependence on R. Insufficient time for the nucleation and growth during the combustion reaction and partial annealing during calcination substantiate these observations.

The lattice strain in all these powders was positively correlated with their XCS, indicating that the larger the crystallite more was the strain. Two regions viz., one below and the other above a critical value of 100 nm could be delineated in the plots depicting the variation in lattice strain with XCS (Fig. 3.8c). In the first region ( $\text{XCS} < 100 \text{ nm}$ ) a nearly linear correlation was observed while in the second ( $\text{XCS} > 100 \text{ nm}$ ) the lattice strain was more or less constant. Thus it is reasonable to conclude that when the powders coarsen and become microcrystalline ( $\text{XCS} > 100 \text{ nm}$ ) the strain approaches a constant value. Further, it was observed that the difference in the

lattice strain in the “A” powders and the “C” powders was correlated with the magnitude of the lattice strain in the “A” powders. This indicates that the lattice strain tends to annul itself upon calcination (annealing), and higher its initial value more would be the tendency for this reduction.

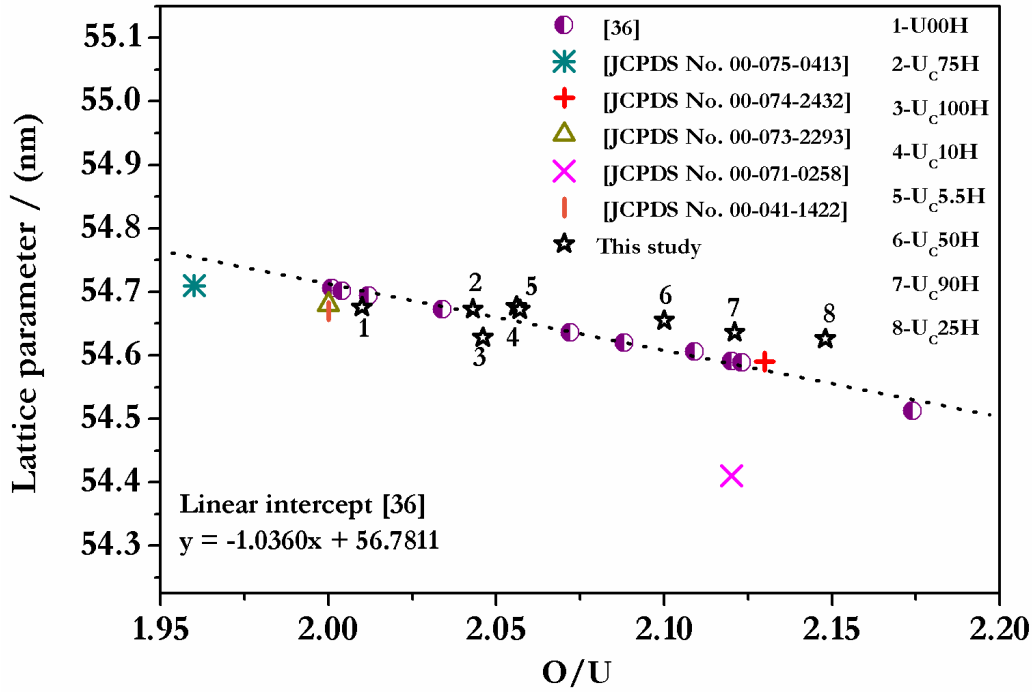


Figure 3.9 Dependence of the Lattice parameter of  $UO_{2+x}$  on oxygen non-stoichiometry ( $O/U$ )

In order to compare the two methods (HW and Sc) used in deriving the XCS, the dimensionless relative crystallite size parameter ( $\Delta XCS = (XCS_{HW} - XCS_{Sc}) / XCS_{HW}$ ) was considered. This parameter represents the error in the Sc estimate of the crystallite size and is caused by neglecting the contribution of lattice strain to the peak broadening. The variation in this parameter with the lattice strain given by eqn. 3.3 was found to be linear. The dependence of the error in the estimate on the lattice strain is given in Fig. 3.8e.

$$\Delta XCS = \frac{XCS_{HW} - XCS_{Sc}}{XCS_{HW}} = \frac{4 \epsilon \tan \theta}{\beta} \quad (3.3)$$



The slopes were found to be more or less identical for both the  $U_3O_8$  and  $UO_2$  powders, i.e. the “C” and “H” powders respectively. However, the error in the estimate caused by neglecting the strain component appears to be less for the “A” powders (higher value of slope) as compared to the “H” and “C” powders. Hence, care should be exercised in using the  $Sc$  estimates for arriving at the crystallite sizes for the gel-combustion derived products. Our results are in keeping with the observations made in ref [38]. Ideally, analysis of the lattice strain and the XCS in conjunction with the microstructure should be carried out, which is beyond the scope of this work.

### 3.5.5 Pore size distribution analysis

Cumulative pore size distribution (CPoSD) in the “C” and “H” powders estimated with the help of mercury porosimetry is presented in the Figs. 3.10 and 3.11 respectively. Fig. 3.6c depicts the total volume of the mercury intruded into the pores of “C” and “H” urania powders. From Fig. 3.10 it is clear that the volume (per unit mass of the powder) of mercury intruded into the pores of calcined urania powders increases with the value of  $R$  up to 0.25 ( $226 \text{ mm}^3\text{g}^{-1}$  to  $1549 \text{ mm}^3\text{g}^{-1}$ ).

The specific pore volume decreases with further increase in the value of  $R$  (0.50) to  $320 \text{ mm}^3\text{g}^{-1}$  and remains constant in the range  $320 - 500 \text{ mm}^3\text{g}^{-1}$  thereafter. The specific pore volume of calcined urania powders exhibits the following trend:

$$V_{U00C} < V_{UC50C} < V_{UC75C} < V_{UC100C} < V_{UC5.5C} \approx V_{UC90C} < V_{UC10C} < V_{UC25C}$$

The total pore volume ( $V_T$ ) of these powders was inversely correlated with their corresponding  $\rho_B$  (eqn. 3.4).

$$\rho_B(\text{Mgm}^{-3}) \propto \frac{1}{V_T(\text{mm}^3\text{g}^{-1})} \quad (3.4)$$

Similarly, the total pore volume of the “H” urania powders was found to increase with R when the latter was increased from 0 to 0.25. Further increase in the value of R led to a decrease in the total pore volume to  $281 \text{ mm}^3 \text{g}^{-1}$ . A comparison of the total volume of mercury intruded into the “C” and “H” urania powders (Fig. 3.6c) indicates that additional pores are generated during hydrogen reduction which leads to an increase in the total pore volume. During the conversion of the orthorhombic  $\text{U}_3\text{O}_8$  into the fluorite  $\text{UO}_2$  phase, new fine pores are generated [24]. This explains the increase in the total pore volume of “H” urania powders:

$$V_{\text{U00H}} < V_{\text{Uc50H}} < V_{\text{Uc90H}} < V_{\text{Uc75H}} < V_{\text{Uc100H}} < V_{\text{Uc5.5H}} < V_{\text{Uc10H}} < V_{\text{Uc25C}}$$

Systematic variation in the pore volume of the gel-combustion derived urania powders has not been investigated so far. However, limited data on the pore size distribution in urania powders prepared by the conventional AUC process has been cited by C. S. Choi et al. [24]. These authors have reported an average total pore volume of  $260 - 380 \text{ mm}^3 \text{g}^{-1}$  for urania powders derived through the AUC process. This value is close to the lowest values of the total pore volume of urania powders prepared in this study.

### **3.5.6 Microstructure and morphology**

The morphology of the powders  $\text{Uc25C}$ ,  $\text{Uc25H}$  and  $\text{Uc50H}$  have been investigated by using SEM. Images pertaining to both  $\text{Uc25C}$  and  $\text{Uc25H}$  (Fig. 3.12 and Fig. 3.13a) were found to have a “broccoli like” exfoliated morphology. It appears that the gel-combustion derived  $\text{UO}_2$  powders are pseudomorphic. High magnification image of the broccoli like pattern in Fig. 3.12 reveals embedded features with faceted cubic crystals and faceted cuboidal pores. The SEM images of  $\text{Uc50H}$  are presented in Fig. 3.13b. Hydrogen reduction leads to lattice restructuring of  $\alpha\text{-U}_3\text{O}_8$  to  $\text{UO}_2$ .

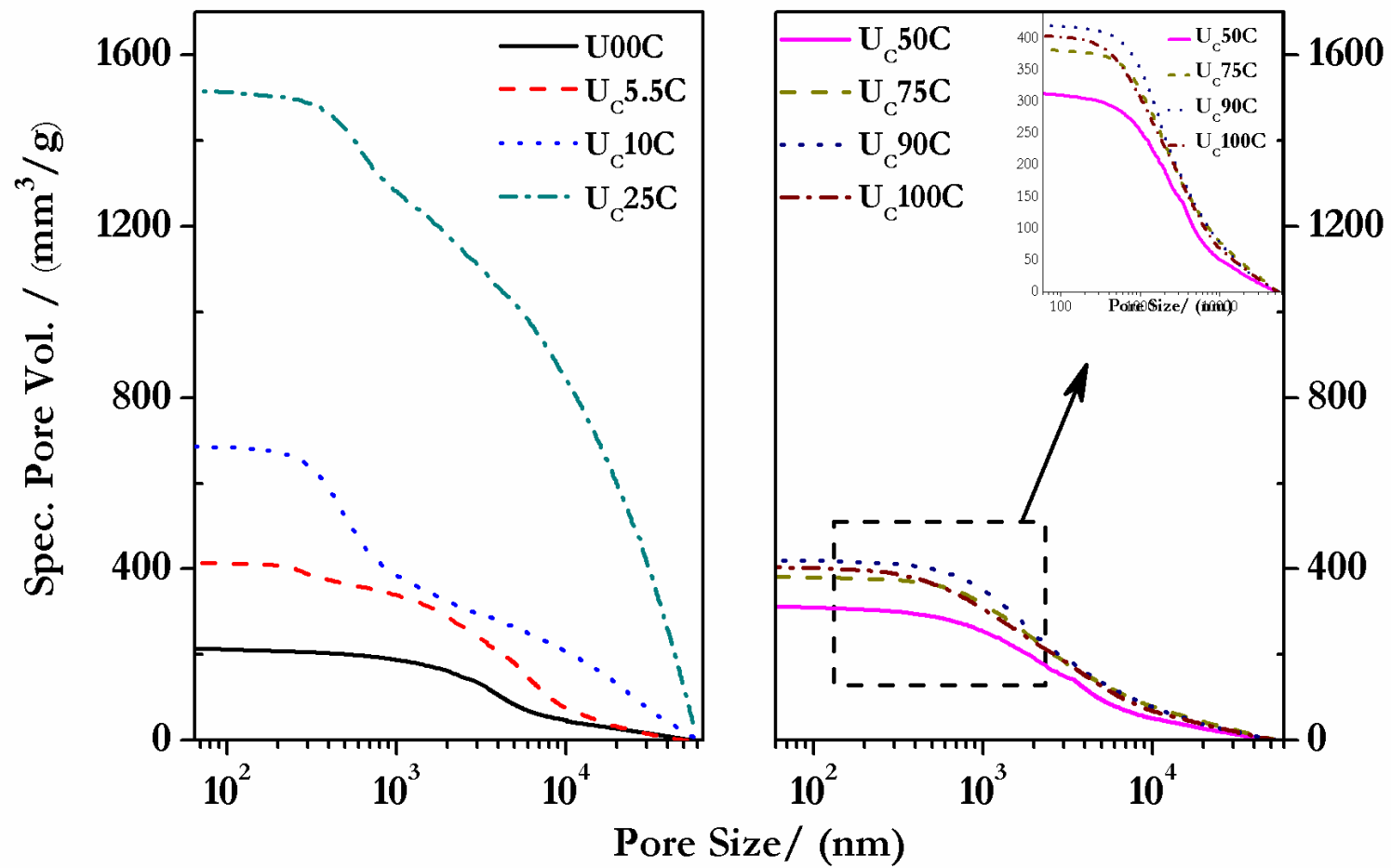


Figure 3.10 Cumulative size distribution of pores in "calcined" urania powders

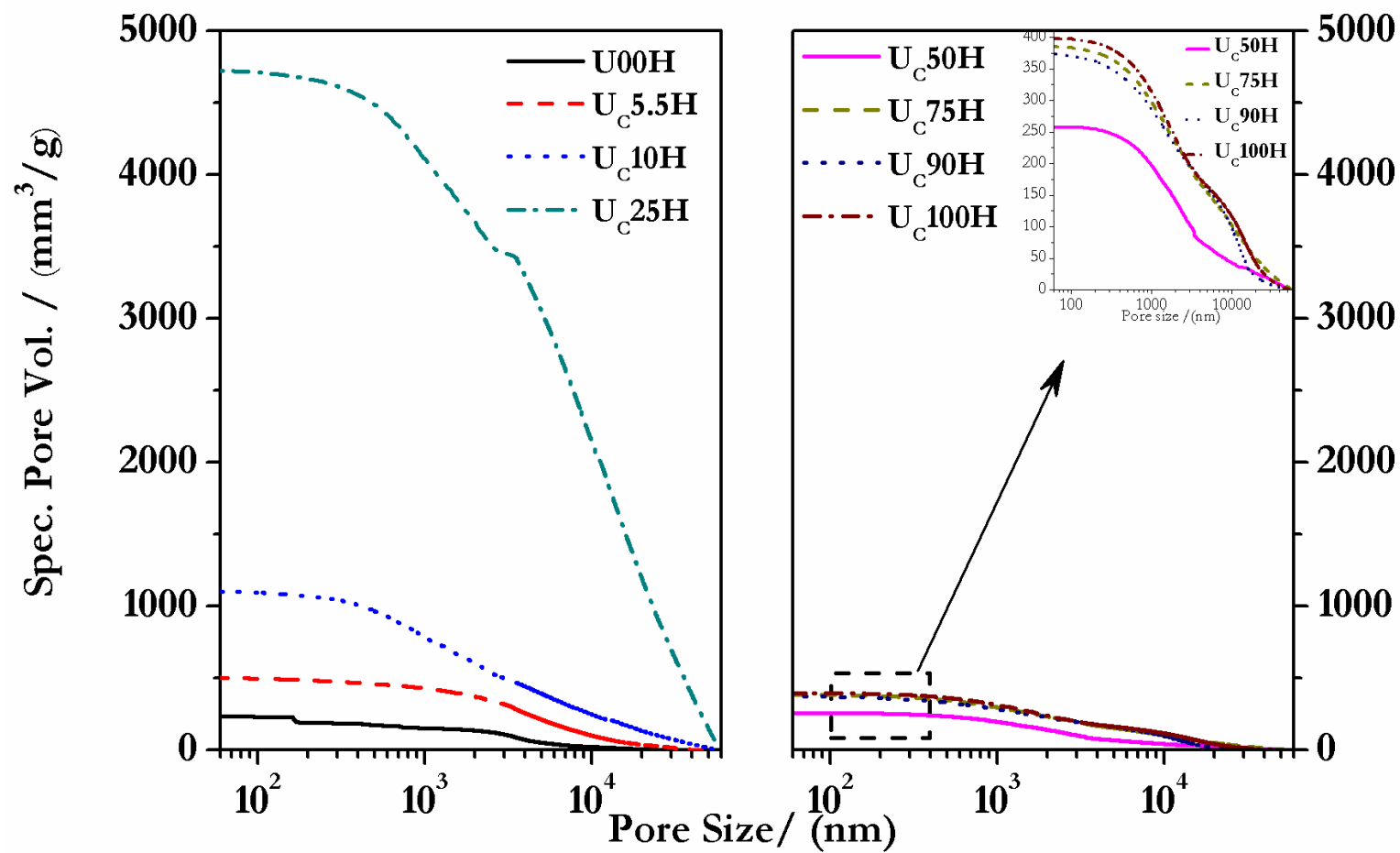


Figure 3.11 Cumulative size distribution of pores in "hydrogen reduced" urania powders

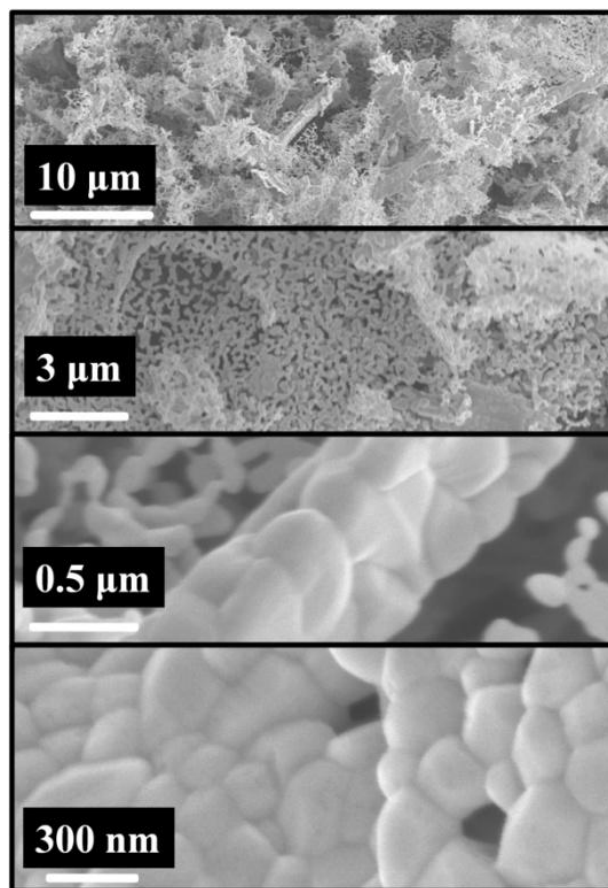


Figure 3.12 SEM images of “calcined” urania powers with an  $R$  value of 0.25

Microstructural analyses carried out by using TEM on the powders  $U_{C25C}$  and  $U_{C25H}$  are given in Figs. 3.14 – 3.16, which reveal the presence of macropores (20 nm). The selected area electron diffraction (SAED) pattern pertaining to these powders confirmed that the calcined and hydrogen reduced samples comprised orthorhombic  $\alpha$ - $U_3O_8$  and fluorite  $UO_2$  respectively. The d-spacings measured from the diffracted images were compared with those pertaining to the star JCPDS pattern. The inverse Fast Fourier Transform images (IFFT) were comparable with the IFFT image generated from CaRIne v3.1<sup>®</sup> software. By using these, the zone axes of the respective samples were also calculated. All the bright and dark field images testified the presence of nanoscopic grains. Macropores with interconnected porosity were also observed, a typical image of which is presented in Fig. 3.15a.

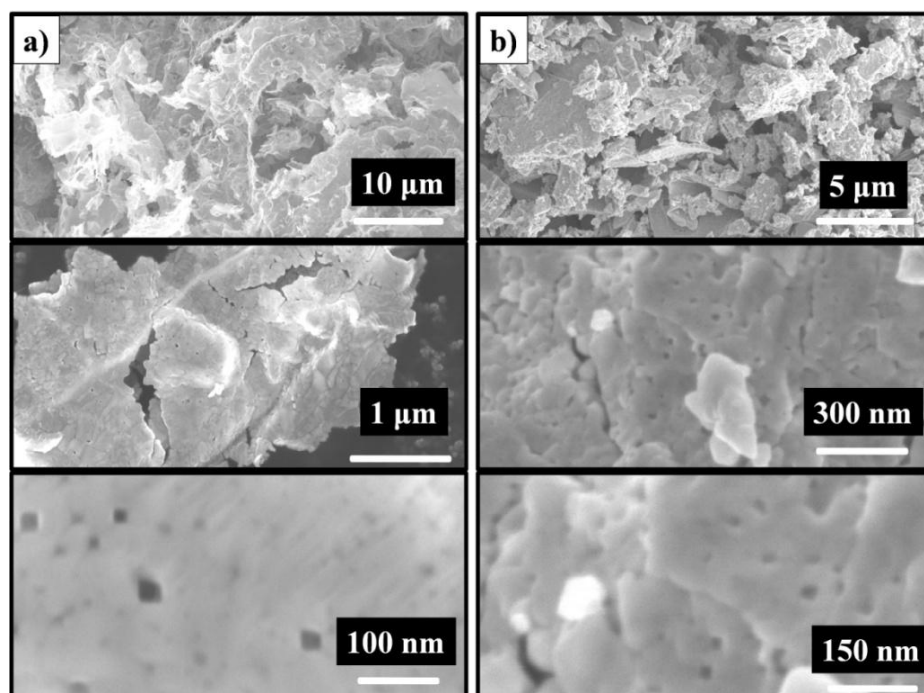


Figure 3.13 SEM images of “hydrogen reduced” urania powers with an  $R$  value of (a) 0.25 and (b) 0.50

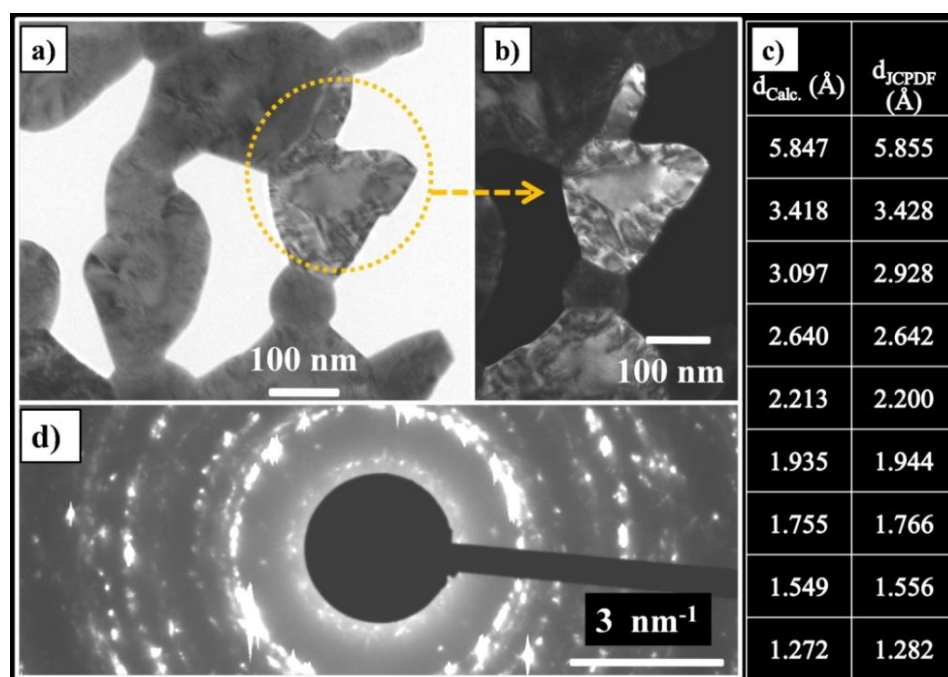


Figure 3.14 TEM images of  $U_{c25C}$  powders: (a) bright field image revealing nano grains; (b) dark field image revealing nano grains; (c) calculated and standard ‘ $d$ ’ spacing from SAED image and (d) SAED image

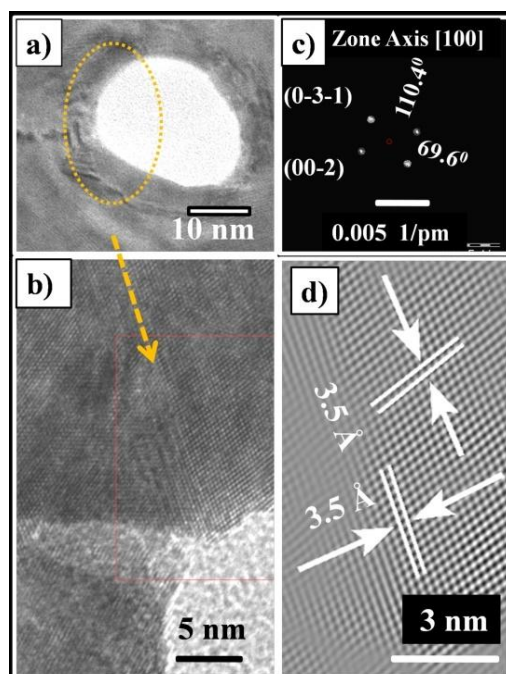


Figure 3.15 TEM images of  $U_{C25C}$  powders: (a) a typical nano pore; (b) HRTEM image with selected area; (c) FFT image revealing zone axis [100] and (d) IFFT image of zone axis [100]

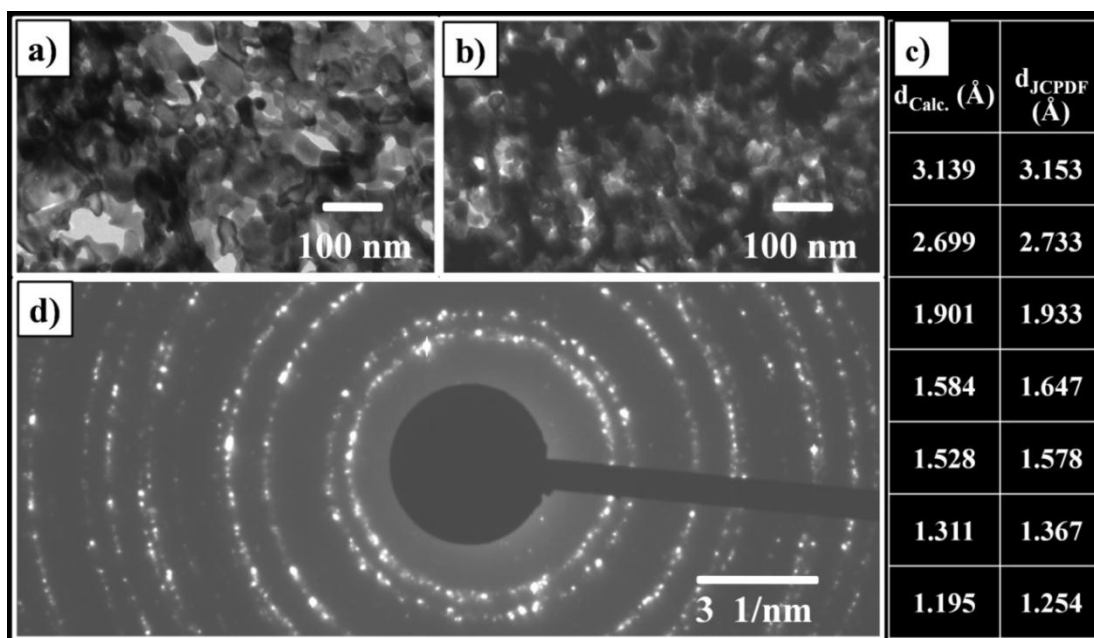


Figure 3.16 TEM images of  $U_{C25H}$  powders: (a) bright field image revealing faceted nano grains; (b) dark field image depicting nano grains; (c) calculated and standard 'd' spacing from SAED image and (d) SAED image

EELS [39-41] was used to ascertain the oxidation states as well as the nature of bonding in the specimen i.e., for  $\alpha$ - $\text{U}_3\text{O}_8$  and  $\text{UO}_2$ . The powders  $\text{U}_\text{C}25\text{C}$ ,  $\text{U}_\text{C}25\text{H}$ ,  $\text{U}_\text{C}50\text{C}$  and  $\text{U}_\text{C}50\text{H}$  were examined. The corresponding O-K edge and  $\text{N}_{4,5}$  ( $4\text{d} \rightarrow 5\text{f}$ ) edges [39] pertaining to these powders are depicted in Fig. 3.17. In order to use the spin-orbit sum rule [42, 43], background correction was carried out initially, following which the branching ratio  $[B = A_{5/2}/(A_{5/2} + A_{3/2})]$  was calculated, wherein  $A_{5/2}$  and  $A_{3/2}$  are the integrated intensities of  $\text{N}_5$  and  $\text{N}_4$  peaks respectively. These values of  $B$  were used for calculating the spin-orbit interaction per hole, using eqn. 3.5 [39, 40].

$$\frac{\langle w^{110} \rangle}{n_h} - \Delta = -\frac{5}{2} \left( B - \frac{3}{5} \right) \quad (3.5)$$

where,  $n_h$  is the number of the 5f holes,  $\Delta$  is the correction factor as given by Cowan's relativistic Hartree-Fock code [44] and  $\langle w^{110} \rangle$  is the expectation value for the angular part of the spin-orbit (5f) parameter. These results are tabulated in Table 3.7. The branching ratio for the powders  $\text{U}_\text{C}25\text{C}$  and  $\text{U}_\text{C}50\text{C}$  are 0.665 and 0.632 respectively. The values of  $B$  pertaining to the powders  $\text{U}_\text{C}25\text{H}$  and  $\text{U}_\text{C}50\text{H}$  are 0.713 and 0.693 respectively. The above results indicate that due to the increase in  $\text{N}_4$  peaks in  $\text{UO}_2$  the branching ratio was found to be high whereas for  $\text{U}_3\text{O}_8$  powders  $B$  value was minimum compared to  $\text{UO}_2$  due to the substantial increase in  $\text{N}_4$  integrated area. The results obtained with  $\text{UO}_2$  samples were comparable to the results indicated by Moore et al. [40] for  $\alpha$ -U metal and  $\text{UO}_2$  powders. These features are typical for urania and are in keeping with the fact that both  $\alpha$ - $\text{U}_3\text{O}_8$  and  $\text{UO}_2$  are predominantly covalent.



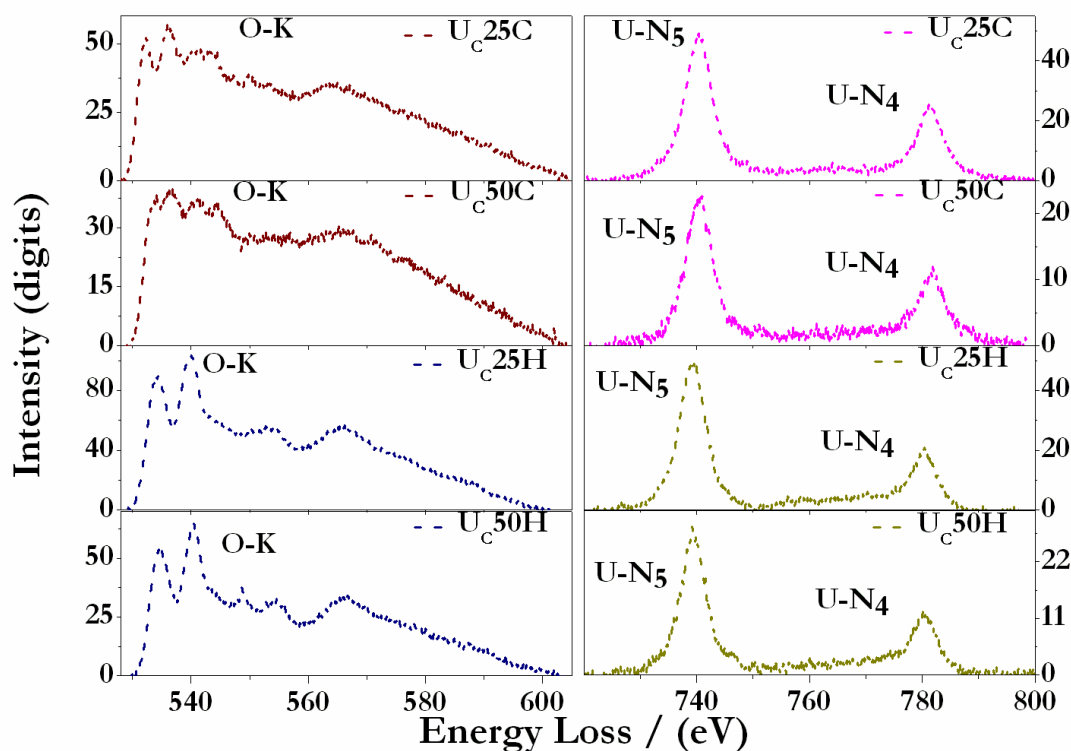


Figure 3.17 EELS of powders  $U_{C25C}$ ,  $U_{C25H}$ ,  $U_{C50C}$  and  $U_{C50H}$  depicting both O-K edge and  $N_{4,5}$  edges

Table 3.7 Parameters derived from the EELS spectra of  $\alpha$ - $U_3O_8$  and  $UO_2$

Sample	f	B	$\langle w^{110} \rangle / n_h - \Delta$	Phase
U <sub>C</sub> 25C		0.665	-0.163	$\alpha$ -U <sub>3</sub> O <sub>8</sub>
U <sub>C</sub> 50C	3	0.632	-0.080	$\alpha$ -U <sub>3</sub> O <sub>8</sub>
U <sub>C</sub> 25H		0.713	-0.283	UO <sub>2</sub>
U <sub>C</sub> 50H		0.693	-0.233	UO <sub>2</sub>

( $\Delta = -0.010$  for  $n = 3$ )

### **3.6 Conclusions drawn from citrate gel-combustion synthesis of nc-urania**

Nc-urania powders were synthesized by using citrate gel-combustion in bulk quantities for the first time. The systematic dependence of the reaction as well as the properties of these nanocrystalline powders on the composition of the combustion mixture (R) was investigated. The course of the combustion reaction in these mixtures was measured with the help of DSC for the first time. These results showed that the rate of this reaction is strongly influenced by the composition of the combustion mixture (R). Mixtures with an R value of 0.25 showed a markedly different behavior compared to the rest and underwent “volume combustion”.

Upon storage the oxygen stoichiometry of the  $\text{UO}_2$  powders was found to change with time, plausibly due to the facile oxidation of these nc powders. All the powders possessed a flaky morphology and comprised agglomerates of nanocrystallites of  $\alpha\text{-U}_3\text{O}_8$  or  $\text{UO}_2$ . The morphology and microstructure of the powders derived from the mixture with the R value of 0.25 were very different from the rest. HRTEM investigations reaffirmed the nanocrystallinity and revealed the presence of faceted nano crystallites and nano pores. The EELS study confirmed the covalency as expected.

It was observed that the  $\rho_B$ , XCS, size distribution of pores and particles, morphology of the powders and their microstructure showed a strong dependence on the value of R. The variation in the bulk density with R and its correlation with the size distribution of particles were investigated. For the first time an attempt was made to de-convolute the particle size distribution data. The contributions from the different size fractions were found to correlate well with the  $\rho_B$ .

The variation in lattice strain in nc- $\text{UO}_2$  derived through citrate gel-combustion and its dependence on size is being reported for the first time. Two distinct regimes viz., nc regime and the microcrystalline regime could be delineated by analyzing the variation in the lattice strain

with the XCS. Further analytical models are required, in order to understand the relation between the lattice strain and the distribution of sizes. It appears that the combustion mixtures with R values ranging from 0.25 to 0.50 would yield powders that are most suitable further processing.

### 3.7 Reaction mechanism and kinetic analysis of citrate gel-combustion synthesis of nc-urania

The kinetics of the gel-combustion reaction in the mixture with R = 0.25 was investigated by using DSC and TG-DTA-MS. The results of thermal analysis (DSC and TG-DTA-MS) are explained in detail in section 3.4.

The general expression for Arrhenius type temperature dependence of rate constant in heterogeneous kinetics under isothermal condition [45] (eqn. 3.6) could be expressed as,

$$\frac{\partial \alpha}{\partial t} = A e^{-\left(\frac{E_a}{RT}\right)} f(\alpha) \quad (3.6)$$

Where  $\alpha$  is degree of conversion (fraction reacted), T is temperature in Kelvin; R is the gas constant;  $E_a$  is activation energy of the reaction; t is time;  $f(\alpha)$  is the conversion function which is dependent on the reaction mechanism and A is the pre-exponential factor. The expression for heterogeneous reaction under non-isothermal condition with constant heating rate [45] ( $\beta$ ) is represented as,

$$\frac{\partial \alpha}{\partial T} = \frac{A}{\beta} e^{-\left(\frac{E_a}{RT}\right)} f(\alpha) \quad (3.7)$$

where  $\beta = \frac{\partial T}{\partial t}$ ; the integral form of eqn. 3.7 could be represented by eqn. (3.8) and this could be solved using numerical integration [46].

$$g(\alpha) \equiv \int_0^\alpha \frac{\partial \alpha}{\partial t} = \int_0^T \frac{A}{\beta} \exp\left(\frac{-E_a}{RT}\right) \partial T \quad (3.8)$$

Where  $g(\alpha)$  is the integral form of  $f(\alpha)$ . The  $E_a$  of the reaction could be obtained by using “model free classical kinetic methods” such as Kissinger method [47], Augis and Bennet method [48] and Mahadevan [49] method.

### 3.7.1 Kissinger method [47]

The activation energy ( $E_a$ ) of the reaction could be obtained by knowing the peak temperature of the thermal analysis curve as a function of heating rate. The Kissinger equation [47] (eqn. 3.9) that employs the peak temperature ( $T_p$ ) to evaluate  $E_a$  is given below.

$$\ln \frac{\beta}{T_p^2} = \text{constant} - \frac{E_a}{RT_p} \quad (3.9)$$

The plot of  $\ln \frac{\beta}{T_p^2}$  vs  $1/T_p$ , would be a straight line with a slope ( $-E_a/R$ ) from which activation energy could be derived.

### 3.7.2 Augis and Bennet method [48]

The expression used by Augis-Bennet [48] (eqn. 10), that employs a constant ( $k_0$ ) for the determination of  $E_a$  is given below.

$$\ln \frac{\beta}{T_p} = \ln k_0 - \frac{E_a}{RT_p} \quad (3.10)$$

The value of  $k_0$  and slope are derived from the graphical representation of the dependence of eqn. 3.10. The activation energy ( $E_a$ ) could then be obtained from the slope.

### 3.7.3 Mahadevan method [49]

Mahadevan [49] proposed eqn. 3.11 for the determination of activation energy ( $E_a$ ).

$$\ln \beta = \text{constant} - \frac{E_a}{RT_p} \quad (3.11)$$

The enumeration of the  $E_a$  in the Mahadevan method [49] is carried out by using the slope obtained from the plot of  $\ln \beta$  against  $1/T_p$ .

The classical methods (Kissinger [47], Augis and Bennet [48] and Mahadevan [49]) of kinetic analysis assume single activation energy for the entire reaction, which may not be correct for a heterogeneous reaction. These classical methods provide a rough estimate of  $E_a$ . Hence it is essential to evaluate  $E_a$  of the reaction as a function of fraction reacted ( $\alpha$ ). Thus, it is necessary to obtain the  $E_a$  by using the isoconversional method [50, 51].

### 3.7.4 Kissinger-Akahira-Sunose (KAS) isoconversional method [50, 51]

Though the overall estimate of  $E_a$  could be carried out with the model free classical methods, it is essential to understand the dependence of the  $E_a$  on the fractional progress of the reaction ( $\alpha$ ). Hence, the isoconversional KAS [50, 51] method was used to evaluate the dependence of  $E_a$  on  $\alpha$ .

The approximate solution was given by the KAS [50, 51] method (also known as the isoconversional method) employs the following eqn. 3.12 to evaluate the  $E_a$  as a function of  $\alpha$ .

$$\ln \frac{\beta}{T_{\alpha,i}^2} = \text{constant} - \frac{E_a}{RT_{\alpha,i}} \quad (3.12)$$

Where the subscript ‘i’ represents heating rates. The degree of conversion ( $\alpha$ ) was determined from the fractional area of the heat flow rate curve at different heating rates ( $\alpha = \frac{A_F}{A_T}$  where  $A_F$  and  $A_T$  are fractional area and total area respectively) [52]. Before evaluating  $\alpha$ , the baseline of the DSC curves were corrected by using blank run. This procedure was adopted for the curves obtained with different heating rates. From the temperature dependence of  $\alpha$  obtained at different heating rates the effective  $E_a$  was computed, by using eqn. 3.12 from a plot of  $\ln \frac{\beta}{T_{\alpha,i}^2}$

vs  $\frac{1}{T_{\alpha,i}}$ .

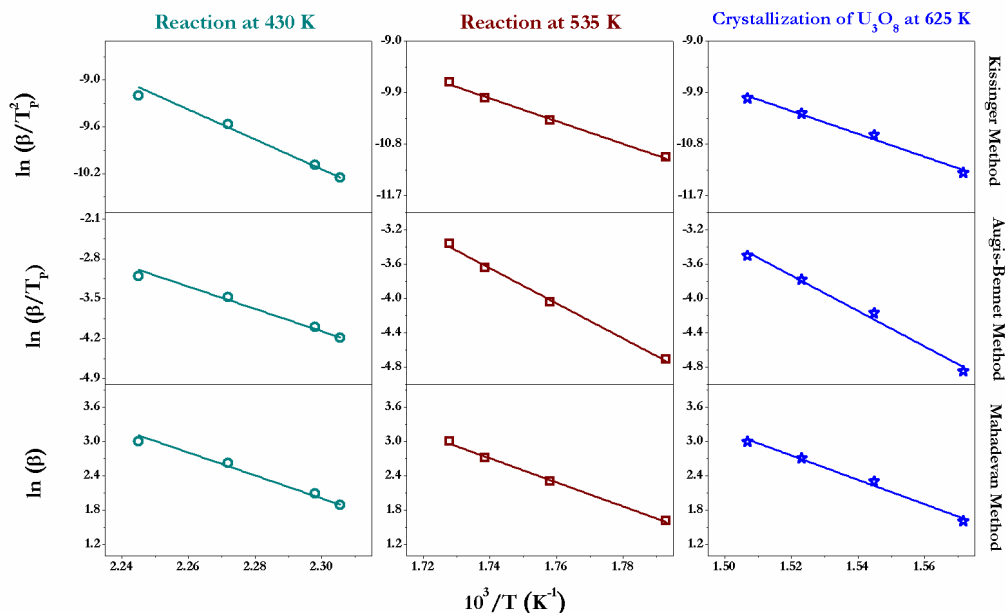


Figure 3.18 Temperature dependence of model variables pertaining to Kissinger [47], Augis and Bennet [48] and Mahadevan methods [49]

It should be mentioned here that the areas of the peaks pertaining to the thermal events varied with the rate of heating ( $\beta$ ). It is well established that the peak area obtained in a heat flux technique would be dependent on  $\beta$  even if the mass of the sample does not vary. This had been demonstrated even in the case of simple melting [45, 46]. Since the heat effects measured here were not calibrated or quantified with respect to the peak area at a given  $\beta$ . The relative area of the peaks corresponding to the different thermal events in an experiment was nearly the same irrespective of the  $\beta$ . Hence, in the relative analysis of the progress of the reaction the variation in the area of the peak with  $\beta$  this is an experimental artifact, may not introduce errors in the estimate of the kinetic parameters.

### 3.8 Determination of activation energy

#### 3.8.1 Classical models

The linear dependence of the model parameters on temperature pertaining to Kissinger [47], Augis - Bennet [48] and Mahadevan methods [49] corresponding to the first,

second and third exothermic peaks are shown in Fig. 3.18. The activation energies computed by using these methods pertaining to the first and second exothermic events as well as that to the crystallization of uranium oxide are listed in Table. 3.8. From these data (Table 3.8) it is evident that the values of  $E_a$  are mutually in agreement within 5 %.

### 3.8.2 Isoconversional method

The DSC curves pertaining to the three exothermic events at different heating rates are shown in Fig. 3.19.

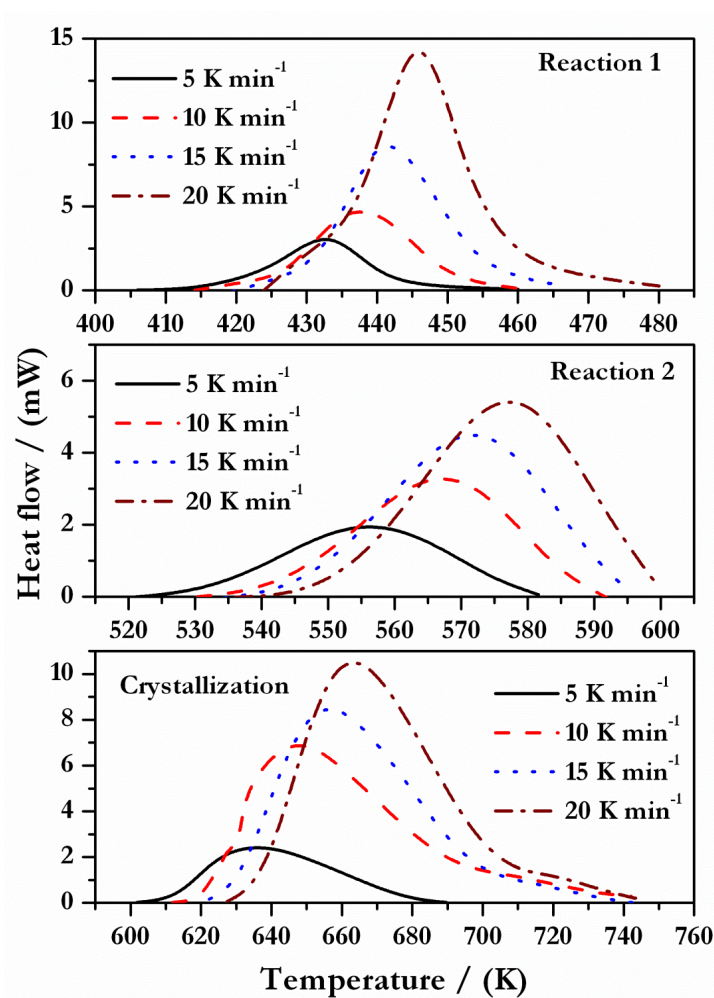


Figure 3.19 Exothermic peaks obtained in the DSC analysis at different steps of the combustion reaction

The variation in  $\alpha$  as a function of temperature pertaining to the three exothermic events on  $\alpha$  is shown in Fig. 3.20. The dependence of  $E_a$  on  $\alpha$  pertaining to the three exothermic events is shown in Fig. 3.21. From these data it is clear that the effective  $E_a$  remains nearly constant for “ $\alpha$ ” values from 0.2 to 0.8. The average value of the  $E_a$  in the  $\alpha$  range of 0.2 to 0.8 for the first, second and third thermal events were found to be  $152 \pm 6 \text{ kJ mol}^{-1}$ ,  $179 \pm 8 \text{ kJ mol}^{-1}$  and  $166 \pm 7 \text{ kJ mol}^{-1}$  respectively. Taylor et al. [53] had reported the  $E_a$  for the formation of  $\text{U}_3\text{O}_8$  in the unirradiated  $\text{UO}_2$  fuel is  $146 \pm 10 \text{ kJ mol}^{-1}$ . The  $E_a$  values obtained by this method are in agreement with those obtained by other classical methods within 5% (Table 3.8).

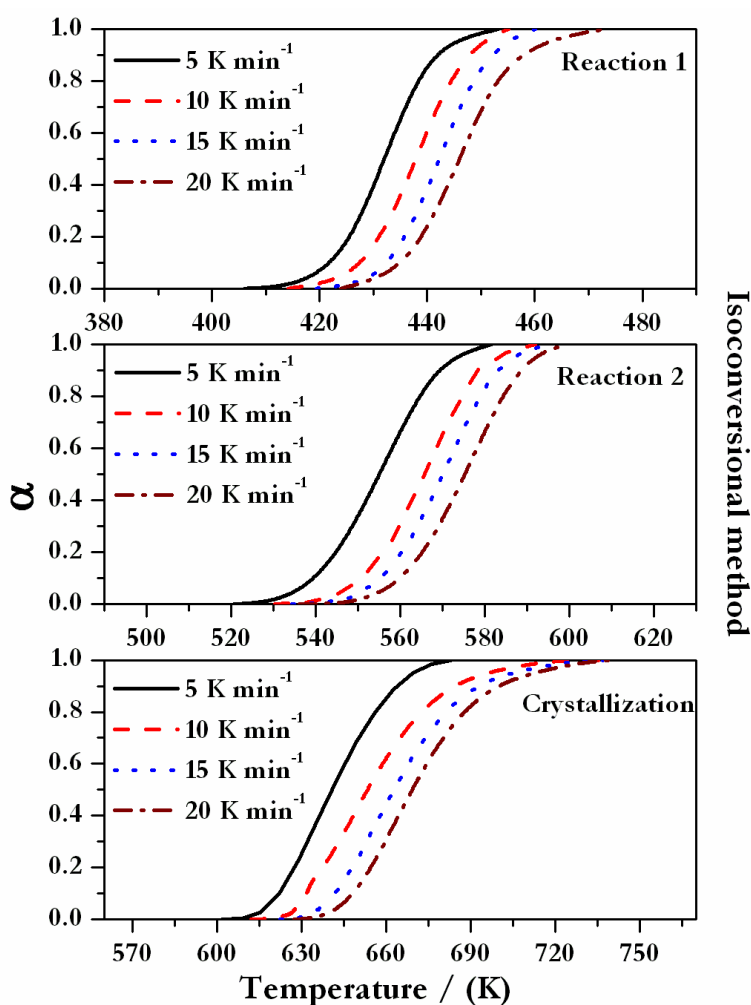


Figure 3.20 Degree of reaction ( $\alpha$ ) as a function of temperatures at different heating rates



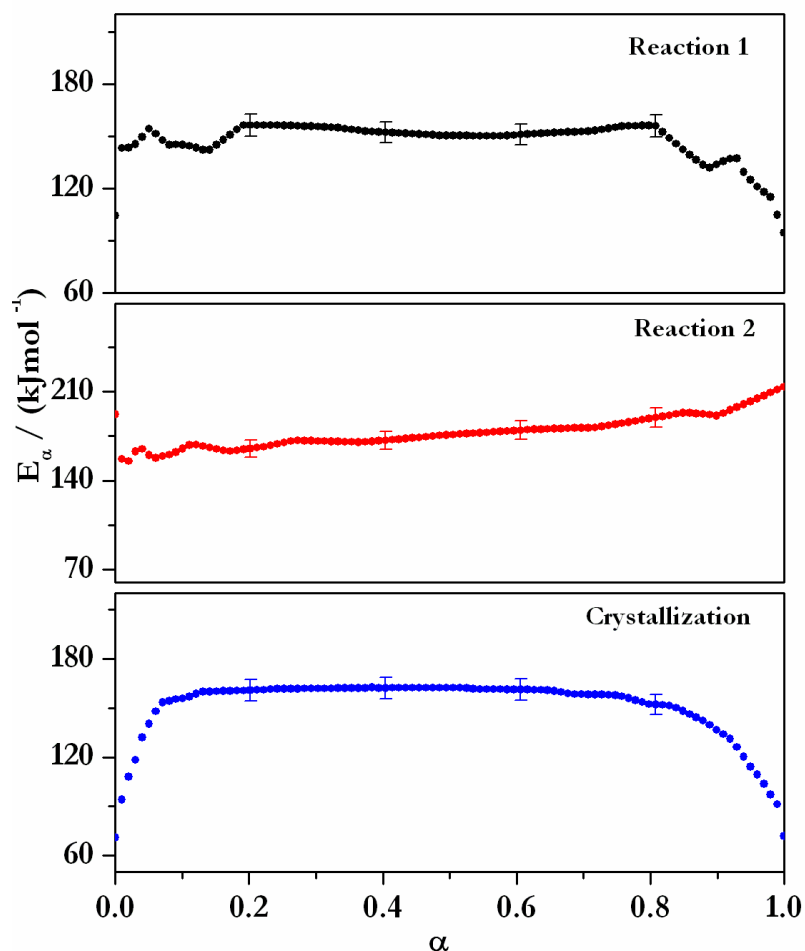


Figure 3.21 Dependence of the  $E_a$  pertaining to the thermal events (DSC)

The dependence of  $E_a$  on  $\alpha$  pertaining to all the three thermal events could be explained as follows. As observed in Fig. 3.21, the activation energies do not vary much during the progress of the reaction ( $\alpha = 0.2$  to  $0.8$ ). In view of the fact that the reaction under investigation is heterogeneous and that many processes are operating simultaneously, it is quite unlikely that the  $E_a$  would be independent of  $\alpha$ . However, the  $E_a$  pertaining to these different processes viz., nucleation, growth, diffusion, localized sintering is operating simultaneously, get internally compensated leading to the consistency of  $E_a$  with  $\alpha$ . In the first reaction, the activation energy appears to be nearly constant up to  $\alpha = 0.8$ , beyond which it decreases indicating that the

mechanism gets more complex with the formation of  $U_3O_8$  and the growth and diffusion of the constituent phases [54].

**Table 3.8 Computed activation energy by using various models**

Methods	$E_a$ (1 <sup>st</sup> reaction) $T_{onset}$ 430 K (kJ mol <sup>-1</sup> )	$E_a$ (2 <sup>nd</sup> reaction) $T_{onset}$ 535 K (kJ mol <sup>-1</sup> )	$E_a$ (Crystallization) $T_{onset}$ 625 K (kJ mol <sup>-1</sup> )
Kissinger	159 ± 2	166 ± 3	167 ± 1
Augis and Bennet	163 ± 1	170 ± 2	172 ± 1
Mahadevan	167 ± 4	175 ± 1	177 ± 2
Isoconversion ( $\alpha$ from 0.20 to 0.80)	152 ± 6	179 ± 8	166 ± 7

During the second stage, though the overall activation energy does not vary much with respect to  $\alpha$ , it shows an increasing trend with  $\alpha$ . This is probably due to a parallel reaction [55] involving the growth of  $U_3O_8$  nuclei and the combustion of citric acid. However, the effect due to the combustion dominates. In the third reaction involving no measurable weight change but only the crystallization of  $U_3O_8$ , the initial increase in the activation energy observed is probably due to the formation of a well-ordered crystalline  $U_3O_8$ . The activation energies pertaining to the formation of  $U_3O_8$  from microcrystalline  $UO_2$  reported by Taylor [53] are marginally lower than those estimated in this study. This is probably due to the additional energy barrier imposed by the nearly amorphous (nc)  $UO_2$  formed during the combustion reaction used in this study. In the stages of the reaction beyond  $\alpha = 0.8$ , along with crystallization, diffusion of oxygen also competes and thus a general trend in decrease in  $E_a$  was observed beyond alpha of 0.80 [54].

### 3.9 Conclusions drawn from the kinetic analysis of citrate gel-combustion

Elucidation of a reaction mechanism for the combustion synthesis of uranium oxide was carried out for the first time. The sample gels were analyzed by using TG-DTA-MS and DSC. Three exothermic peaks were observed in both the DTA and DSC analyses. The proposed

reaction mechanism was supported by the mass spectrometric analysis of the evolved gases. The  $E_a$  estimated for the first two thermal events were  $152 \pm 6$  and  $179 \pm 8$  kJ mol<sup>-1</sup> respectively. The  $E_a$  for the third thermal event (crystallization of U<sub>3</sub>O<sub>8</sub>) was found to be  $166 \pm 7$  kJ mol<sup>-1</sup>. In this study gels with a fuel to oxidant ratio of 0.25 were investigated. However, the reaction mechanisms and the activation energies will depend on the fuel (citric acid) to oxidant (nitrate) ratio of the gels. Further investigations are required to study the systematic variation of citrate gel-combustion of urania with different fuel to nitrate ratio (R).

### **3.10 Compaction and sintering of nc-UO<sub>2</sub>**

#### **3.10.1 Green density ( $\rho_G$ )**

The variation in the  $\rho_G$  with the compaction pressures pertaining to U<sub>C</sub>XXH powders is presented in Fig. 3.22 and Table 3.9. The  $\rho_G$  of these pellets was found to vary from 44.6 – 57.2 % T.D. The lowest  $\rho_G$  was observed for the sample U<sub>C</sub>90H (44.6 % T.D) when compacted at 60 MPa while the highest  $\rho_G$  (57.2 % T.D) was obtained for the U<sub>C</sub>25H powders at a CP of 353 MPa. All the powders except U<sub>C</sub>10H could be compacted to a  $\rho_G$  more than 50 % T. D. at a pressure above 180 MPa. To obtain a pellet with good handling strength (except U00H) a CP of about 60 MPa was found necessary. However to consolidate the powder U00H into a defect free pellet with good handling strength a minimum CP of 120 MPa was required. U<sub>C</sub>5.5H and U<sub>C</sub>25H exhibited nearly identical compaction behavior (Fig. 3.22). Their  $\rho_G$  are found to increase linearly with the CP up to 210 MPa. Probably at this pressure the harder agglomerates undergo fracture and rearrangement leading to a further increase in the  $\rho_G$  with pressure. The powder U00H and U<sub>C</sub>10H exhibit a multimodal size distribution of particles. Hence, it is reasonable to assume that these powders would undergo a better packing. From the results depicted in Fig. 3.22 it is evident that upon compaction, the powders U<sub>C</sub>10H and U00H yield a higher  $\rho_G$

than the powders  $U_{C5.5H}$  and  $U_{C25H}$ . It is also clear from Fig. 3.22 that the powders  $U_{C50H}$ ,  $U_{C75H}$ ,  $U_{C90H}$  and  $U_{C100H}$  exhibit similar variation in  $\rho_G$  with CP with a sharp discontinuity in the pressure dependence at 280 MPa.

$U_{00H}$  yielded pellets with a maximum  $\rho_G$  of 58.3 % T.D at 280 MPa. Further increase in the CP up to 353 MPa did not bring about any appreciable change in the  $\rho_G$ . It is reported in the literature [56] that it is difficult to compact nc powders to a higher  $\rho_G$  as compared to their microcrystalline counterparts. This behavior is ascribed to the following reasons; viz, i) presence of higher friction during compaction, ii) fracturing of finer particles requiring excessive stress and iii) presence of steeper pressure gradients within the compact. However, the powders used in this study behaved very much like microcrystalline powders. Even though they possessed a nano-substructure, the size of the particle aggregates was as big as 10-100  $\mu m$ . Thus the gel-combustion derived powders offer the dual advantage of possessing nano-crystallites and the microcrystalline particle aggregates.

In the literature [19, 22-27, 57-63], pressures in the range of 50-392 MPa has been reported (Table 3.12) for the consolidation of microcrystalline urania. The maximum  $\rho_G$  obtained is about 58 % T.D [19, 24]. While Sakamura [60], Ayaz [57], Furhrman [58], Harada [59], Ching-Tsven [19], Choi [24] and Yi-Ming [61] had used lubricants during compaction many others [22-27, 62, 63] have compacted without the aid of a lubricant. Most authors could obtain a  $\rho_G$  of about 50 % T.D. Murty et al. [64] reported that a CP of 250 - 275 MPa is best suited for the compaction of  $UO_2$  derived through the ADU route. The  $\rho_G$  obtained in this work (44.6 to 57.2 % T.D) is comparable with those reported in the literature [18, 19, 22-24, 26, 27, 57-63]. Our results revealed that all the gel-combustion derived powders are suitable for binderless consolidation due to their good flowability and favorable size distribution.

**Table 3.9 Green density ( $\rho_G$ ) of  $UO_2$  pellets derived through citrate gel-combustion method**

CP (MPa)	U00H	U <sub>C</sub> 5.5H	U <sub>C</sub> 10H	U <sub>C</sub> 25H	U <sub>C</sub> 50H	U <sub>C</sub> 75H	U <sub>C</sub> 90H	U <sub>C</sub> 100H
	% T.D <sup>x</sup>							
<b>60</b>	-	45.0 ± 0.2	48.1 ± 0.5	46.0 ± 0.6	45.7 ± 0.8	45.1 ± 0.4	44.6 ± 0.6	45.2 ± 0.3
<b>120</b>	49.6 ± 0.4	48.3 ± 0.6	50.9 ± 0.5	48.8 ± 0.5	48.8 ± 0.7	48.9 ± 0.2	48.1 ± 0.5	48.7 ± 0.1
<b>180</b>	54.2 ± 0.9	50.7 ± 0.2	53.4 ± 0.5	51.1 ± 0.5	52.0 ± 0.2	51.1 ± 0.5	51.4 ± 0.2	51.4 ± 0.2
<b>244</b>	57.7 ± 0.7	52.5 ± 0.4	55.3 ± 0.4	52.5 ± 0.6	53.8 ± 0.4	53.0 ± 0.4	52.8 ± 0.6	53.3 ± 0.3
<b>280</b>	58.3 ± 0.5	52.7 ± 0.4	55.7 ± 0.4	52.9 ± 0.5	54.8 ± 0.6	54.4 ± 0.4	54.1 ± 0.4	53.9 ± 0.1
<b>317</b>	58.3 ± 0.9	54.2 ± 0.5	56.4 ± 0.7	54.4 ± 0.6	55.8 ± 0.4	55.2 ± 0.5	54.2 ± 0.6	54.3 ± 0.3
<b>353</b>	57.6 ± 0.3	54.9 ± 0.6	57.2 ± 0.2	55.3 ± 0.9	55.7 ± 0.4	56.1 ± 0.5	55.2 ± 0.3	54.8 ± 0.6

<sup>x</sup> indicates the mean value of five independent measurements

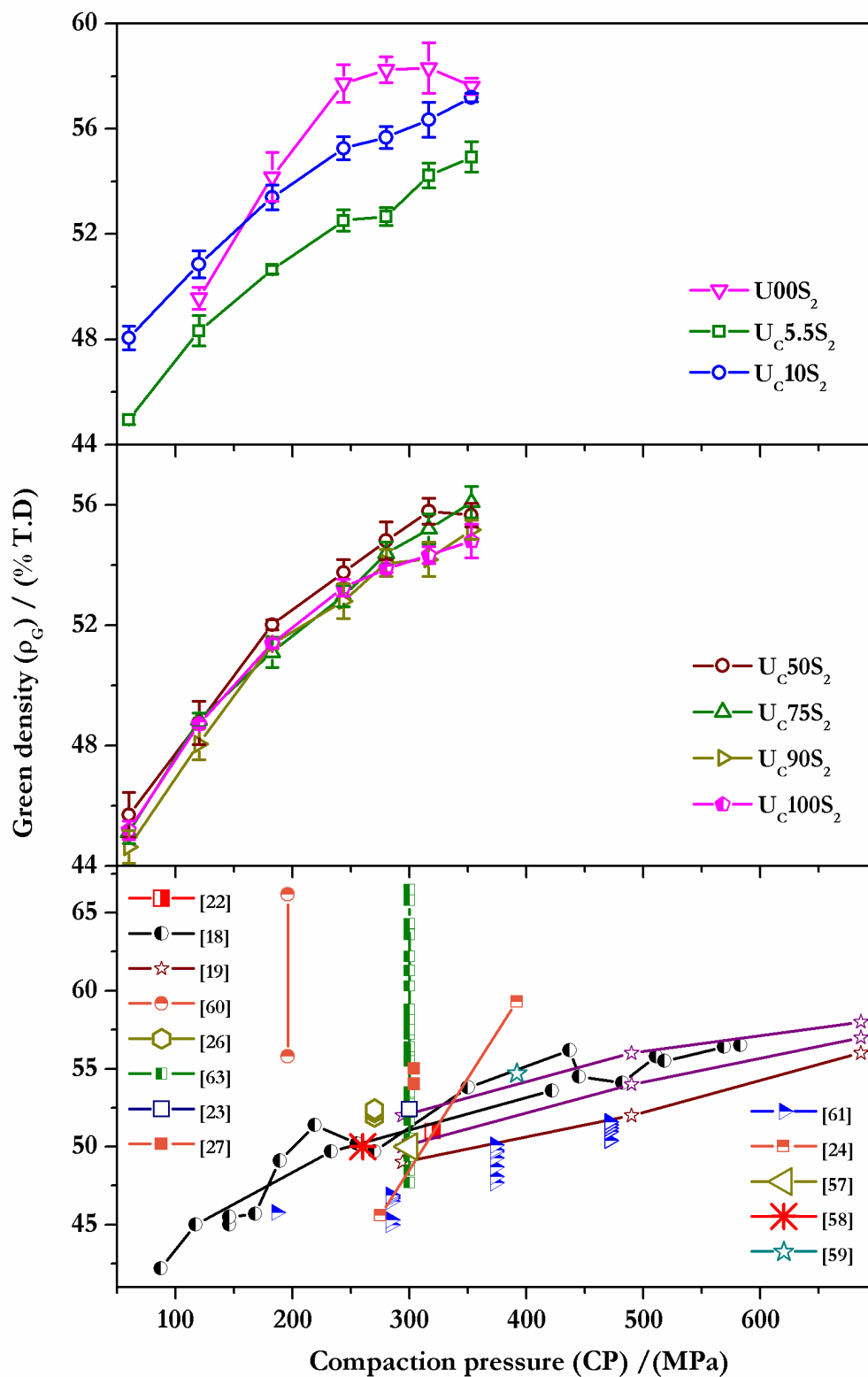


Figure 3.22 Variation in the  $\rho_G$  with CP [“hydrogen reduced”  $\text{UO}_2$  powders]

### 3.10.2 Sintering studies on U<sub>C</sub>25H

The densification of nc materials depends on many process variables viz., size distribution of particles, SSA of the powders, porosity,  $\rho_G$ , sintering temperature and sintering atmosphere [65]. The variables viz., stability of pores, the dihedral angle between the grains and the number of grains are indicative of the degree of densification. The densification could be enhanced by destabilizing the trapped pores which in turn depends mainly on the rate of sintering and final soaking temperature [65-67].

U<sub>C</sub>25H exhibited powder properties markedly different from the rest and comprised smallest crystallites. From the data cited in the literature [68-71] it is evident that powders with small crystallites exhibit “run-away” sintering leading to a reduction in the sintered density when sintered at higher temperatures. Often modification of the sintering routine helps alleviate this problem. To study the difference between the CS and TSS [72] in the case of nc-UO<sub>2</sub>, the powder U<sub>C</sub>25H was chosen as a “typical” sample. The dependence of the relative  $\rho_s$  on the CP of the pellets U<sub>C</sub>25S<sub>C</sub>, U<sub>C</sub>25S<sub>1</sub> and U<sub>C</sub>25S<sub>2</sub> are presented in Fig. 3.23 and Table 3.10. These data reveal that CS yielded  $\rho_s$  ranging from 81.1 %T.D (at 60 MPa) to 95.9 % T.D (at 244 MPa). The  $\rho_s$  of the specimens U<sub>C</sub>25C is found to be increase linearly with the CP in the range 60 to 150 MPa, beyond which it is found to be independent of the latter. It is found that when CS is employed, the pellets compacted at 150 MPa, yield a  $\rho_s$  of 94.5 % T.D.

Porosity values reveal that beyond 150 MPa, the open pore fraction decreases to 1 %, leaving behind a closed porosity of about 3.5 %. It is also observed that the open pore fraction is inversely correlated with the CP. The total porosity in the sintered pellet decreases drastically from 19 % to 6 % in sintered UO<sub>2</sub> pellets when the CP is increased from 60 MPa to 150 MPa.

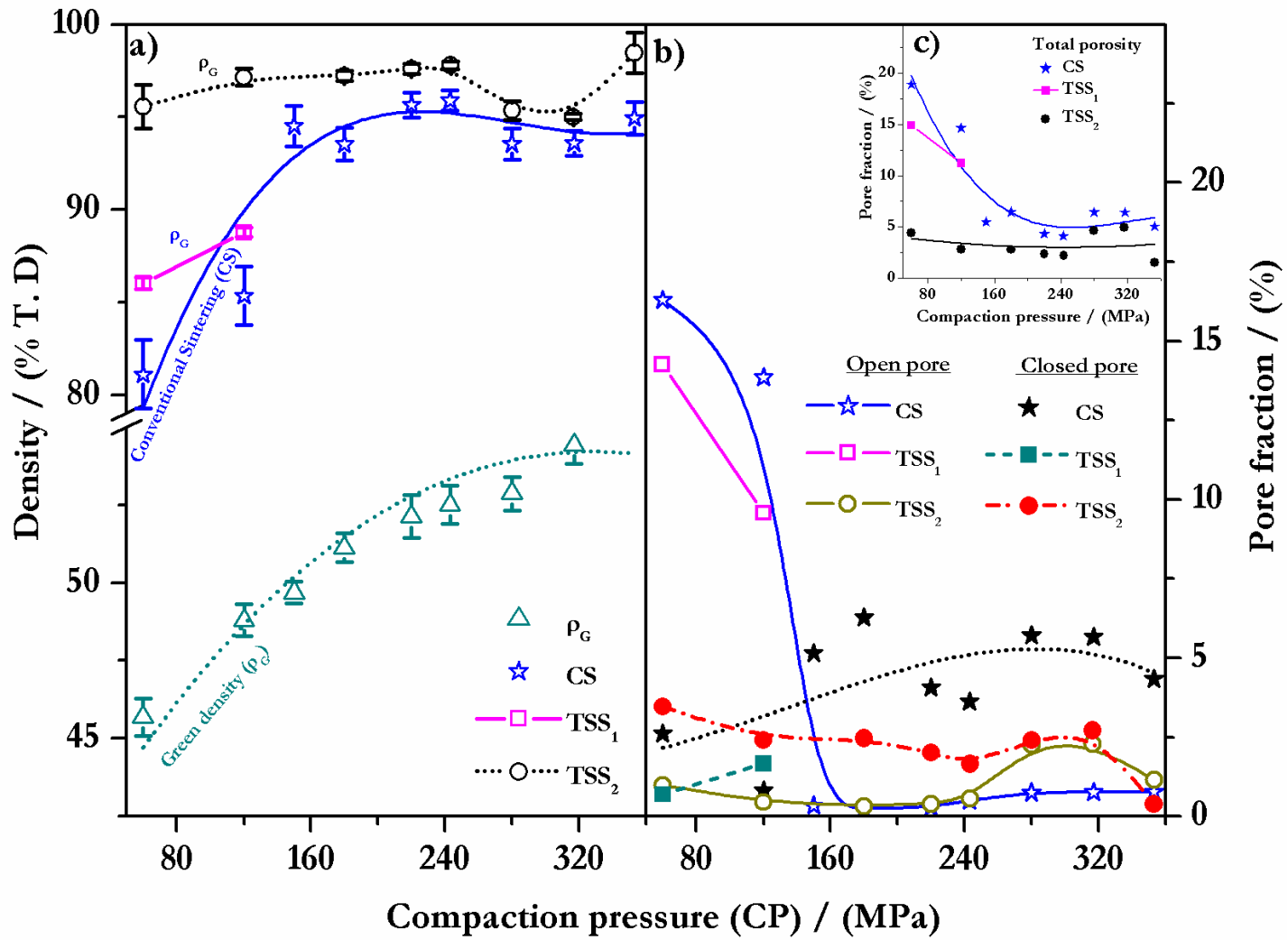


Figure 3.23 Compaction and sintering curves – UC25H, under different sintering conditions: (a) dependance of green and sintered density with CP, (b) variation of open and closed pore fraction with CP and (c) variation of total porosity with the CP



**Table 3.10 Sintered density ( $\rho_s$ ) of  $\text{UO}_2$  pellets obtained from  $\text{U}_C25\text{H}$  powders**

<b>Conventional sintering (CS) [Soaking temperature 1673 K 4 h]</b>	
<b>CP (MPa)</b>	<b>% T.D<sup>x</sup></b>
60	81.1 $\pm$ 1.9
120	85.4 $\pm$ 1.6
150	94.5 $\pm$ 1.1
180	93.5 $\pm$ 0.9
220	95.7 $\pm$ 0.7
244	96.0 $\pm$ 0.5
280	93.6 $\pm$ 0.9
317	93.6 $\pm$ 0.7
353	94.9 $\pm$ 0.9
<b>Two-step sintering (TSS<sub>1</sub>) [Step 1: 1073 K 2h; Step 2: 1473 K 4 h]</b>	
60	86.0 $\pm$ 0.3
120	88.8 $\pm$ 0.3
<b>Two-step sintering (TSS<sub>2</sub>) [Step 1: 1073 K 2h; Step 2: 1673 K 4 h]</b>	
60	95.6 $\pm$ 1.2
120	97.2 $\pm$ 0.5
180	97.2 $\pm$ 0.3
244	<b>97.8 <math>\pm</math> 0.2</b>
280	95.4 $\pm$ 0.5
317	95.0 $\pm$ 0.2
353	<b>98.5 <math>\pm</math> 1.1</b>

<sup>x</sup> indicates the mean value of five different measurements

It appears that at a CP of 150 MPa the  $\rho_G$  approaches 50% T.D, which is just about optimum for obtaining a defect free sintered product. A minimum CP of 150 MPa was found necessary in order to obtain a sintered product with a density above 90 % T.D. From the

foregoing it could be concluded that the CS method when applied to nc-UO<sub>2</sub> powders yields a maximum density of 96 % T.D at 1673 K.

U<sub>C</sub>25H powders were compacted at 60 and 120 MPa and sintered by using TSS<sub>1</sub> method (Fig. 3.23 and Table 3.10). The results indicate that U<sub>C</sub>25S<sub>2</sub> compacts densified to marginally higher densities as compared to those sintered by CS (Table 3.10). A  $\rho_s$  of 86.0 % T.D (60 MPa) and 88.8 % T.D (120 MPa) were obtained by using TSS<sub>1</sub>, while the CS had yielded a  $\rho_s$  of 81.1 % T.D (60 MPa) and 85.4 % T.D (120 MPa). It is further observed that the open pore fraction had decreased with the CP with a concomitant increase in the closed pore fraction.

Shrinkage data pertaining to these compacts also revealed that both the axial shrinkage (AS) and radial shrinkage (RS) decrease with the CP. Among them, the reduction in AS is found to be more pronounced (higher slope) than that in the RS. These results ( $\rho_s$ , shrinkage and porosity of U<sub>C</sub>25S<sub>1</sub>) suggest that even though TSS<sub>1</sub> has the potential to yield a better sintered product, the  $\rho_s$  needs to be improved by appropriate process optimization. Hence, a new procedure was devised by which higher densities could be realized. Our results (Fig. 3.24 & Table 3.10) revealed that U<sub>C</sub>25H compacts could be sintered to a density of  $95.6 \pm 1.2$  % T.D (60 MPa) and  $97.2 \pm 0.5$  % T.D (120 MPa) by this new method. Hence, this “TSS” with a final sintering temperature of 1673 K (TSS<sub>2</sub>) was used to sinter all the other powders.

### **3.10.3 Two-Step Sintering (TSS<sub>2</sub>)**

The  $\rho_s$  of the compacts sintered by TSS<sub>2</sub> are presented in Fig. 3.24 and Table 3.11. It was observed that the UO<sub>2</sub> compacts derived through the de-nitration method (U00H) had yielded the lowest  $\rho_s$ . The  $\rho_s$  of the U00S<sub>2</sub> monoliths increase with the CP up to 244 MPa (85.1 %T.D). Pellets compacted at 317 MPa showed a lower  $\rho_s$  (75.7 % T.D). This behavior could be explained by considering the porosity and shrinkage of the respective samples (Fig. 3.25).

Sintered  $\text{UO}_2$  compacts (U00H) revealed that both AS and RS are negatively correlated with the CP (up to 317 MPa) and the monolith derived at 317 MPa exhibited the lowest shrinkage. Among all the U00H compacts maximum porosity was observed when the CP was in the range of 280 to 317 MPa. It is interesting to note that the open porosity in the sintered compacts have increased from 12 % to 24 % while the closed porosity remained constant at less than 1 % independent of the CP. The characteristics of the U00H powders and its sintering behavior were markedly different from the rest of the citrate gel-combustion derived powders.

Among the powders derived through citrate gel-combustion method a clear trend was discernible. The powders could be separated into two sets, viz., **set 1**:  $\text{U}_{\text{C}5.5\text{H}}$ ,  $\text{U}_{\text{C}10\text{H}}$  and  $\text{U}_{\text{C}25\text{H}}$  and **set 2**:  $\text{U}_{\text{C}50\text{H}}$ ;  $\text{U}_{\text{C}75\text{H}}$ ,  $\text{U}_{\text{C}90\text{H}}$  and  $\text{U}_{\text{C}100\text{H}}$ . The powders in **set 1** exhibited higher sinterability (Table 3.10 & 3.11 & Figs. 3.23-3.24). The powders  $\text{U}_{\text{C}10\text{H}}$  and  $\text{U}_{\text{C}25\text{H}}$  which were derived through “volume combustion” yielded higher densities than  $\text{U}_{\text{C}5.5\text{H}}$  under identical conditions. All these three powders exhibited nearly similar shrinkage anisotropy and low open porosity and densified to a maximum density of 98 % T.D (317 MPa). The reduction in the  $\rho_{\text{s}}$  in these pellets (**set 1**) obtained by compacting at pressures between 200 and 240 MPa is due to the reasons cited in the foregoing discussions on U00H. The values of sintered densities of these compacts (with low  $\rho_{\text{s}}$ ) bear an inverse relation with open porosity.

The shrinkage anisotropy [65] in highly densified monoliths  $\text{U}_{\text{C}10\text{S}_2}$  and  $\text{U}_{\text{C}25\text{S}_2}$  was pronounced and its correlation with the density was markedly different. From the foregoing it is evident that the nc-urania powders derived through volume combustion ( $\text{U}_{\text{C}10\text{H}}$  and  $\text{U}_{\text{C}25\text{H}}$  powders) could be sintered to a density of about 97.0 % T.D by employing a compaction pressure as low as 120 MPa and sintering with the TSS<sub>2</sub> method. Even though a CP of 317 MPa

yielded higher densities, in order to maintain the shrinkage anisotropy ( $\alpha$ ) close to unity, it is found that a CP of 180 MPa would be most ideal for these powders (set 1).

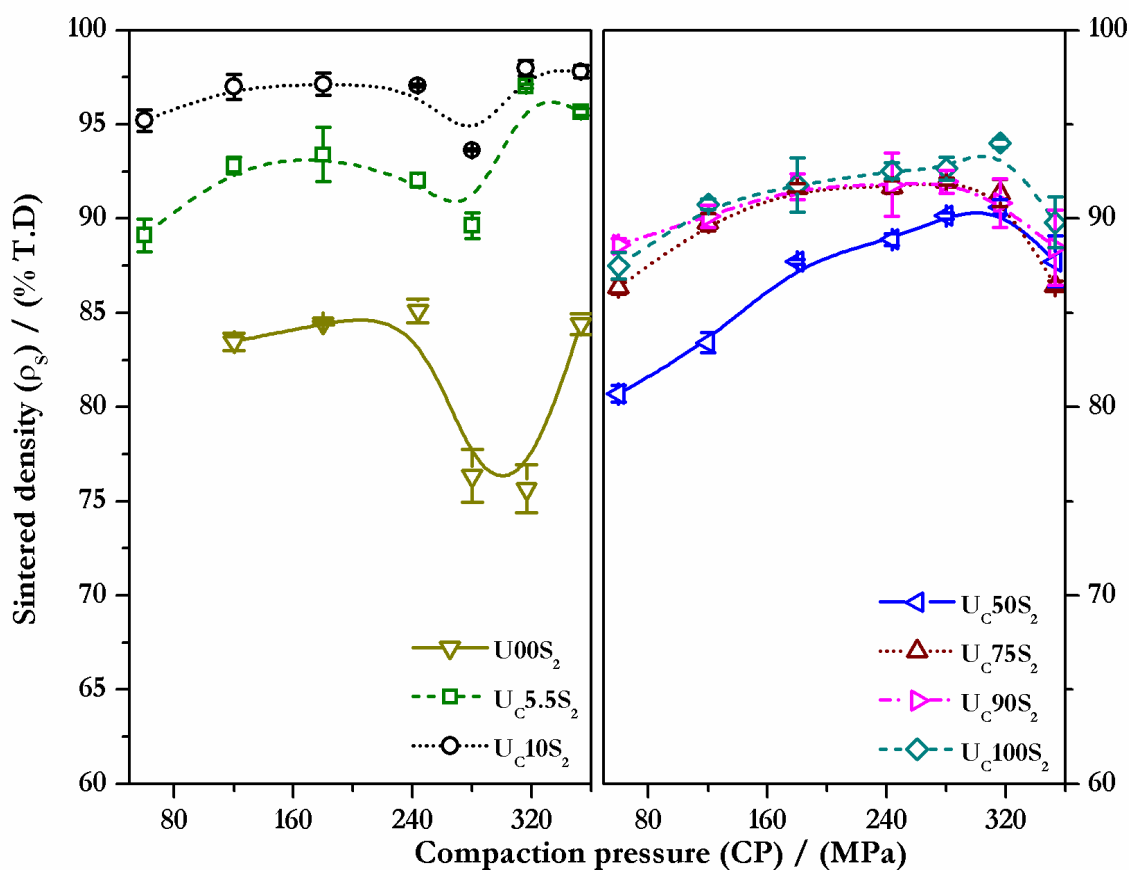
The maximum density that could be realized with the powders in “set 2” was limited to 94 % T.D ( $U_C100S_2$ , 317 MPa). However, the reduction in  $\rho_s$  in the “set 1” compacts (280 MPa and 317 MPa) was not observed in these powders. The absence of harder agglomerates, testified by the dependence of the  $\rho_G$  on CP (Fig. 3.22) supports the fact that these powders undergo uniform compaction with less residual stress. Thus, it is evident that, apart from surface activity and sinterability, other physical characteristics, viz., flowability and particle size distribution contribute significantly towards the sinterability of nc- $UO_2$ .

Table 3.12 and Fig. 3.26 enlists the data cited in the literature on CS of microcrystalline  $UO_2$ . From these data it is evident that the  $\rho_s$  in the range of 68.2 to 98.5 % T.D have been realized and that the sintering temperatures in the range of 1423 to 2053 K and CP in the range of 87 – 471 MPa have been employed by different authors [18, 24, 64, 73, 74]. Among these the work reported in ref. [25] and [74] are different and interesting variations. Kang et al. [25] had sintered  $UO_2$  monoliths (2003 K; 4h; 294 MPa and  $H_2$ ) derived through the ADU method and re-oxidation method (mixture of  $UO_2$  and  $U_3O_8$ ) to a  $\rho_s$  of 97.9 % T.D and 96.3 % T.D respectively. Yang et al. [74] had sintered  $UO_2$  pellets which employed “additive type pellets” and “matrix type pellets” wherein the former involves mixing, compacting, crushing and pressing to form green pellets while the latter were prepared by mixtures containing  $UO_2$  powders, ammonium oxalate (pore former) and zinc stearate (binder). These authors had obtained sintered monoliths of 93.3-94.0 % T.D and 94.3-94.8 % T.D (1673 K; 1-3 h &  $N_2$ - $CO_2$ ) respectively.

Table 3.11 Sintered density ( $\rho_s$ ) of  $\text{UO}_2$  pellets derived through TSS<sub>2</sub> method

CP (MPa)	$\text{U00S}_2$	$\text{U}_{\text{C}5.5\text{S}_2}$	$\text{U}_{\text{C}10\text{S}_2}$	$\text{U}_{\text{C}50\text{S}_2}$	$\text{U}_{\text{C}75\text{S}_2}$	$\text{U}_{\text{C}90\text{S}_2}$	$\text{U}_{\text{C}100\text{S}_2}$
	% T.D. <sup>x</sup>						
<b>60</b>	-	89.1 ± 0.9	95.2 ± 0.6	80.7 ± 0.5	86.4 ± 0.4	88.6 ± 0.4	87.5 ± 0.7
<b>120</b>	83.5 ± 0.5	92.8 ± 0.4	97.0 ± 0.7	83.4 ± 0.6	89.8 ± 0.5	90.1 ± 0.6	90.8 ± 0.3
<b>180</b>	84.5 ± 0.1	93.4 ± 1.4	97.2 ± 0.6	87.7 ± 0.1	91.6 ± 0.2	91.7 ± 0.7	91.8 ± 1.4
<b>244</b>	85.1 ± 0.6	92.0 ± 0.4	97.1 ± 0.1	88.9 ± 0.3	91.7 ± 0.3	91.8 ± 1.7	92.5 ± 0.4
<b>280</b>	76.3 ± 1.4	89.6 ± 0.7	93.6 ± 0.1	90.2 ± 0.2	92.0 ± 0.2	92.0 ± 0.6	92.7 ± 0.6
<b>317</b>	75.7 ± 1.3	97.0 ± 0.1	<b>98.0 ± 0.4</b>	90.6 ± 0.4	91.4 ± 0.7	90.8 ± 1.3	94.0 ± 0.2
<b>353</b>	84.4 ± 0.5	95.7 ± 0.2	97.8 ± 0.3	87.7 ± 1.4	86.4 ± 0.3	88.5 ± 0.9	89.8 ± 1.4

<sup>x</sup> indicates the mean value of five different measurements

Figure 3.24 Sintered density ( $\rho_s$ ) of TSS<sub>2</sub> compacts with the CP

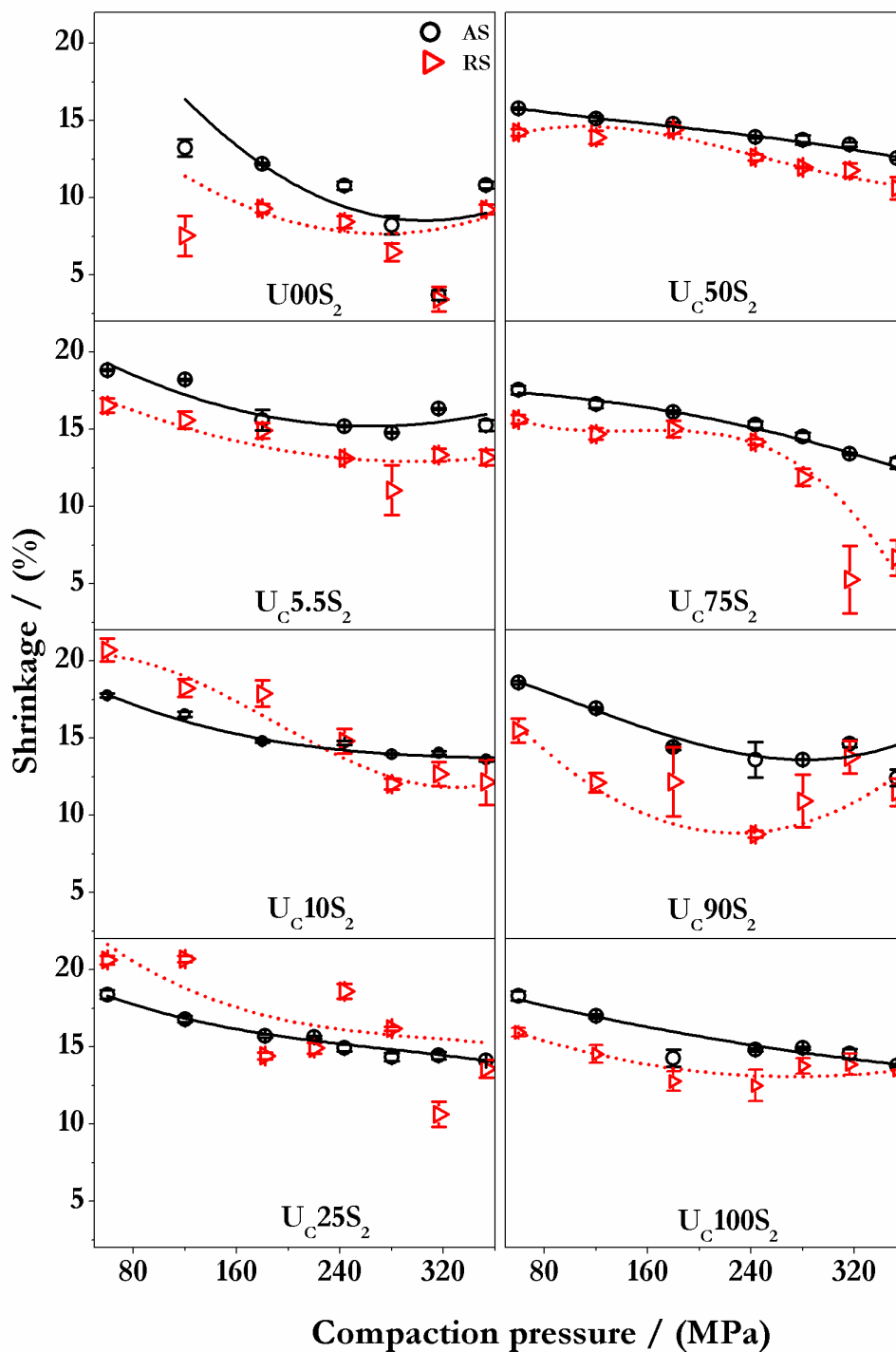


Figure 3.25 Axial (AS) and radial shrinkage (RS) in  $TSS_2$   $UO_2$  pellets

From the data presented Table 3.12 it is evident that many authors had successfully prepared sintered  $UO_2$  pellets from microcrystalline  $UO_2$  with a density of 97 to 98 % T.D

(Fig. 3.26) without the addition of a binder or a lubricant. However, these authors (Table 3.12 and Fig. 3.26) had employed a temperature as high as 1973 K to realize such high densities. In the present study a density as high as 98 % T.D has been realized at a temperature as low as 1673 K by using nc-UO<sub>2</sub>. Thus, it has been amply demonstrated that citrate gel-combustion derived nc-UO<sub>2</sub> undergoes facile densification even at lower temperatures, as compared to its microcrystalline analogue.

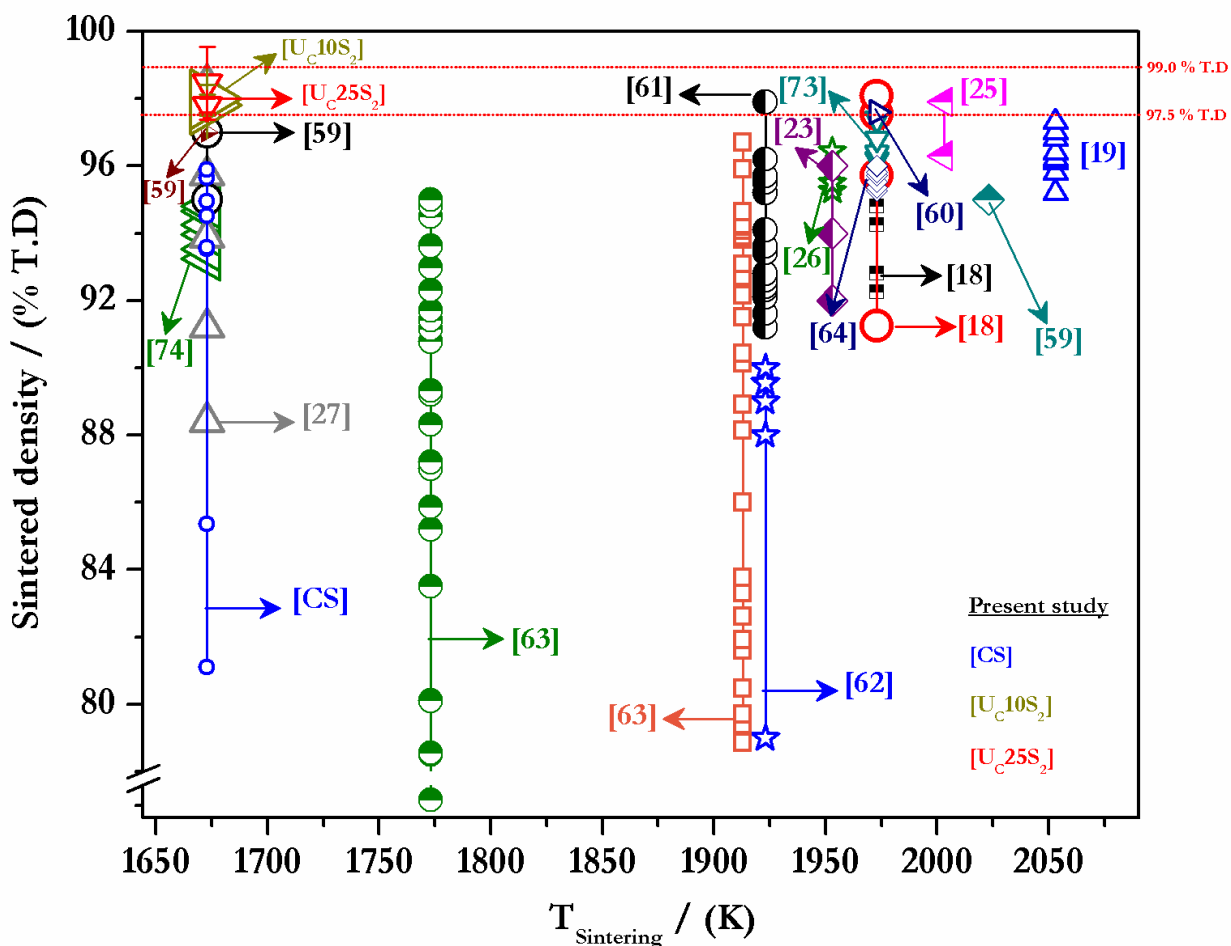


Figure 3.26 Effect of  $T_{\text{sintering}}$  on the  $\rho_s$  of  $\text{UO}_2$

**Table 3.12 Comparison of UO<sub>2</sub> powder characteristics and  $\rho_s$  reported in the literature**

<b>R<sup>binder/lubricant</sup></b>	<b>Method</b>	<b>SSA (m<sup>2</sup>g<sup>-1</sup>)</b>	<b>CP (MPa)</b>	<b>T<sub>s</sub> / time / atmosphere</b>	<b>ρ<sub>G</sub> (% T.D)</b>	<b>ρ<sub>s</sub> (% T.D)</b>
[22]	AUC	5.96	320	1573 / 0.1-40 h / (CO <sub>2</sub> -H <sub>2</sub> ) 1773/0.1-40 h / (CO <sub>2</sub> -H <sub>2</sub> )	51.0	-
[18] <sup>ZS</sup>	AUC	4.29-6.66	87-422	1973 / 2 h / H <sub>2</sub>	45.6-56.5	92.3-97.6
	ADU	6.04	146-573		41-53.8	91.3-98.1
[19] <sup>SA</sup>	ADU	2.16-4.9	343	2053 / 4 h / H <sub>2</sub>	49-58	95.2-97.3
[73]	ADU	0.5	300	1973 / 4 h / H <sub>2</sub>	-	96.2-97.4
[25]	ADU	0.6-1.4	294	2003 / 4 h / H <sub>2</sub>	-	97.9
	RO				-	96.3
[74] <sup>ZS</sup>	A	4.7	-	1673 / 1-3 h / N <sub>2</sub> -CO <sub>2</sub>	-	93.3-94.0
	M					94.3-94.8
[64]	ADU	-	250	1973 / - / cracked NH <sub>3</sub>	-	95.3-96.0
[60]	-	-	196	1973 / 2 h / N <sub>2</sub> -13% H <sub>2</sub>	55.8-66.2	97.6
[62]	ADU	5.31	-	1923 / 3 h / H <sub>2</sub>	38-54	79-90
[26]	AUC	5	270	1953 / 4 h / H <sub>2</sub>	51.9-52.4	95.3-96.4
[63]	-	0.2-5.9	300	1773 / 4 h / H <sub>2</sub>	47.7-66.5	68.2-95.0
				1913 / 4 h / H <sub>2</sub>		71.9-96.7
[23]	AUC	5	300	1953 / 4 h / CO <sub>2</sub> -H <sub>2</sub>	52.4	92.0-96.0
[27]	ADU	1.1-6.2	304	1673 / 16 h / H <sub>2</sub>	54.0-55.0	88.1- <b>98.5</b>
[61] <sup>SA</sup>	AUC	7.5-10.6	186	1923 / 4 h / H <sub>2</sub>	45.8	91.6
			284		45.0-46.9	91.2-95.2
			373		48.1-50.1	92.1-95.7
			471		50.4-51.4	92.8- <b>97.9</b>
[24]	AUC	4.5-5.5	275-392	-	45.6-59.3	93.0-96.6
[57] <sup>ZS</sup>	ADU	4.8	300	1423 / 4 h / H <sub>2</sub> O-CO <sub>2</sub> -H <sub>2</sub>	50	95.0
[58] <sup>PVA</sup>	ADU		260	1473-1573 / 6 -7 h / N <sub>2</sub> -H <sub>2</sub>	50	92.0- <b>98.0</b> (g)
[59] <sup>ZS</sup>	ADU	2.3-2.4	392	2023 / 5 h / H <sub>2</sub>		95.0
				1673 / 8 h / (H <sub>2</sub> /N <sub>2</sub> )-air-(H <sub>2</sub> -N <sub>2</sub> )	54.7	97.0
				1673 / 4 h / (H <sub>2</sub> /N <sub>2</sub> )-air-(H <sub>2</sub> -N <sub>2</sub> )		95.0
<b>This study</b>	D	5.66	60-353	1673 / 4 h / 8 % Ar-H <sub>2</sub>	49.6-58.3	75.7-85.1
	CGC	5-9.7		1473 / 4 h / 8 % Ar-H <sub>2</sub>	44.6-56.4	81.1-95.9
				1673 (TSS <sub>2</sub> ) / 4 h / 8 % Ar-H <sub>2</sub>		80.7- <b>97.8</b>

ADU - Ammonium diuranate; AUC - ammonium uranyl carbonate; CP – compaction pressure; TSS<sub>2</sub> – “two-step sintering”; g - geometrical density; A- Additive type; M-Matrix type; CGC-citrate gel-combustion; D-direct denitration; <sup>PVA</sup>-poly vinyl alcohol; <sup>ZS</sup>- zinc stearate; <sup>SA</sup>- stearic acid and T<sub>s</sub>-Sintering temperature (K); RO-Re-Oxidised



### 3.10.4 Morphological analysis by using SEM

Selected samples of sintered  $\text{UO}_2$  pellets were examined for their microstructure by using SEM (Figs. 3.27-3.29). All these pellets were investigated for the sizes of grains, pores and dihedral angle between the grains. SEM images revealed that these monoliths comprised grains with unimodal size distribution (fine grained monoliths). It was observed that the  $\text{U}_{\text{C}}25\text{S}_2$  monoliths possessed faceted grains with well defined grain boundaries.

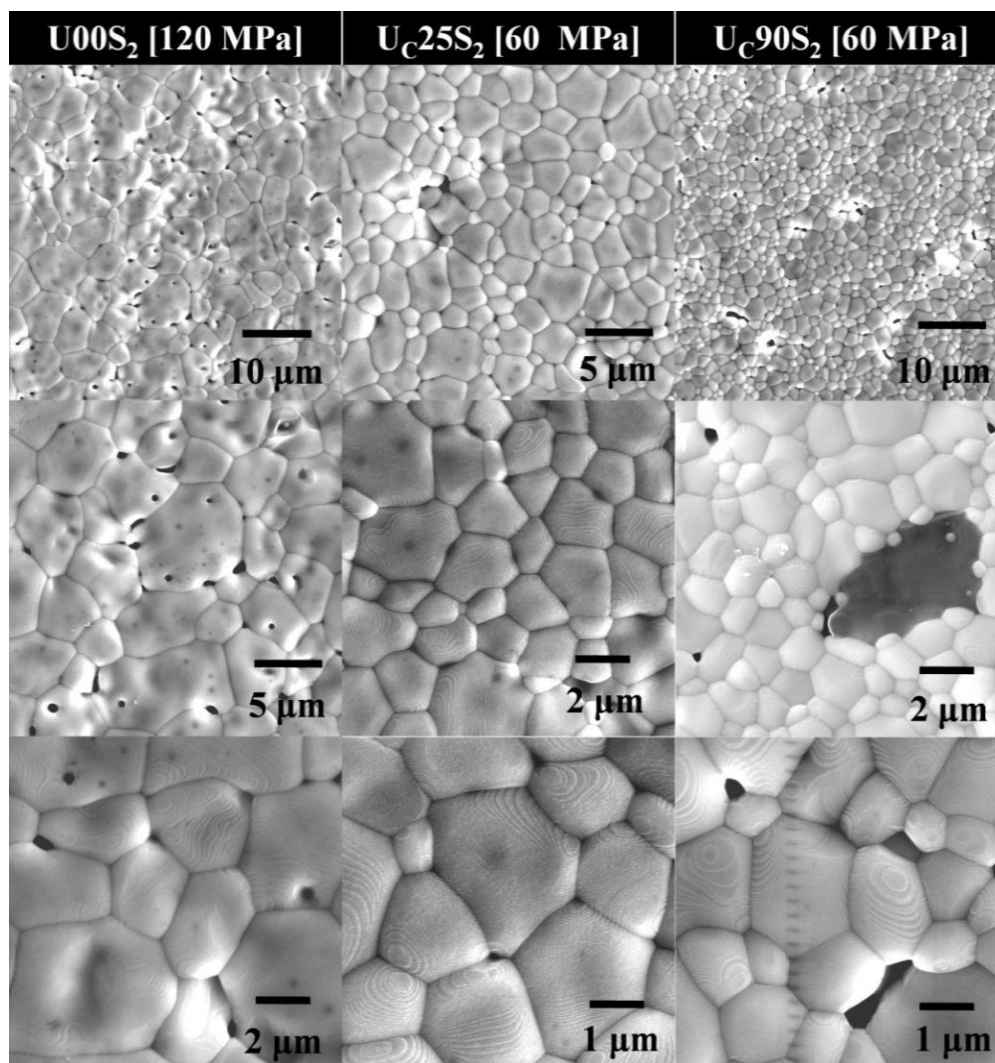


Figure 3.27 SEM images of  $\text{UO}_2$  monoliths: a)  $\text{U00S}_2$  [120 MPa], b)  $\text{U}_{\text{C}}25\text{S}_2$  [60 MPa] and c)  $\text{U}_{\text{C}}90\text{S}_2$  [60 MPa] which were sintered by  $\text{TSS}_2$

On the other hand it was observed that  $U_C50S_2$ ,  $U_C90S_2$  and  $U_C100S_2$  monoliths comprised grains in the submicron regime. This implies that powders derived through citrate gel-combustion ( $R > 0.25$ ) would yield fine grained  $UO_2$  pellets when sintered by using  $TSS_2$ .

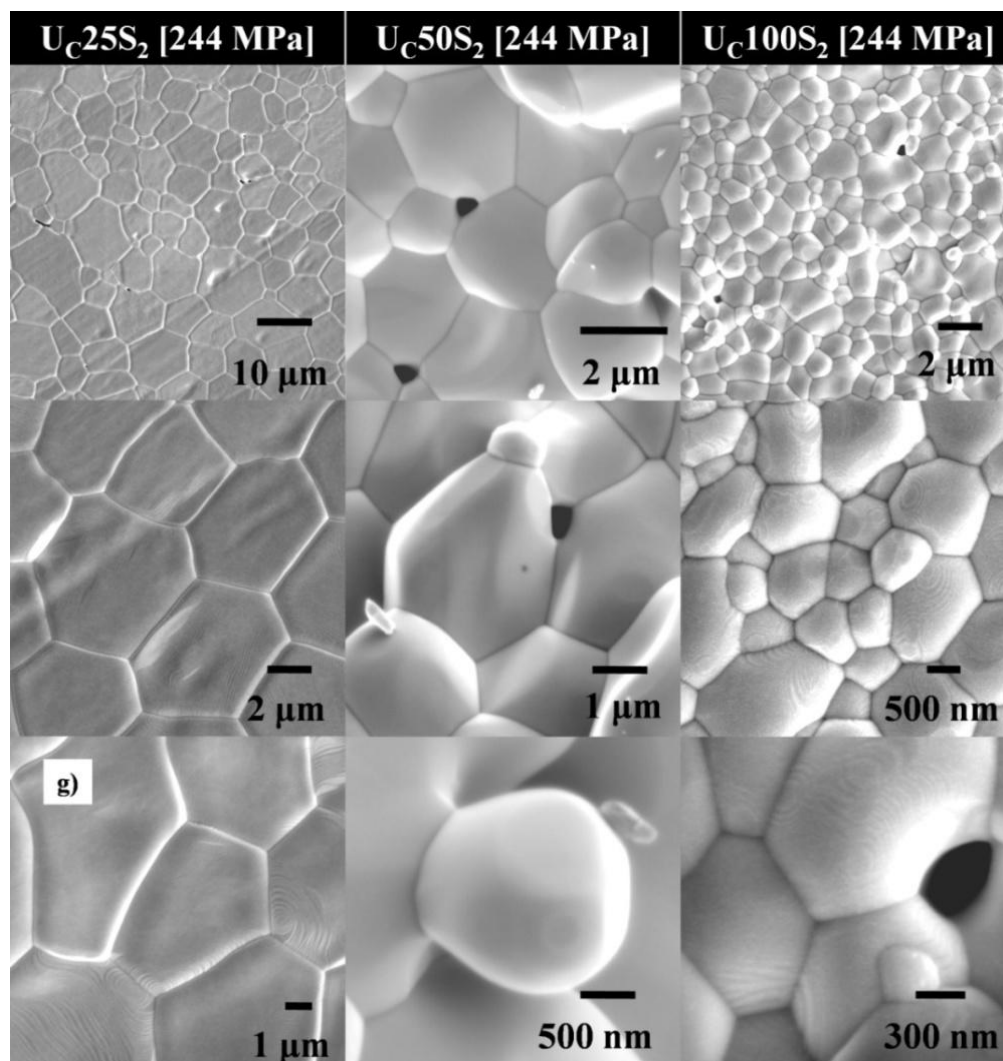


Figure 3.28 SEM images of  $UO_2$  monoliths: a)  $U_C25S_2$  [244 MPa], b)  $U_C50S_2$  [244 MPa] and c)  $U_C100S_2$  [244 MPa] which were sintered by using  $TSS_2$

Fractured surface of these pellets were investigated for their pores both isolated (intragranular) and between the grains (intergranular), fissures and dihedral angle by using SEM. The most important characteristic of a sintered body is its porosity (open and closed). Besides pore size, its distribution also plays an important role during densification. Hence, to achieve a

desired  $\rho_s$  it is vital to understand the pore characteristics viz., their morphology, size distribution, dihedral angle and coordination number [number of grains surrounding the pores (N)] in order to optimize the sintering process [65, 66]. Thermodynamically it could be shown that the stability of a pore depends on the Gibbs energy change during the shrinkage, the dihedral angle ( $\Psi$ ) between the grains, grain boundary energy ( $\gamma_{gb}$ ) and surface particle/pore interfacial energy ( $\gamma_{sv}$ ). The equilibrium shape of the pore is related to its dihedral angle by eqn. 3.13 [65].

$$\cos\left(\frac{\Psi}{2}\right) = \frac{\gamma_{gb}}{2\gamma_{sv}} \quad 3.13$$

Further, it can be shown in 2-D that the pores with  $N < 6$  would shrink because the surface of the pore will move inward towards its centre of curvature (concave grain boundary) while with  $N > 6$  would grow [65, 66]. In other words, the resultant Gibbs energy change indicates that the decrease in energy due to the reduction in the pore surface area is greater than the increase in energy due to growth of the grain boundary ( $N < 6$ ). For  $N > 6$ , the Gibbs energy change is just the opposite [65, 66]. When  $N = 6$  [critical coordination number ( $N_c$ )] the pore is said to be in a metastable state with a dihedral angle of  $120^\circ$  [65, 66].

Kingery and Francois [75] had reported that the stability of a pore could be ascertained by measuring its dihedral angle. Further, these authors had demonstrated that the pores with a dihedral angle beyond a certain threshold value (3D: critical angle =  $120^\circ$ ; critical number of grains surrounding the pore = 12) with a few grains surrounding them would shrink while those with a dihedral angle less than the critical angle and a large number of grains surrounding them would coarsen (pore growth). Rahaman [65] and Chaim [76] had reported that pores that are larger than the grains surrounding them would be thermodynamically stable and it is difficult to eliminate them. Thus, it is important to compact powders into a body with high  $\rho_G$  and with a uniform size distribution of smaller pores such that the value of N is smaller than 12 [76]. These

pores could then be removed easily during sintering, resulting in a dense product. Anisotropic shrinkage would result in a defective sintered product [65]. Thus, in order to obtain a defect free sintered product, it is necessary to optimize the process parameters such that the shrinkage anisotropy and relative pore fraction are minimal.

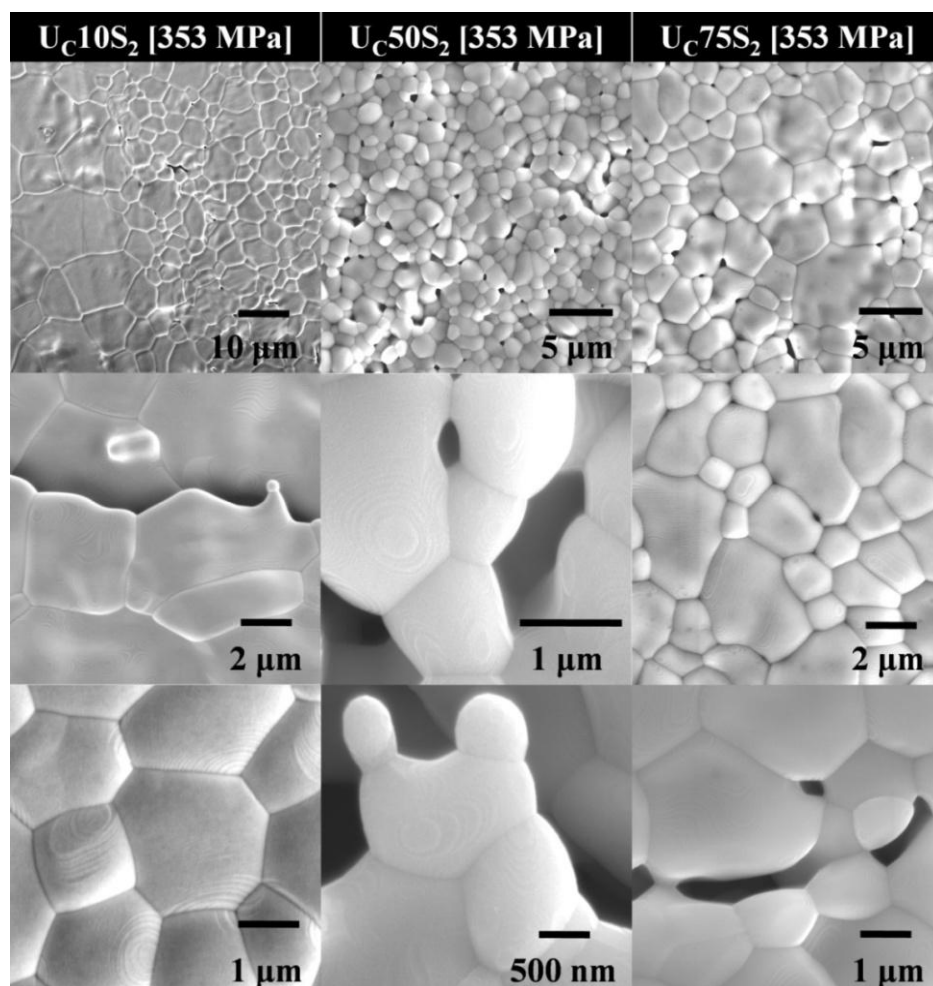


Figure 33.29 SEM images of  $UO_2$  monoliths: a)  $U_C10S_2$  [353 MPa], b)  $U_C50S_2$  [353 MPa] and c)  $U_C75S_2$  [353 MPa] which were sintered by using  $TSS_2$

Shrinkage anisotropy factor ( $\alpha$ ) is defined as the ratio of AS to that of RS [ $\alpha = \frac{AS}{RS}$ ] while the relative pore fraction is the ratio of open or closed porosity to that of total porosity (Figs. 3.30-3.31). The desirable value of  $\alpha$  is about 1 while that of relative porosity is less than 1% [65].

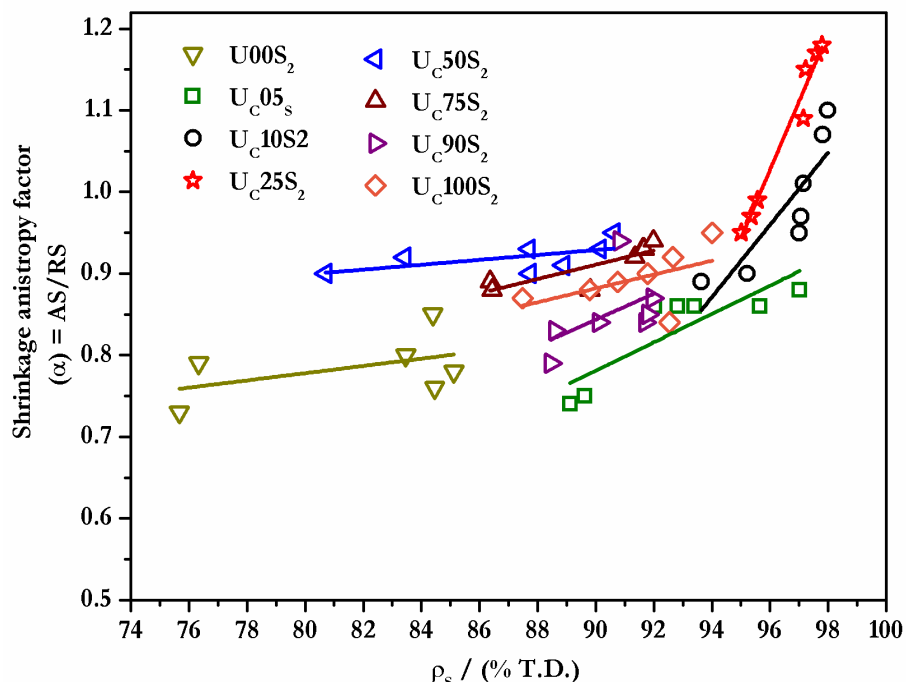


Figure 3.30 Dependence of shrinkage anisotropy factor ( $\alpha$  = ratio of axial to radial shrinkage) on the  $\rho_s$  of  $\text{UO}_2$  monoliths (TSS<sub>2</sub>)

All other process variables viz., steps in the powder preparation and the characteristics of powders and green body and the sintering cycle need to be optimized such that an  $\alpha$  close to unity and a closed porosity near to 1 % are achieved. In general, it is observed that  $\alpha$  varies linearly with the  $\rho_s$  while the open pore fraction decreases with the same. The variation in closed porosity with the  $\rho_s$  plays a predominant role in the final stage of sintering [65, 76-78]. A study of the relative variation in the porosity and  $\alpha$  with the  $\rho_s$  helps to optimize the critical CP wherein both closed and open pore fraction are nearly equal beyond which there would be no appreciable change in the  $\rho_s$ . Since most of the pores observed in the sintered pellets obtained in this study (Figs. 3.27-3.29 & 3.31) have dihedral angles between  $115^\circ$  to  $128^\circ$ , it is reasonable to assume that they would shrink upon prolonged sintering. This testifies the fact that in the TSS<sub>2</sub> method sintering has been taken up to the “final stage”.

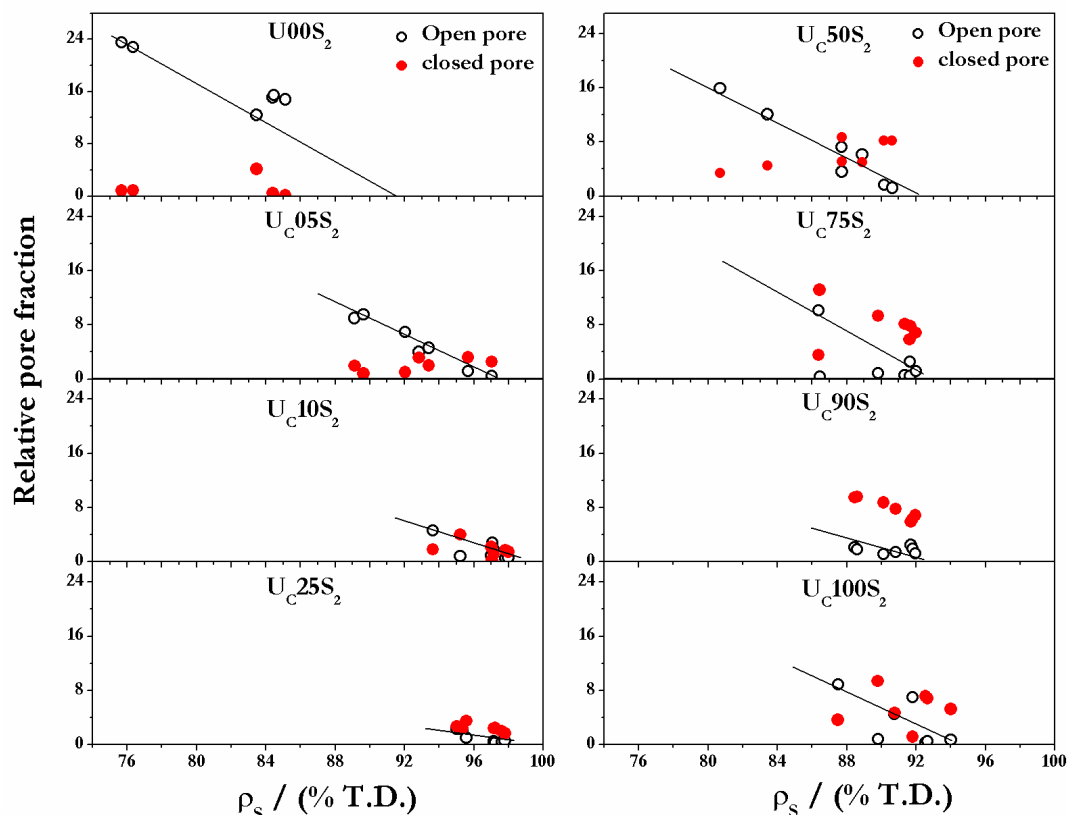


Figure 3.31 Dependence of the volume fraction of pores (open and closed) on the  $\rho_s$

Nanocrystalline powders usually tend to yield sintered bodies with significant grain coarsening. Usually the grains size is in the range of 10-50  $\mu\text{m}$  but often the distribution of sizes of these grains is not uniform. Our aim was to obtain dense compacts with near unimodal size distribution. In addition the sintered densities obtained with the method used in our study are much higher as compared to the methods proposed by other authors for sintering of nanocrystalline urania. However, further studies would help to optimize the process parameters to obtain nanostructured sintered monoliths. Probably a techniques that suppresses grains coarsening viz., SPS might yield a product with nanograins.

### 3.10.5 Phase characterization and residual carbon

XRD analysis of the sintered  $\text{UO}_2$  pellets (selected samples) revealed that the sintered  $\text{UO}_2$  compacts comprised the fluorite phase (Fig. 3.32).



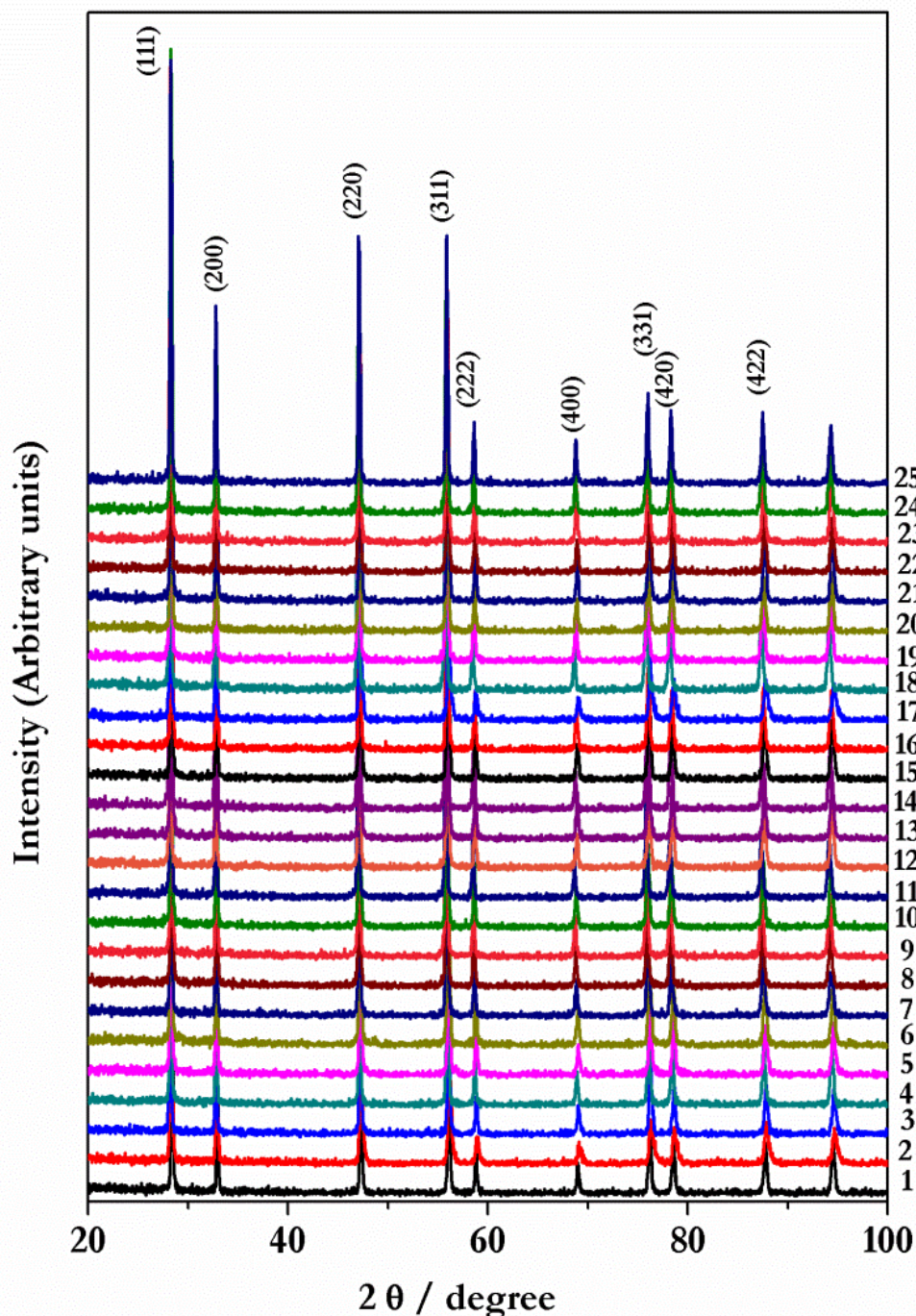


Figure 3.32 XRD plot of  $U_CXS_2$ -YYY samples [where -YYY indicates compaction pressure]  
 1)  $U_C100S_2$ -317, 2)  $U_C100S_2$ -280, 3)  $U_C100S_2$ -244, 4)  $U_C100S_2$ -120, 5)  $U_C90S_2$ -280, 6)  $U_C90S_2$ -244, 7)  $U_C90S_2$ -180, 8)  $U_C90S_2$ -060, 9)  $U_C50S_2$ -244, 10)  $U_C25S_2$ -353, 11)  $U_C25S_2$ -280, 12)  $U_C25S_2$ -244, 13)  $U_C10S_2$ -317, 14)  $U_C10S_2$ -280, 15)  $U_C10S_2$ -244, 16)  $U_C10S_2$ -120, 17)  $U_C10S_2$ -060, 18)  $U_C5.5S_L$ -317, 19)  $U_C5.5S_2$ -280, 20)  $U_C5.5S_2$ -244, 21)  $U_C5.5S_2$ -180, 22)  $U_C5.5S_2$ -120, 23)  $U00S_2$ -280, 24)  $U00S_2$ -244, 25)  $U00S_2$ -180

Carbon residue present in the sintered  $\text{UO}_2$  compacts was found to vary between 67 – 103 ppm (Table 3.13). The carbon residue in the sintered  $\text{UO}_2$  pellets are well meet the specification of nuclear grade sintered  $\text{UO}_2$  pellets (ASTM- CC776-06) [79]. Thus, the sintered  $\text{UO}_2$  monoliths are comparable to the reactor grade sintered  $\text{UO}_2$  pellets.

**Table 3.13 Carbon residue in sintered  $\text{UO}_2$  pellets derived through TSS<sub>2</sub>**

CP (MPa)	U00S <sub>2</sub>	U <sub>C</sub> 5.5S <sub>2</sub>	U <sub>C</sub> 10S <sub>2</sub>	U <sub>C</sub> 25S <sub>2</sub>	U <sub>C</sub> 50S <sub>2</sub>	U <sub>C</sub> 75S <sub>2</sub>	U <sub>C</sub> 90S <sub>2</sub>	U <sub>C</sub> 100S <sub>2</sub>
	(ppm)							
<b>60</b>	78	96	92	68	88	91	95	85
<b>120</b>	88	83	90	90	103	76	82	86
<b>180</b>	84	96	95	92	81	88	99	89
<b>243</b>	96	99	79	85	95	99	91	74
<b>280</b>	79	83	83	96	96	92	84	97
<b>317</b>	67	74	93	86	89	89	96	85
<b>353</b>	90	72	87	79	83	94	102	81

<sup>x</sup> indicates the mean value of five independent measurements

### 3.11 Conclusion from investigations on the sintering of nc- $\text{UO}_2$

Systematic investigation on sintering of nc- $\text{UO}_2$  powders derived through citrate gel-combustion method was carried out, by using three different methods, viz., i) conventional method (CS), ii) two-step sintering (TSS<sub>1</sub>) and iii) two-step sintering (TSS<sub>2</sub>). Among these, the TSS<sub>2</sub> method was found most suitable. Powders derived from starting mixtures with an R value of 0.10 and 0.25 were found to be highly sinterable and yielded a maximum  $\rho_s$  of  $\approx 98\%$  T.D with uniform grains (1 – 15  $\mu\text{m}$ ). Through optimization trials, 180 MPa and TSS<sub>2</sub> were found to be the ideal conditions to obtain high density  $\text{UO}_2$  pellets from these powders. Shrinkage anisotropy factor ( $\alpha$ ) in the sintered  $\text{UO}_2$  monoliths were investigated for the first time. Relative size fraction of open and closed pore fraction of sintered  $\text{UO}_2$  monoliths were also investigated. The method employed in this study has led to a new fabrication procedure which would be an



energy and cost efficient method for obtaining  $\text{UO}_2$  pellets with a uniform grain size of about 1-15  $\mu\text{m}$ .

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## Chapter 4

### Preparation of $\text{UO}_2$ foam and porous pellets of $\text{UO}_2$

*In this chapter the results obtained in the investigations on the preparation of urania foam and porous pellets are discussed*

#### 4.1 Purity of starting material

Nuclear grade urania was used for the preparation of both  $\text{UO}_2$  foam and porous  $\text{UO}_2$  pellets. The reagents that were used in this study were devoid of any significant impurities that would influence sintering.

#### 4.2 Preparation of $\text{UO}_2$ foam by using sucrose-gel combustion method

Since this is the first study on the preparation of urania foam through sucrose-gel combustion, the conditions best suited for the preparation of the foam had to be optimized. The value of R is a key parameter [1], and it had to be optimized in order to obtain  $\text{UO}_2$  foam with desirable properties. Initial trials revealed that sucrose-uranyl nitrate gels with an R value below 1.5, yielded powders while those with an R value above 2.6 yielded foams that were too fragile to handle. Hence, investigations were carried out on gels prepared from mixtures whose R value was between 1.50 and 2.60. Sucrose gets hydrolyzed into glucose and fructose in the presence of hydronium ions. These in turn are oxidized into a mixture of hydroxy carboxylic acids viz., gluconic acid, saccharic acid, glycolic acid and tartaric acid, in acidic medium. Hence, heating a mixture containing uranyl nitrate and sucrose would lead to the formation of carbohydrate molecule followed by formation of mixtures of hydroxy carboxylic acids. Upon continued heating these mixtures polymerize to form a resin. This resin decomposes slowly upon continued heating to form  $\text{CO}$ ,  $\text{CO}_2$  and  $\text{NO}_x$  gases. Evolution of these gases from the resin leads to

foaming. From the data presented in Table 4.1 it is seen that the specific surface area increases by two orders of magnitude (i.e. from 1.24 – 198.64 m<sup>2</sup>g<sup>-1</sup>) when the value of R was increased from 1.5 to 2.6. The carbon residue and porosity were found to increase with R, while the  $\rho_B$  decreased from 0.51 g cm<sup>-3</sup> to 0.10 g cm<sup>-3</sup>. Since the carbon residue would have a significantly lower density than urania the reduction in density could be attributed to the presence of a significant quantity of the former. While the XRD patterns (Fig. 4.1) pertaining to the sintered foam confirms the presence of UO<sub>2</sub>, there is no evidence for the presence of graphite. Plausibly the final product comprises amorphous carbon (which has much lower density than graphite) (Fig. 4.1). In view of the above it is reasonable to argue that the reduction in density is due to the presence of significant amount of both amorphous carbon and porosity.

The SEM images of the UO<sub>2</sub> foam derived through sucrose gel precursor (R = 2.4 and 2.6) presented in Fig. 4.2 reveal that these foams are highly porous and comprise both meso and macro pores. In view of the fact that the presence of high carbon residue (that would lead to electronic conductivity, which is not desirable for the DOR process); they are not well suited for the intended end use.

### **4.3 Preparation of porous pellets by using citrate gel combustion method**

In order to obtain porous monoliths devoid of significant quantities of carbon, citrate gel-combustion synthesis of nc-urania was pursued. In this investigation the R value was so tailored as to get a porous sintered pellet. In earlier investigation (Chapter 3) it was observed that the powders derived from mixtures with an R value of 0.25 (U<sub>C</sub>25A) show very different properties than those derived from mixtures with other values of R. Hence a mixture with this R value (0.25) was chosen for investigation along with a powder derived from mixtures with an R value of 1.00 (U<sub>C</sub>100A). Investigations on both these powders were carried out for comparison.

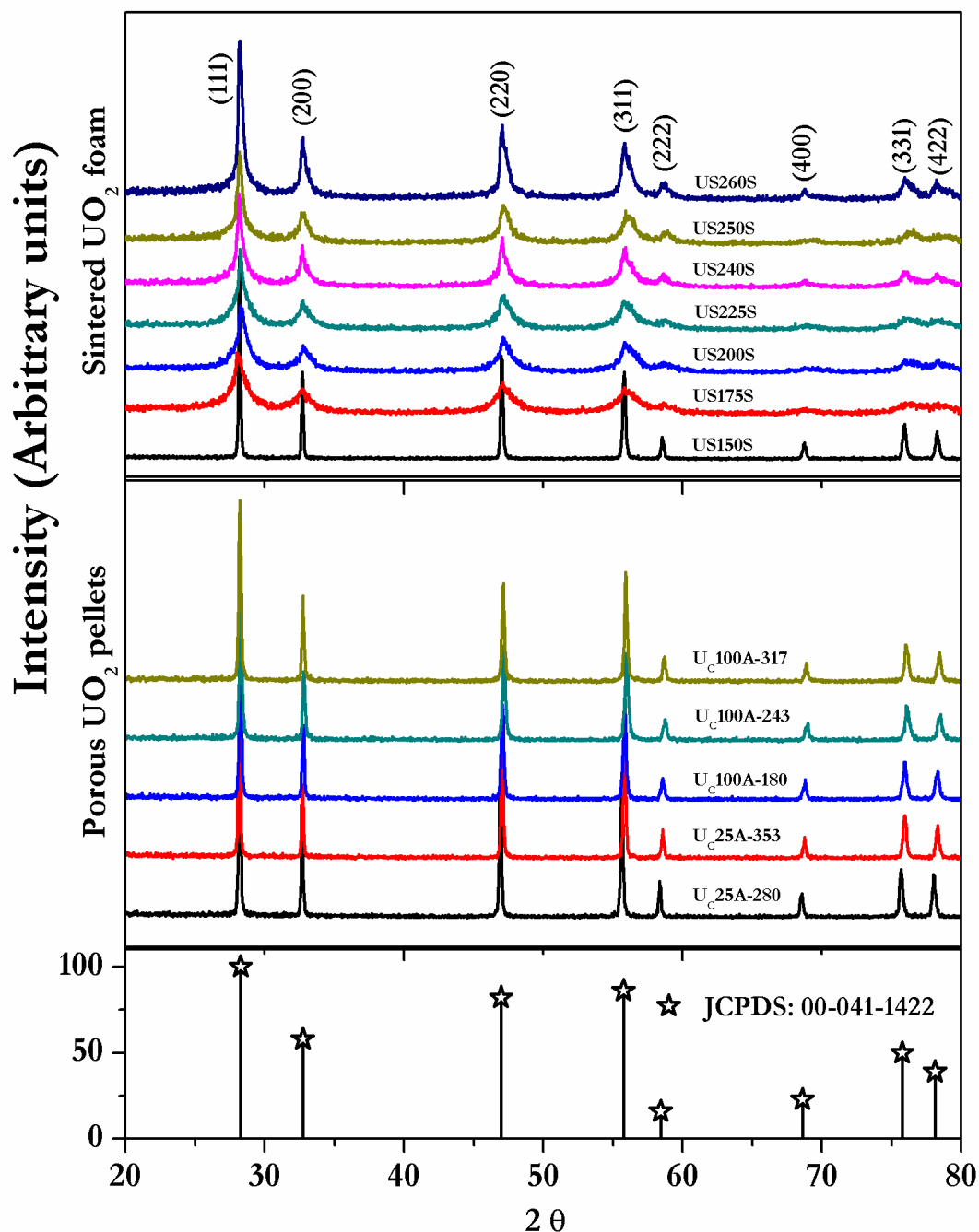


Figure 4.1 XRD of porous  $\text{UO}_2$  foam and sintered  $\text{UO}_2$  pellets [Sintered foams and porous  $\text{UO}_2$  pellets were designated as USXXXXS and UCXXA-P respectively, where XXX and XX indicates the value of “R” in % and the suffix S denotes that the foam is a sintered body, P denotes compaction pressure and “A” reflects the fact that the “as prepared” powder has been used as such in the sintering without calcination.]

The SSA pertaining to U<sub>C</sub>25A and U<sub>C</sub>100A were found to be 18 m<sup>2</sup>g<sup>-1</sup> and 6 m<sup>2</sup>g<sup>-1</sup> respectively. The  $\rho_G$  and  $\rho_S$  of the urania pellets (U<sub>C</sub>25A and U<sub>C</sub>100A), are presented in Figs 4.3a & 4.3b.

The  $\rho_G$  of all these urania pellets were found to increase linearly (from 45 to 60 % T. D) with the CP (60 to 180 MPa). When the CP was increased beyond 180 MPa and up to 353 MPa, this increase was less pronounced.

The  $\rho_S$  of U<sub>C</sub>100A were nearly independent of the CP (being constant at 75  $\pm$  5% T. D) while the  $\rho_S$  of U<sub>C</sub>25A exhibited a greater variability. The following trend was observed in the compaction experiments carried out with the U<sub>C</sub>25A powders. The  $\rho_S$  of U<sub>C</sub>25A remained constant at 60  $\pm$  5 % T. D between 60 and 180 MPa, increased sharply between 180 MPa and 320 MPa (90  $\pm$  2 % T. D) and then declined to 70  $\pm$  2 % T. D at 353 MPa. It must be noted that the sintering experiments carried out in this study are very different from those reported in section 3.10, the powders used here are the “as prepared” powders containing a high carbon residue not the “calcined” powders that are discussed in the former.

No evidence of cracks or other physical defects like layering, hour glassing and end capping was noticeable in these pellets (Fig. 4.4a & 4.4d). However, the variation in the shrinkage of these pellets with the CP exhibited a definite trend.

Murthy et al. [2] observed that UO<sub>2</sub> powders need to be compacted at a CP of about 250 – 275 MPa in order to get “defect free” sintered products. From the discussions presented in Chapter 3 (section 3. 11) it is evident that a critical compaction pressure of 180 MPa would best suit both U<sub>C</sub>25H and U<sub>C</sub>100H. However, the optimum pressure for **U<sub>C</sub>25A** and **U<sub>C</sub>100A** had to be experimentally optimized.



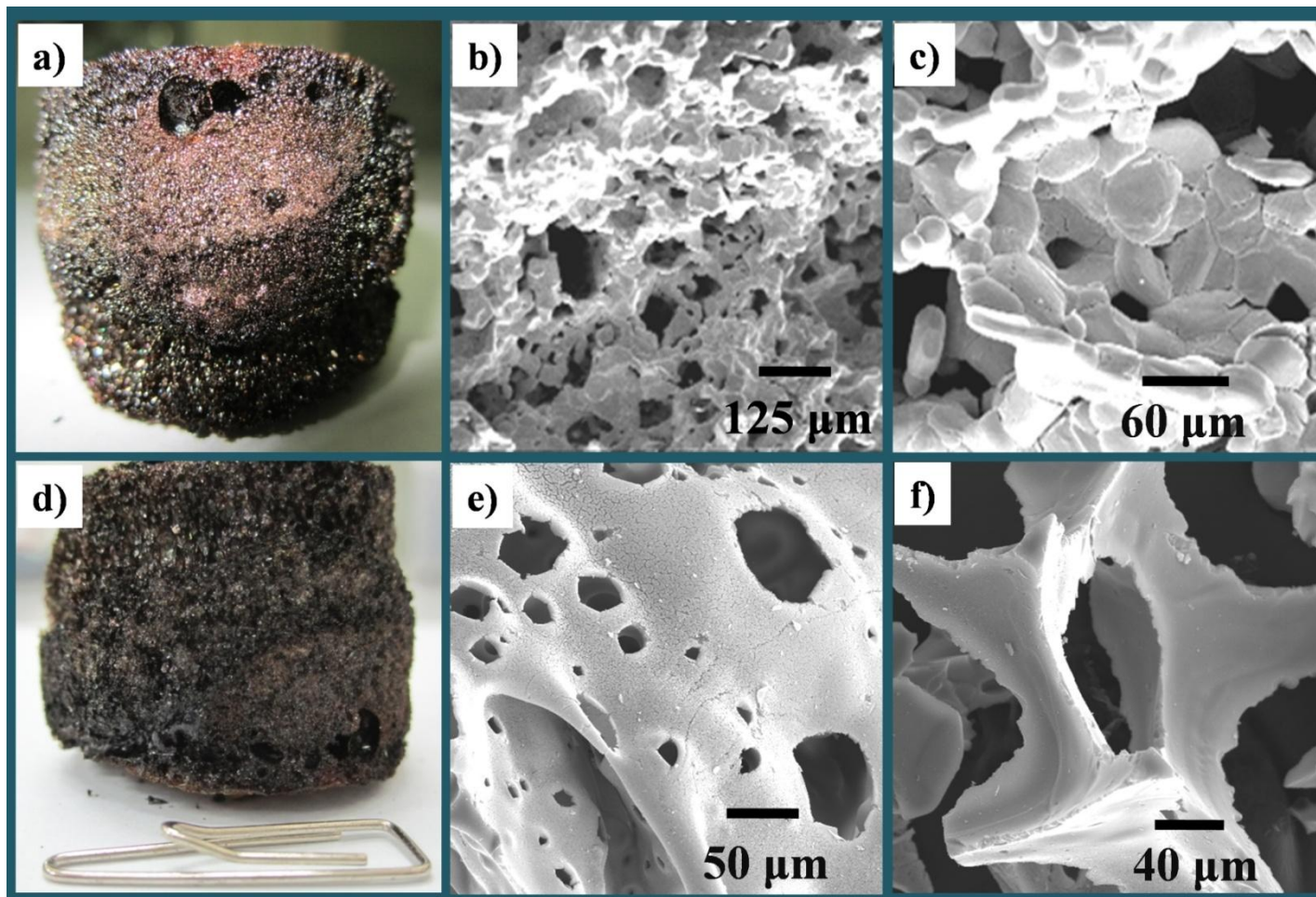


Figure 4.2 (a-c) Images of US240S: (a) Green foam (b-c) SEM images of sintered foam; (d-f) Images of US260S: (d) green foam, (e-f) SEM images of sintered foam

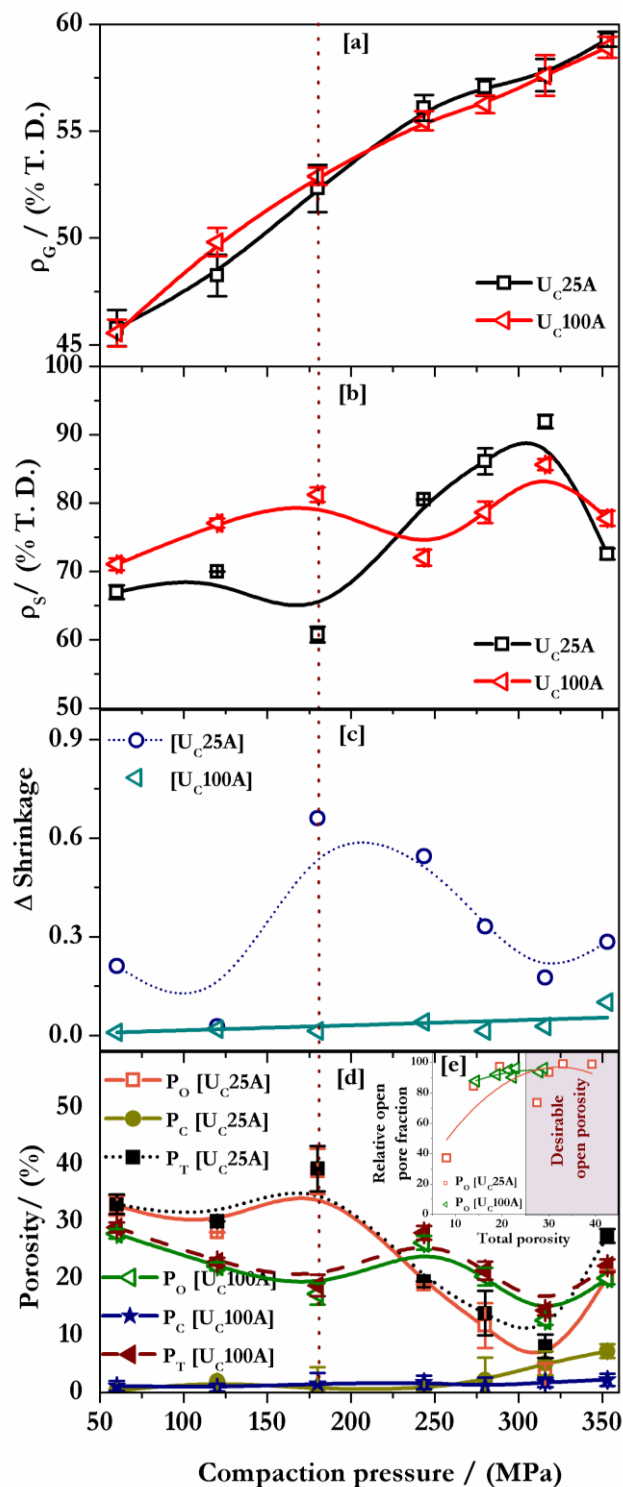


Figure 4.3 (a) Variation of  $\rho_G$  with CP; (b) variation of  $\rho_s$  with CP, (c) dependence of shrinkage ( $\Delta S$ ) on CP; (d) interdependence of open and closed porosity with CP and (e) interdependence of the volume fractions of open porosity with total porosity [Where:  $P_o$ ,  $P_c$  and  $P_T$  indicates open, closed and total porosity respectively; whereas the error bar shown in Fig (a-e) depict  $1\sigma$  (standard deviation)]

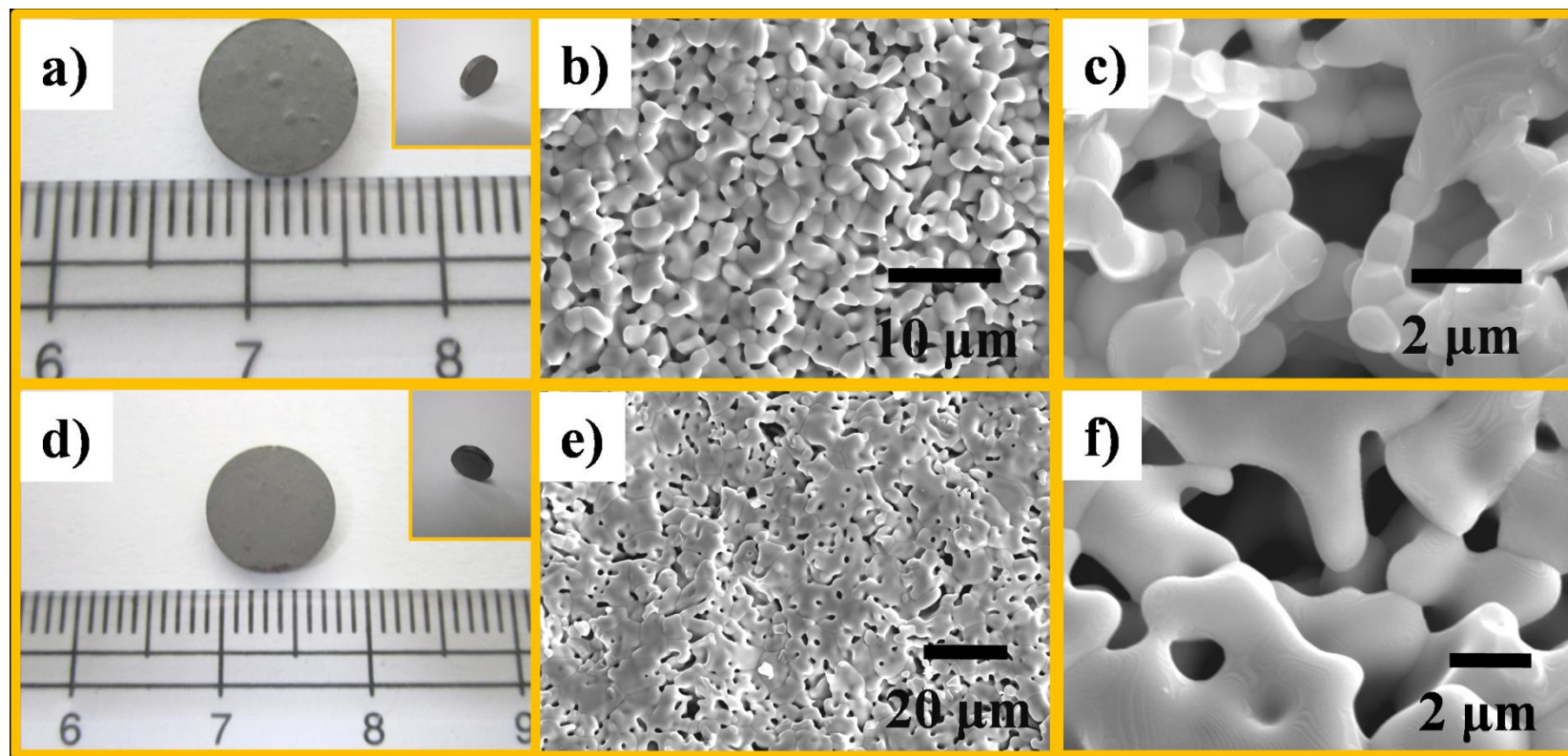


Figure 4.4 Images obtained with sintered  $UO_2$  pellets (180 MPa) derived from (a-c)  $U_{C25A}$  and (d-f)  $U_{C100A}$ : (a and d) Photograph showing porous sintered  $UO_2$  pellets; SEM images of (b and e) the sintered surfaces (c and f) fractured surface

**Table 4.1 Characteristics of the UO<sub>2</sub> foams and pellets**

Foam derived through sucrose gel precursor						Pellets derived through citrate gel precursor				
Sample	$\rho_B$ (g cm <sup>-3</sup> )	RC (wt %)	SSA (m <sup>2</sup> g <sup>-1</sup> )	Porosity (%)	Total specific pore volume (mm <sup>3</sup> g <sup>-1</sup> )	U <sub>C</sub> 25A			U <sub>C</sub> 100A	
						CP / MPa	Density (% T. D) <sup>#</sup>			
							$\rho_G$	$\rho_S$	$\rho_G$	$\rho_S$
US150S	0.51	20	1	94.5	211	60	45.8 ± 0.9	66.9 ± 1.0	45.6 ± 0.6	71.1 ± 0.9
US175S	0.45	26	14	94.8	140	120	48.4 ± 0.0	70.0 ± 0.0	49.8 ± 0.7	77.1 ± 0.7
US200S	0.38	27	18	95.6	130	180	52.3 ± 1.1	60.8 ± 1.2	52.9 ± 0.4	81.2 ± 1.1
US225S	0.28	29	19	96.7	229	243	56.1 ± 0.6	80.5 ± 0.0	55.5 ± 0.5	72.0 ± 1.2
US240S	0.24	30	33	97.1	170	280	57.1 ± 0.4	86.1 ± 0.9	56.3 ± 0.4	78.7 ± 1.5
US250S	0.12	31	127	98.5	593	317	57.6 ± 0.8	92.0 ± 0.0	57.7 ± 0.0	85.6 ± 0.8
US260S	0.10	33	199	98.8	723	353	59.3 ± 0.4	72.6 ± 0.8	58.9 ± 0.5	77.8 ± 1.1

<sup>#</sup> The values represent mean of five measurements

In order to compare the sintering behavior of  $U_{C25A}$  and  $U_{C100A}$  the dimensionless relative shrinkage parameter ( $\Delta S$ ) of these powders was considered. This parameter is defined as follows;  $\Delta S^* = \frac{AS-RS}{AS}$ . At the critical CP the value of  $\Delta S$  would be zero. For the  $U_{C100A}$  powder the value of  $\Delta S$  was found to be close to zero at all the CP employed in this study. However, in the case of  $U_{C25A}$  it was much higher than the corresponding values of  $\Delta S$  pertaining to  $U_{C100A}$  for CP between 180 and 320 MPa. This could be attributed to the non uniform density within the compacts made with  $U_{C25A}$ .  $\Delta S$  showed a progressive increase with the CP. It was however more pronounced in the case of  $U_{C25A}$ . However, the  $\Delta S$  of the pellets made from  $U_{C25A}$  at CP below 180 MPa and above 320 MPa followed a trend similar to that exhibited by  $U_{C100A}$ , indicating that at these CP, distribution of density within the  $U_{C25A}$  compacts is rather uniform. To minimize the defects in the green compact, it is desirable to choose the minimum pressure [2] adequate to yield a good green compact. Hence, the pressure of 180 MPa would be well suited for compacting  $U_{C25A}$  powders.

From the data presented in Fig. 4.3a – 4.3e, it is clear that  $U_{C25A}$  powders yield a product with a higher porosity as compared to  $U_{C100A}$  at CP below 180 MPa. It is evident that open pores form a significant fraction of the total porosity and that the former increases with the total porosity (Fig. 4.3e). When the total porosity is more than 30 % (i.e.  $\rho_s = 70$  % T.D) the relative fraction of open porosity is above 90%.

In view of the above, 180 MPa is the optimum pressure suitable to compact the powder  $U_{C25A}$ . Even though the pellets derived from  $U_{C100A}$  exhibit uniform sinterability, the pellets made out of  $U_{C25A}$  possess more open porosity and are hence, more desirable. The microstructures (Fig 4.4b-c & Fig. 4.4e-f) reveal that these samples contain interconnected pores

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\* The shrinkage values reported here cannot be compared with those mentioned in section 3.11, because these pellets were made from the  $U_{C25A}$  powders and not from the  $U_{C25H}$  powders

which are typically a few micrometers in size. From the foregoing it is evident that U<sub>C</sub>25A would be well suited for the DOR process.

#### **4.4 Conclusions from the studies on foam and porous pellets of nc-UO<sub>2</sub>**

UO<sub>2</sub> foam was successfully prepared for the first time by using a sucrose-gel precursor. This comprised both meso and macro pores and possessed sufficient crush strength. However, the presence of large amounts of carbon residue would limit its utility for the intended application, viz., DOR, owing to the electronic conductivity brought about by carbon. Typically 30 to 40% porosity would be ideal for the DOR process. However, the densities of these foams are far lower than the optimum value suitable for the end use.

Porous urania pellets were successfully obtained for the first time from nc-urania powders obtained through citrate gel-combustion method. A fuel to oxidant ratio (R) of 0.25, a CP of 180 MPa and a TSS<sub>3</sub> (Sintering schedule (Table 2.3)) with a maximum temperature of 1473 K were found to be the optimum conditions for obtaining a product with a desirable density of about 60 to 70 % T. D.

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## Chapter 5

# *Synthesis, Characterization and Sintering of Nanocrystalline Thoria*

*This chapter deals with bulk synthesis of nc-ThO<sub>2</sub> by using citrate gel-combustion method. The nc-ThO<sub>2</sub> powders were compacted at different pressures and were sintered by using the “two-step sintering” method. The microstructural investigations on nc-ThO<sub>2</sub> powders were carried out by using both SEM and TEM.*

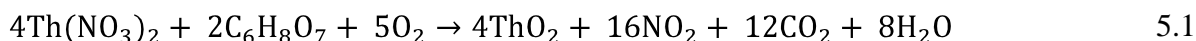
### 5.1 Assay of starting material

Nuclear grade thorium nitrate crystals were used in this study. ICPMS analysis of thorium nitrate was carried out and the impurities present are given in Table 5.1. Since, the impurities present are insignificantly low, it is reasonable to conclude that their presence would not alter the gel-combustion synthesis as well as the sinterability of the powders.

### 5.2 Citrate gel-combustion synthesis

Nc-ThO<sub>2</sub> was prepared through citrate gel-combustion with a view to observe “volume combustion” in Th<sup>4+</sup> ion containing gels as well as to re-establish the systematic dependence of powder properties on R. During the gel-combustion synthesis of nc-ThO<sub>2</sub>, a white precipitate was formed and upon continued heating of the starting mixture it got re-dissolved subsequently. The white precipitate was probably due to the formation of thorium citrate [1, 2]. Upon heating, these mixtures underwent precipitation, re-dissolution of the precipitate, dehydration, gelation and decomposition (combustion reaction). All these reactions took place in an open glass bowl. No attempt was made to measure the reaction temperature. Among all the mixtures used, those with R = 0.125 and 0.17 were found to undergo a “vigorous” and “moderate volume combustion

reaction” respectively while those mixtures with R values of 0.25 and 0.50 exhibited auto-ignition that ensued with smoldering. Earlier, Chandramouli et al. [1] had reported the citrate gel-combustion synthesis of nc-ThO<sub>2</sub> with R values ranging from 0.31 to 1.27. These authors did not observe “volume combustion” in the citrate gel-combustion of nc-ThO<sub>2</sub>. Since, these authors [1] had used mixtures with a higher R value beyond the stoichiometric ratio (R = 0.125) for VCR, these authors could not observe VCR. In this study, the value of R was varied between 0 and 0.50. However, we observed for the first time that “volume combustion reaction (VCS)” [3] in the citrate gel-combustion synthesis of thoria takes place in mixtures with R = 0.125.



### 5.3 Thermal analysis and evolved gas analysis of gel-combustion reaction

The thermogram, DTA curve, DSC curves as well as the evolved gas analysis pertaining to the pyrolysis of citrate gels containing Th<sup>4+</sup> (R = 0.50) are presented in Fig. 5.1. The thermogravimetric curve (R = 0.50) shows three mass loss steps; their onset temperatures being 398 K, 438 K and 609 K respectively. The DSC curve of this mixture (R = 0.50) shows an endothermic peak at 398 K and three exothermic peaks at 438 K, 624 K and 659 K. Evolved gas analysis of this mixture (R = 0.50) revealed the evolution of water at 396 K and 438 K. The first peak could be ascribed to the dehydration of the gel (onset 396 K), while the other peak could be due to the pyrolysis of this gel (438 K). These observations were further substantiated by both the DSC and evolved gas analyses. The latter showed that loss of water begins at 398 K and the liberation of other gases (NO, NO<sub>2</sub>, CO and CO<sub>2</sub>) sets in at 418 K. So far evolved gas analysis of the combustion of Th<sup>4+</sup> containing citrate gels had not been reported. In addition, it is also observed that H<sub>2</sub>O (g), O (g), NO (g), NO<sub>2</sub> (g), CO (g) and CO<sub>2</sub> (g) evolve at 434 K close to the exothermic peak observed in the DSC curve (438 K). These observations confirm that this gel



undergoes dehydration followed by the combustion reaction. The exothermic peak (438 K) in the DSC curve shows a minor hump that could not be resolved further. This could be attributed to simultaneous reactions. Further it is observed that in the combustion of  $\text{Th}^{4+}$  containing gels  $\text{N}_2$  gas is not liberated. This is a new observation and is at variance with the general reaction proposed in the literature [4].

At still higher temperatures the thermogravimetric curve and the DSC curves show a weight loss (609 K onset) and two exothermic peaks (624 K and 659 K) respectively. The evolved gas analysis reveals the liberation of  $\text{H}_2\text{O}$  (g), O (g), CO (g) and  $\text{CO}_2$  (g) at 619 K and CO (g) and  $\text{CO}_2$  (g) at 658 K. These emanate from the combustion of the carbonaceous residue. It is interesting to note that a reduction in the  $\text{O}_2$  availability is testified by the mass spectrum pertaining to  $\text{O}_2$  at 424 K and 605 K. Probably,  $\text{O}_2$  available in the ambience is consumed by the combusting mass. From the foregoing discussion it is clear that the the citrate gel-combustion synthesis of thoria is completed within 500 K and the subsequent reactions pertain to the combustion of the unburnt residue.

## **5.4 Characterization of the powders**

### **5.4.1 Bulk density ( $\rho_B$ ), PSD and SSA**

The  $\rho_B$  of all the  $\text{T}_\text{C}\text{XXA}$  powders were lower compared to that of the  $\text{T}_\text{C}\text{XXC}$  powders (Table 5.2 & Fig. 5.2a). These were found to vary from 1.0 – 7.4 % T.D and 1.2 – 8.3 % T.D respectively. The powders derived from the simple denitration possessed a  $\rho_B$  of 18.5 % T.D ( $\text{T}_\text{C}\text{XXA}$ ) and 32.1 % T.D ( $\text{T}_\text{C}\text{XXC}$ ). The thoria powders ( $\text{T}_\text{C}13\text{A}$ ) derived through VCR were found to be highly porous. This powder exhibited the lowest  $\rho_B$  (1.0 % T.D).

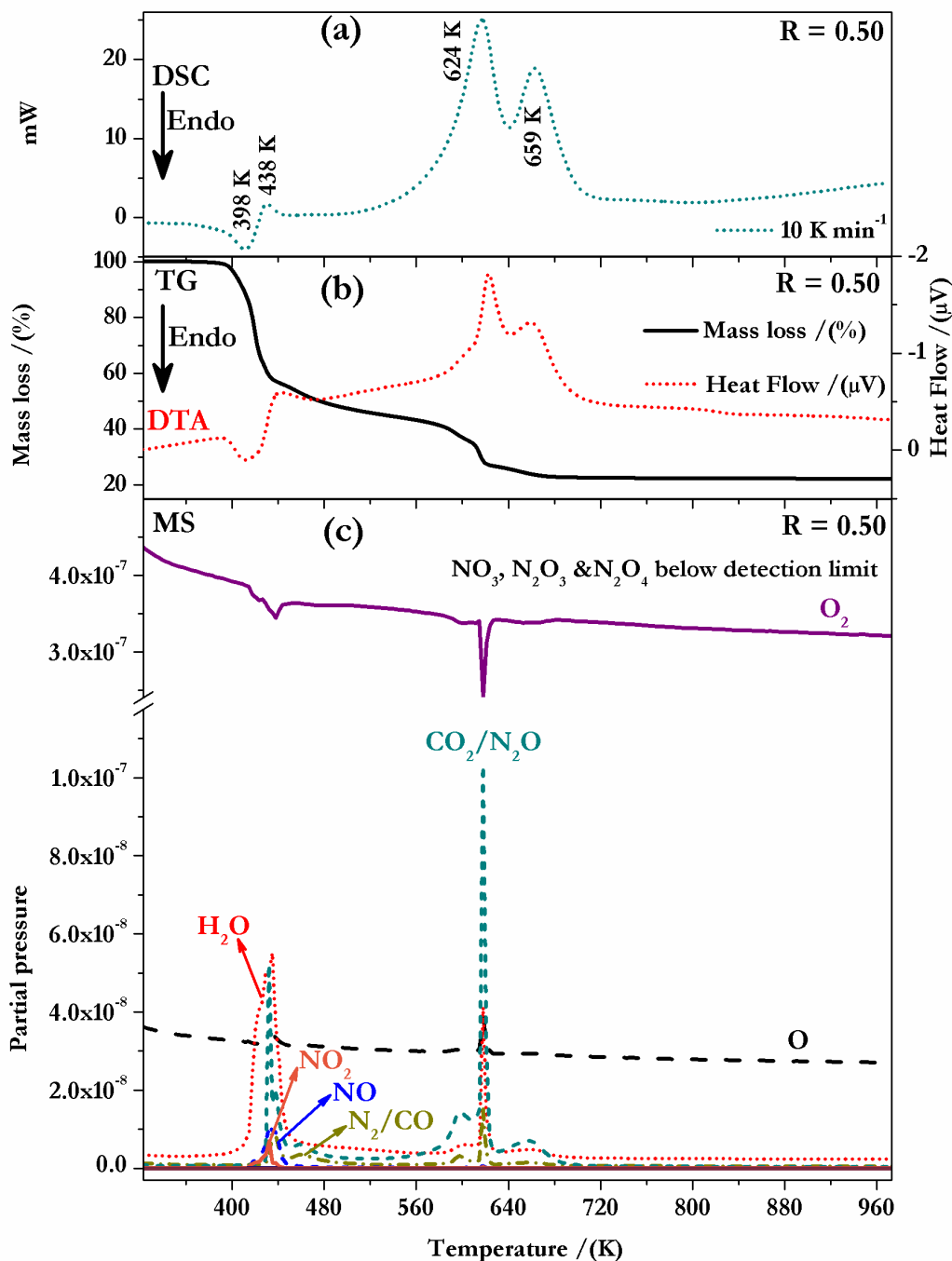


Figure 5.1 Thermal decomposition in a mixture with an  $R$  value 0.50 in  $O_2$  atmosphere with  $10\text{ K min}^{-1}$  heating rate by using (a) DSC (b) TG-DTA and (c) evolved gas analysis

Very much like nc-urania (Chapter 3) and nc-yttria (Chapter 6) obtained through volume combustion, nc- $ThO_2$  also exhibited lowest  $\rho_B$ . Ananthasivan et al. [5] had reported that the  $\rho_B$  of thoria powders derived through oxalate de-agglomeration was varying between 11.0 % T.D to

18.3 % T.D. Pope and Radford [6] found that the  $\rho_B$  of thoria powders prepared through precipitation and denitration were 10.0 % and 25.0 % T.D respectively. Thus, it is evident that the  $\rho_B$  of nc-ThO<sub>2</sub> powders prepared in this study through citrate gel-combustion are lower than those reported earlier [5, 6].

**Table 5.1 Impurities in the thorium nitrate (ICP-MS)**

Elements	Co	Mn	Mo	Ba	Al	Sr	Ti	Pb	Cr	Zn	Fe	Cu	V	Ni	Mg
Concentration of Impurities /ppm	<20	14	15	51	< 16	16	<20	<15	<17	<15	25	<25	<18	<17	6

**Table 5.2 Characteristics of the nc-ThO<sub>2</sub> powder synthesized by “gel-combustion”**

Sample	Mole ratio (R)	$\rho_B$ % T. D <sup>*</sup>		RC <sup>1</sup> (ppm)		SSA <sup>1</sup> (m <sup>2</sup> g <sup>-1</sup> )	
		A	C	A	C	A	C
T00	0	18.5	32.1	137	105	27	16
T <sub>C</sub> 5.5	0.055	2.9	3.0	1206	560	34	18
T <sub>C</sub> 13	0.125	1.0	1.2	1528	537	37	24
T <sub>C</sub> 17	0.166	1.5	1.8	1553	425	25	17
T <sub>C</sub> 25	0.250	2.3	3.5	1591	323	20	15
T <sub>C</sub> 50	0.500	7.4	8.3	1501	568	21	16

<sup>1</sup>and <sup>\*</sup> - averaged of three and five independent measurements

SSA of the nc-ThO<sub>2</sub> powders prepared in this study is presented in Fig. 5.2b and in Table 5.2. It is observed that the SSA of T<sub>C</sub>XXA powders is higher than that of T<sub>C</sub>XXC powders. T<sub>C</sub>13A and T<sub>C</sub>13C which were derived through volume combustion reaction exhibited the highest SSA of 37 m<sup>2</sup> g<sup>-1</sup> and 24 m<sup>2</sup> g<sup>-1</sup> respectively. Rest of the powders were found to have a SSA of about 16 m<sup>2</sup> g<sup>-1</sup>. Chandramouli et al. [1] had reported the dependence of SSA of citrate gel-combustion derived nc-ThO<sub>2</sub> on the value of R. The values of SSA of the powders obtained

from mixtures with different “R” reported by these authors are as follows; a) hot plate ( $R = 0.64 \text{ m}^2 \text{ g}^{-1}$  to  $1.01 \text{ m}^2 \text{ g}^{-1}$ ,  $\text{SSA} = 14.93 \text{ m}^2 \text{ g}^{-1}$  to  $15.18 \text{ m}^2 \text{ g}^{-1}$ ) and b) microwave heating ( $R = 0.31 - 1.27$ ,  $\text{SSA} = 9.92 - 15.18 \text{ m}^2 \text{ g}^{-1}$ ). SSA of thoria powders reported by other authors is presented in Table 5.3.

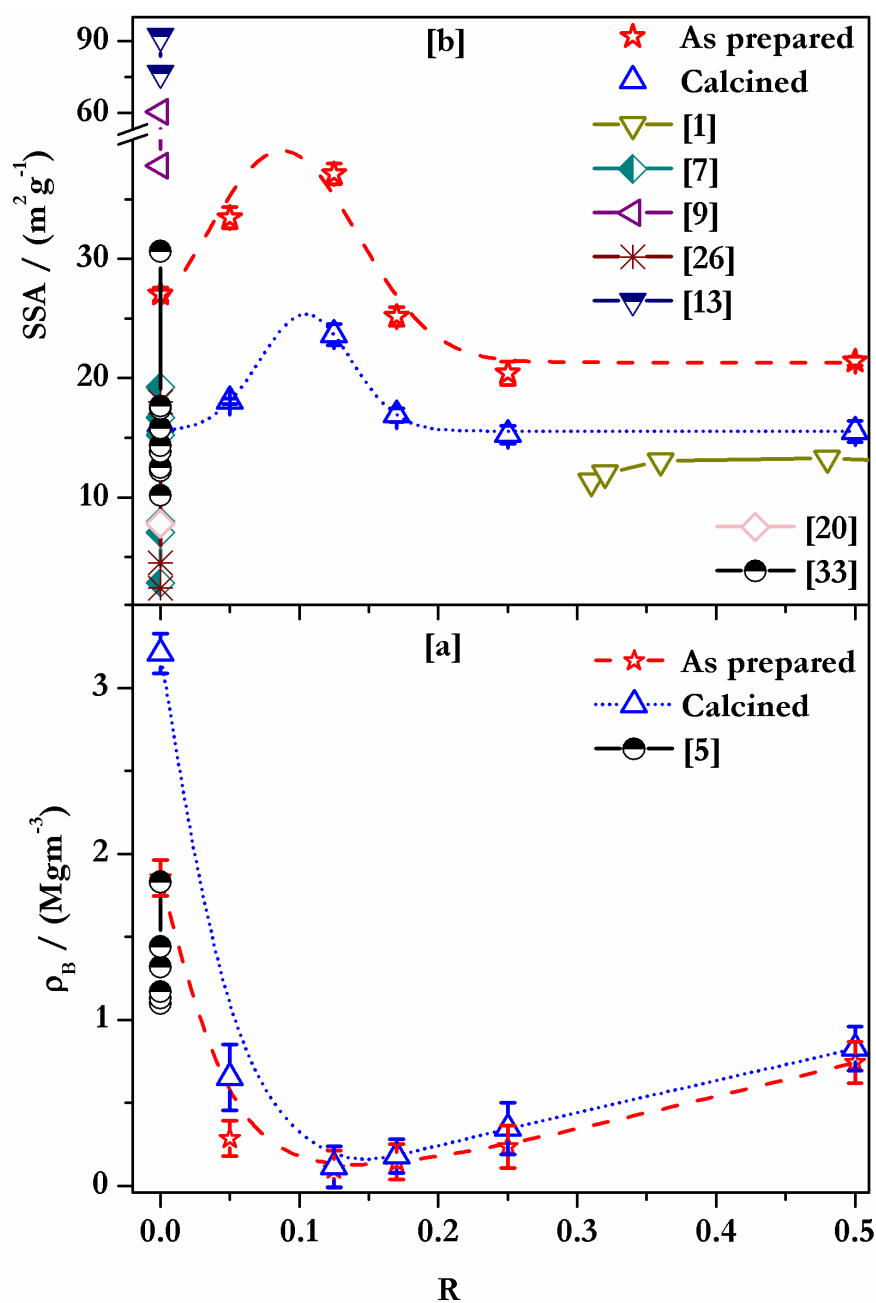


Figure 5. 2 Dependence of (a)  $\rho_B$  of the nc-ThO<sub>2</sub> powder and (b) SSA of the nc-ThO<sub>2</sub> powder on the value of R [14, 15, 24, 26-28, 40]

It should be noted that in the BET analysis, reliable values of SSA could be obtained only when the quantity of the powder sample taken for investigation is about half a gram or more. Also, representative sampling from the bulk has to be ensured. In view of the above, and the fact that we measured SSA values by using sufficient quantity of the sample (about 1g), our results are reliable.

**Table 5. 3 Comparison of RC and SSA of thoria powders reported in the literature**

Ref.	Method	RC	SSA (m <sup>2</sup> g <sup>-1</sup> )	Quantity / Batch size
[7]	Th-Ox	20 – 1400 ppm	2.84 – 19.25	-
[5, 8]	Th-Ox (deagglomeration)	1000 – 1800 ppm	12.8 – 19.8	≈ 25 g
[9]	Hydrothermal	-	-	0.114 g
[10]	Th-Ox	873 K; 1h	1.9 wt % (as CO <sub>3</sub> <sup>2-</sup> )	-
		873 K; 2h	1.6 wt % (as CO <sub>3</sub> <sup>2-</sup> )	
		973 K; 2h	1.0 wt % (as CO <sub>3</sub> <sup>2-</sup> )	
		1073 K; 2h	0.5 wt % (as CO <sub>3</sub> <sup>2-</sup> )	
[11]	Glycine GC	0.3 – 0.4 wt %	53 – 90	-
[12]	PIR	≤ 0.3 %	7.8	-
[13]	electro-deposition	-	76.6 – 92.1	-

*Th-Ox – thorium oxalate; GC – gel combustion and PIR- photo chemically induced reaction*

In order to understand the packing and compaction behavior of the powders it is useful to investigate the dependence of size distribution of particles on the bulk density and SSA in the powders T<sub>C</sub>XXA and “T<sub>C</sub>XXC. The size distribution of particles in T<sub>C</sub>XXA and T<sub>C</sub>XXC powders are presented in Table 5.4 and in Fig. 5.3. The size distribution histograms were deconvoluted to delineate the contribution from different size fractions. The thick solid lines depict the experimentally observed particles while the thin solid lines depict the deconvoluted curves. It was observed that the size distribution of particles in T<sub>C</sub>XXA exhibited both unimodal and bimodal size distributions while T<sub>C</sub>XXC powders exhibited bimodal and trimodal size distribution of particles. It was observed that the T00A powders had the highest ρ<sub>B</sub> while T<sub>C</sub>13A had the lowest. T<sub>C</sub>5.5A, T<sub>C</sub>17A, T<sub>C</sub>25A and T<sub>C</sub>50A have moderately higher ρ<sub>B</sub> than T<sub>C</sub>13A.

The following general trends are discernible. T<sub>C</sub>5.5C, T<sub>C</sub>13C and T<sub>C</sub>17C have markedly higher SSA than T00C, T<sub>C</sub>25C and T<sub>C</sub>50C. Probably the former set of powders possesses a higher fraction of pores. Among the first set the following trend was discernible:  $\rho_{B(TC5.5C)} > \rho_{B(TC17C)} > \rho_{B(TC13C)}$ . This trend positively correlates with the fraction of heavier particles present in the powders. A similar trend is also observed among the other powders i.e.,  $\rho_{B(T00C)} > \rho_{B(TC50C)} > \rho_{B(TC25C)}$ . Nc-ThO<sub>2</sub> powders derived through oxalate deagglomeration method had exhibited multimodal size distribution of particles with their size ranging from 0.1  $\mu\text{m}$  to 1000  $\mu\text{m}$ . Rahaman et al. [14] had reported that the powders with variable size distribution of particles would undergo abnormal sintering leading to differential densification and a defective product. It is reported that the differential densification [14-16] could be averted by employing powders with near unimodal size distribution of particles. From the results presented above, it is evident that the powders derived with R values 0.125 and 0.17 are likely to undergo better densification as compared to other thoria powders prepared in this study.

**Table 5.4 Particle size distribution in thoria powders**

Sample	Particle size distribution (vol %)					
	10 vol. % of sample has size less than ( $\mu\text{m}$ )		50 vol. % of sample has size less than ( $\mu\text{m}$ )		90 vol. % of sample has size less than ( $\mu\text{m}$ )	
	A	C	A	C	A	C
T00	2	14	22	66	69	158
T <sub>C</sub> 5.5	4	10	23	67	89	266
T <sub>C</sub> 13	8	12	38	125	143	415
T <sub>C</sub> 17	15	8	111	106	371	480
T <sub>C</sub> 25	11	4	102	25	364	168
T <sub>C</sub> 50	11	10	76	65	304	241

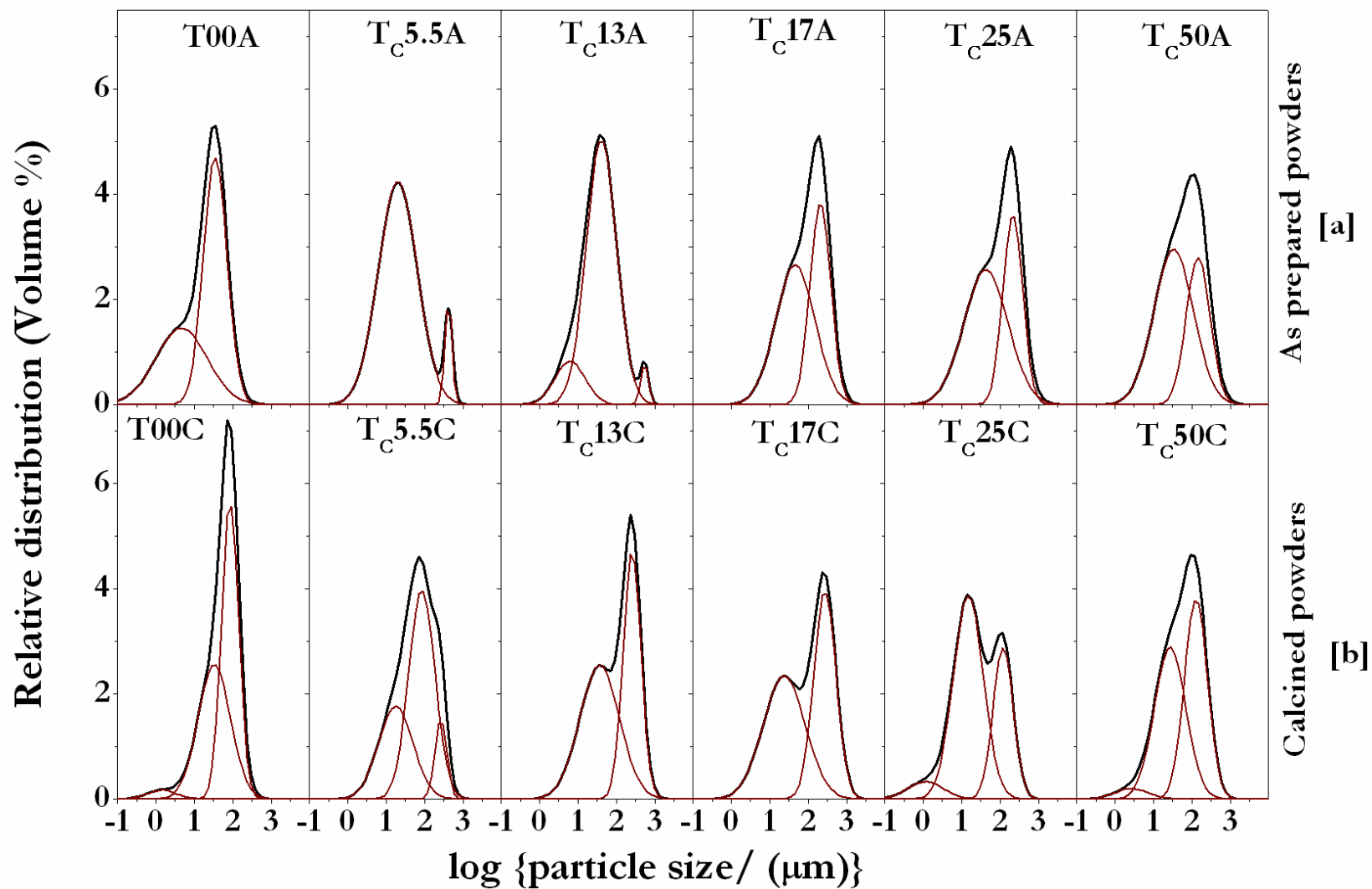


Figure 5.3 Size distribution of particles in the (a) “A” and (b) “C” nc-ThO<sub>2</sub> powders prepared by using citrate gel-combustion method [thick solid line – experimental curve and thin solid line – deconvoluted curve]

### 5.4.2 Residual Carbon

Carbon residue present in the T<sub>C</sub>XXA and T<sub>C</sub>XXC powders was found to vary between 137 and 1591 ppm and 105 and 568 ppm respectively (Table 5.2). As expected, the thoria powders prepared by direct denitration were found to contain minimum carbon residue. From the data presented in Table 5.2 it is evident that the nc-ThO<sub>2</sub> powders (calcined) prepared in this study were found to contain much lower carbon residue as compared to the methods reported in the literature [5, 7, 8, 10-12]. Carbon residue in sintered thoria pellets (selected samples) were found to vary between 70 to 150 ppm.

### 5.4.3 Phase characterization, XCS, lattice strain and stoichiometry

The XRD patterns of thoria powders (T<sub>C</sub>XXA and T<sub>C</sub>XXC) are presented in Figs. 5.4. The measured values of XCS (Sc [17] and HW [17]) and lattice strain are presented in Table 5.5 and in Fig. 5.5. The crystallite sizes of the T<sub>C</sub>XXA thoria powders were found to be 4 – 9 nm (Sc) and 5 - 10 (HW) while that of the T<sub>C</sub>XXC powders were found to be between 14 & 19 nm (Sc) and 17 & 22 nm (HW). In all these powders XCS shows nearly uniform change upon calcination. The XCS of both these powders exhibited a very weak dependence on the value of “R”. The lattice strain however showed a significant linear dependence on “R” (Fig. 5.5), especially in the T<sub>C</sub>XXA powders, similar to the observations made on nc-UO<sub>2</sub> (Chapter 3). Many authors had investigated [1, 5, 10-13, 18-20] the XCS of nc-ThO<sub>2</sub> the details of which are presented in Table 5.5. However, no systematic correlation between XCS and lattice strain has been reported so far. From the data presented in Table 5.5 it is evident that thoria derived ex-oxalate exhibits the lowest XCS and gel-combustion derived thoria exhibit XCS in the range 5-20 nm. Our TEM data (Figs. 5.6-5.7) testifies the mean XCS values obtained through the HW analysis of the XRD data.



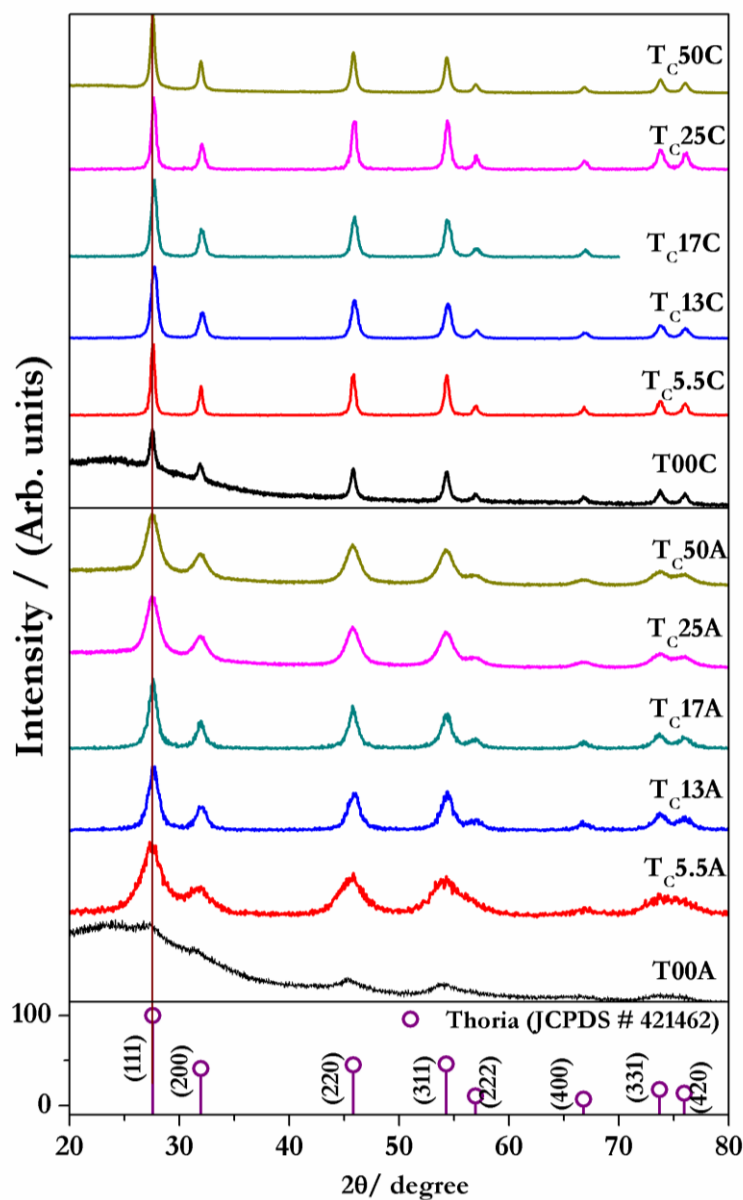


Figure 5.4 XRD pattern of the “A” and “C” nc-ThO<sub>2</sub> powders derived through citrate gel-combustion method

The dimensionless lattice strain of T<sub>C</sub>XXA powders measured by using HW method was found to be higher than that of T<sub>C</sub>XXC powders (Figs. 5.5b & 5.5c). This observation is in line with our earlier results on nc-UO<sub>2</sub> powders [Chapter 3]. However, in general, it is observed that the dimensionless lattice strain in the T<sub>C</sub>XXA powders is higher than that of the thorium powders obtained through precipitation method [10].

**Table 5.5 XCS and lattice strain of nc-ThO<sub>2</sub> powders measured in this study along with those reported in the literature**

Sample	X-ray Crystallite size						TEM A (nm)	Ref.	Sc	HW	TEM	
									(nm)	(nm)	(nm)	
	A			C					HP	5	-	-
									MW	11	-	-
	Sc	HW	Strain x 10 <sup>-3</sup>	Sc	HW	Strain x 10 <sup>-3</sup>			[18]	20.1 – 43.2	-	-
(nm)	(nm)		(nm)	(nm)			[10]	5 - 34	-	-		
T0	4	-	-	17	18	0.55	-	[5]	2.2 – 19.3	10 - 11	5-10	
T <sub>C</sub> 5.5	4	7	3.01	19	22	0.67	-	[19]	6	-	-	
T <sub>C</sub> 13	8	9	4.87	14	15	0.14	11 - 25	[11]	53 & 90	-	-	
T <sub>C</sub> 17	9	10	6.71	16	22	2.14	6 - 16	[20]	27	23	12	
T <sub>C</sub> 25	4	5	2.00	16	17	0.45	-	[12]	4.6	-	-	
T <sub>C</sub> 50	5	6	1.69	17	19	0.60	-	[13]	30	-	10 - 30	

*Ref. – References; HP-hot plate heating and MW-microwave mode of heating*

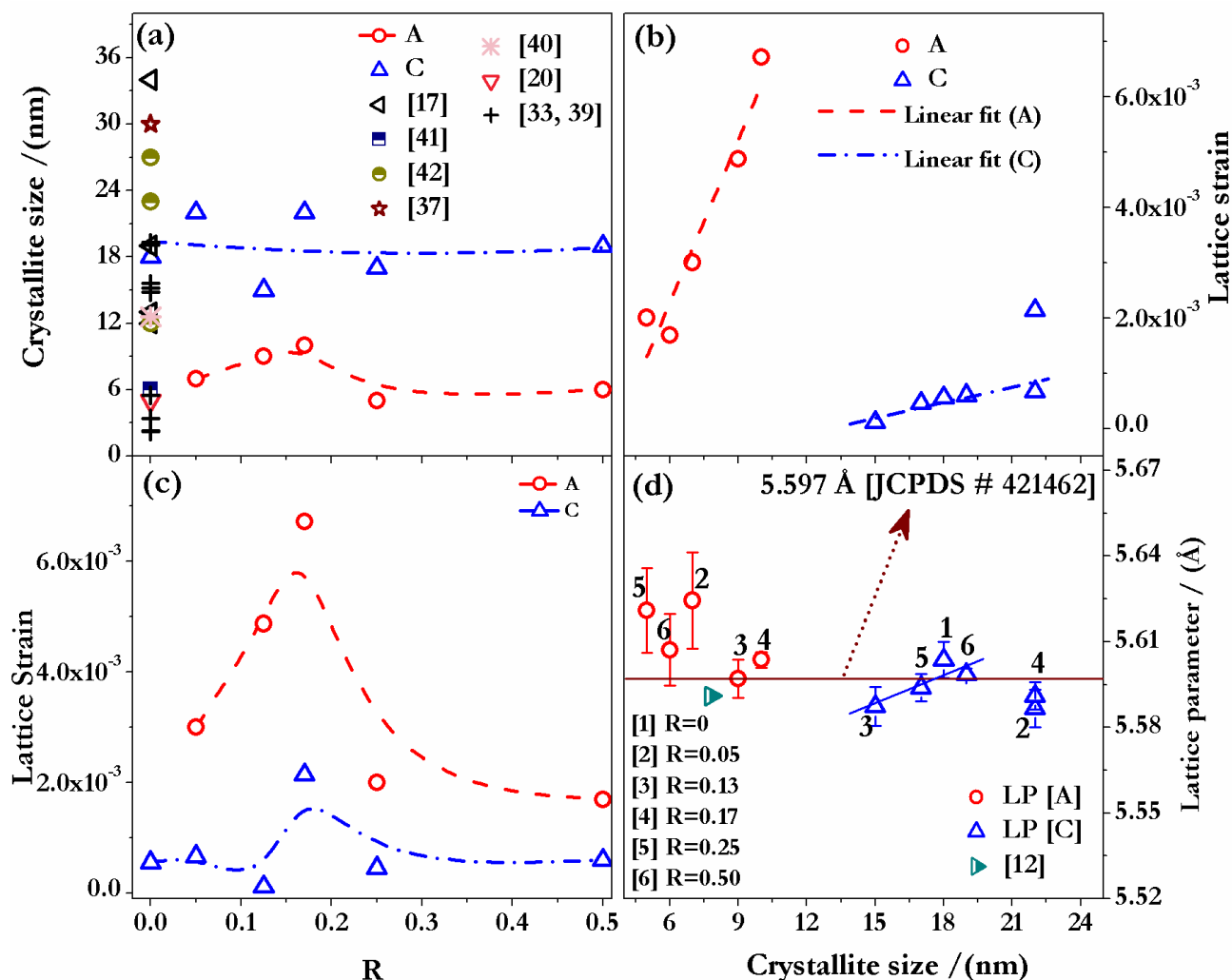


Figure 5.5 (a) Dependence of the XCS (HW method) on R values; (b) variation of lattice strain in crystallites with R values; (c) variation of lattice strain with XCS in “as prepared (A)” and “calcined (C)” thoria powders and (d) variation of the lattice parameter with XCS in nc “A” and “C” thoria powders

The combustion reaction is a self propagating fast reaction, which accentuates the formation of nanocrystallites with a higher lattice strain. However, this lattice strain gets annulled upon calcination (1073 K). The measured values of lattice strain in the  $T_CXXA$  and  $T_CXXC$  powders (Table 5.5) further support this premise. The lattice strain in the powders derived through volume combustion ( $T_C17A$  and  $T_C17C$ ) was found to be the highest. This is due to the rapid formation of crystallite during the combustion of the mixtures with  $R = 0.125$  and  $0.25$ , which not only

disperses the product but also does not allow sufficient time for grain coarsening / annealing of strain.

The lattice parameter (LP) of the thoria powders prepared in this study was computed from their respective X-ray diffractograms. The LP of T<sub>C</sub>XXA powders were higher than that of T<sub>C</sub>XXC powders (Fig. 5.5d). Further, it was observed that the LP approaches the value cited in JCPDS No. 00-42-1462 (5.597 Å) for powders with XCS 17 nm or more.

High resolution TEM images did not reveal any lattice defects. EELS analysis was also carried on T<sub>C</sub>13A and T<sub>C</sub>17A samples (Fig. 5.8). The O-K and N<sub>4,5</sub> ( $4d \rightarrow 5f$ ) edges are presented in Fig. 5.8. Selection rule states that  $d_{3/2}$  electrons can only be excited to empty  $f_{5/2}$  level which means the relative occupation of  $5f_{5/2}$  and  $5f_{7/2}$  could be calculated by measuring the area beneath N4 ( $4d_{3/2} \rightarrow 5f_{5/2}$ ) and N5 ( $4d_{5/2} \rightarrow 5f_{5/2}, 5f_{7/2}$ ) peak [21, 22]. The branching ratio [ $B = A_{5/2} / (A_{3/2} + A_{5/2})$ ], where  $A_{3/2}$  and  $A_{5/2}$  denotes areas within  $4d_{3/2}$  and  $4d_{5/2}$  peaks [21, 22] corresponding to the N4 and N5 edges of T<sub>C</sub>13A and T<sub>C</sub>13C were measured from the background corrected spectra. The values of B pertaining to T<sub>C</sub>13A and T<sub>C</sub>13C powders are 0.5786 and 0.5608. Increase in the integrated area of N4 edge had led to decrease in B value in calcined thoria powders. The measured peak maxima pertaining to N4 and N5 edges are comparable to the values reported earlier [21, 22] for pure Th metal. This corresponds to an oxidation state of (IV). Hence it is reasonable to conclude that the EEL spectrum did not show any evidence for the presence of Th ions in oxidation states other than (IV). Pavelkova et al. [12] had reported the LP of 5.591 Å for the nc-ThO<sub>2</sub> powders with an XCS of 7.8 nm. While Tyrpekl et al. [10] had reported the LP of 5.6006 Å (293 K) for the nc-ThO<sub>2</sub> powders. However, so far no confirmatory evidence has been presented to substantiate the origin of substoichiometry in the oxygen sublattice of this oxide.

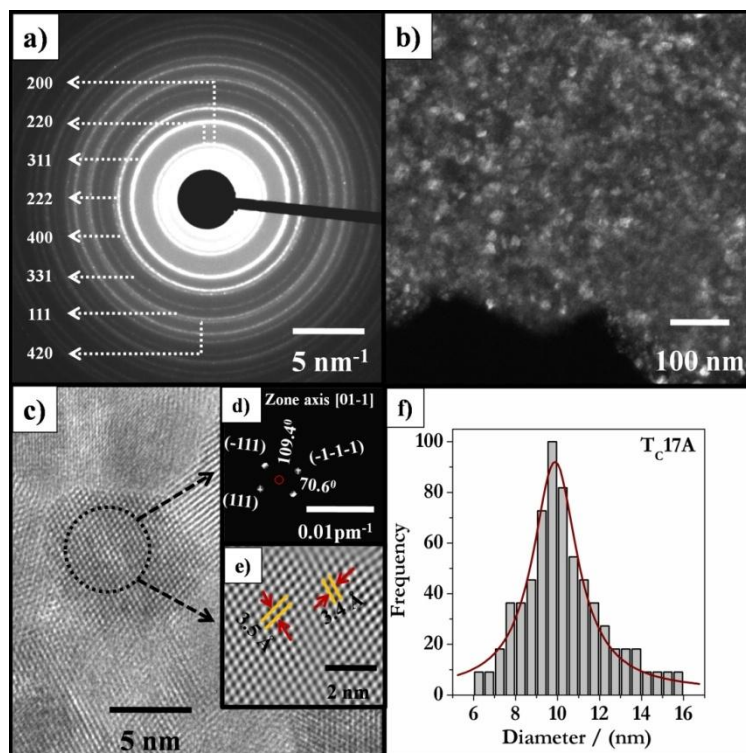


Figure 5.6 TEM images of  $T_{C17A}$  powders; (a) SAED image; (b) bright field image; (c) HRTEM image of a nanograin; (d-e) FFT and filtered IFFT image revealing zone axis  $[01-1]$  and (f) grain size distribution

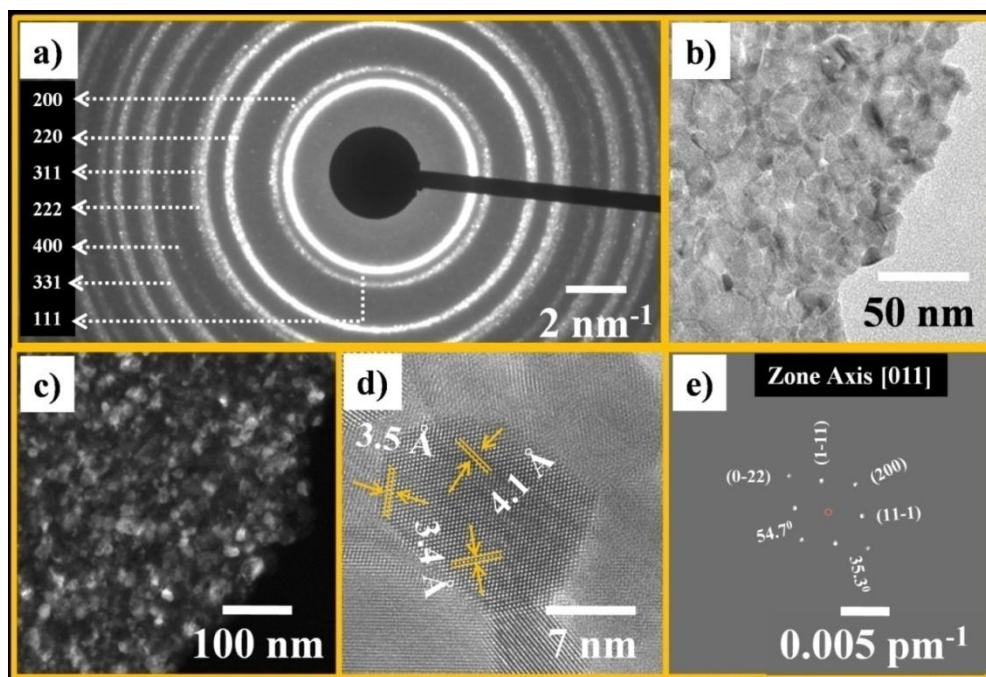


Figure 5.7 TEM images of  $T_{C13A}$  ( $ThO_2$ ) powders: (a) SAED image; (b-d) bright field, dark field image and HRTEM image of nano grain and (e) FFT image with the zone axis  $[011]$

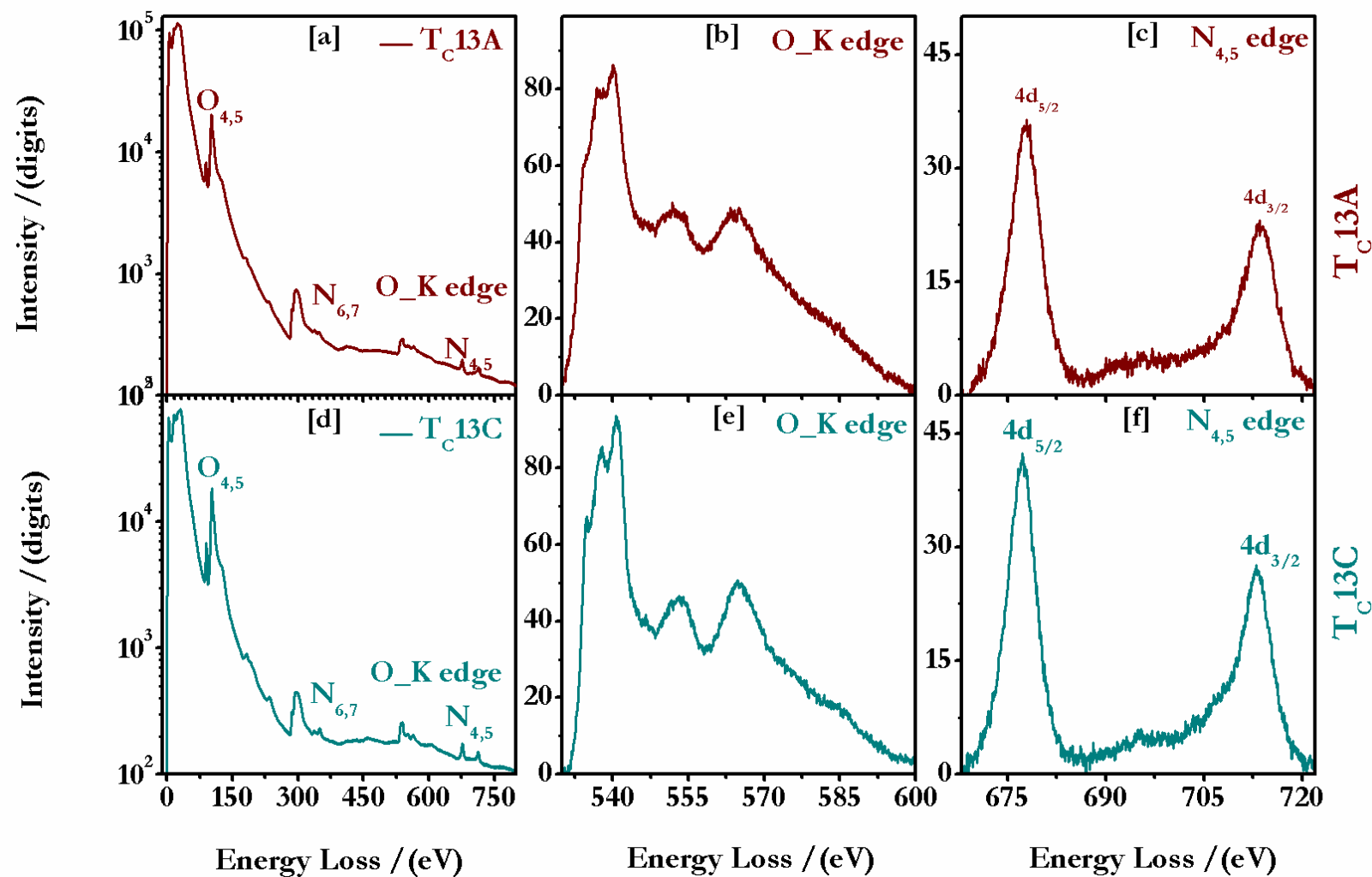


Figure 5. 8 EELS of  $T_{C13A}$  and  $T_{C13C}$  depicting (a & d) background corrected full spectra; (b & e) O-K edges and (c & f)  $N_{4,5}$  ( $4d \rightarrow 5f$ ) edges

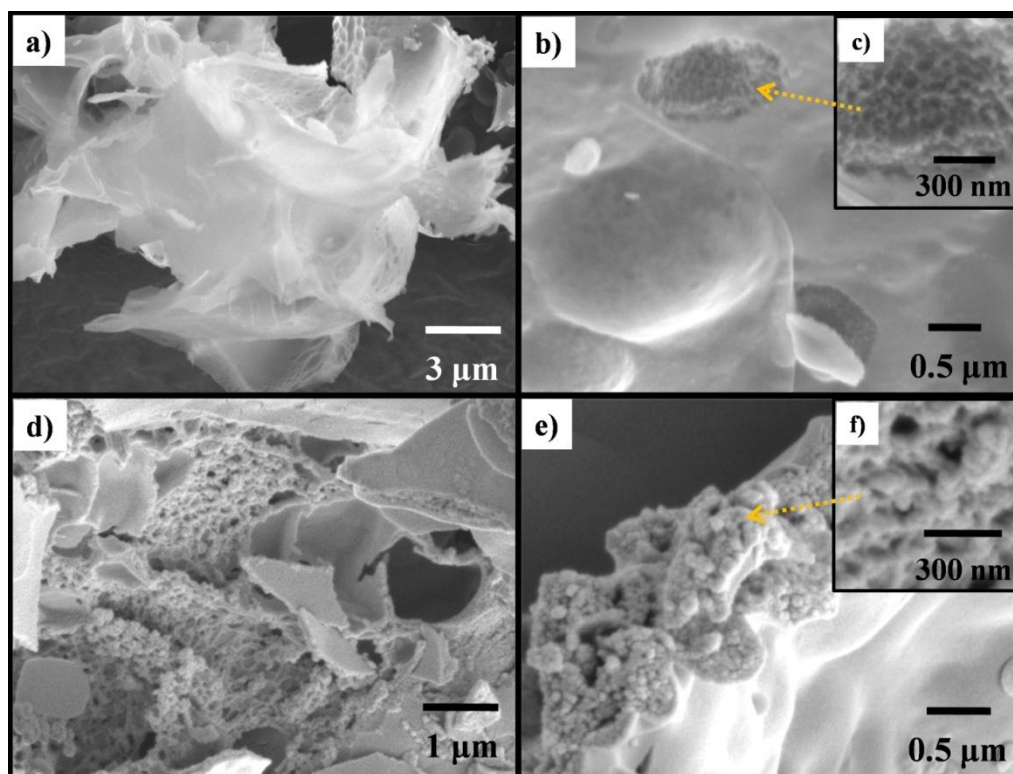


Figure 5.9 SEM images of thoria powders (a-c)  $T_{C17A}$  and (d-f)  $T_{C25A}$

#### 5.4.4 Microstructural analysis by using SEM and TEM

Low magnification images showed a flaky pattern (Fig. 5.9) while the high magnification SEM images revealed that the  $T_{C17A}$  and  $T_{C25A}$  comprised a network of porosity (Fig. 5.9). It was also observed that these powders comprised both micro and macropores (Fig. 5.9).

TEM investigations carried out on the powders  $T_{C13A}$  and  $T_{C17A}$  (Fig. 5.6 – 5.7) revealed a broccoli like pattern with porous morphology. Bright field and dark field images of  $T_{C17A}$  powders confirmed the presence of nanograins with interconnected pores. The SAED images of  $T_{C13A}$  and  $T_{C17A}$  powders (Figs. 5.6a and 5.7a) confirmed the presence of fluorite structure and nanocrystallinity. The “d-spacing” measured in this powder were comparable to those cited in the standard JCPDS pattern (No. 00-42-1462). The grain size distribution was mainly unimodal with a maxima at 10 nm.

## 5.5 Compaction and sintering of nanocrystalline thoria powders

### 5.5.1 Green density ( $\rho_G$ )

It was observed that the  $\rho_G$  of the thoria pellets increases with the CP (Fig. 5.10a & Table 5.8). The plot depicting the variation of  $\rho_G$  with the CP reveals a discontinuity in the slope at a compaction pressure of 175 MPa in all these powders. Further, it is observed that the values of the  $\rho_G$  varies in the following order  $\rho_{G(TC13C)} < \rho_{G(TC17C)} < \rho_{G(TC25C)} < \rho_{G(TC50C)} < \rho_{G(TC5.5C)} < \rho_{G(T00C)}$ , irrespective of the CP. It was observed that this trend is akin to the trend in the variation in the  $\rho_B$  of these powders. Thoria powders which comprised near unimodal size distribution of particles did not yield pellets with high  $\rho_G$ , while the powders that comprised multimodal size distribution of particles yielded compacts with high  $\rho_G$ . Thoria powders derived through direct denitration method yielded fragile compacts when compacted at 60 MPa.

The maximum green density that could be obtained was  $58.2 \pm 0.6$  % T.D ( $T_C13C$ ) and  $60.2 \pm 0.2$  % T.D ( $T_C17C$  - 353 MPa). Further, it was observed that the green compacts of these powders ( $T_C13C$  and  $T_C17C$ ) showed sufficient handling strength even when a CP as low as 60 MPa was employed. The powders  $T00C$ ,  $T_C5.5C$  and  $T_C50C$  (set I) exhibited higher  $\rho_G$  than  $T_C13C$ ,  $T_C17C$  and  $T_C25C$  (set II). This trend is similar to that observed in their  $\rho_B$  i.e.  $\rho_{G(\text{set I})} > \rho_{G(\text{set II})}$ . The higher fraction of fines in the (set II) powders probably led to a lower  $\rho_G$ . Chandramouli et al. [1] had employed a CP of 200 MPa to compact nc-thoria powders. However, these authors have not reported the values of  $\rho_G$ . It was observed that the  $\rho_G$  values obtained in this study for nc- $\text{ThO}_2$  powders are higher as compared to those reported earlier (Table 5.6). In addition, the thoria compacts derived in this study are superior compared to those reported earlier [5, 7, 8, 12, 18, 23, 24] as these nc- $\text{ThO}_2$  powders did not require any additional consolidation aids viz., pre-compaction, grinding, addition of lubricants or binders during compaction.



**Table 5.6 Comparison of  $\rho_G$  of thoria compacts reported in the literature**

Reference	CP; Lubricant/binder	$\rho_G$
[23]	345 MPa; stearic acid	59.6 – 60.3 %
[7]	-	56 – 64 %
[24]	200 MPa; zinc stearate	56 %
[18]	276 MPa; zinc stearate	56 – 64 % T.D
[5, 8]	Pre & post compaction-120 MPa and 200 MPa	50 % TD
[12]	500 MPa; stearic acid	53.8 % T.D

### 5.5.2 Studies on the sintering of nc-ThO<sub>2</sub>

Both CS and TSS experiments were carried out with nc-ThO<sub>2</sub> powders (T<sub>C</sub>13C: 317 MPa) derived through “volume combustion” (Table 5.7). Our results revealed that the “TSS<sub>2</sub>” carried out at a final temperature of 1773 K, yielded a denser product as compared to TSS<sub>1</sub> (T<sub>C</sub>13S<sub>1</sub>) and CS (T<sub>C</sub>13S<sub>CS1</sub> and T<sub>C</sub>13S<sub>CS2</sub>) (Table 5.7). Hence, these thoria compacts were sintered by using the “TSS<sub>2</sub> method” at a final sintering temperature of 1773 K (Table 5.7). Hence, thoria compacts were sintered by using the TSS at a final sintering temperature of 1773 K (TSS<sub>2</sub>).

The  $\rho_S$  are presented in Fig. 5.10b and in Table 5.8. These were found to vary between  $79.3 \pm 0.2$  % to  $98.9 \pm 0.3$  % T.D. Harada et al. [25] obtained a  $\rho_S$  of 75 % T.D for the thoria powders derived through denitration. These authors compacted the thoria powders blended with stearic acid (binder) and CCl<sub>4</sub> (lubricant) at 138 MPa. The T00C powders are in fact powders derived through direct denitration. Our results show that the processing protocol used in this study resulted in a density more than that reported by Harada et al. [25], despite the fact that no binder or lubricant was used in our work. This highlights the fact that the “TSS<sub>2</sub>” helps enhance the  $\rho_S$ . The dependence of the  $\rho_S$  of these two sets of powders set I and set II on the CP followed a trend quite opposite to that observed in the variation of  $\rho_G$ , i.e.  $\rho_{S \text{ set II}} > \rho_{S \text{ set I}}$ .

**Table 5.7 Sintering parameters and  $\rho_s$  of ThO<sub>2</sub> (T<sub>C</sub>13C; 317 MPa)**

$\rho_G$	CS <sub>1</sub> (T <sub>C</sub> 13S <sub>CS1</sub> )	CS <sub>2</sub> (T <sub>C</sub> 13S <sub>CS2</sub> )	TSS <sub>1</sub> (T <sub>C</sub> 13S <sub>1</sub> )	TSS <sub>2</sub> (T <sub>C</sub> 13S <sub>2</sub> )
% T. D.				
56.7 ± 0.0	95.8 ± 0.1	96.1 ± 0.1	96.6 ± 0.8	97.8 ± 0.3

CS<sub>1</sub> – 1673 K 4h   CS<sub>2</sub> - 1773 K 4h   TSS<sub>1</sub>   Step 1 - 1873 K 30 min; Step 2 - 1673 K 4 h   TSS<sub>2</sub>   Step 1 - 1873 K 30 min; Step 2 - 1773 K 4 h

**Table 5.8  $\rho_G$  and  $\rho_s$  of thoria pellets (sintered by using TSS<sub>2</sub> method)**

CP (MPa)	Density / (%T.D)*											
	T00C	T00S <sub>2</sub>	T <sub>C</sub> 5.5C	T <sub>C</sub> 5.5S <sub>2</sub>	T <sub>C</sub> 13C	T <sub>C</sub> 13S <sub>2</sub>	T <sub>C</sub> 17C	T <sub>C</sub> 17 S <sub>2</sub>	T <sub>C</sub> 25C	T <sub>C</sub> 25S <sub>2</sub>	T <sub>C</sub> 50C	T <sub>C</sub> 25S <sub>2</sub>
	$\rho_G$	$\rho_s$	$\rho_G$	$\rho_s$	$\rho_G$	$\rho_s$	$\rho_G$	$\rho_s$	$\rho_G$	$\rho_s$	$\rho_G$	$\rho_s$
<b>60</b>	59.0 ± 0.5	-	58.2 ± 0.9	84.9 ± 0.6	45.6 ± 0.7	94.8 ± 0.3	47.7 ± 0.2	95.4 ± 0.5	49.2 ± 0.7	93.5 ± 0.4	52.9 ± 0.5	83.5 ± 0.2
<b>120</b>	62.5 ± 1.3	79.3 ± 0.2	61.4 ± 0.5	89.5 ± 0.5	49.9 ± 0.3	97.8 ± 0.7	51.6 ± 0.3	95.9 ± 0.3	53.7 ± 0.5	94.2 ± 0.5	56.5 ± 0.6	88.4 ± 0.9
<b>180</b>	65.4 ± 0.4	80.6 ± 0.4	64.5 ± 0.6	91.1 ± 0.3	53.5 ± 0.3	97.9 ± 0.7	55.3 ± 0.2	97.4 ± 0.4	57.9 ± 0.5	95.8 ± 0.8	59.9 ± 0.2	90.7 ± 0.6
<b>243</b>	66.7 ± 0.3	82.6 ± 0.2	65.6 ± 0.7	92.2 ± 0.2	55.8 ± 0.5	<b>98.8 ± 0.3</b>	57.2 ± 0.4	97.6 ± 0.2	58.9 ± 0.5	96.5 ± 0.2	62.0 ± 0.3	92.2 ± 0.6
<b>317</b>	67.9 ± 1.4	83.8 ± 0.3	68.4 ± 0.5	92.5 ± 0.3	56.7 ± 0.3	<b>98.9 ± 0.3</b>	58.8 ± 0.5	<b>98.2 ± 0.7</b>	59.6 ± 1.1	96.7 ± 0.4	63.1 ± 0.9	95.3 ± 0.5
<b>353</b>	68.4 ± 0.2	84.9 ± 0.2	68.0 ± 0.1	93.1 ± 0.2	58.2 ± 0.6	<b>98.3 ± 0.7</b>	60.2 ± 0.2	97.6 ± 0.2	61.7 ± 0.3	96.9 ± 0.2	64.8 ± 0.2	95.5 ± 0.2

\*represents the mean of five measurements

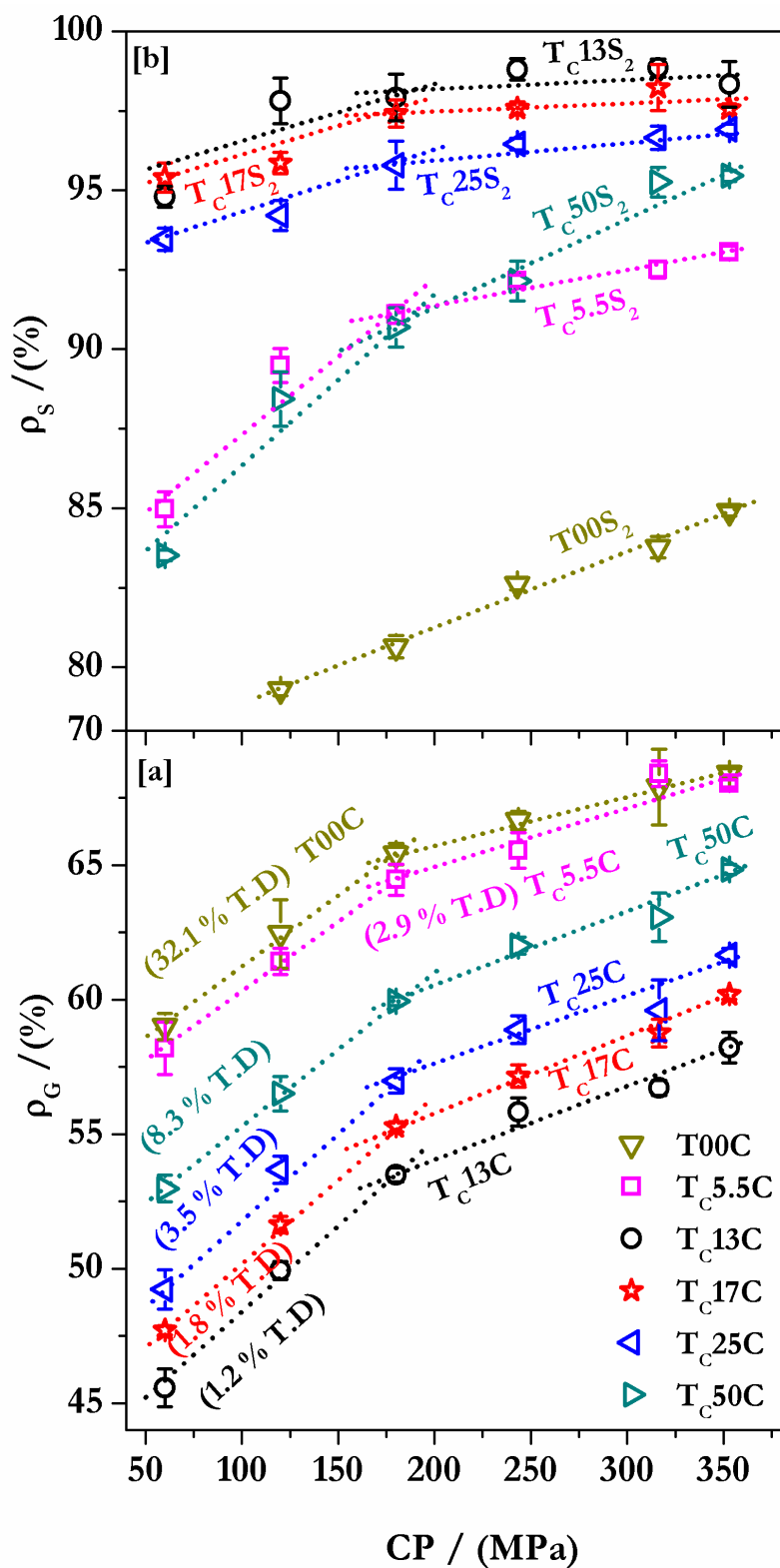


Figure 5.10 Variation of (a)  $\rho_G$  and (b)  $\rho_s$  with CP [ $\rho_B$  of the respective thoria powders are presented in parenthesis]

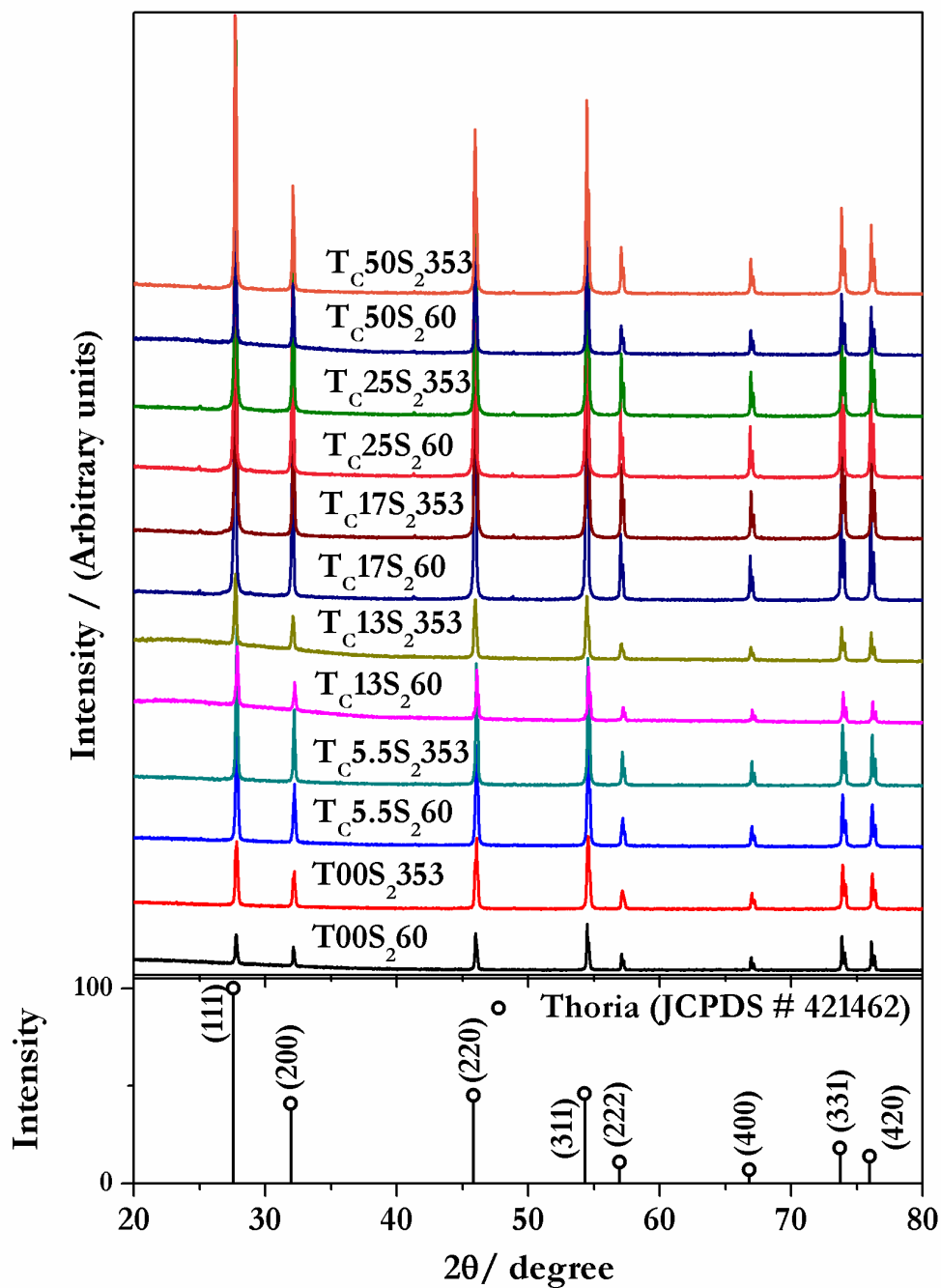


Figure 5.11 XRD patterns of some sintered thoria monoliths

The XRD patterns of sintered thoria monolith are presented in Fig. 5.11.  $\rho_s$  of  $T_{C13C}$ ,  $T_{C17C}$  and  $T_{C25C}$  thoria monoliths varied from  $93.5 \pm 0.4 \%$  to  $98.9 \pm 0.3 \%$  T.D. A CP as low as 60 MPa was found to be sufficient to obtain high  $\rho_s$ . The  $\rho_s$  of the  $T_{C13C}$  compacts [243 MPa

(1773 K)] is marginally higher ( $98.8 \pm 0.3$  % T.D) than those obtained at 317 MPa [ $97.8 \pm 0.3$  % T.D (1773 K)]. This observation reveals that nc-ThO<sub>2</sub> could be sintered by the TSS method to just about the same density but by employing a lower CP. This is the highest  $\rho_s$  reported so far for citrate gel-combustion derived nc-ThO<sub>2</sub> powders. However, removal of 1-2 % porosity from these monoliths would be a challenging task. White et al. [18] obtained sintered monoliths whose densities ranged from 81.4 – 96 % T.D (276 MPa; 1923 K and He-6% H<sub>2</sub>). Yayli et al. [24] sintered thoria monoliths of 96.0 % T.D (200 MPa; 1973 K 4 h and Ar-10% H<sub>2</sub>). Purohit et al. [11] had reported a  $\rho_s$  of 97.0 % T.D (187 MPa; 1573 K 3h and air). However, these authors did not report detailed microstructural investigations of the sintered products obtained by them [1, 5, 8, 18, 23, 24].

Fig. 5.12 depicts the temperature dependence of the sintered densities of thoria, prepared through different routes reported in earlier investigations. From the data presented in Fig. 5.12 it is evident that the thoria derived ex-oxalate [23] when sintered by using CS yields only lower  $\rho_s$  ( $\approx 86$  % T.D.). The results reported in refs. [1, 5, 8, 11, 26, 27] reveal that for sintered ThO<sub>2</sub>, densities above 95 % T.D. could be obtained at temperatures as low as 1550 K. Ex-tannate powders [23], glycine combustion product [11], citrate gel-combustion derived powder [1] and ex-deagglomerated oxalate powders [5] of thoria have all yielded high densities. However, information on the microstructure of the sintered products obtained from them [5, 11, 23] is either limited or not available. Further, citrate gel-combustion derived powders when sintered beyond a certain threshold temperature could yield undesirably low densities owing to “run-away” sintering [8].

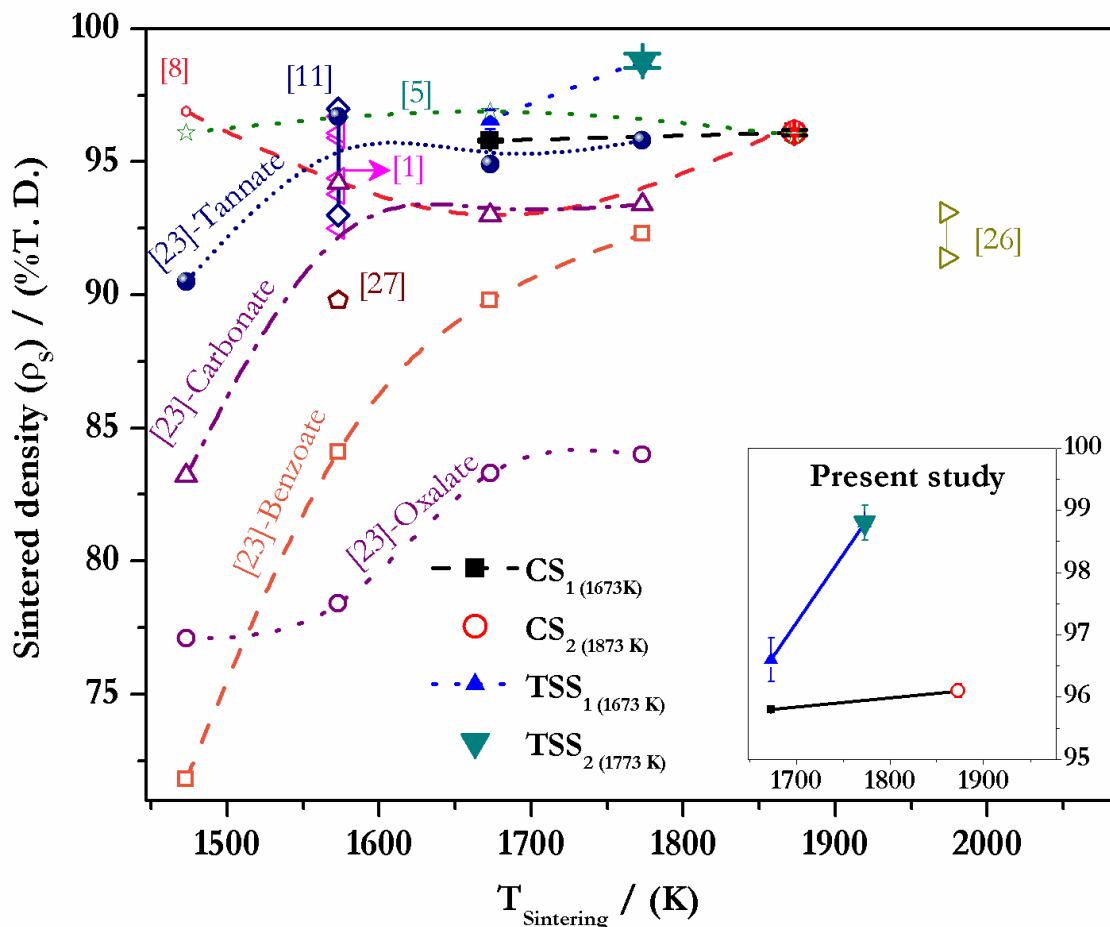


Figure 5.12 Effect of  $T_{\text{Sintering}}$  on the  $\rho_s$  of  $\text{ThO}_2$

Our investigations (1673 K) on the “TSS<sub>2</sub>” of nc-UO<sub>2</sub> presented in Chapter 3, reveals that this technique yields a product with a high density and a desirable microstructure. Even though the results reported in refs. [1, 5, 8, 11, 26, 27] show high densities, the usefulness of these methods need to be reinvestigated for they do not provide information on the microstructure [1, 5, 8, 11, 26, 27] and temperature dependence [11] of the  $\rho_s$ . Our results on the “TSS<sub>2</sub>” sintering of ThO<sub>2</sub> clearly indicate that the  $\rho_s$  reported in this study ( $98.8 \pm 0.3$  % T. D; 243 MPa) is the highest among the values reported so far at 1773 K. Further a monotonous increase in  $\rho_s$  is being reported for nc-ThO<sub>2</sub> for the first time when the final temperature is raised from 1673 to 1773 K.

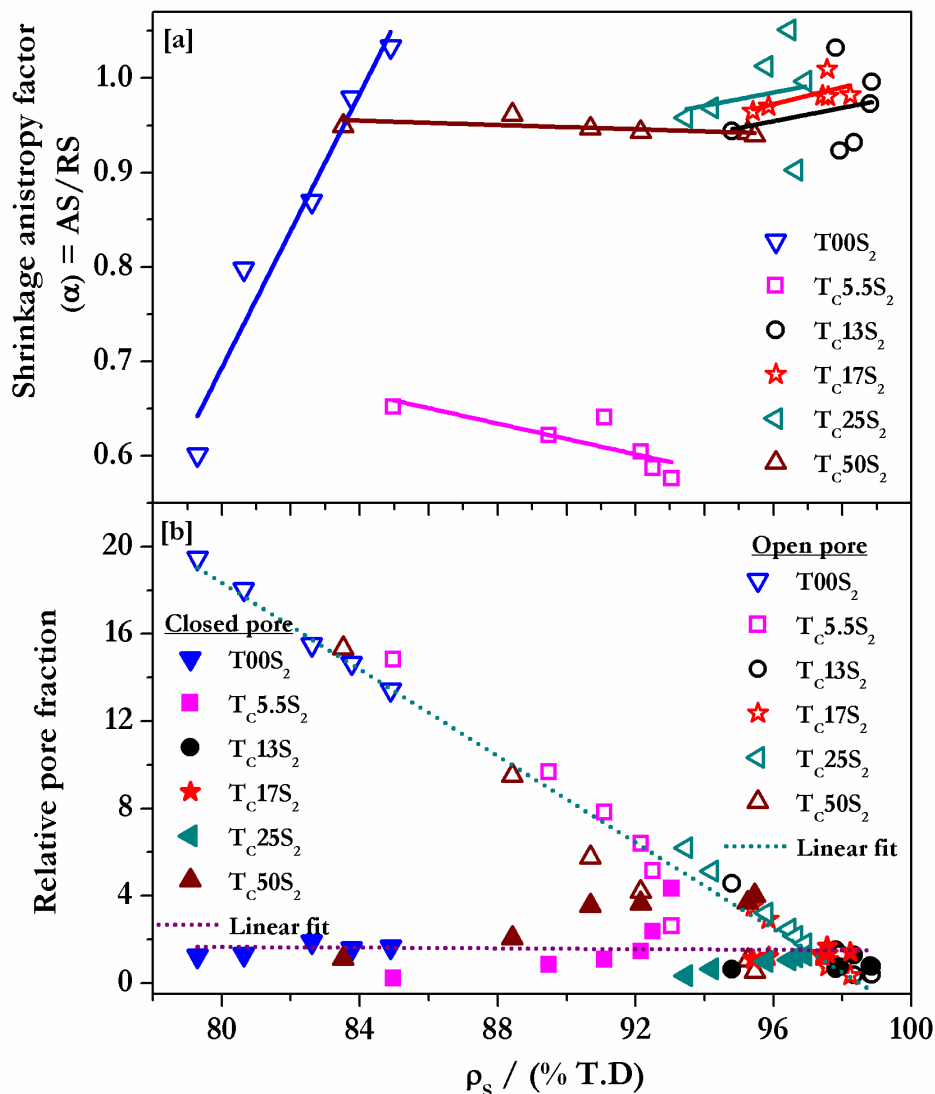


Figure 5.13 Dependence of a) shrinkage anisotropy factor ( $\alpha$ ) and (b) open and closed porosity on  $\rho_s$  in the sintered  $\text{ThO}_2$  monoliths

The variation in the relative pore fraction (open and closed pore) and shrinkage anisotropy factor ( $\alpha$ ) [14] with the  $\rho_s$  is given in Fig. 5.13. Fig. 5.13a reveals that  $\alpha$  is linearly correlated with the  $\rho_s$ . Further, the variation is less pronounced for the compacts made from T<sub>C</sub>13C, T<sub>C</sub>17C, T<sub>C</sub>25C and T<sub>C</sub>50C. This figure (Fig. 5.13) also reveals that T00C and T<sub>C</sub>5.5C compacts exhibited differential densification while all other compacts showed uniform (isotropic) densification. These results are important from an industrial point of view to obtain defect free sintered bodies with near net shapes [14, 28]. As expected, the relative fraction of

pores varies linearly with the  $\rho_s$ . This plot (Fig. 5.13b) also reveals that the relative pore fraction nearly becomes equal in all compacts when their  $\rho_s$  approaches 97 % T.D.

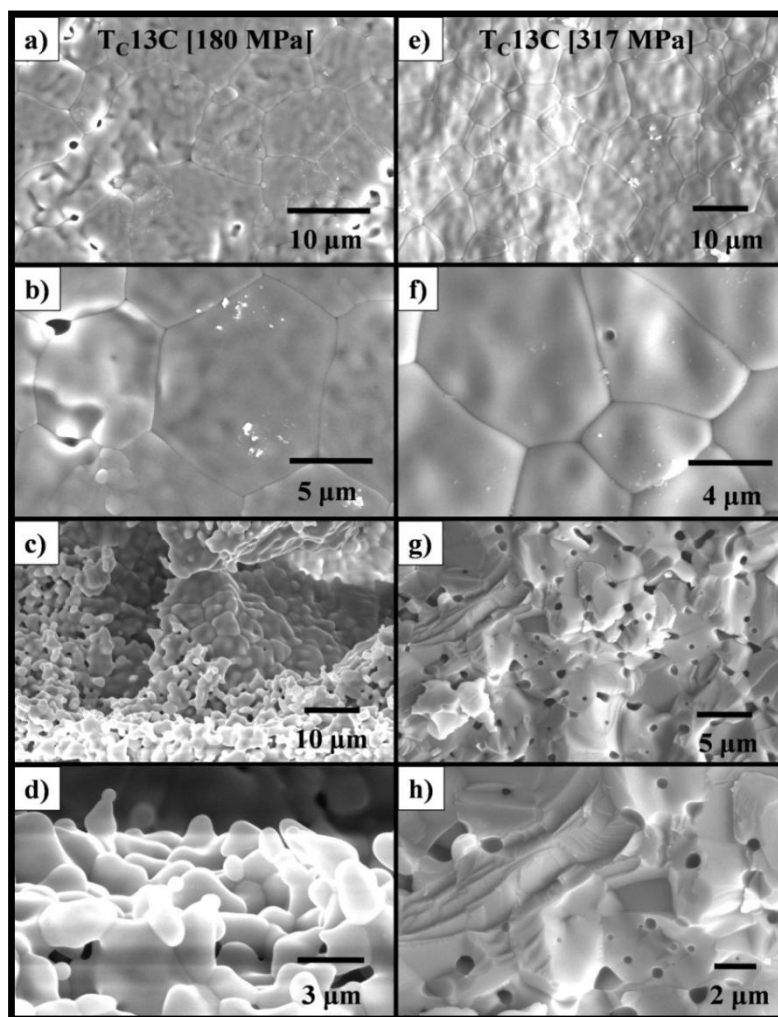


Figure 5.14 SEM images of sintered  $T_{C13C}$  pellets compacted at (a-d) 180 MPa and (e-f) 317 MPa [(a, b, e & f) sintered surface showing well defined grain boundaries and (c, d, g & h) fractured surface showing intra and intergranular pores]

### 5.5.3 Morphological analysis by using SEM

Microstructure of the sintered thoria monoliths are presented in Figs. 5.14-5.16. The SEM images reveal that these monoliths comprised uniform grains with well-defined grain boundary (faceted morphology) and near unimodal size distribution of grains with their size ranging between 6 – 15  $\mu\text{m}$ . Surface morphology of the sintered thoria shows that majority of the grains possess pentagonal or hexagonal boundaries. Investigations of a fractured surface revealed the



smaller grains submerged into the larger one (Ostwald ripening [29]) and that the grains in the fractured surface are also faceted.

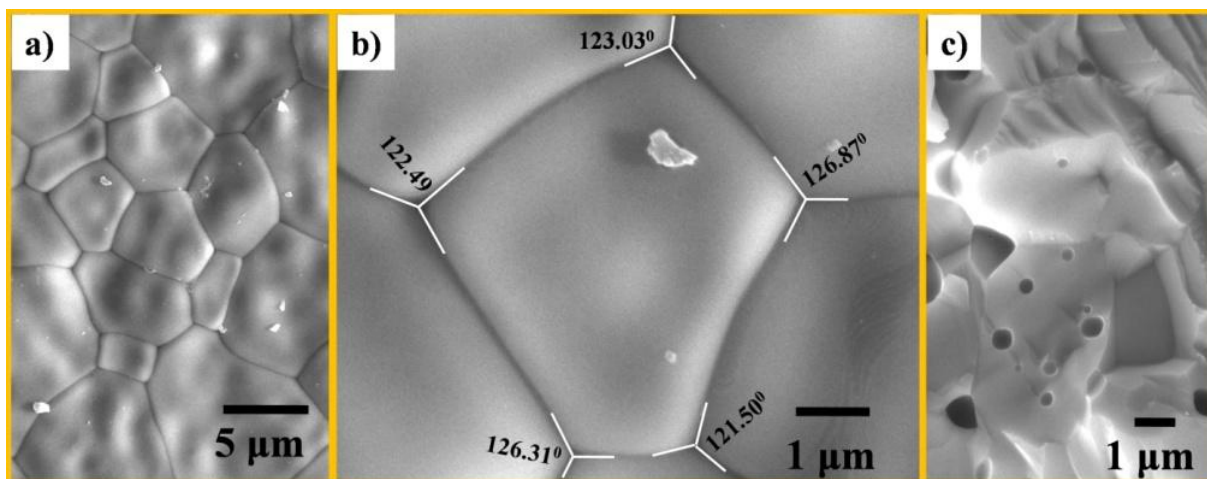


Figure 5.15 (a-c) SEM images of sintered pellets of thoria (TC13S<sub>2</sub>-317 MPa); (a) pellet surface revealing faceted grains; (b) typical pentagonal grains revealing  $\approx 121$ - $127^\circ$  dihedral angle and (c) Image of fractured surface revealing intra and intergranular pores

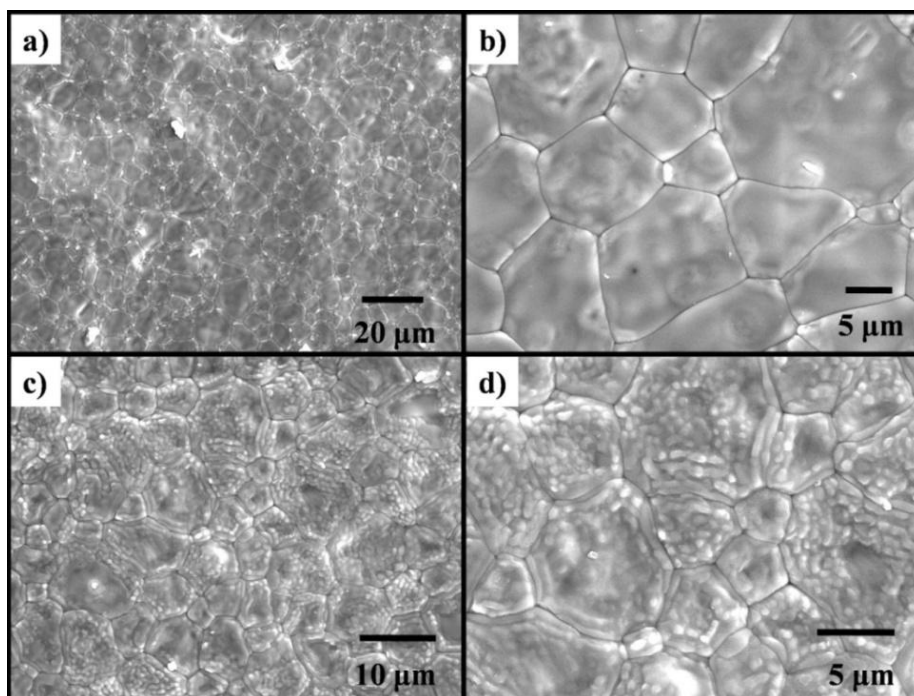


Figure 5.16 SEM images of sintered T<sub>c</sub>13C pellets (353 MPa) (a) unpolished pellet surface revealing uniform grains; (b) high magnification image of pellet surface showing faceted grains; (c) low magnification image of the polished fractured surface showing uniform grains and (d) high magnification image of the fractured polished sintered surface showing well defined grain boundaries

## 5.6 Conclusions from the investigations on nc-ThO<sub>2</sub>

Nc-ThO<sub>2</sub> powders were prepared by using citrate gel-combustion method in bulk quantities by varying the fuel to nitrate mole ratio ( $R = 0$  to  $0.50$ ). The systematic dependence of the properties of nc-ThO<sub>2</sub> powders on  $R$  was investigated. It was observed that the  $\rho_B$ , SSA, PSD, XCS and lattice strain showed a systematic dependence on the  $R$  value. The combustion reaction in the mixture with an  $R$  value of  $0.50$  was investigated with DTA, DSC and mass spectrometry. Direct evidence for consumption of oxygen during combustion was observed for the first time. It was observed that the mixture with  $R$  values  $0.13$  and  $0.17$  exhibited vigorous and moderate volume combustion respectively. Microstructural investigations revealed that the volume combustion derived thoria powders were porous and comprised aggregates of nanograins. TEM investigation reaffirmed the nanocrystallinity. For the first time, EELS investigation was carried out on the nc-ThO<sub>2</sub> powders and the branching ratio ( $B$ ) was calculated for both the “as prepared” and “calcined” powders. No evidence could be obtained for the existence of thorium in multiple oxidation states. TEM investigations also revealed that the nc-ThO<sub>2</sub> comprised unimodal grain size distribution with their size ranging between  $6 - 16$  nm with maxima at  $10$  nm.

It was observed that the volume combustion derived nc-ThO<sub>2</sub> powders were highly sinterable. A CP of  $243$  MP and TSS with a final sintering temperature of  $1773$  K is sufficient to sinter it to a  $\rho_S$  of  $98.8 \pm 0.3$  % T.D for TC13C powders. Microstructural analysis of polished and thermally etched sintered thoria monoliths revealed that it comprised uniform faceted grains with well-defined grain boundaries. For the first time,  $\alpha$  was estimated and it revealed that the ThO<sub>2</sub> compacts had undergone near isotropic shrinkage. This work describes a cost and energy efficient method for the production of high density pellets and small crucibles from nc-ThO<sub>2</sub>.

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## **Chapter 6**

### ***Synthesis, Conventional Sintering and SPS of nanocrystalline Yttria***

*This chapter describes the experiments on the VCR in the citrate gels containing the  $Y(NO_3)_3$  and the studies on the sintering of nc- $Y_2O_3$  derived by using this reaction.*

#### **6.1 Starting material**

Yttrium nitrate was used as such. The starting materials used in the preparation of the combustion mixtures were devoid of impurities that would significantly alter the characteristics of the gel-combustion derived powders.

#### **6.2 The combustion reaction**

VCR was observed in the mixtures containing yttrium nitrate with an R value of 0.17. The plausible reaction pertaining to the VCR in the preparation of  $Y_2O_3$  is given in Eqn. (6.1).



#### **6.3 Powder characterization**

$\rho_B$  of all the “as prepared” yttria powders were lower than that of their “calcined” counterparts (Table 6.1). Upon calcination the yttria powders showed a significant increase (300 %) in the  $\rho_B$  which were comparable to those reported in earlier investigations [1, 2].

Size distribution of particles in the “as prepared” and “calcined” powders of yttria is presented in the Fig. 6.1 and in Table 6.2. From these data it is evident that the “as prepared” powders comprised particles with lower size as compared to the calcined products derived from them. The influence of the relative distribution of size fractions on the  $\rho_B$  of nc- $UO_2$  has been explained in chapter 3. A similar trend is observed among nc- $Y_2O_3$  as well.

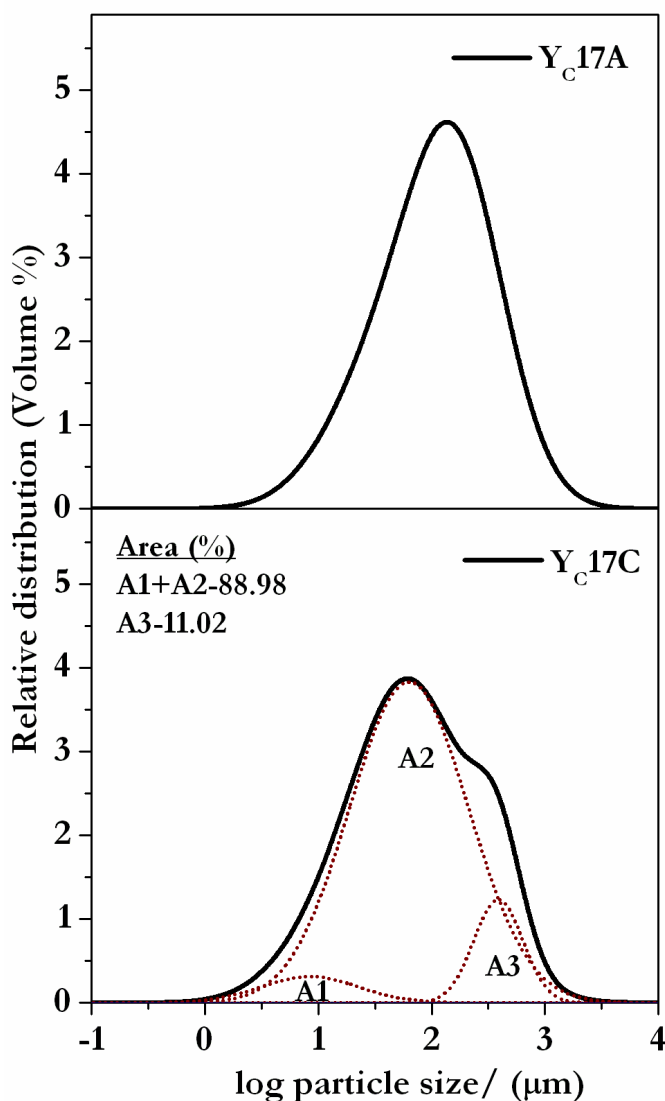


Figure 6.1 Distribution of sizes among particles in the “A” and “C” yttria powders (Thick solid lines – experimental curve, thin solid line – deconvoluted curves)

The size distribution of particles in the calcined powders was nearly bimodal and comprised a larger fraction of the fines (below 100  $\mu\text{m}$ ) than their “A” precursors. The latter exhibited a nearly unimodal distribution. Thus the presence of fines would have helped increase the  $\rho_B$  of the calcined yttria powders. The SSA values of the “A” powders were higher as compared to that of the “C” powders derived from them. Hence, it is evident that calcination leads to a reduction in the SSA and porosity due to grain coarsening. It is observed that the values of the  $\rho_B$  and SSA are inversely correlated.

Table 6.1 Characteristics of the nc-yttria powders derived through VCR

Sample	R	$\rho_B$ (% T. D)	RC (ppm)	SSA ( $\text{m}^2\text{g}^{-1}$ )	XCS		
					Sc (nm)	HW (nm)	Strain $\times 10^{-3}$
Y <sub>C</sub> 17A	0.166	0.6	1350	57	12	13	1.02
Y <sub>C</sub> 17C	0.166	1.8	621	24	18	19	0.15

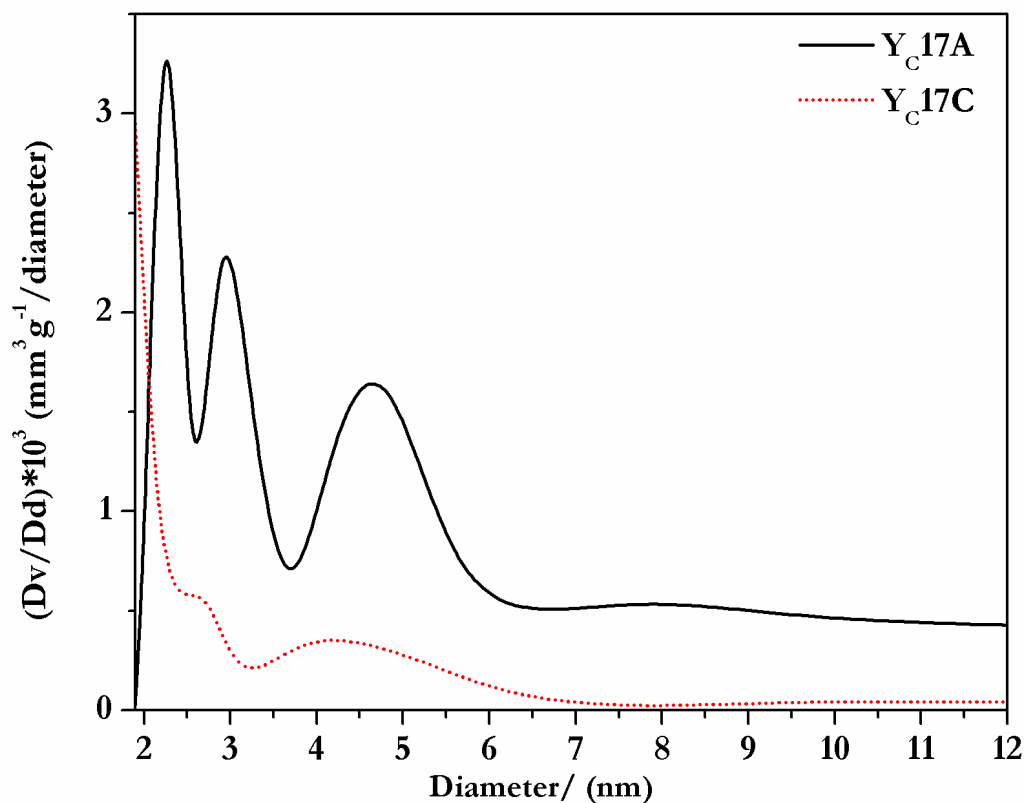


Figure 6.2 Size distribution of pores in nc-yttria powders

Table 6.2 Size distribution among particles and porosity in nc-yttria powders

Sample	Particle size distribution (Vol %)			Average size of the pore (nm)	Maximum size of the pore (nm)	Specific pore volume ( $\text{mm}^3\text{g}^{-1}$ )
	10 vol. % of sample has size less than ( $\mu\text{m}$ )	50 vol. % of sample has size less than ( $\mu\text{m}$ )	90 vol. % of sample has size less than ( $\mu\text{m}$ )			
Y <sub>C</sub> 17A	12	68	275	2.27	5.4	71
Y <sub>C</sub> 17C	11	64	364	1.89	2.1	36

Size distribution of pores in  $\text{Y}_2\text{O}_3$  (Fig. 6.2) powders derived by using the BET  $\text{N}_2$  adsorption isotherm are presented in Table 6.2. The specific pore volume of these powders was found to vary from  $34 \text{ mm}^3\text{g}^{-1}$  to  $71 \text{ mm}^3\text{g}^{-1}$ , and it decreased by a factor of 2 upon calcination ( $\text{Y}_2\text{O}_3$ :  $71 \text{ mm}^3\text{g}^{-1}$  to  $36 \text{ mm}^3\text{g}^{-1}$ ). These observations further substantiate the fact that pore elimination and grain coarsening take place during calcination.

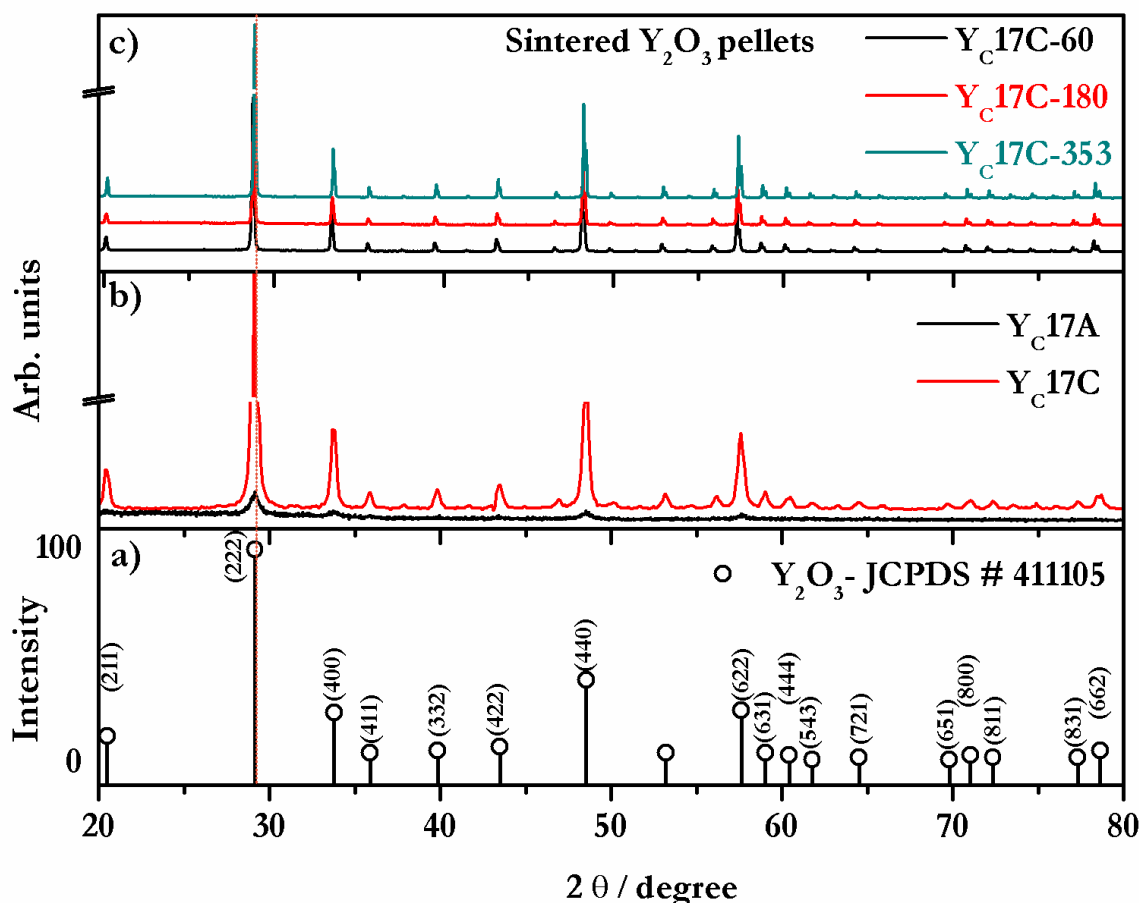


Figure 6.3 XRD of yttria a) JCPDS pattern [# 411105]; b) “A” and “C” volume combustion derived powders and c) sintered yttria monoliths

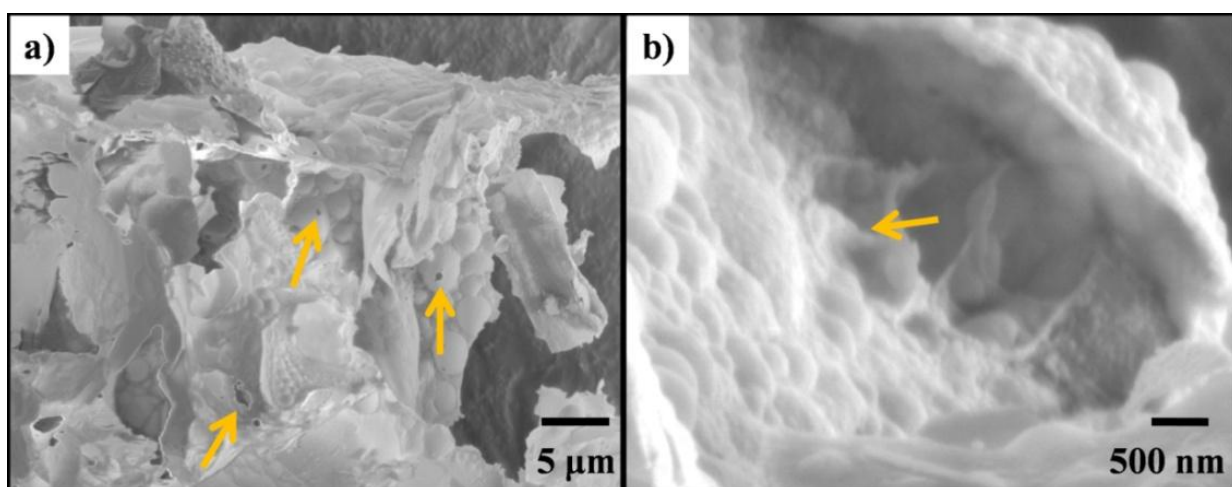
The XRD patterns of the powders are presented in the Fig 6.3. The “A” powders were found to possess crystallites with a mean size of about 13 nm. Upon calcination these crystallites grew to about 19 nm. The lattice strain in the “A” powders, estimated by the HW method [3] was found to decrease by a factor of 7 (Table 6.1) after calcination. It was observed that the error



(due to the strain component) in the estimates of the crystallite size obtained by the Sc method was rather insignificant. This observation is quite different than the trends observed in the XCS of nc-urania [Chapter 3] derived through citrate gel-combustion. Probably the precipitation of  $\text{U}_3\text{O}_8$  and its conversion back into  $\text{UO}_2$  would have induced a higher lattice strain in the latter. It is evident from the data presented in Table 6.1 that the “A” powders had a higher carbon residue, than the “C” powders.

#### **6.4 Microstructural investigations on nc- $\text{Y}_2\text{O}_3$ powders**

The SEM images of the “A” powders are presented in Fig. 6.4. These images show that these powders comprise irregular agglomerates. An image of the “A” yttria powder at a higher magnification confirms the presence of nano pores. The TEM images also confirm the same (Fig. 6.5). Microstructural characterization (TEM) of volume combustion derived  $\text{Y}_2\text{O}_3$  powders further ascertained that these powders comprised grains of uniform size in the nano regime (20 – 30 nm). SAED patterns confirmed both their size and nanocrystallinity (Figs. 6.5a-6.5c). HRTEM images (Fig. 6.5d and 6.5f) of these samples depict the values of the “d” spacings that are in agreement with the standard values cited in JCPDS [ $\text{Y}_2\text{O}_3$  – 00-41-1105].



*Figure 6.4 SEM images of powders a) and b) “as-prepared”  $\text{Y}_2\text{O}_3$  powders ( $\text{Y}_{\text{C17A}}$ )*

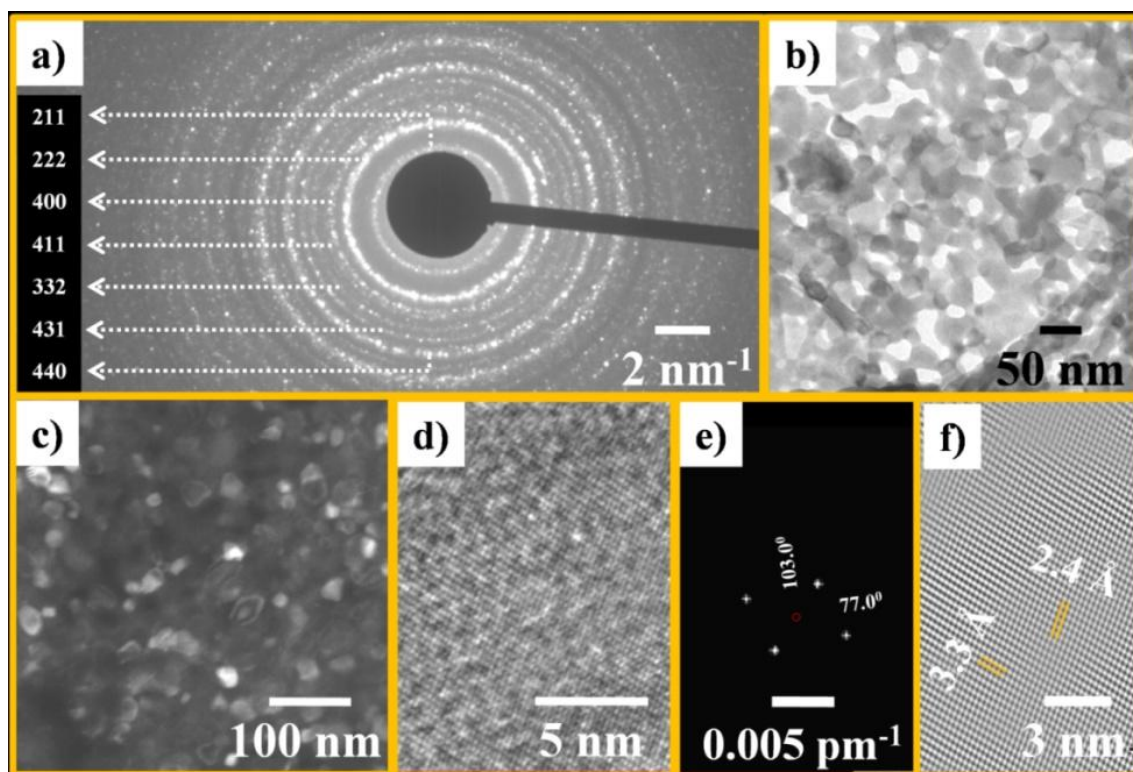


Figure 6.5 TEM images of  $Y_{C17A}$  powders: (a) SAED image; (b) bright field image revealing nano grains; (c) dark field image revealing nano grains; (d) HRTEM image of nano grain within the selected area; (e) FFT image and (f) filtered IFFT image

## 6.5 Compaction and sintering of nc- $Y_2O_3$

### 6.5.1 Green density ( $\rho_G$ )

The dependence  $\rho_G$  of the nc- $Y_2O_3$  powders on the CP was studied to optimize the compaction process (Fig. 6.6a). The  $\rho_G$  versus CP plot of yttria could be divided into two linear regions. In the “first region” from 60 – 180 MPa a linear correlation between  $\rho_G$  and CP was observed. Beyond this CP there was no significant increase in the  $\rho_G$  with the CP. These experiments revealed that a  $\rho_G$  of about 54 % T.D. could be obtained at a pressure of 317 MPa ( $Y_2O_3$ ), which was used to prepare the pellets for sintering.

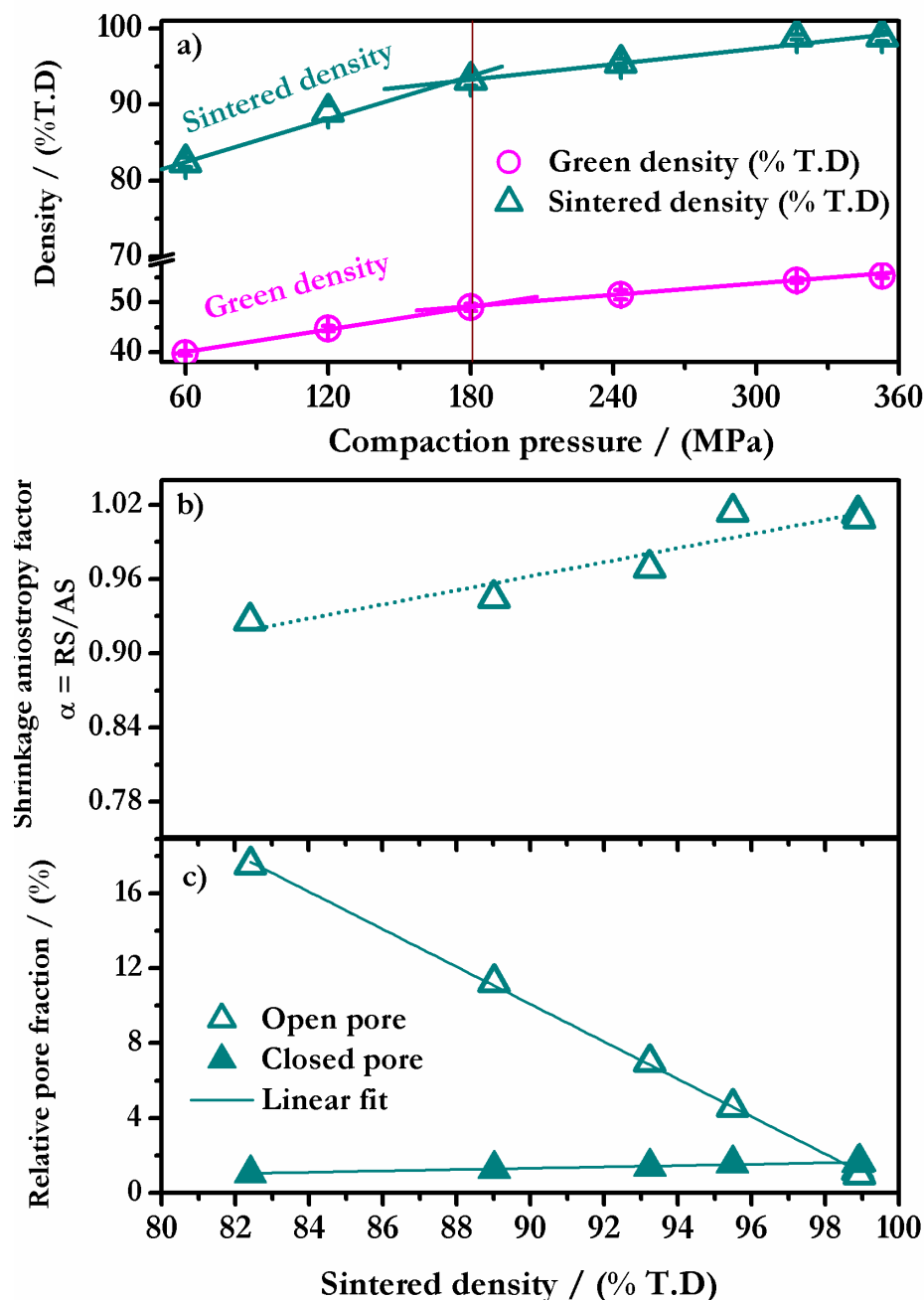


Figure 6.6 (a) variation of  $\rho_G$  and  $\rho_S$  with the CP; (b) dependence of shrinkage anisotropy factor ( $\alpha$ ) with the  $\rho_S$  and (c) dependence of open and closed pore fraction with the sintered density

### 6.5.2 Sintering of nc- $Y_2O_3$

Tables 6.3-6.4 depict the characteristics of the compacts. The data presented in Table 6.3 reveals that the “TSS $_1^Y$ ” sintering leads to a better densification as compared to that of CS (CS $_1^Y$ )

and  $CS^Y_2$ ). It is interesting to note that in the “ $TSS^Y_1$ ” method, a final temperature as low as 1673 K is sufficient to obtain a  $\rho_s$  of 98.9 % T. D. Hence,  $Y_2O_3$  compacts were sintered by using the  $TSS_1$  at a final sintering temperature of 1673 K. The variation of  $\rho_s$  with the CP reveals two regions (separated at 180 MPa) and in both these regions the  $\rho_s$  is linearly correlated with the CP. A maximum  $\rho_s$  of about 98.9 % T. D was obtained at 317 MPa and 353 MPa which indicates that a CP of 317 MPa is sufficient to obtain yttria monoliths of 99 % T. D (grain size  $< 3 \mu m$ ). It was also observed that the shrinkage anisotropy factor ( $\alpha$ ) [4] and relative pore fraction are linearly correlated with the compaction pressure (Fig. 6.6).

**Table 6.3 Sintering parameters and  $\rho_s$  of  $Y_2O_3$  ( $Y_C17C$ ; 317 MPa)**

	$CS^Y_1$	$CS^Y_2$	$TSS^Y_1$	$TSS^Y_2$
$\rho_G$	$Y_C13S_{CS1}$	$Y_C13S_{CS2}$	$Y_C13S_1$	$Y_CXXS_2$
% T. D				
$54.4 \pm 0.4$	$98.2 \pm 0.4$	$98.3 \pm 0.1$	$98.9 \pm 0.1$	$98.4 \pm 0.4$

$CS^Y_1$  – 1673 K 4h     $CS^Y_2$  - 1773 K 4h     $TSS^Y_1$     Step 1 - 1873 K 30 min  
Step 2 - 1673 K 4 h     $TSS^Y_2$     Step 1 - 1873 K 30 min  
Step 2 - 1773 K 4 h

**Table 6.4 Characteristics of yttria compacts**

P (MPa)	$\rho_G$ (% T.D)	$\rho_s$ (% T.D)
<b>60</b>	$39.8 \pm 0.5$	$82.4 \pm 0.6$
<b>120</b>	$44.7 \pm 0.5$	$89.0 \pm 0.8$
<b>180</b>	$49.0 \pm 0.7$	$93.2 \pm 0.8$
<b>243</b>	$51.5 \pm 0.9$	$95.5 \pm 0.5$
<b>317</b>	$54.4 \pm 0.4$	$98.9 \pm 0.3$
<b>353</b>	$55.4 \pm 0.5$	$98.9 \pm 0.6$

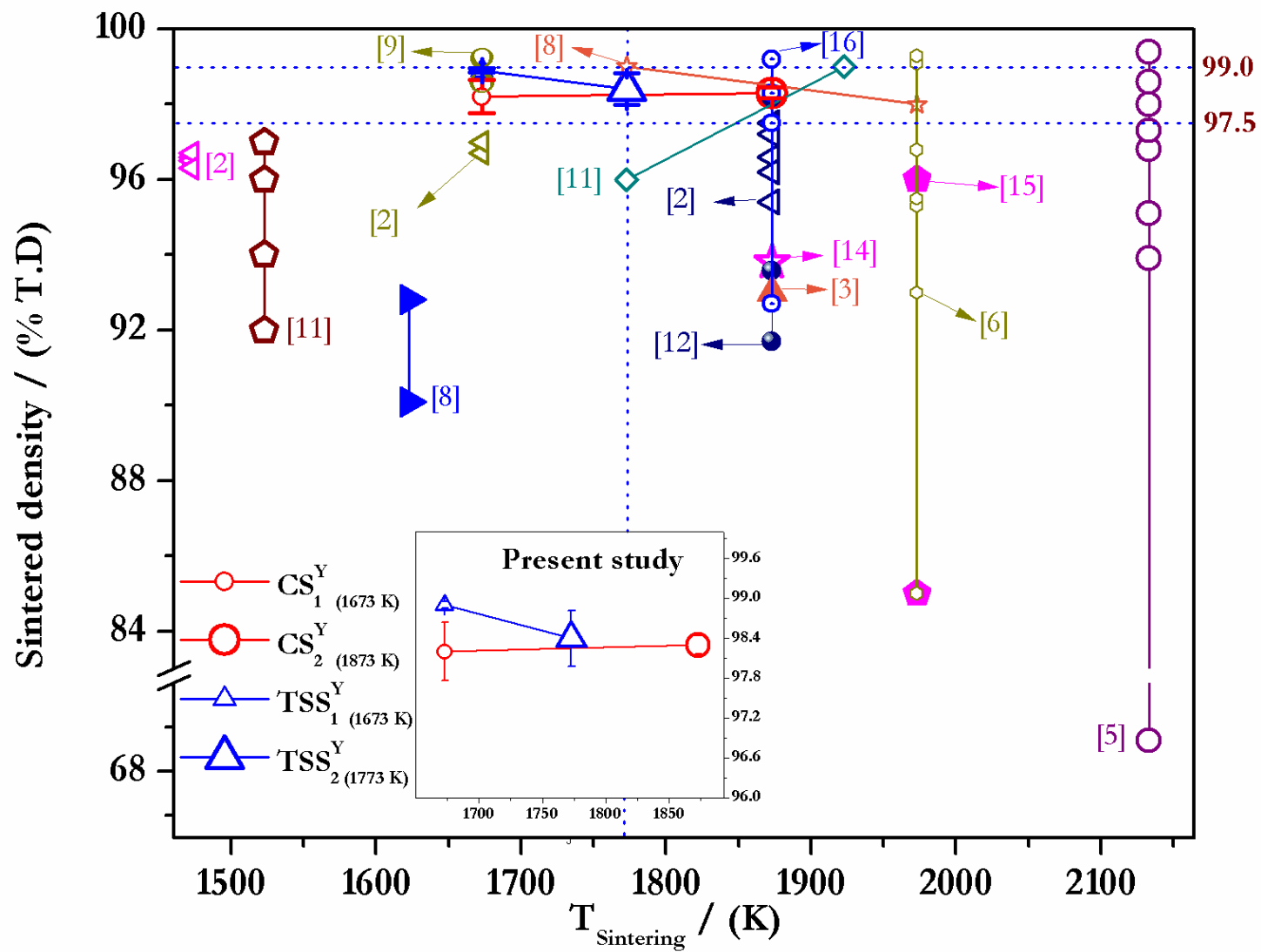


Figure 6.7 Dependence of the sintered density of  $\text{Y}_2\text{O}_3$  with the sintering temperature ( $T_{\text{Sintering}}$ )

Fig. 6.7 depicts the temperature dependence of the  $\rho_s$  of yttria prepared through different routes reported in earlier investigations [2, 5-16]. From the data presented in this Fig. 6.7 it is evident that sintering of yttria by the conventional method yields samples with a lower  $\rho_s$ . These powders could be sintered to full density by doping aliovalent cations in yttria [8, 12], vacuum sintering at high temperature [10] or by using hot isostatic pressing [6]. But these methods require either deliberate addition of impurities or are energy intensive. However, recent studies have revealed that yttria could be sintered to very high densities ( $\leq 97$  % T. D.) by tailoring the methods used for both the powder preparation [6, 17] as well as sintering [8, 17, 18]. Fig. 6.8 shows the SEM images of the sintered pellets.

In the present study, we have also reaffirmed that CS could also be used to sinter  $Y_2O_3$  to a high density but elimination of the final residual porosity (1-2 %) is extremely difficult. From Fig. 6.6 and Fig. 6.7 it is evident that the TSS method yields highly sintered products (99 % T.D) at a sintering temperature as low as 1673 K. Upon increasing the final temperature to 1773 K the  $\rho_s$  was found to decrease marginally to 98.4 % T. D.

**Table 6.5 Comparison of  $\rho_s$  of yttria monoliths reported in the literature**

Ref.	Method	Sintering temperature / Condition	$\rho_s$ (% T. D)
[12]	glycine gel-combustion	1873 K / Air	98.2
[5]	precipitation	2133 K / Vacuum	99.4
[9]	glycine gel-combustion	1673 K / Air	99.0
[10]	yttrium carbonate	1873 K / Vacuum	99.0
[16]	yttrium carbonate	1873 K / Air	99.2

From the data presented in Table 6.5, it is evident that yttria powders were sintered at temperature higher than 1673 K in earlier investigations [5, 9, 10, 12, 16]. Further, the spread in the values of  $\rho_s$  of yttria observed in the present study is quite insignificant as compared to those cited in earlier investigations [6, 9, 12]. The preparation method presented here is amenable for

scale-up. In addition owing to the reduced quantities of fuel (citric acid) employed, the sintered product has only insignificantly low amounts of carbon residue.

### 6.5.3 Spark plasma sintering of nc-Y<sub>2</sub>O<sub>3</sub>

Calcined VCR derived nc-Y<sub>2</sub>O<sub>3</sub> powder was used as such without any further processing step in the SPS studies. Nc-Y<sub>2</sub>O<sub>3</sub> powders were sintered at 1873 K at a heating rate of 100 K min<sup>-1</sup> and 50 MPa. These pellets were calcined in air at 1873 K for 1 h to remove the graphite adhering to their surface and were subjected to further analysis viz., phase identification, densification and microstructural investigation. XRD pattern pertaining to the spark plasma sintered pellets revealed that they comprised c-Y<sub>2</sub>O<sub>3</sub> and that the carbon residue in the sintered compacts after annealing in air at 1673 K for 1 h was found to be 647 ppm (Table 6.6).

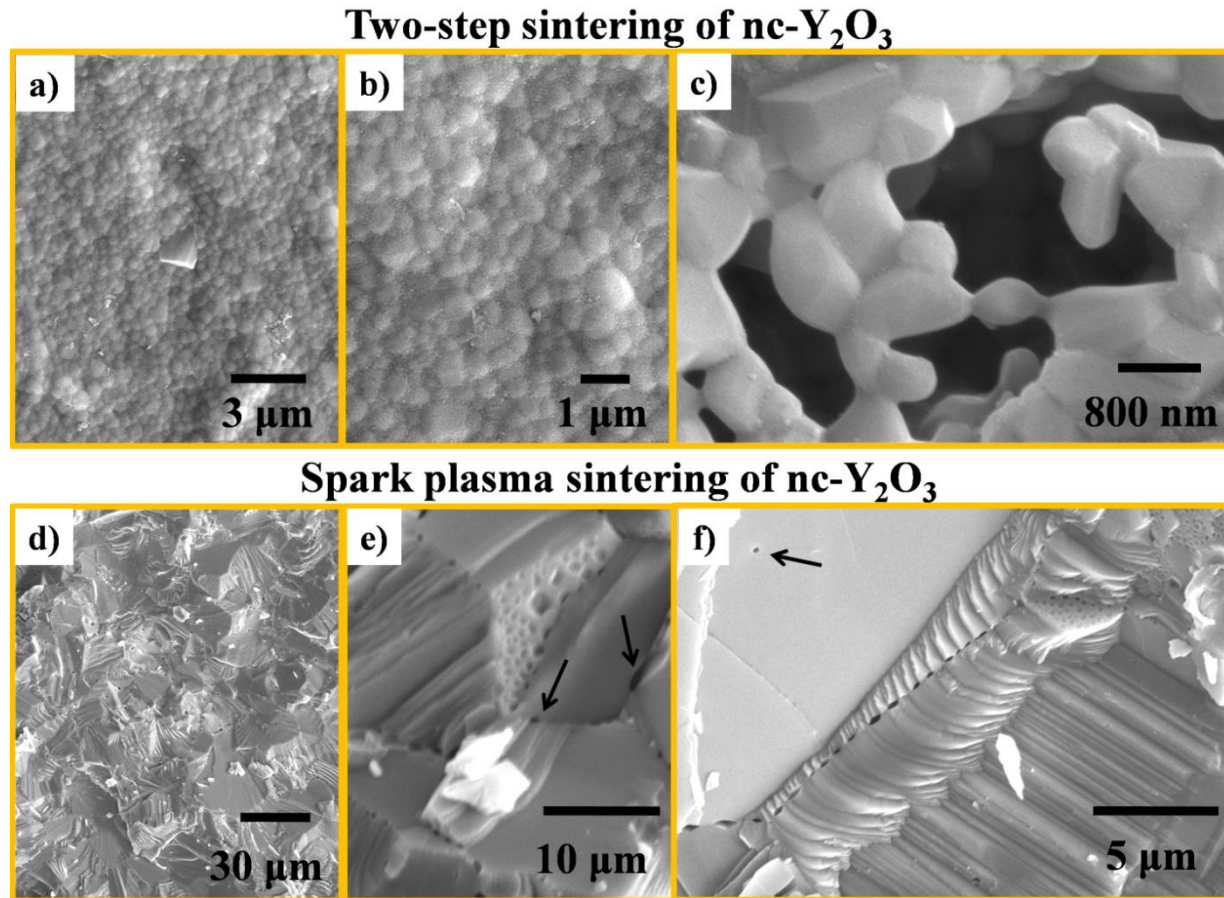
**Table 6.6 Sintered density of yttria monolith derived through SPS**

Material	Sample Index	Initial phase composition	Heating rate (K min <sup>-1</sup> )	ρ <sub>s</sub> (% T. D)	RC (ppm)	T <sub>s</sub>
Y <sub>2</sub> O <sub>3</sub>	Y <sub>C</sub> 17C	c	100	99.3 ± 0.2	647	1873 K 7 min

*c – cubic and T<sub>s</sub> - Sintering schedule*

**Table 6.7 Comparison of ρ<sub>s</sub> of yttria monoliths derived by using SPS with the reported values in the literature**

Ref.	Method	TS / time / pressure (MPa)	ρ <sub>s</sub> (% T. D)	Average grain size (μm)
[19]	commercial nc-Y <sub>2</sub> O <sub>3</sub>	1673 K/ 5 min / 100	98.5	4
		Above 1673 K	93 - 94	5 – 6
		923 K / - / 83	-	0.10
[20]	commercial nc-Y <sub>2</sub> O <sub>3</sub>	1123 K / - / 83	-	0.50
		1123 K / - / 83	-	0.7
		1873 K / - / 83	98	-
[21]	hydrothermal	1773 K / - / 100	99.6	1 - 1.12
[22]	commercial Y <sub>2</sub> O <sub>3</sub> / ball milled	1473 K to 1873 K / - / 100	98 - 99	0.24 - 2



**Figure 6.8** SEM images of sintered pellets of yttria (a-c)TSS<sub>1</sub> and (d-f) SPS; (a) pellet surface revealing fine grains, (b) high magnification image of pellets surface revealing nearly uniform grains, (c) Image of fractured pellet surface, (d) low magnification image of fractured pellet surface, (e) high magnification images of fractured pellet surface revealing entrapped closed pores and (e) high magnification images of fractured pellet surface revealing isolated pore and intragranular cracks



The  $\rho_s$  of this compact was found to be  $99.3 \pm 0.2$  % T.D (Table 6.6). Visual examination of this compact did not reveal any defects viz., cracks or hour glassing. Many authors (Table 6.7) had derived nc-Y<sub>2</sub>O<sub>3</sub> powders by using different method (hydrothermal method, precipitation, etc.) and had sintered these powders by using SPS with different sintering schedules. However, no reports so far been published in the literature pertaining to SPS of nc-Y<sub>2</sub>O<sub>3</sub> powders derived through citrate gel VCR.

Thus, from the foregoing discussion it is evident that the  $\rho_s$  of the yttria monoliths derived in this study by SPS are comparable to those reported in the literature (Table 6.7).

Microstructural investigation of the SPS monoliths of nc-Y<sub>2</sub>O<sub>3</sub>, (SEM) had revealed that the compacts had undergone uniform densification with no visible pores. However, higher magnification images of fractured surface revealed the presence of closed pores. These images also revealed that grains are faceted and had a typical size ranging from 6-12  $\mu\text{m}$ . Further optimization is required to obtain nanostructured (grain size  $< 1 \mu\text{m}$ ) monoliths.

## **6.6 Conclusions drawn from the investigations on nc-Y<sub>2</sub>O<sub>3</sub>**

It was demonstrated for the first time that VCR takes place in mixtures containing yttrium nitrate with citric acid with an R value of 0.17. The powders derived through VCR were found to be nanocrystalline, fine grained and highly porous ( $60 - 70 \text{ mm}^3\text{g}^{-1}$ ).

All the powders comprised nc aggregates. It was demonstrated that the  $\rho_B$ , SSA, PSD, XCS and the morphology of these powders were unique as compared to the powders derived through other methods reported in the literature [2, 5-16]. Microstructural analysis of the “A” powders carried out by using TEM confirmed the presence of nc c-Y<sub>2</sub>O<sub>3</sub>. Both TEM and SEM investigations revealed that these powders possessed nano pores.

The calcined products were found to be highly sinterable. It was demonstrated that  $\text{Y}_2\text{O}_3$  pellets with a density as high as 98.9 % T. D. could be produced by using the “two-step sintering” method ( $\text{TSS}_1^{\text{Y}}$ ) at a final temperature as low as 1673 K. Shrinkage anisotropy factor ( $\alpha$ ) and relative pore fraction of sintered  $\text{Y}_2\text{O}_3$  were linearly correlated with the compaction pressure. Similarly, it was observed that citrate gel-combustion derived nc- $\text{Y}_2\text{O}_3$  could be sintered to a density of 99.3 % T. D by using SPS (1873 K 7 min; 50 MPa and grain size: 6-12  $\mu\text{m}$ ).

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## Chapter 7

# Synthesis, Characterization and Sintering of Nanocrystalline $\text{HfO}_2$ and YSH powders by SMS

*This chapter deals with the results obtained in the investigations on the bulk synthesis and sintering of nc- $\text{HfO}_2$  and nc-YSH powders by using salt melt synthesis.*

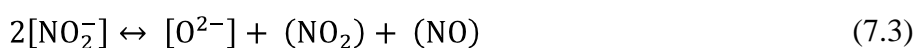
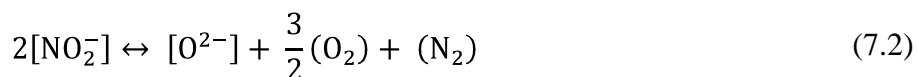
### 7.1 Purity of starting material and the final product

The cationic impurities present in  $\text{HfCl}_4$  were insignificantly low (Table 7.1) and are unlikely to influence the characteristics of the final products. The latter were found to contain lesser quantities of impurities (Table 7.2).

### 7.2 The salt melt synthesis (SMS) of nc-Hafnia

The salt melt synthesis (SMS) has been used in the past for the preparation of ceramic powders to prepare single phase materials with minimum impurities [1, 2]. The SMS involves the decomposition of a precursor in a pool of alkali metal nitrates. The reaction that ensues could be viewed based on the Lux-Flood concept [3], as an acid-base reaction, in which a base donates its oxide ion to an acid. Kerridge [4] and Durand et al. [5] had carried out extensive work on SMS. Benamira et al. [6] had demonstrated that m- $\text{HfO}_2$  could be prepared by the reaction between  $\text{HfCl}_4$  and an equimolar mixture of  $\text{NaNO}_3$  and  $\text{KNO}_3$  at 723 K. Ternary mixtures containing 7 mol%  $\text{NaNO}_3$ , 53 mol%  $\text{KNO}_3$ , and 40 mol %  $\text{NaNO}_2$  are quite stable up to about 873 K [7]. In the presence of oxygen, this mixture could be held without decomposing up to about 973 K. The decomposition of  $\text{NaNO}_3$  and  $\text{NaNO}_2$  could be described based on the equilibria [7, 8], represented in the equations (7.1) to (7.4). It is clear from these equilibria that a mixture richer in nitrate would be more oxidizing. Further, the nitrate ion decomposes through

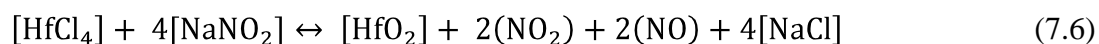
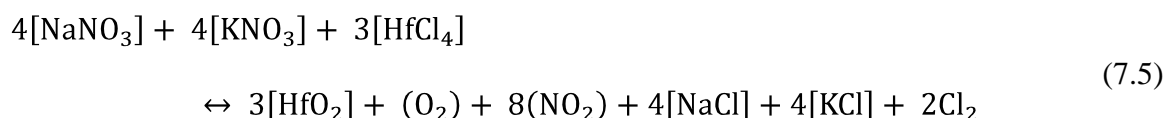
the formation of  $\text{NO}_2^-$ . Thus nitrite rich mixtures would be less oxidizing because of the lesser oxygen availability by virtue of the equilibrium described in eqn. (7.1) which would be shifted towards the left, in the presence of excess nitrite.



$$K_{\text{Eq}} = \frac{a_{\text{NO}_2^-}}{a_{\text{NO}_3^-}} p_{\text{O}_2}^{\frac{1}{2}} \quad (7.4)$$

Thus carrying out the reaction under the flow of argon helps accelerate the forward reaction leading to the formation of the products given in the equations (7.1) to (7.3). The nitrite rich mixtures exhibit less vigorous reaction.

The reactions in the melt could be described through eqns. (7.5-7.6) which represent the extreme conditions of reacting  $\text{HfCl}_4$  with either the alkali nitrate [eqn. (7.5)] or the alkali nitrite alone [eqn. (7.6)], respectively.



Thus the gaseous products would contain different oxides of nitrogen [eqn. (7.7)]. In the mixtures rich in nitrate which are more oxidizing, the  $\text{O}_2$  and  $\text{NO}_2$  would be present while less oxidizing mixtures would lead to the formation of  $\text{NO}_2$  and  $\text{NO}$ . It is reported in Ref. [9] that

evolution of  $\text{N}_2$  is brought about only when the reaction is carried out in a closed container. When the melt is allowed to decompose in an open vessel, evolution of  $\text{NO}$ ,  $\text{NO}_2$  and  $\text{O}_2$  would be observed [9]. From the visual observation it was evident that  $\text{NO}_2$  does evolve during the course of the reaction. Y. Du and D. Inman [10] proposed that  $\text{AlCl}_3$  reacts with molten nitrate (or nitrite) mixture to form  $\alpha\text{-Al}_2\text{O}_3$  with the liberation of  $\text{NO}$  and  $\text{NO}_2$ . These researchers [10] also showed that the reaction mechanism was altered by the composition of the melt and the experimental conditions. Thus by changing the composition of the melt (varying nitrite content) the reaction mechanism could be altered. Du et al. [11] have reported that the addition of a Lux-Flood base would reduce the reaction temperature due to increase in basicity. In this study, even though no attempt was made to elucidate the kinetics of the salt melt reaction, thermal analysis coupled with evolved gas analysis (EGA) was carried out on all mixtures. These results are discussed below.

**Table 7.1 ICP-MS analysis of  $\text{HfCl}_4$  powders**

Elements	Li	Ca	Sr	Ba	Ti	Zr	Al	Ga	Ta	As	Bi	Fe	Mo	Ni	Si	Cr
ppm	0.1	0.3	1.2	1.2	53	81	2.7	0.1	5.1	2.1	3.0	0.6	0.2	0.3	0.1	<0.2

**Table 7.2 Analysis of  $\text{HfO}_2$  by ICP-OES, AAS<sup>#</sup> and Ion selective electrode<sup>\*</sup>**

Elements	Sample	Na <sup>#</sup>	K <sup>#</sup>	Zr	Si	Cl <sup>*</sup>
	m- $\text{HfO}_2$	10.1	2.1	3.0	7.1	<1
ppm	c- $\text{HfO}_2$	14.4	3.5	2.6	6.3	<1
	30YSH	11	2.5	2.8	6.6	<1

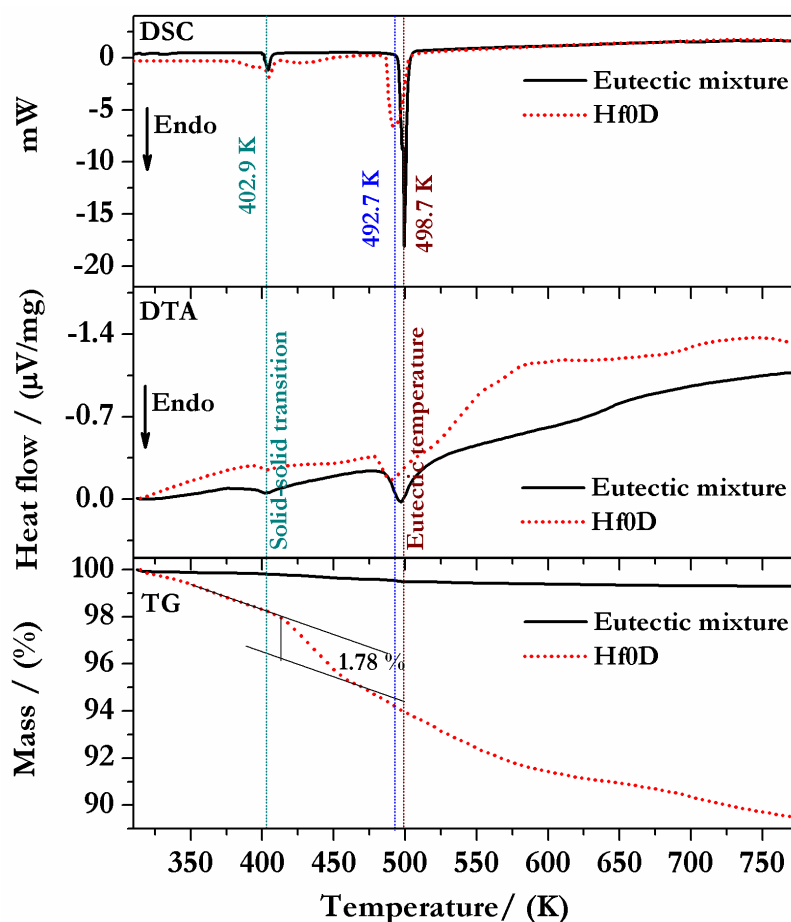


Figure 7.1 Thermal analyses of the salt mixtures revealing the heat effects during the salt melt reaction [where, Hf0D –hafnia powders prepared without the use of  $\text{NaNO}_2$ ]

### 7.3 Thermal analysis of salt mixture

The DSC curves depict the heat effect during the course of the reaction (Fig. 7.1). Data cited in the literature [7] pertaining to  $\text{KNO}_3\text{-NaNO}_3$  and  $\text{KNO}_3\text{-NaNO}_3\text{-NaNO}_2$  (HITEC<sup>®</sup>) [12] reveal that these systems are being studied extensively and that the solid state transitions as well as melt equilibria are being investigated in order to establish the pertinent phase diagrams. Recent investigations revealed that in the subsolidus region, a phase transition occurs at 367 K and 390 K in the systems  $\text{KNO}_3\text{-NaNO}_3\text{-NaNO}_2$  (HITEC<sup>®</sup>) [12] and  $\text{KNO}_3\text{-NaNO}_3$  [13] respectively.

Thermogram, DTA curve, DSC curve and evolved gas analyses of the salt mixtures are presented in Figs. 7.1-7.3. The endotherms observed at 403 K and 499 K in the DSC curves of



the pure nitrate mixture (Fig. 7.1) and TG-DTA-MS are in agreement with the temperatures pertaining to the subsolidus transformation reported in the literature and the pseudo-binary eutectic isotherm. Additionally, it was observed that the eutectic mixture is thermally stable till 773 K (TG and EGA). The mass loss of 0.2% observed at the eutectic temperature could be ascribed to the loss of water of crystallization. No exothermic peak was observed in the DTA curve at the eutectic temperature in all these mixtures. However, weight loss corresponding to gas evolution (mass spectra) was observed. This is probably due to the following phenomena which take place simultaneously; fusion (endothermic) and oxidation of HfCl<sub>4</sub> (exothermic). Since, 80 % of the melt contains the eutectic mixture the heat effect pertaining to the exothermic reaction probably gets masked by that due to the endothermic fusion.

Even though DTA curves obtained with the other salt mixtures reveal that the eutectic isotherm shifts to lower values with the addition of NaNO<sub>2</sub> while there is no change in the subsolidus phase transformation temperature (Fig. 7.2). It is observed that the salt melt reaction takes place close to the eutectic isotherm. This was further reaffirmed by evolved gas analysis (evolution of NO, NO<sub>2</sub>, Cl<sub>2</sub>, O<sub>2</sub> and HCl).

In general it was observed that the relative proportion of NO gas liberated increases with NaNO<sub>2</sub> addition whereas evolution of Cl<sub>2</sub> was observed only in mixtures without NaNO<sub>2</sub> (Fig. 7.3). Liberation of HCl and N<sub>2</sub>O [eqn. (7.7)] was observed when NaNO<sub>2</sub> was present in the mixture. However, the relative proportion of these gases was less compared to that of NO (Fig. 7.3). Traces of O, O<sub>2</sub> and NO<sub>2</sub> were also observed (Fig. 7.3). The presence of O could be due to the gas phase dissociation of oxygen during ionization in the mass spectrometer. However, the presence of both O<sub>2</sub> and O testify the release of oxygen during the reaction. From

the foregoing it is evident that the reaction mechanism is significantly altered when nitrite is added to the reaction mixture.

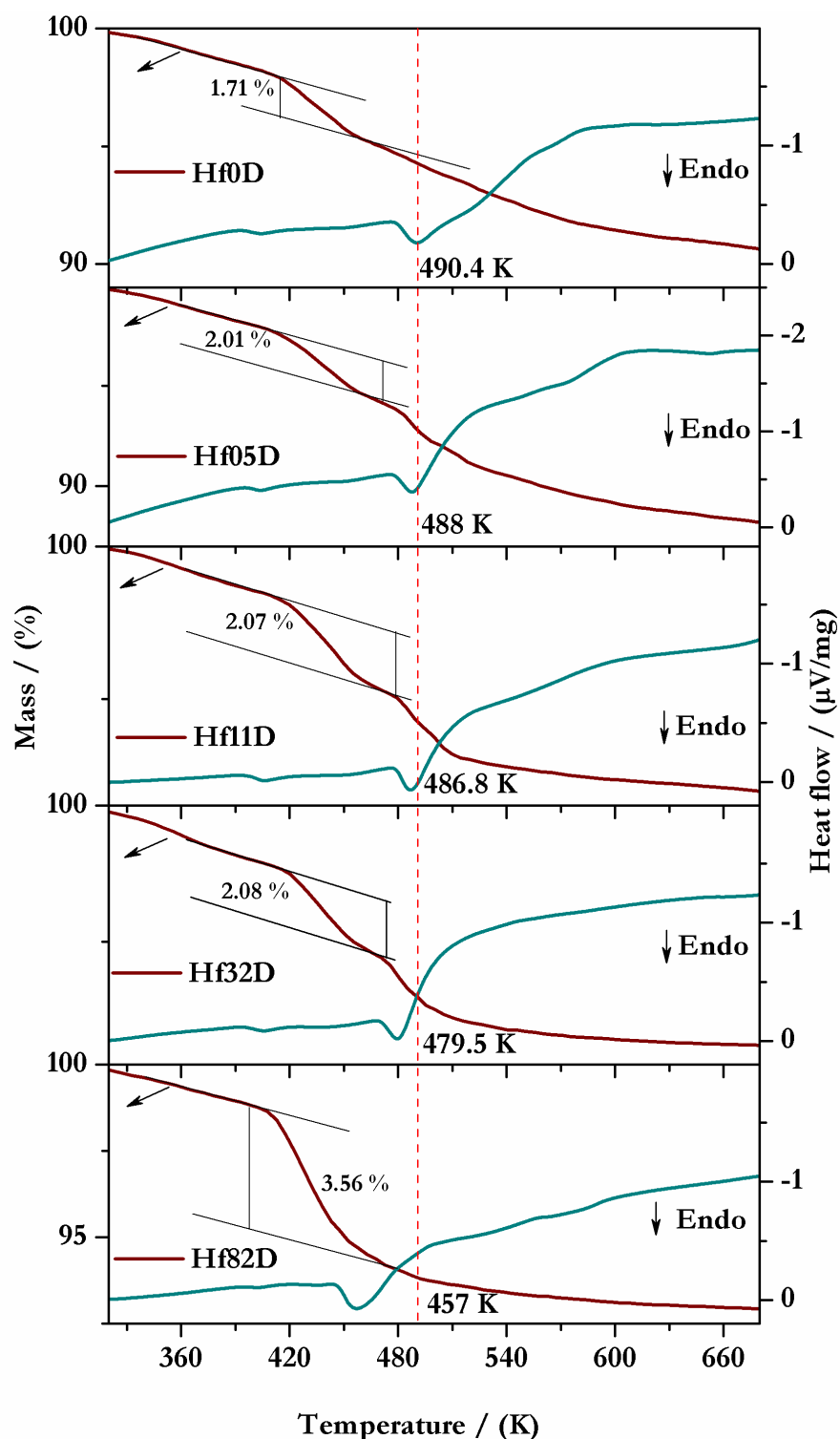


Figure 7.2 Thermal analyses of salt mixtures with varying  $\Phi$  values (where  $\Phi = 0, 0.055, 0.11, 0.32$  and  $0.82$ ) revealing the shift in the eutectic temperature

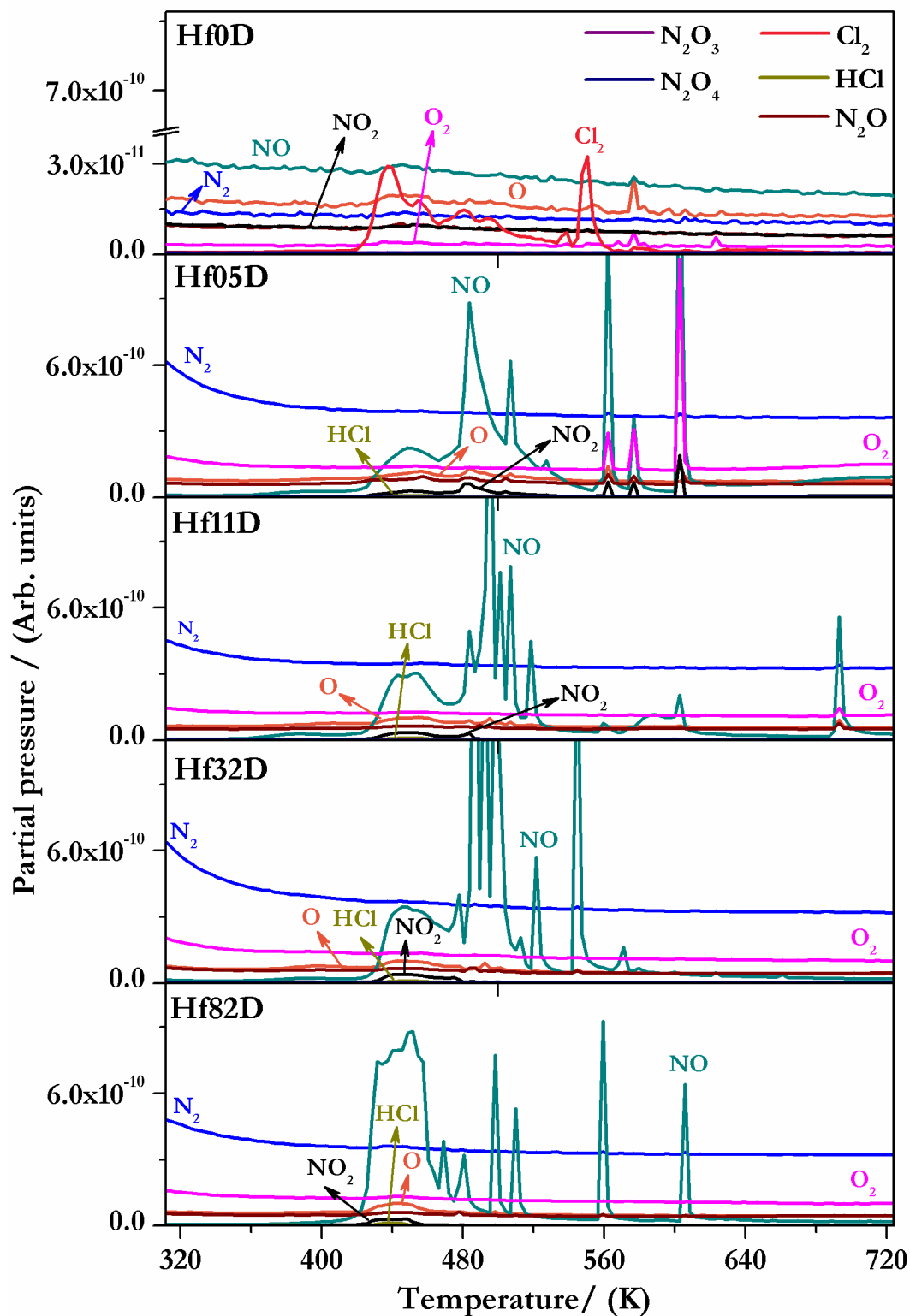


Figure 7.3 Evolved gas analysis of the reaction mixtures with varying  $\Phi$  values (where  $\Phi = 0, 0.055, 0.11, 0.32$  and  $0.82$ )

**Table 7.3 Characteristics of HfO<sub>2</sub> powders obtained through SMS from mixtures with different composition**

Sample	$\Phi$	$\rho_B$ (Mg m <sup>-3</sup> )	RC (ppm)	SSA (m <sup>2</sup> g <sup>-1</sup> )	XCS (nm)											
					673 K			873 K			1073 K			1473 K		
					Sc	HW	Strain x10 <sup>-2</sup>	Sc	HW	Strain x10 <sup>-2</sup>	Sc	HW	Strain x10 <sup>-2</sup>	Sc	HW	Strain x10 <sup>-2</sup>
Hf0D	0	1.58	498	81	7	13	0.983	12	16	0.356	16	22	0.214	52	99	0.143
Hf05D	0.05	1.72	618	68	8	13	0.905	14	21	0.334	20	25	0.185	68	138	0.147
Hf11D	0.11	1.67	528	57	9	14	0.584	14	25	0.377	31	36	0.171	41	113	0.172
Hf32D	0.32	1.66	621	38	9	26	0.411	15	27	0.255	23	32	0.167	39	83	0.127
Hf82D	0.82	1.52	717	26	22	38	0.131	23	38	0.115	23	39	0.105	55	130	0.132

$$\Phi = \frac{\text{Moles of NO}_2^-}{\text{Moles of NO}_3^-}$$

#### 7.4 Bulk density ( $\rho_B$ ), PSD and SSA of nc- $\text{HfO}_2$ powders

The characteristics of the powders obtained in this study are listed in Table 7.3. From the results presented it is evident that the  $\rho_B$  of nc- $\text{HfO}_2$  powders prepared in this study varies from  $1.52 - 1.72 \text{ Mg m}^{-3}$  and it is not a strong function of the concentration of nitrite in the melt. These powders were found to be free flowing and thus make an ideal press feed.

Size distribution of particles in the “as prepared” nc-hafnia powders is presented in Fig. 7.4. From these data it is evident that these powders are nearly unimodal and comprised particles with a mean size of  $10 \mu\text{m}$ .

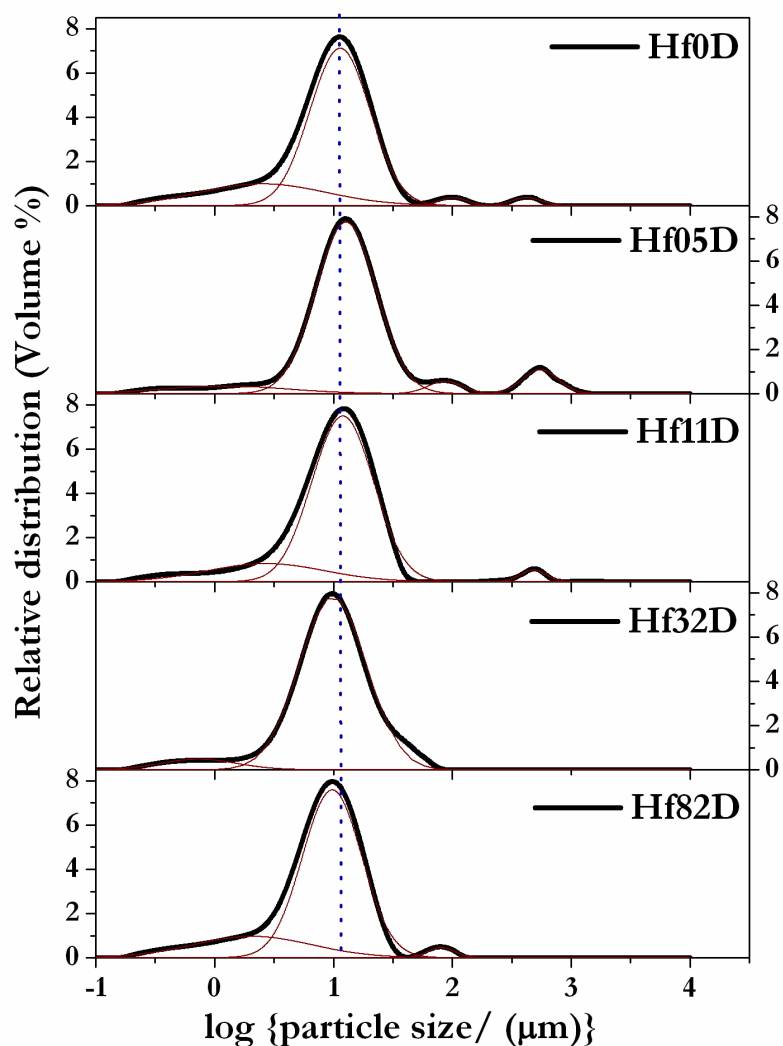


Figure 7.4 Distribution of sizes among particles in nc- $\text{HfO}_2$  powders prepared by using SMS (Thick solid lines - experimental curve and thin solid lines -deconvoluted curves)

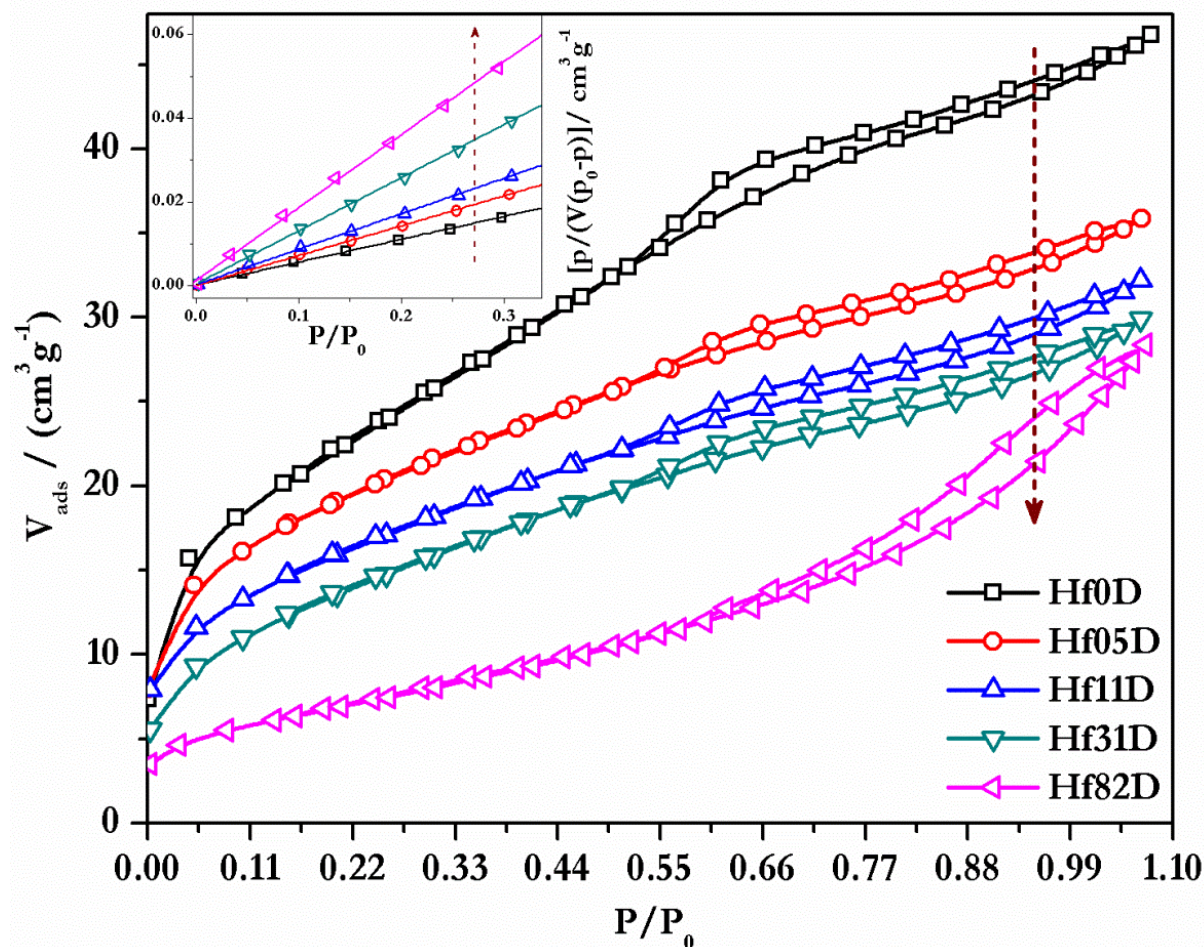


Figure 7.5 Adsorption isotherms of nc- $\text{HfO}_2$  derived through SMS, inset shows linear BET plot

The adsorption isotherms of the nc- $\text{HfO}_2$  obtained in this study are depicted in Fig. 7.5 along with their respective linear BET plots. From the hysteresis in the adsorption-desorption limbs of these isotherms, it is evident that these samples possess micropores. Further, the hysteresis patterns are identical revealing the similarity in the distribution of sizes of pores. The SSA of these nc- $\text{HfO}_2$  powders were found to vary systematically with the value of  $\Phi$  (Fig. 7.6a). The SSA is related to the grain (crystallite) size which in turn is strongly influenced by the course of the decomposition reaction. The highly oxidizing nitrate rich melts ( $\Phi = 0$ ) yield powders with a SSA of  $81 \text{ m}^2 \text{ g}^{-1}$ . When the same reaction is performed in a mixture rich in the nitrite ( $\Phi = 0.82$ ) the surface area is brought down to a value of  $25 \text{ m}^2 \text{ g}^{-1}$  (Fig. 7.6a).

During the chemical separation of the hafnium oxide from the solidified reaction mass, the latter had to be treated with propan-2-ol. Hence, the final product was found to have carbon residue of about 700 ppm (Table 7.3).

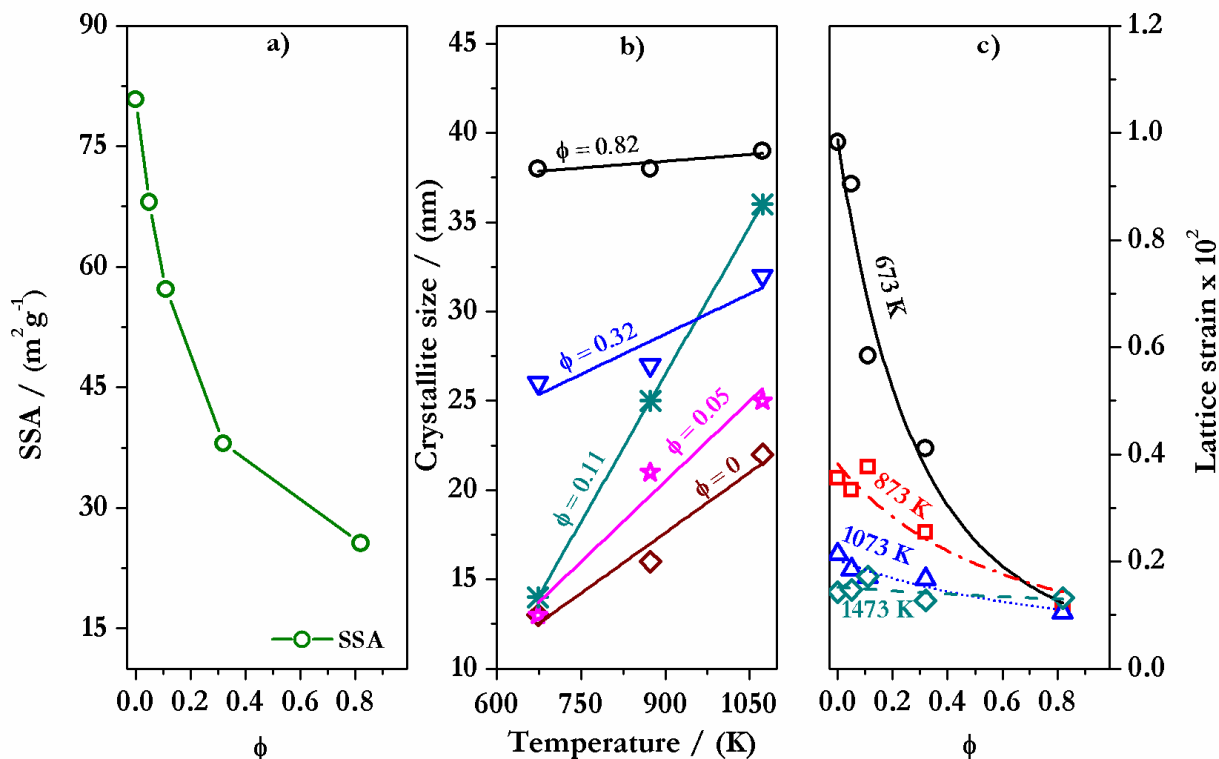


Figure 7.6 (a) Dependence of the SSA of the powders on the composition of the melt ( $\phi$ ); (b) Linear correlation of the XCS with the calcination temperature and (c) Dependence of the lattice strain on both the calcination temperature and on the value of  $\phi$

### 7.5 Phase identification, XCS, lattice strain and microstructure of nc- $\text{HfO}_2$

Hafnium oxide exists in the monoclinic form  $\text{HfO}_2$  ( $\text{P2}_1/\text{c}$ ) which is thermodynamically stable under ambient conditions [14, 15]. Above 1973 K it transforms into the tetragonal ( $\text{P4}_2/\text{nmc}$ ) phase [15] and finally takes the cubic form ( $\text{Fm}3\text{m}$ ) at temperatures above 2873 K [15]. The XRD patterns pertaining to the products obtained in this study are presented in Fig. 7.7.

All the powders synthesized in this study excepting Hf82D were found to comprise the monoclinic form of this oxide. The powder Hf82D was the cubic analogue. It retained the cubic

phase even upon further heating upto 1073 K. However, when heated at 1473 K it transformed into the monoclinic phase. Thus, for the first time the salt melt technique has been gainfully used for synthesizing metastable c-HfO<sub>2</sub> at a temperature as low as 673 K. Since this was observed only with the fusion mixture that was rich in nitrite, it is apparent that the latter aids the formation of the metastable cubic phase. Ling Gao et al. [16] synthesized Mn doped cubic HfO<sub>2</sub>, Hf<sub>1-x</sub>Mn<sub>x</sub>O<sub>2-δ</sub> with x=0.5 which was stabilized at room temperature. These authors suggested that the high temperature cubic phase is stabilized in Hf<sub>0.70</sub>Mn<sub>0.30</sub>O<sub>2-δ</sub> due to the presence of variable oxidation state of Mn ions which in turn affects the oxygen vacancy. Further, the oxidation state of Mn depends on the synthesis atmosphere and temperature. We observed the stabilization of the cubic phase, in the present study in the powders prepared from melts in which the oxygen availability is rather less compared to the rest. Further, plausibly annealing in air at high temperature restores the monoclinic form by the re-introduction of oxygen into the lattice. XRD pattern pertaining to the same powders that were heated in air at 1473 K supports this phase reversal. The HRTEM images (Fig. 7.8) show that the cubic phase is devoid of cationic inclusions. XRD patterns of c-HfO<sub>2</sub> do not show any peak splitting at higher diffraction angle which indicates that the product (cubic phase) were formed without tetragonal phase. In addition, the XRD pattern of c-HfO<sub>2</sub> does not show any asymmetry in the peaks pertaining to (200), (311) and (222). However, no evidence could be obtained to establish the oxygen stoichiometry and it is not certain if the oxygen deficiency in the melt or the sluggish reaction is responsible for the stabilization of the cubic phase. These results indicate the absence of the tetragonal phase formation and hence it could be concluded that c-HfO<sub>2</sub> phase has not been formed by the stabilization of the cubic to tetragonal phase.



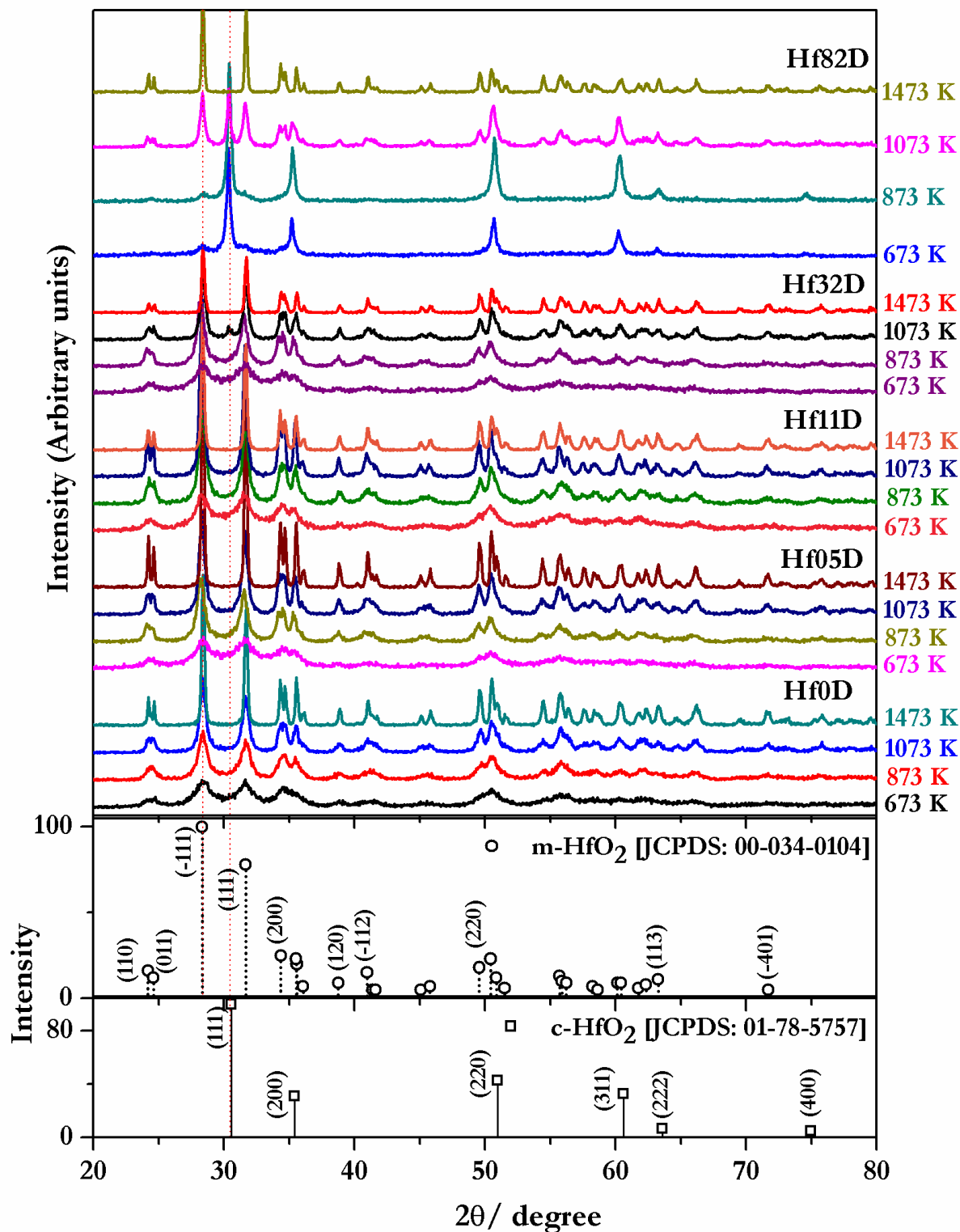


Figure 7.7 XRD pattern of the  $\text{HfO}_2$  powders derived through SMS annealed at different temperature

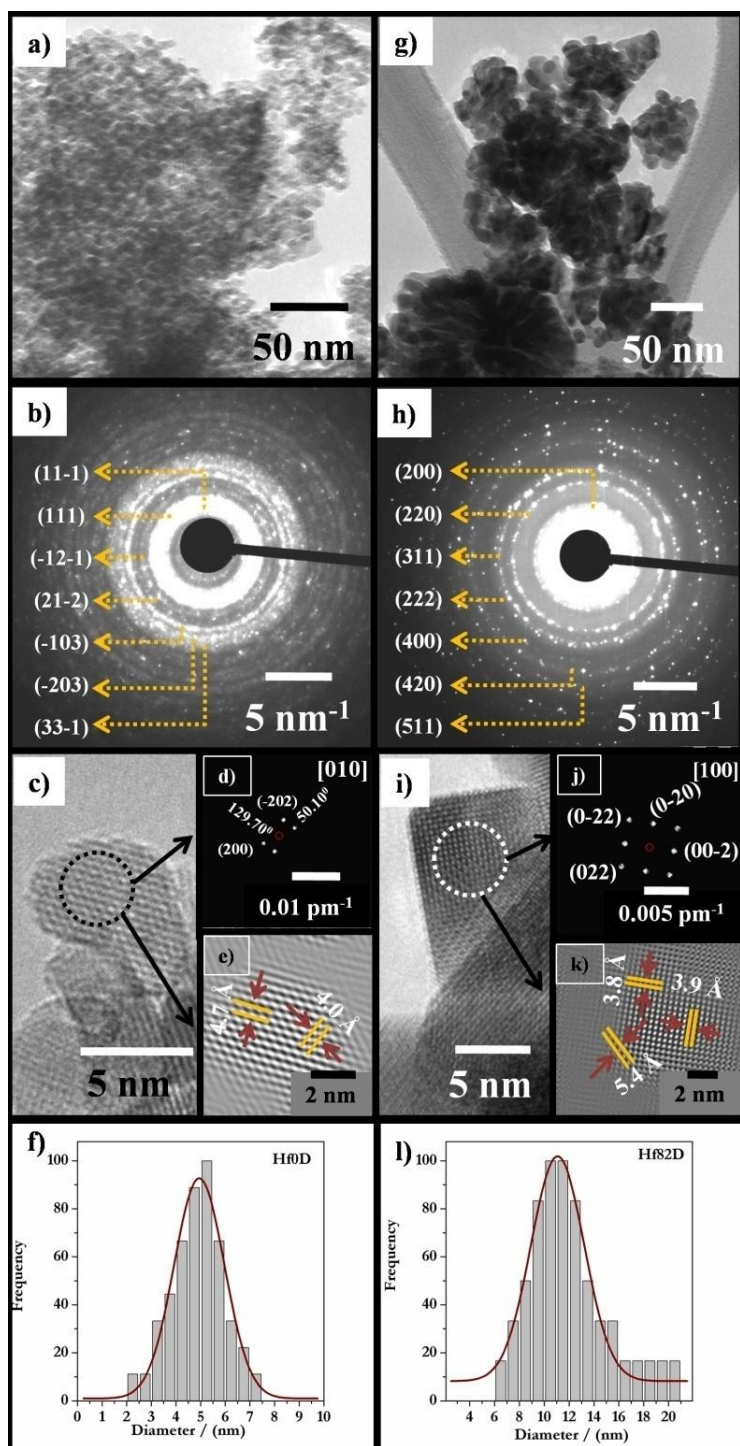


Figure 7.8 TEM images of  $\text{HfO}_2$  powders derived through SMS: [a-f]  $m\text{-HfO}_2$  (Hf0D): (a) bright image revealing nano grains; (b) SAED image; (c) HRTEM image of nano grains; (d-e) FFT and filtered IFFT image revealing zone axis [010]; (f) grain size distribution of  $m\text{-HfO}_2$  [g-l]  $c\text{-HfO}_2$  (Hf82D) (g) dark field image revealing nano grains; (h) SAED image; (i) HRTEM image of nano grains; (j-k) FFT and filtered IFFT image revealing zone axis [100]; (l) grain size distribution of  $c\text{-HfO}_2$

Analysis of X-ray diffractograms revealed that these powders were nanocrystalline. The XCS determined by using the Sc method [17] was found to be less than the estimates of the same obtained through the HW [17] analysis of the XRD data. A closer look at the values of the XCS pertaining to the powders obtained by calcination up to 1073 K reveals that the XCS increases linearly with the calcination temperature (Fig. 7.6b). In an earlier study it was observed that the XCS of nc-ThO<sub>2</sub> obtained by decomposition of thorium oxalate exhibited an exponential dependence on the calcination temperature [18]. Allred et al.<sup>1</sup> reported that the XCS of thoria derived from thorium oxalate increases exponentially with the calcination temperature. Ananthasivan et al. [18] confirmed this trend for thorium oxalate product from aqueous and non-aqueous media. Thus, it is evident that the calcination temperature strongly influences the XCS of nc-oxide powders. Nc powders would coarsen even at relatively low temperatures employed for calcining their precursors. For the hafnia powders synthesized in this study probably the threshold temperature for the onset of grain coarsening lies between 1073 K and 1473 K as evidenced by the substantial increase in the XCS, when calcined at 1473 K.

The lattice strain in the powders obtained in the present study, elucidated through HW analysis of the XRD data are presented in Table 7.3. The dependence of lattice strain on both the calcination temperature and the composition of the fusion mixture are depicted in Fig. 7.6b. From these data it is evident that the lattice strain in all these powders except Hf82D decreases progressively with both the calcination temperature and the quantity of nitrite in the melt (Fig. 7.6c). Calcination reduces the lattice strain through annealing. It is evident from the TG-DTA-MS curve (Fig. 7.3) that the formation of nc c-HfO<sub>2</sub> takes place at around 457 K. The powder Hf82D prepared from a mixture with  $\Phi = 0.82$  possesses minimum residual lattice strain which does not seem to vary significantly with the calcination temperature. Thus, when the melt

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<sup>1</sup> V. D. Allred et al. *J. Phys. Chem.*, **1957**, 61 (1), 117–120.

was maintained at 673 K for 1 h, c- $\text{HfO}_2$  had undergone both annealing as well as grain coarsening (Fig. 7.6b & 7.6c).

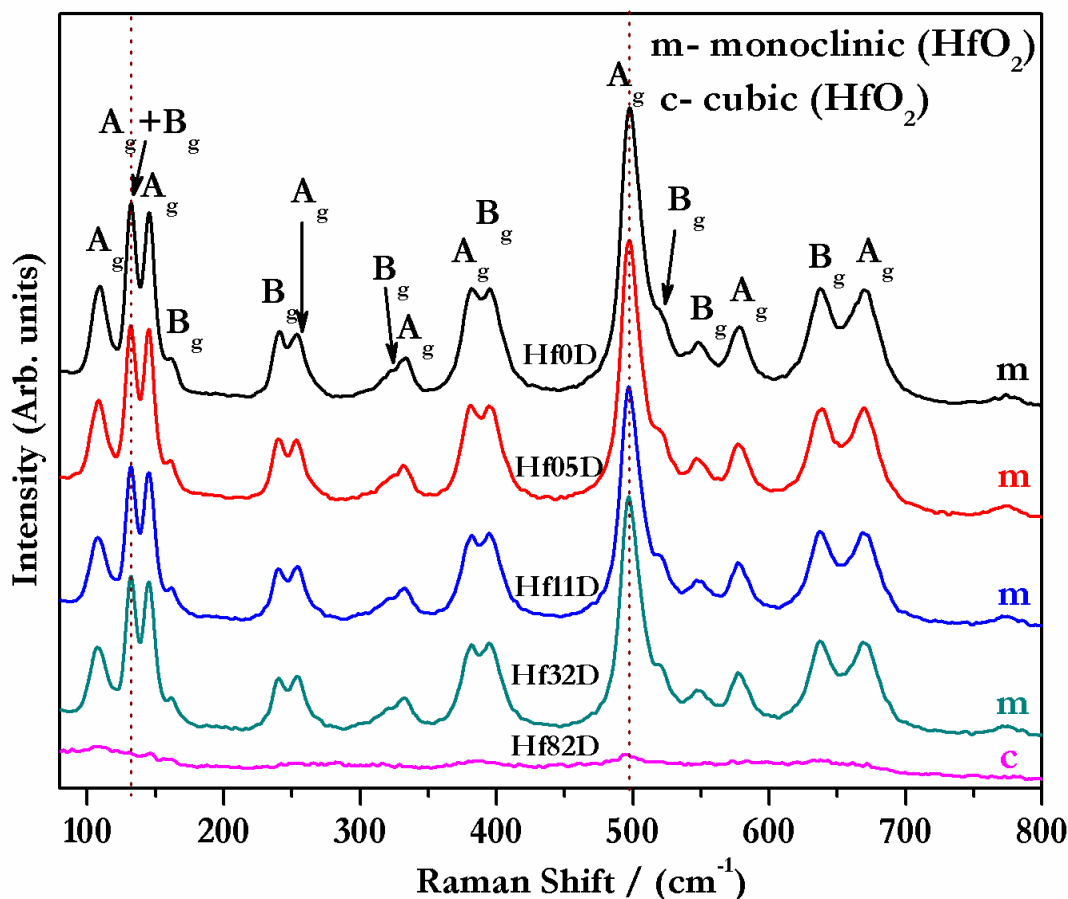


Figure 7.9 Raman spectrum of nc- $\text{HfO}_2$  powders prepared with varying  $\Phi$  value (where  $\Phi = 0, 0.055, 0.11, 0.32$  and  $0.82$ ) revealing the absence of the tetragonal phase

## 7.6 Raman spectroscopy investigations on nc- $\text{HfO}_2$

The optical phonon modes of m- $\text{HfO}_2$  (space group:  $P2_1/c$ ) [14] and c- $\text{HfO}_2$  (space group:  $Fm3m$ ) [14] were obtained by using group theoretical analysis [19, 20]:

$$\Gamma(\text{Monoclinic}) = 9A_g(\text{R}) + 9B_g(\text{R}) + 8A_u(\text{IR}) + 7B_u(\text{IR}) + 2B_u(\text{a}) + A_u(\text{a}) \quad (7.8)$$

$$\Gamma(\text{Cubic}) = F_{2g}(\text{R}) + F_{2u}(\text{IR}) + F_{1u}(\text{a}) \quad (7.9)$$

where: R = Raman mode; IR = Infrared mode and a = Acoustic mode. The unit cell contains 4 formula units that result in 36 degrees of freedom. Since all modes in the monoclinic phase are

non-degenerate 18 Raman bands are expected. The c-HfO<sub>2</sub> unit cell contains only 1 formula unit; leading to 3 phonon modes [a Raman active mode, an Infrared active mode and an acoustic mode]. Raman spectra (Fig. 7.9) of all nc-hafnia powders (except Hf82D) are similar to those reported in the literature [19, 21, 22] for m-HfO<sub>2</sub>. Additionally, the Raman shifts observed in this study for the nanocrystalline m-HfO<sub>2</sub> are in agreement with the data presented in Ref. [23]. Studies by Rui Wu et al. [19] showed that the band observed at 133 cm<sup>-1</sup> in m-HfO<sub>2</sub> is due to overlapping of the bands at 134 cm<sup>-1</sup> (A<sub>g</sub>) and 131 cm<sup>-1</sup> (B<sub>g</sub>) and cannot be resolved by a conventional instrument. Nanocrystalline m-HfO<sub>2</sub> powders prepared in this study also exhibit a Raman band at 132 cm<sup>-1</sup> that could be due to the combination of two frequencies mentioned above. Nanocrystalline c-HfO<sub>2</sub> powders prepared in this study do not show any Raman active mode in the spectrum. The increased width of the Raman bands (from 10 cm<sup>-1</sup> for the bulk to 18.98 cm<sup>-1</sup> for the present sample) is indicative of phonon confinement effects.

### **7.7 Microstructural investigation on nc-HfO<sub>2</sub>**

Microstructural characterization (TEM) of the m-HfO<sub>2</sub> and c-HfO<sub>2</sub> powders further ascertained that these powders comprised grains with uni-modal distribution of size [Hf0D: 3-8 nm and Hf82D: 6-21 nm] (Fig. 7.8). The SAED patterns confirmed the presence of m-HfO<sub>2</sub> - P2<sub>1</sub>/c [14] - (Hf0D) and c-HfO<sub>2</sub> - Fm3m [14] - (Hf82D). SAED image also confirmed their nanocrystallinity (Fig. 7.8).

The d-spacings derived from the diffraction patterns were comparable to the standard JCPDS pattern [m-HfO<sub>2</sub> – PDF No. 00-034-0104; c-HfO<sub>2</sub> – PDF No. 01-078-5757]. Both bright and dark field images revealed the presence of nanograins. The HRTEM images (Fig. 7.8) of these samples depict the values of the “d” spacing that are in agreement with the values (JCPDS)

mentioned above. The Fast Fourier Transform images (FFT) of both m- $\text{HfO}_2$  and c- $\text{HfO}_2$  were comparable with the FFT image generated with appropriate zone axes.

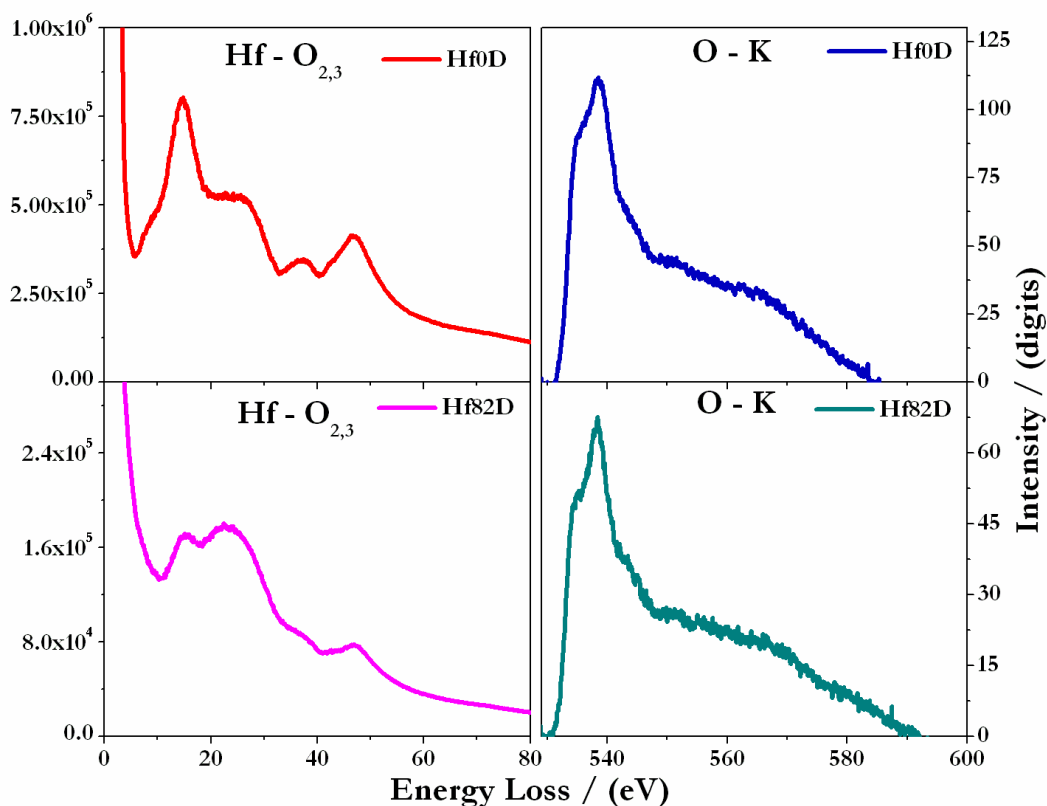


Figure 7.10 EELS of m- $\text{HfO}_2$  ( $\Phi = 0$ ) and c- $\text{HfO}_2$  ( $\Phi = 0.82$ ) powders depicting  $\text{O}_{2,3}$ , O-K and Hf- $\text{M}_{4,5}$  edges

EELS was used to understand the characteristics of the bonding in nc- $\text{HfO}_2$  [m- $\text{HfO}_2$  (Hf0D) and c- $\text{HfO}_2$  (Hf82D)] (Fig. 7.10). Presence of oxygen defects [24], crystallinity [25, 26] and cationic inclusions [26] in the unit cell will influence the characteristics of the EEL spectrum at both low and high loss regions [26]. Hence, EEL spectra of the nc-hafnia powders prepared in this study were compared and analyzed with that of the microcrystalline sample. In the low loss region, O-K edge and  $\text{M}_{4,5}$  edges in the samples (m- $\text{HfO}_2$  and c- $\text{HfO}_2$ ) reveal that the peaks are broad and the energy corresponding to the onset of these peaks are shifted compared to that observed in the bulk sample (annealed at high temperature-1273K) [27]. Rauwel et al. [26] have reported that the reduction in peak intensities and shift in peak onset could plausibly be due to

the presence of oxygen vacancies and nano size (quantum confinement). Thus, these observations further suggest the presence of oxygen vacancies. Mizoguchi et al. [28] reported the partial density of states (pDOS) on O-K edge in the three polymorphs (monoclinic, tetragonal and cubic form) of HfO<sub>2</sub>. Calculation pertaining to pDOS [28] shows that the O-K edge observed in both the cubic and tetragonal phase is sharp as compared to that in the monoclinic phase. This variation has been ascribed to the octahedral (O<sub>h</sub>) symmetry [26, 28, 29]. In c-HfO<sub>2</sub>, the tetrahedral (T<sub>d</sub>) oxygen is coordinated to 4 Hf atoms while the m-HfO<sub>2</sub> contains two different O atoms coordinated with 3 and 4 Hf atoms respectively [26, 28, 29]. The low loss and O-K edge fine splitting would not be visible in an EEL spectrometer with an energy resolution of 0.6 eV [26]. In this study, m-HfO<sub>2</sub> exhibited a broad peak (O-Kedge) with maxima at 538.8 eV, while c-HfO<sub>2</sub> exhibited a sharp peak with maxima at 538.4 eV. A closer look at the O-Kedge in c-HfO<sub>2</sub> shows that it comprises two peaks, which when resolved through deconvolution is shown to comprise two peaks with their maxima at 534.8 eV and 538.4 eV. These values are in good agreement with the values reported in the literature [29]. Hf M<sub>4,5</sub> edges in m-HfO<sub>2</sub> are observed at 1684 eV and 1699 eV while for c-HfO<sub>2</sub> they are found at 1684 and 1697 eV. In general it was observed that the intensities of all the peaks in the powder Hf0D (m-HfO<sub>2</sub>) were higher than those in the powder Hf82D (c-HfO<sub>2</sub>). Since the EEL spectrum corresponding to Hf<sup>4+</sup> occurs in the higher energy range ( $\approx$ 1700 eV) it was not possible to resolve it to delineate the contributions from Hf in other oxidation states.

## **7.8 Compaction and sintering of nc-HfO<sub>2</sub>**

### **7.8.1 Green density ( $\rho_G$ )**

In order to enhance densification in nc powders and to obtain compacts with uniform microstructure, the characteristics of the powders used for making green compacts need to be

appropriately tailored. In general the  $\rho_G$  of all the powders were nearly identical, probably due to similar size distribution of particles, in the latter. The relative  $\rho_G$  of hafnia pellets exhibit a linear positive correlation ( $38.1 \pm 0.7$  % T.D to  $54.8 \pm 0.5$  % T.D) with the CP (60 to 353 MPa) (Table 7.4 and Fig. 7.11a) and nitrite content in the salt mixture. In addition, these nc powders could not be compacted to a very high density owing to higher frictional resistance [30-32]. Further, the powder Hf32D yielded green compacts with a higher density which could be due to the presence of excess fine fraction of particles. Chaim et al. [32] had reported that the particle which deviates from sphericity would require higher CP as compared to spherical particles owing to the presence of large interparticle frictional force in the former. The particles in the powder Hf82D were cuboidal and faceted, while the rest of the powders comprised irregular particles. Thus, it is reasonable to assume that a higher degree of “asphericity” in the Hf82D powders could have led to a lower  $\rho_G$ .

**Table 7.4  $\rho_G$  of HfO<sub>2</sub> derived through salt melt synthesis**

CP	Hf0D	Hf05D	Hf11D	Hf32D	Hf82D
(MPa)	% T.D				
60	$41.2 \pm 0.9$	$38.1 \pm 0.7$	$39.6 \pm 0.3$	$44.1 \pm 0.5$	$39.4 \pm 0.3$
120	$43.8 \pm 0.2$	$41.9 \pm 0.5$	$43.0 \pm 0.3$	$46.7 \pm 0.6$	$42.5 \pm 0.3$
180	$46.5 \pm 0.2$	$44.1 \pm 0.3$	$45.4 \pm 0.4$	$48.6 \pm 0.7$	$43.6 \pm 0.6$
244	$48.4 \pm 0.7$	$46.3 \pm 0.6$	$47.6 \pm 0.9$	$50.3 \pm 0.6$	$45.4 \pm 0.4$
317	$50.3 \pm 0.3$	$48.2 \pm 0.9$	$49.4 \pm 0.3$	$52.3 \pm 0.5$	$47.3 \pm 0.6$
353	$51.9 \pm 0.5$	$49.0 \pm 0.5$	$50.2 \pm 0.7$	$54.8 \pm 0.5$	$47.9 \pm 0.2$



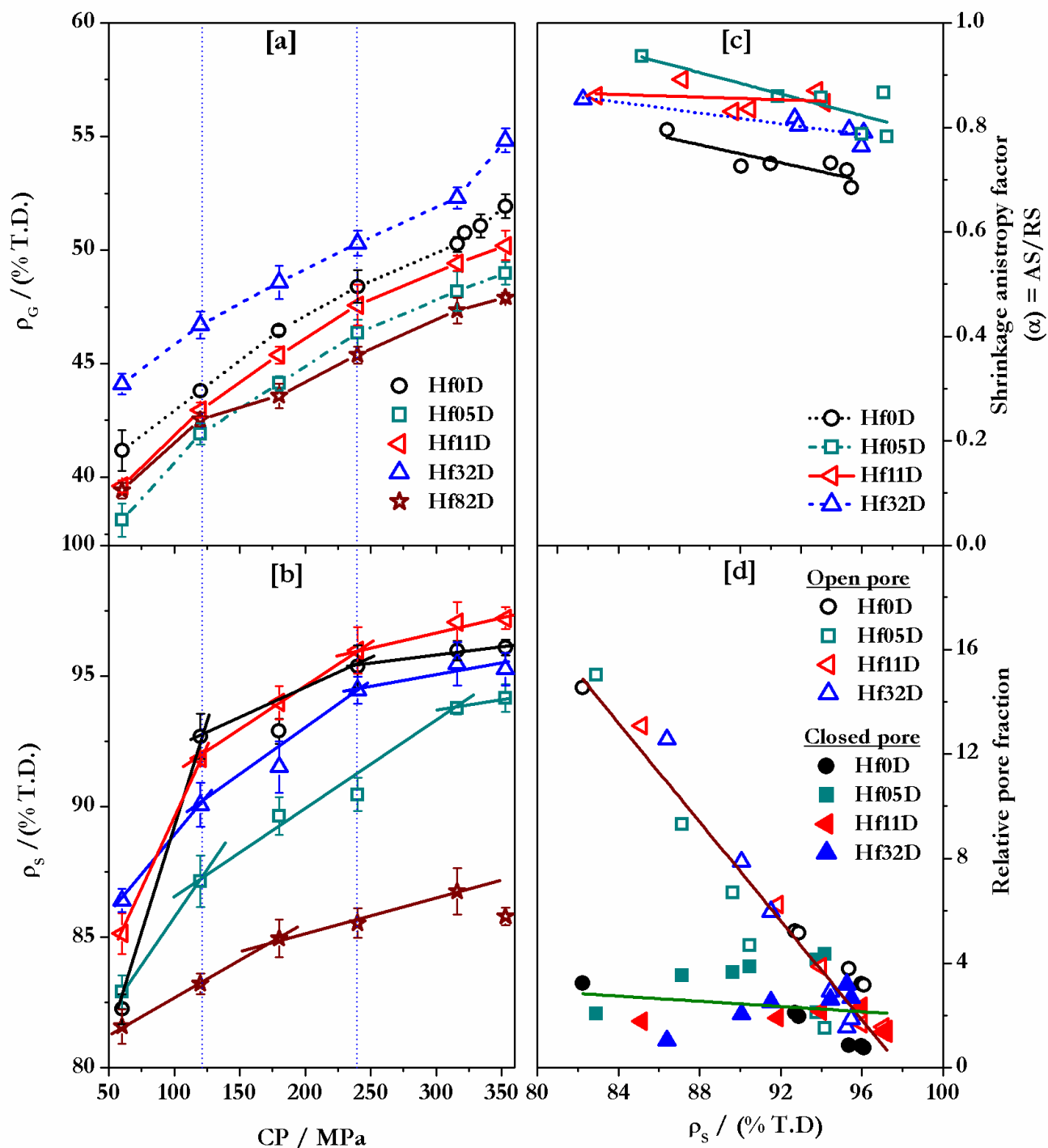
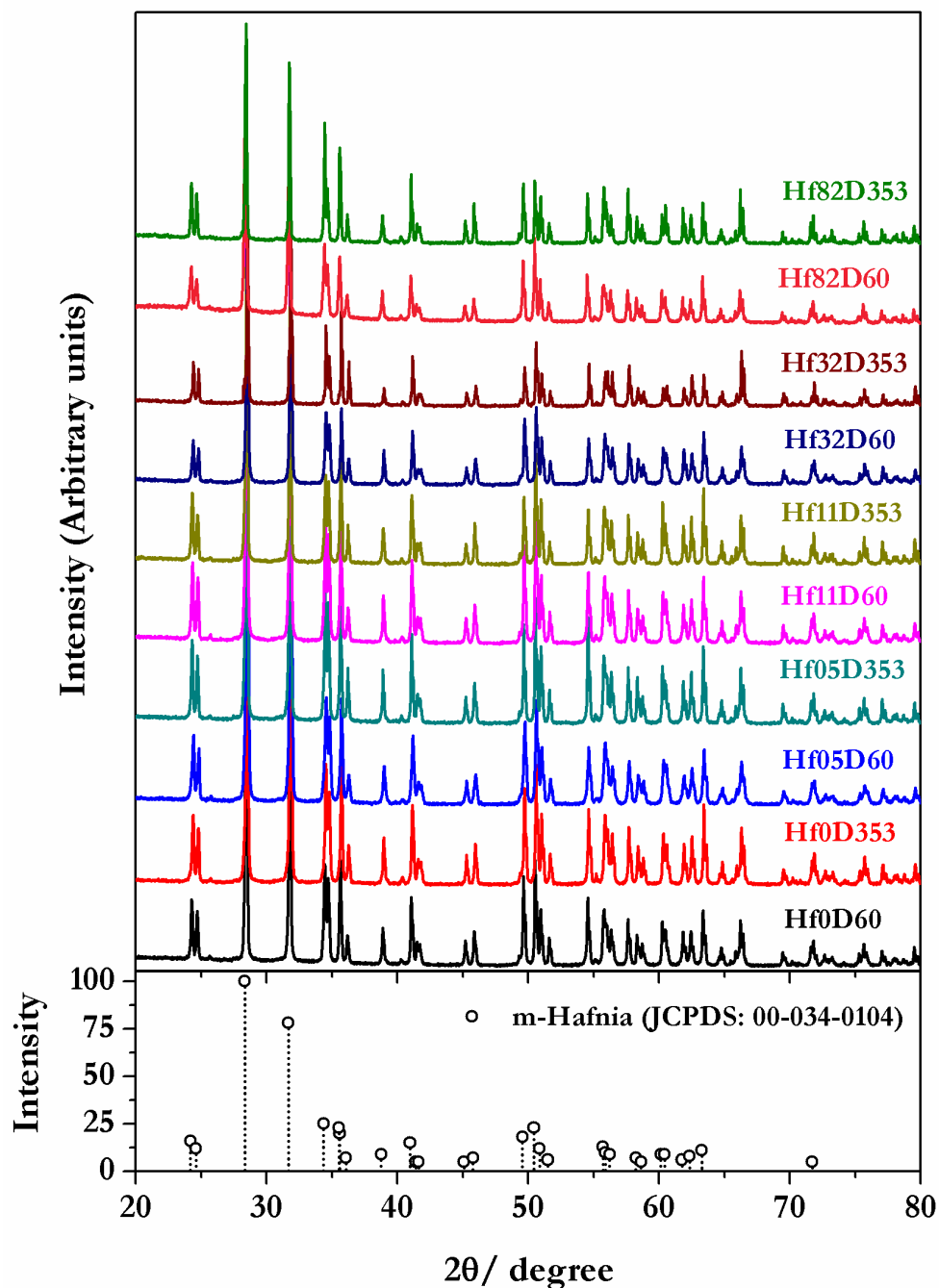


Figure 7.11 Variation of (a)  $\rho_G$  and (b)  $\rho_s$  with the CP; (c) variation of shrinkage anisotropy factor ( $\alpha$ ) with the  $\rho_s$  and (d) dependence of pore fraction on the  $\rho_s$

Figure 7.12 XRD of sintered  $\text{HfO}_2$  monoliths

### 7.8.2 Phase characterization and carbon residue in sintered hafnia monoliths

Selected samples of sintered hafnia monoliths were analyzed by using XRD (Fig. 7.12), which revealed that they comprised the thermodynamically stable, room temperature, monoclinic phase. The XRD analysis further reaffirms that even though the powders Hf82D initially

comprised the cubic phase at the end of the sintering cycle they had reverted back to the thermodynamically stable m-HfO<sub>2</sub> phase. The XRD patterns are indexed appropriately by comparing them with those reported in JCPDS (m-HfO<sub>2</sub> - JCPDS No. 00-034-0104). According to the ASTM (C1076-09 [33]) specification, hafnia to be used in nuclear applications should contain carbon residue below 1000 ppm. Selected samples of sintered hafnia monoliths were analyzed for carbon residue and it was observed that it was varying between 81 to 151 ppm. Hence, this procedure could be deployed for the production of nuclear grade HfO<sub>2</sub>.

### **7.8.3 Sintering and microstructural investigations on HfO<sub>2</sub> monoliths**

To optimize the sintering, selected samples of hafnia powders were compacted at 317 MPa and were sintered by using both CS (HfYD<sub>CS1</sub>, HfYD<sub>CS2</sub> and HfYD<sub>CS3</sub>) and TSS (TSS<sub>1</sub> and TSS<sub>2</sub>) procedures (Chapter 2). The  $\rho_s$  are presented in Tables 7.5 & 7.6. These data reveal that the monoliths derived through TSS<sub>2</sub> method had sintered better as compared to those subjected to CS. Hence, all the hafnia powders were compacted at 60, 120, 180, 244, 317 and 353 MPa and were sintered in air by using the TSS<sub>2</sub> method.

The characteristics of the sintered pellets derived through TSS<sub>2</sub> are presented in Table 7.6 and in Fig. 7.11b. In general, it was observed that all the hafnia compacts (except Hf82D) had undergone better densification when sintered by using the TSS<sub>2</sub> method. The TSS<sub>2</sub> method with final sintering temperature of 1773 K and a CP of 353 MPa yield monoliths with a high  $\rho_s$  ( $94.2 \pm 0.5$  T.D to  $97.2 \pm 0.4$  % T.D). It was observed that Hf0D and Hf11D compacts had undergone higher densification as compared to all other compacts. Their  $\rho_s$  were found to be almost identical and were independent of the CP. The  $\rho_s$  values of Hf32D were found to be marginally higher than that of Hf05D owing to a higher  $\rho_G$  of the former. Hf82D compacts had yielded monoliths with  $\rho_s$  ranging between  $81.6 \pm 0.7$  % to  $86.6 \pm 0.9$  % T.D. These values are indeed much lower as compared to that of the rest.

**Table 7.5 Sintering parameters and  $\rho_s$  of HfO<sub>2</sub> (317 MPa; CS and TSS method)**

Sample	$\rho_G$	$\rho_S$				
		$CS_1$	$CS_2$	$CS_3$	$TSS_1$	$TSS_2$
		$HfYD_{CS1}$	$HfYD_{CS2}$	$HfYD_{CS3}$	$HfYDS_1$	$HfYDS_2$
		% T. D.				
Hf0D	$50.3 \pm 0.3$	$90.5 \pm 0.6$	$91.4 \pm 0.2$	$94.1 \pm 0.6$	$94.9 \pm 0.3$	$96.0 \pm 0.4$
Hf05D	$48.2 \pm 0.9$	$89.0 \pm 0.1$	$90.4 \pm 0.2$	$92.2 \pm 0.3$	$92.9 \pm 0.2$	$93.8 \pm 0.3$
Hf11D	$52.3 \pm 0.5$	$91.1 \pm 0.7$	$91.3 \pm 0.2$	$94.8 \pm 0.5$	$95.1 \pm 0.5$	$97.1 \pm 0.8$

$$Y = \Phi^* 100$$

CP - 317 MPa   CS<sub>1</sub> - 1673 K 4 h   CS<sub>2</sub> - 1773 K 4 h   CS<sub>3</sub> - 1873 K 4 h   TSS<sub>1</sub>   Step 1 - 1873 K 1 h  
Step 2 - 1673 K 4 h   TSS<sub>2</sub>   Step 1 - 1873 K 1 h  
Step 2 - 1773 K 4 h

**Table 7.6 Characteristics of sintered HfO<sub>2</sub> monoliths derived through TSS<sub>2</sub> method**

CP (MPa)	Hf0D	Hf05D	Hf11D	Hf32D	Hf82D
	% T.D				
<b>60</b>	82.2 ± 0.6	82.9 ± 0.6	85.1 ± 0.8	86.4 ± 0.4	81.6 ± 0.7
<b>120</b>	92.7 ± 0.9	87.2 ± 0.1	91.8 ± 0.1	90.1 ± 0.8	83.2 ± 0.4
<b>180</b>	92.9 ± 0.5	89.6 ± 0.7	94.0 ± 0.6	91.5 ± 0.9	85.0 ± 0.7
<b>244</b>	95.4 ± 0.8	90.5 ± 0.6	96.0 ± 0.9	94.5 ± 0.5	85.5 ± 0.6
<b>317</b>	96.0 ± 0.4	93.8 ± 0.3	97.1 ± 0.8	95.5 ± 0.8	86.6 ± 0.9
<b>353</b>	96.1 ± 0.3	94.2 ± 0.5	<b>97.2 ± 0.4</b>	95.3 ± 0.6	85.8 ± 0.3

These monoliths Hf82D were found to have undergone significant “warping” and had cracks on the pellet surface. Cubic HfO<sub>2</sub> reverts to the monoclinic form at around 1073 K. Recently Piluso et al. [15, 34] had reported that the phase transformation of hafnia crystals is accompanied by a volumetric expansion of about 3.4 % (from the tetragonal to monoclinic phase upon cooling) which induces cracks. Thus, from the above discussion it is evident that the phase transformation from the metastable cubic to the stable monoclinic phase is responsible for the poor sinterability of Hf82D.

The shrinkage anisotropy factor ( $\alpha$ ) [35] and relative pore fraction (ratio of open/closed porosity to that of total porosity) were measured to understand the extent of densification and to evaluate the quality of the final sintered product (Fig. 7.11c & Fig. 7.11d). The desirable value of relative pore fraction is less than 2 % while that of shrinkage anisotropy factor is 1. Dependence of the relative pore fraction on  $\rho_s$  reveals that the open pore fraction decreases while the closed pore fraction increases (marginally) with the  $\rho_s$  (Fig. 7.11d). Fig. 7.11d also reveals that the fraction of both open and closed pores becomes nearly equal at around 96 % T.D. Further, this plot reveals that the removal of closed pores from hafnia monolith is tedious and to remove the residual porosity further optimization is necessary. The shrinkage anisotropy factor ( $\alpha$ ) [35] of hafnia monoliths were found to be linearly correlated with their  $\rho_s$  (Fig. 7.11c).

Microstructures of sintered hafnia pellets (Hf0D; 60 MPa and Hf0D; 353 MPa) are shown in Fig. 7.13. The SEM images reveal that the hafnia monoliths compacted at 60 MPa (Fig. 7.13a -b) exhibit both intra and intergranular pores on both the polished as well as the fractured surfaces. The hafnia monoliths derived from the greens compacted at 353 MPa showed the presence of faceted grains with dihedral angles ranging between 109° to 130° (Fig. 7.13d-e). The values of the dihedral angle suggest that sintering has proceeded nearly up to the “final stage”

[35, 36]. The polished surfaces also showed the presence of well defined grain boundaries with grain size ranging between  $1\ \mu\text{m}$  to  $3\ \mu\text{m}$ . Point scan by using energy dispersive X-ray analysis of sintered hafnia monoliths revealed that it comprised only hafnia and was devoid of any other impurity.

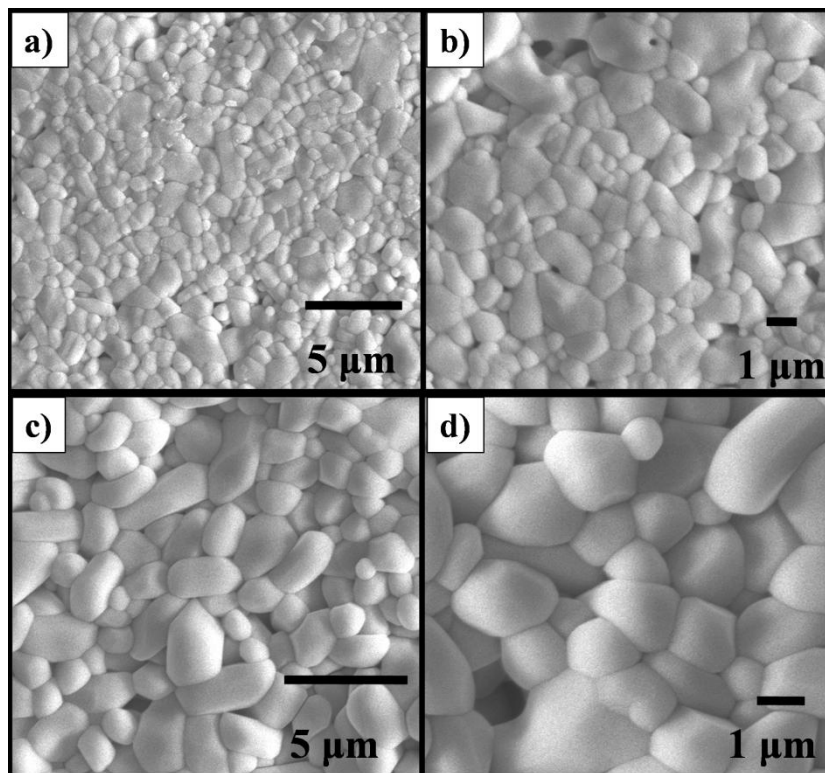


Figure 7.13 Sintered  $\text{Hf0D}$  (a-b) 60 MPa and (c-d) 353 MPa; SEM images of  $\text{Hf0D}$  (a & c) low magnification image of 60 MPa and 353 MPa monoliths; (b & d) high magnification image of 60 MPa and 353 MPa monoliths

#### 7.8.4 Crucibles from nc- $\text{HfO}_2$

It was observed that nc- $\text{HfO}_2$  powders compacted at 353 MPa pressure and sintered by using  $\text{TSS}_2$  had yielded monoliths with the highest  $\rho_s$ . By using this method the powders  $\text{Hf0D}$  and  $\text{Hf11D}$  could be sintered to a maximum density of about 96 % T.D. Hence, these two powders were chosen for making crucibles. The powders  $\text{Hf0D}$  and  $\text{Hf11D}$  were compacted at 353 MPa and sintered by using  $\text{TSS}_2$  method. The sintered densities of  $\text{Hf0D}$  and  $\text{Hf11D}$  crucibles were found to be  $95.8 \pm 0.3\%$  T.D and  $97.0 \pm 0.1\%$  T.D respectively. It was observed

that these sintered crucibles were devoid of any visual defects viz., cracks, chipping, deformation and end-capping (Fig. 7.14). These crucibles were parted and were subjected to microstructural analysis by using SEM. The fractured surfaces were found to possess grains with sizes ranging between 1 – 4  $\mu\text{m}$ . Both Hf0D and Hf11D sintered crucibles could be used for melting uranium bearing alloys. Hf11D crucibles are more suitable for they contain a lesser porosity (< 3%).

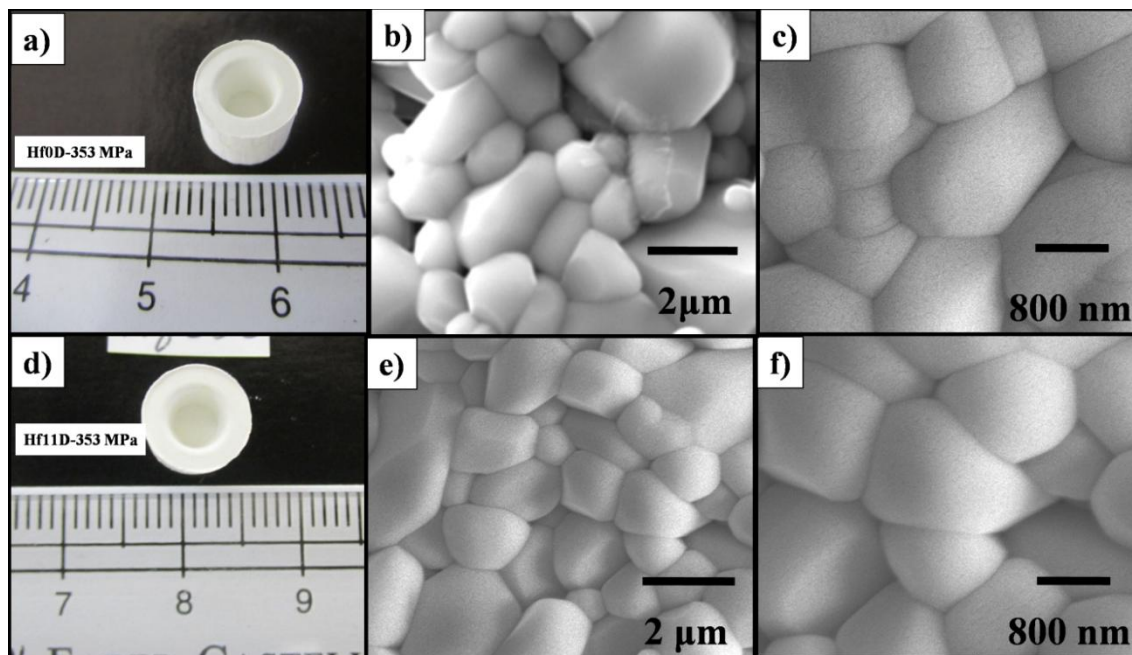


Figure 7.14 (a-c) Hf0D sintered cup derived with 353 MPa pressure and (d-f) Hf11D derived with 353 MPa pressure; (a and d) photograph of sintered hafnia crucibles and (b and e) low magnification SEM image fractured surfaces of sintered  $\text{HfO}_2$  crucibles and (c & f) high magnification SEM image fractured surfaces of sintered hafnia crucibles

## 7.9 Conclusions drawn from the preparation of nc- $\text{HfO}_2$ by SMS and its sintering

For the first time nc powders of metastable c- $\text{HfO}_2$  was prepared by the SMS. It was also demonstrated that either the metastable cubic form or the thermodynamically stable monoclinic form could be derived at room temperature by tailoring the composition of the melt.

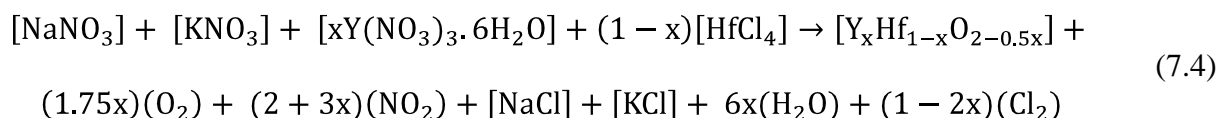
The addition of nitrite to the salt melt mixture probably brings about a reduction in the oxygen potential of the melt which in turn controls the reaction kinetics as well as the characteristics of the product. The SSA and lattice strain decreased with the nitrite content while

the XCS showed a reverse trend. Microstructural analysis of these powders by using TEM reaffirmed their nanocrystallinity as well as their crystallite size estimated from XRD (20 to 40 nm). Further, both XRD and Raman spectra ascertained that the starting mixtures with  $\Phi$  values of 0 - 0.32 and 0.82 yielded m-HfO<sub>2</sub> and c-HfO<sub>2</sub> respectively. Comparison of the Raman spectra pertaining to both microcrystalline and nc samples revealed that the latter exhibited broader peaks due to quantum confinement. EELS of m-HfO<sub>2</sub> ( $\Phi = 0$ ) and c-HfO<sub>2</sub> ( $\Phi = 0.82$ ) were consistent with the observations made in the other investigations. However, further direct evidence in support of the presence of Hf in an oxidation state lower than 4+ could not be obtained.

A CP of 353 MPa was required to compact and sinter hafnia to a  $\rho_s$  of  $97.2 \pm 0.4$  % T.D by using TSS<sub>2</sub> method. Point scan (EDS) of hafnia powders and sintered monoliths did not reveal the presence of any impurity. Morphological analysis of polished and thermally etched sintered monoliths revealed the presence of uniform grains with well-defined grain boundaries. The dihedral angle in sintered hafnia monoliths was found to be varying between 119-130°. Shrinkage anisotropic factor ( $\alpha$ ) revealed that the hafnia compacts had undergone near isotropic shrinkage. Small crucibles made out of both Hf0D and Hf11D were devoid of visual cracks and physical defects.

### **7.10 Salt melt synthesis and two-step sintering of nc-YSH powders**

The reaction observed in the preparation of YSH through SMS was quite similar to those observed in the preparation of HfO<sub>2</sub>. The generalized equation pertaining to the salt melt synthesis of nanocrystalline YSH powders could be written as given in eqn. (4):





The XRD pertaining to YSH containing 6 mol% of yttrium indicated the presence of both m- $\text{HfO}_2$  and c-YSH phase whereas nc-YSH powders containing 10-30 mol % yttrium revealed the presence of only the cubic phase.

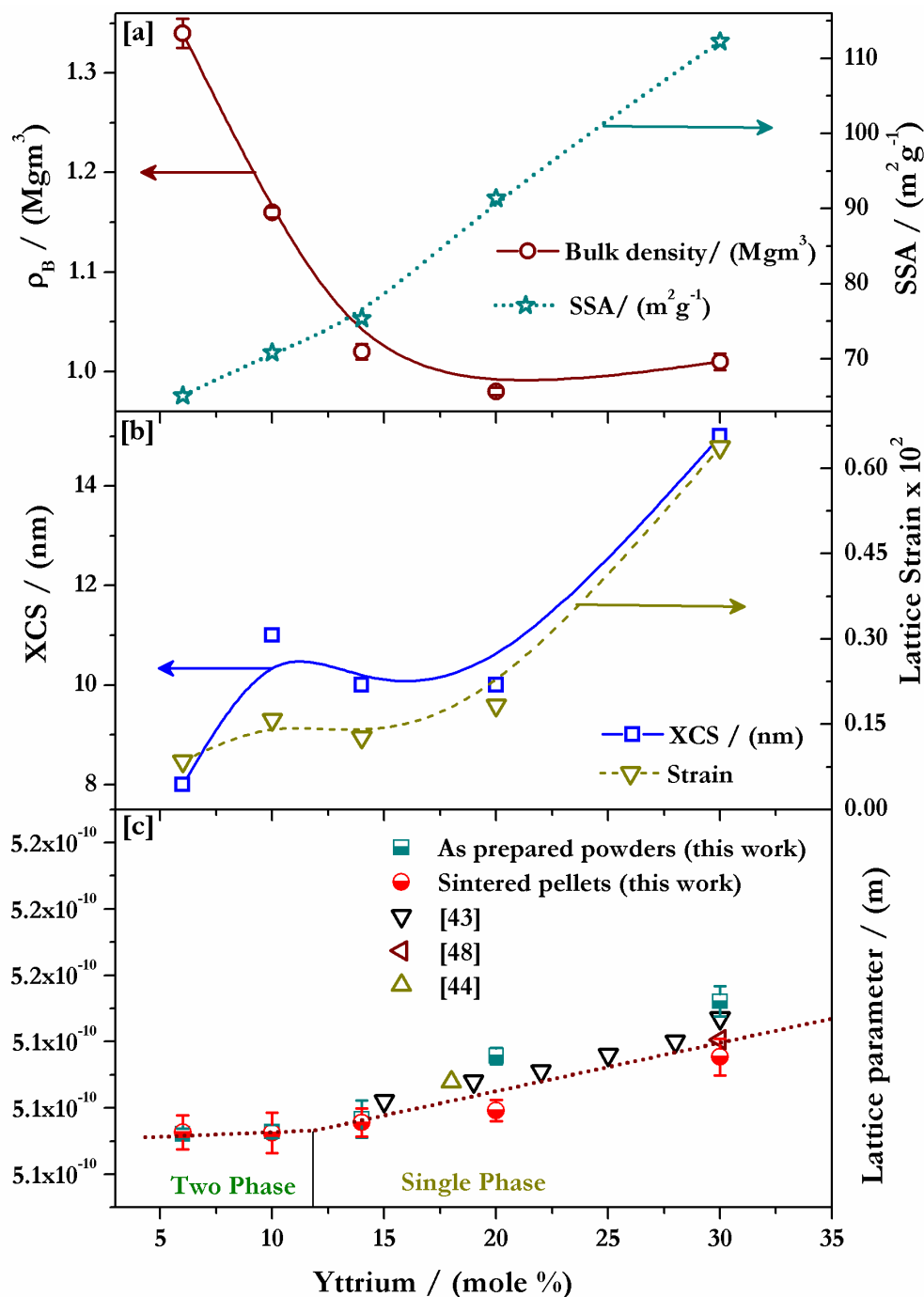


Figure 7.15 (a) Dependence of the  $\rho_B$  and SSA with yttrium content; (b) Dependence of XCS and lattice strain with yttrium content; (c) variation of lattice parameter with yttrium (mole %)

**Table 7.7 Characteristics of nc-YSH powders**

Sample	$\rho_B$ (Mg m <sup>-3</sup> )	RC (ppm)	SSA (m <sup>2</sup> g <sup>-1</sup> )	XCS (nm)			Particle size distribution		
							10 vol. % of sample has size less than (μm)	50 vol. % of sample has size less than (μm)	90 vol. % of sample has size less than (μm)
				Sc	HW	Strain x10 <sup>-2</sup>			
6YSH	1.34	415	65	7	8	0.085	4	12	38
10YSH	1.16	263	71	9	11	0.158	5	16	47
14YSH	1.02	425	75	9	10	0.127	4	14	38
20YSH	0.98	485	91	8	10	0.183	5	17	49
30YSH	1.01	451	112	7	15	0.637	7	21	80

### 7.11 Bulk density ( $\rho_B$ ), PSD and SSA

The powder characteristics of nc-YSH powders are presented in Table 7.7. The  $\rho_B$  of the nc-YSH powders decreases exponentially with the yttrium content (Fig. 7.15a). The decrease in  $\rho_B$  with the quantity of dopant was found to be more pronounced up to a dopant concentration of 14 mole % Y, beyond which there was no appreciable change. This variation in  $\rho_B$  could be due to the variation in the size distribution of particles (Fig. 7.16). From the Fig. 7.16 it is evident that all YSH powders exhibit bimodal size distribution of particles with the maximum size fraction at around 10  $\mu\text{m}$  (about 81 % of the fraction of particles possessed an average size of 10  $\mu\text{m}$ ).

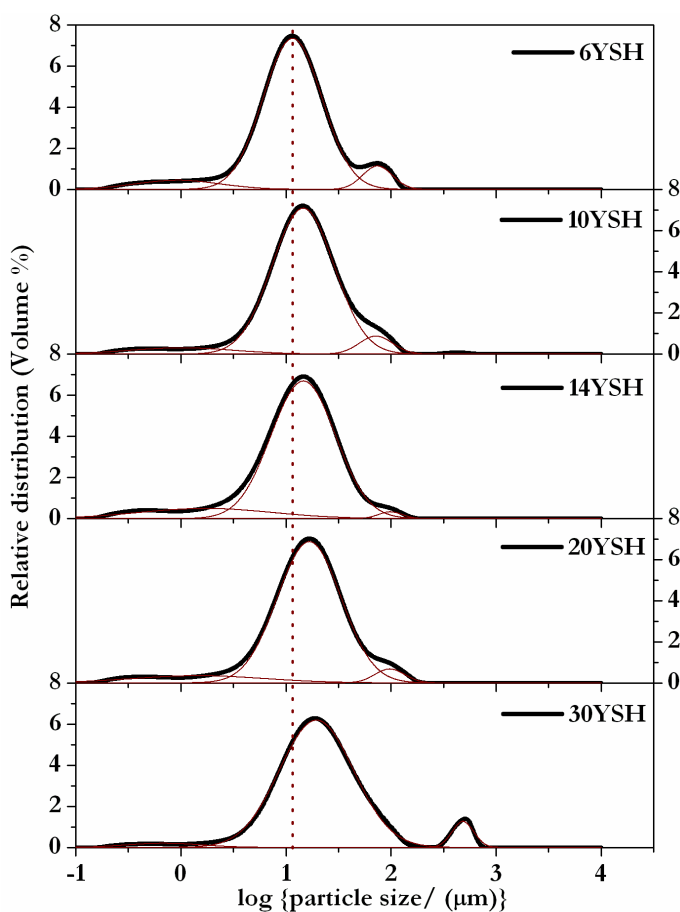


Figure 7.16 Size distribution of particles in nc-YSH powders (Thick solid lines – experimental curve, thin solid line – deconvoluted curves)

It is evident from Fig. 7.16 that 6YSH powders possess two size fractions of particles (lower fraction:  $\approx 92\%$  and higher fraction:  $\approx 8\%$ ). All other powders exhibited a “near unimodal” size distribution of particles. A closer observation reveals that increase in the yttrium content shifts the peak maxima towards a higher size fraction (Fig. 7.16).

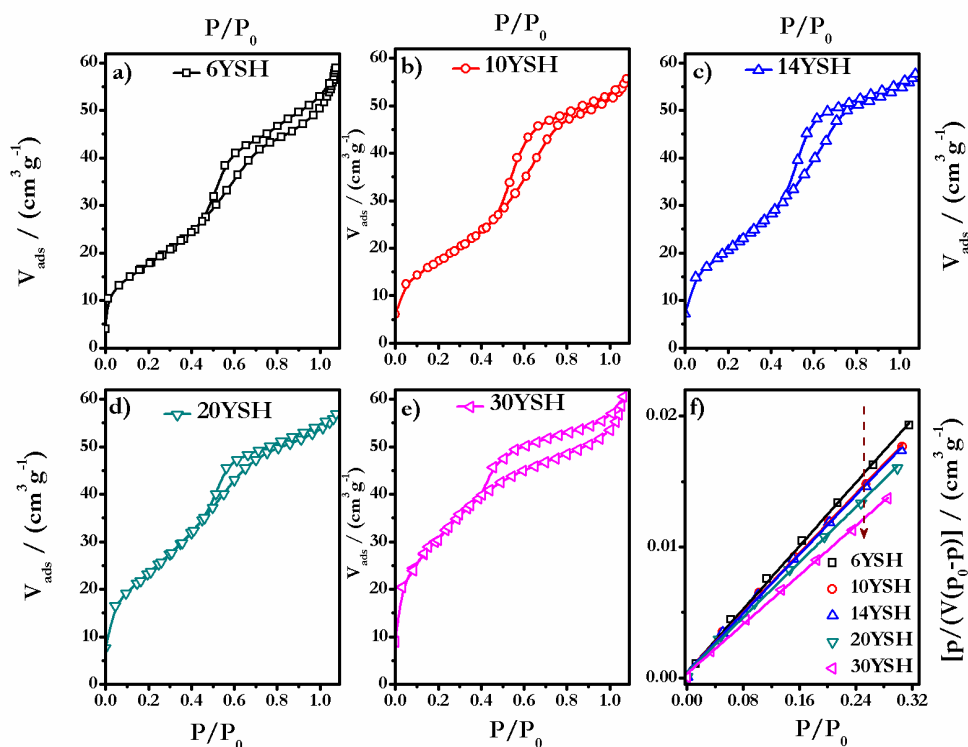


Figure 7.17 (a-e) BET adsorption isotherm of nc-YSH derived through SMS and (f) linear BET adsorption isotherm

All the YSH powders possessed high SSA ( $65$  to  $112\text{ m}^2\text{g}^{-1}$ , Fig. 7.15a) and were higher compared to that reported for powders prepared by precipitation [37]. Fig. 7.15a shows the variation of SSA of nc-YSH powders with yttrium content. The adsorption isotherms and the corresponding linear BET isotherm plots pertaining to the nc-YSH powders are depicted in Fig. 7.17. The hysteresis in their adsorption isotherm suggested that these powders were microporous. Further, the BET adsorption isotherms reveal that the slope decreases with yttrium addition. In other words, this plot (Fig. 7.15a) indicates that the SSA of YSH powders increases

with yttrium content as a result of formation of microporosity (hysteresis in BET isotherm). Probably interparticle cohesion was also enhanced due to Y<sup>3+</sup> doping.

### **7.12 Carbon residue**

The impurity levels in nanocrystalline powders which are to be used in sensor [38] and nuclear application should be within 1000 ppm [33]. The YSH powders obtained in this study were found to contain carbon residue varying from 250 – 500 ppm. Thus, this method does not necessitate additional calcination step for removing the residual carbon. Hence, these nanopowders could be used as such without any further processing.

### **7.13 Phase identification, XCS and lattice strain**

The XRD patterns pertaining to the YSH powders are presented in Fig. 7.18. From this figure (Fig. 7.18) it is evident that these powders comprise only the cubic phase. However, the powder 6YSH comprised both the monoclinic and cubic phases. Porter and Heuer [39] have reported that the volume fraction of monoclinic phase present in c-YSH could be evaluated from the XRD pattern by considering the multiplicity factor and linear absorption coefficient of m-HfO<sub>2</sub> and c-YSH phases. It was found that 6YSH powders contain 21 % and 79 % of m-HfO<sub>2</sub> and c-YSH phase. The volume fraction of c-YSH in 6YSH was higher as compared to the values reported in reference [15]. Thus, it could be concluded that SMS helps in stabilizing a higher fraction of YSH phase as compared to the solid state route [15].

The XCS values derived by using both Sc [17] and HW [17] are in good agreement except for those pertaining to the 30YSH powders (Table 7.7 & Fig. 7.15b). This difference in XCS between the Sc and HW estimate in 30YSH could be attributed to lattice strain. The Sc method leads to erroneous XCS values especially for nc materials possessing high lattice strain [40]. The measured values of the lattice parameter pertaining to all the YSH powders are shown

in Fig.15c. It is observed that the lattice parameter increases with yttrium addition [41] (Fig. 7.15c). The empirical (Vegard's) equation [42] was used as the reference to compare the measured values of lattice parameter. The lattice parameter of powders reported in this study (Fig. 7.15c) is marginally higher (0.15 %) as compared to those reported in other investigations [42-44]. However the powders employed in the studies reported in references [18, 43, 44] were microcrystalline.

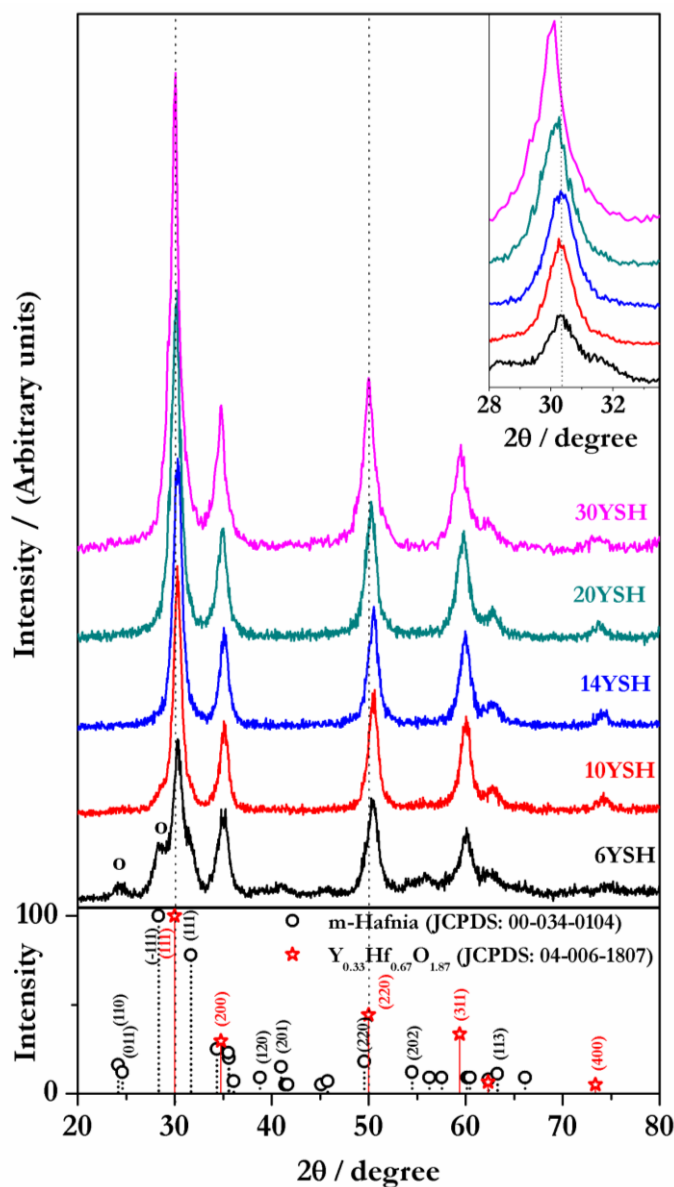


Figure 7.18 XRD pattern of nc-YSH powders derived through SMS

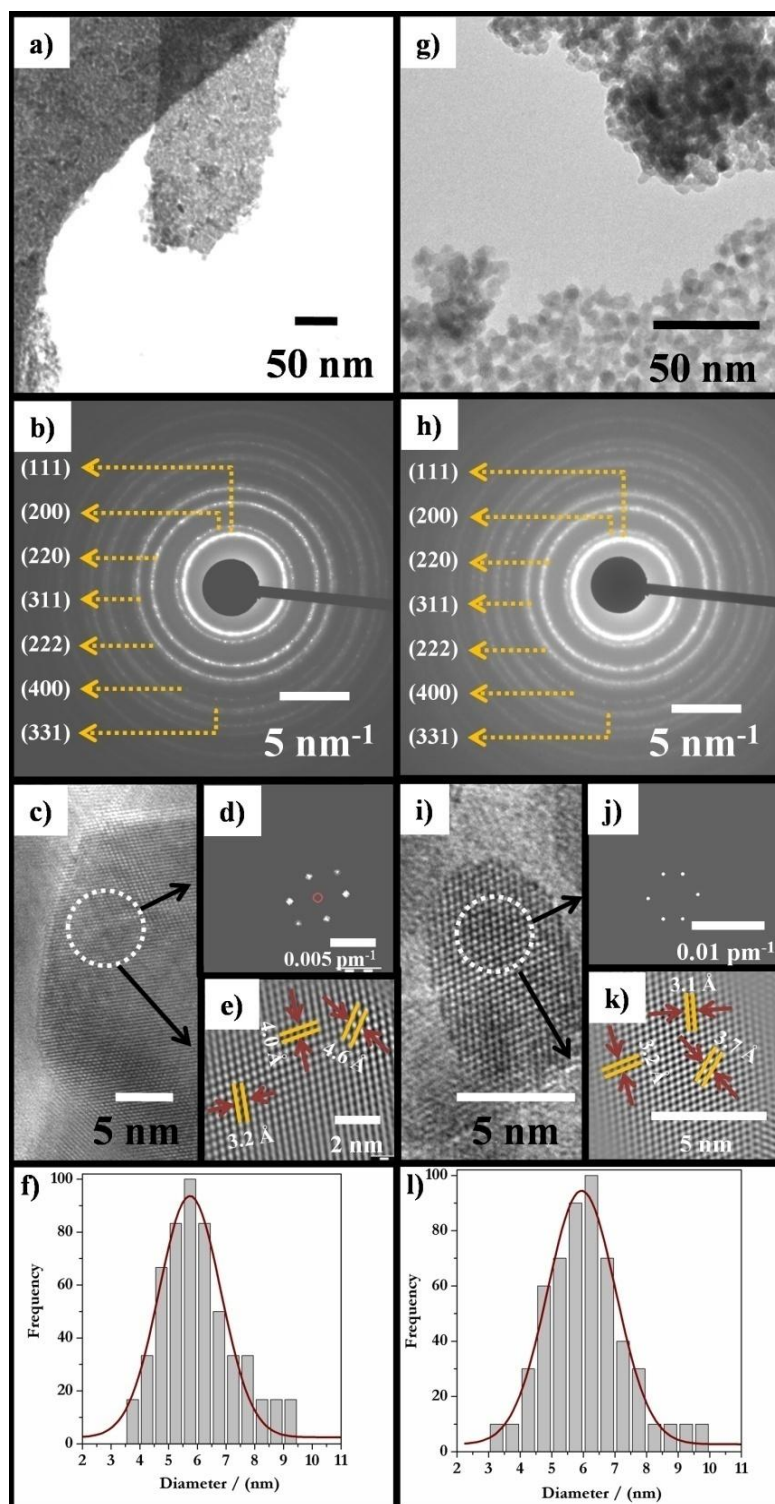


Figure 7.19 TEM images of YSH [10YSH (a-f) and 14YSH (g-l)] revealing: (a & g) bright field image showing uniform nano grains; (b & h) SAED image revealing the cubic phase; (c & i) HRTEM image revealing nano grains; (d & j) FFT of selected area; (e & k) IFFT of the corresponding FFT and (f & l) grain size distribution plot

#### **7.14 Microstructural analysis by using SEM and TEM**

TEM investigation also revealed a “near unimodal” distribution of grains (Fig. 7.19). The unimodal distribution of sizes among the agglomerates as well as grains is possibly due to homogeneous nucleation and growth. Both 10YSH and 14YSH powders revealed that the YSH powders (Fig. 7.19) comprised unimodal size distribution of grains with maxima ranging between 5-6 nm (Fig. 7.19f & Fig. 7.19l). SAED patterns of 10YSH and 14YSH confirmed their nanocrystallinity and that they comprise cubic phase (Fig. 7.19b & Fig. 7.19h). HRTEM images (Fig. 7.19c & Fig. 7.19i) of these samples depict the values of the “d-spacings” that are in agreement with the values cited in JCPDS [YSH [45] – PDF No. 04-006-1807]. It was also observed that the grain sizes measured from TEM images are comparable with the XCS [10YSH (Sc: 9 nm, HW: 11 nm) and 14YSH (Sc: 9 nm, HW: 10nm)]. Elemental mapping and “point mode” analysis on YSH powders for yttrium by using SEM revealed that it is distributed uniformly in the YSH powders and the measured dopant concentrations (approximately) are comparable to the values pertaining to the overall composition.

#### **7.15 Sintering of nc-YSH**

##### **7.15.1 Green pellets**

Compaction experiments revealed that the  $\rho_G$  of all the YSH pellets increase linearly (35 % T. D to 47 % T. D) with the CP (60 MPa to 353 MPa). Table 7.8 and Fig. 7.20a depict the characteristics of these green compacts. The  $\rho_G$  values obtained in this study are rather low possibly due to the smaller size of agglomerates and lack of multi modal distribution of sizes [31]. Segal et al. [46] had reported that if the powders contain weak or no agglomerates, it would result in uniform distribution of pores in the compacts and sintering of such compacts would result in monoliths with very high density. Similarly, Ma et al. [47] had shown that the green



pellets derived with multimodal size distribution of particles has a detrimental effect on the density due to differential densification during the final stage of sintering as well as multimodal size distribution of grains in the final product. Variation in  $\rho_G$  with the CP obtained for all the different powders did not show any significant variation. This could be attributed to the similarity in the particle size distribution in them.

**Table 7.8  $\rho_G$  of YSH pellets derived through SMS**

CP (MPa)	6YSH	10YSH	14YSH % T.D	20YSH	30YSH
<b>60</b>	$35.8 \pm 0.5$	$34.8 \pm 0.3$	$34.8 \pm 0.7$	$36.0 \pm 0.3$	$36.0 \pm 0.7$
<b>120</b>	$39.0 \pm 0.1$	$37.9 \pm 0.1$	$38.0 \pm 0.3$	$39.2 \pm 0.4$	$37.4 \pm 0.1$
<b>180</b>	$41.0 \pm 0.6$	$40.1 \pm 0.1$	$39.6 \pm 0.4$	$41.6 \pm 0.4$	$40.5 \pm 0.3$
<b>244</b>	$44.1 \pm 0.4$	$42.7 \pm 0.2$	$42.5 \pm 0.6$	$43.6 \pm 0.4$	$42.3 \pm 0.2$
<b>317</b>	$45.8 \pm 0.3$	$44.9 \pm 0.2$	$44.3 \pm 0.2$	$45.8 \pm 0.2$	$44.3 \pm 0.4$
<b>353</b>	$47.3 \pm 0.1$	$45.9 \pm 0.2$	$45.5 \pm 0.2$	$46.6 \pm 0.3$	$45.2 \pm 0.4$

### 7.15.2 Phase characterization and carbon residue in sintered YSH monoliths

Fig. 7.21 shows the X-ray diffraction patterns pertaining to the sintered YSH. These patterns were indexed appropriately by comparing them with the standard JCPDS pattern [m- $\text{HfO}_2$  – JCPDS No. 00-034-0104; c-YSH – JCPDS No. 04-006-1807]. Lattice parameter values of the sintered YSH pellets were determined and are presented in Fig. 7.15c. The values of lattice parameter derived were compared with those cited in the literature [43, 44, 48]. An empirical equation presented in ref. [48] was also used to derive the lattice parameter of YSH as a function of its yttrium content [mol %] (Fig. 7.15c). These values are in agreement with the data presented in ref. [43, 44, 48]. Fig. 7.15c also reveals that the lattice parameters of the “as prepared” nc-YSH powders were higher as compared to that of the sintered YSH as well as those predicted by the empirical equation. This deviation could be due to the increased lattice strain in the nanocrystalline YSH. Fig. 7.15b shows that lattice strain increases with yttrium addition and

that calcination anneals the lattice strain and leads to grain coarsening. Carbon residue of the randomly selected sintered YSH pellets was found to vary from 51 – 140 ppm.

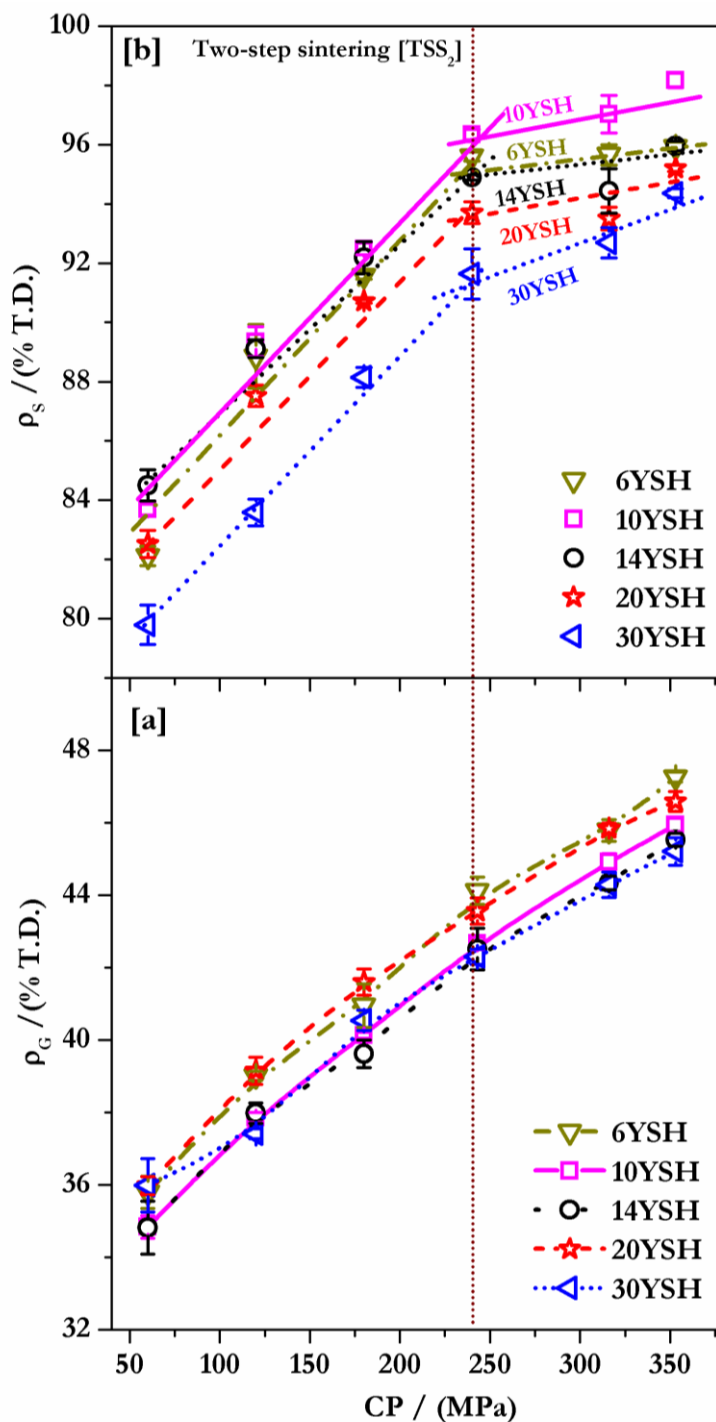


Figure 7.20 Variation of (a)  $\rho_G$  and (b)  $\rho_S$  with the CP

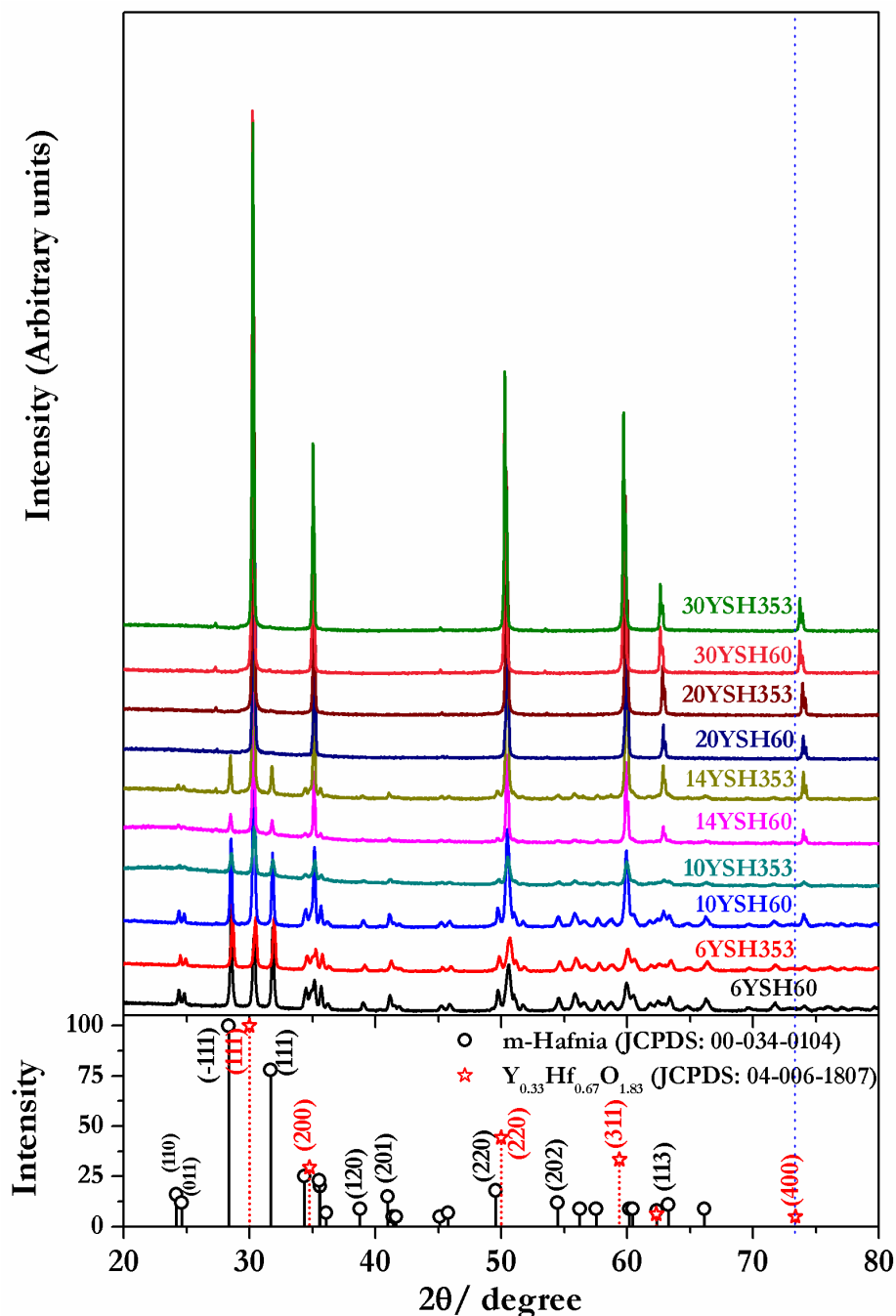


Figure 7.21 XRD pertaining to sintered YSH monoliths

### 7.15.3 Sintering nc-YSH and microstructural investigations on sintered YSH monoliths

To identify an appropriate sintering procedure and its impact on the final densification, selected samples of YSH pellets were sintered by using CS ( $\text{xxYSH}_{\text{CS1}}$ ,  $\text{xxYSH}_{\text{CS2}}$  and  $\text{xxYSH}_{\text{CS3}}$ ) and TSS ( $\text{TSS}_1$  and  $\text{TSS}_2$ ) procedures (Chapter 2). The values of the  $\rho_s$  are tabulated

in Table 7.9 - 7.10. The pellets sintered by TSS<sub>2</sub> showed better densification as compared to those sintered by TSS<sub>1</sub> and CS (Table 7.9 - 7.10). Hence, the TSS<sub>2</sub> method was used to sinter all the YSH compacts.

Table 7.10 and Fig. 7.20b depicts the variation in the  $\rho_s$  with the CP pertaining to the YSH pellets derived through TSS<sub>2</sub>. In general, it was observed that doping HfO<sub>2</sub> with Y<sup>3+</sup> leads to a decrease in  $\rho_s$  (except for 10YSH). TSS<sub>2</sub> method with a final temperature as low as 1773 K (353 MPa) yields monoliths with a high  $\rho_s$  ( $94.4 \pm 0.2$  % T.D to  $98.2 \pm 0.3$  % T.D). These values of  $\rho_s$  were higher than those reported in the literature [15, 34, 43, 48]. Fig. 7.20 depicts the variation in the green and sintered densities of the YSH powders. The sintered densities are directly correlated with the corresponding green densities. The green density is found to decrease with the Y<sup>3+</sup> content in the starting material. However the XCS and SSA are found to increase with the Y<sup>3+</sup> content. The increase in the former is due to grain coarsening. Size distribution of particles of YSH powders reveals that the formation of larger size fraction of particles was found to increase with Y<sup>3+</sup> doping (Fig. 7.16) i.e., agglomeration increases with yttrium doping and compaction of these powders would result in compacts with lower green density. Thus more Y<sup>3+</sup> doping led to an increase in the size fraction of larger particles and inefficient packing. This in turn brought down the green density and the corresponding sintered density. Thus the effect of interparticle cohesion seems to overwhelm the influence due to increased SSA.

The increase in SSA and BD is probably due to the introduction of microporosity in the powder. However, the particles (i.e. agglomerates of crystallites) grow with Y<sup>3+</sup> doping (Fig. 7.16). Thus the increased porosity and inefficient packing in the bimodal powders have brought down the BD. Moreover the trend in the variation in the green density with Y<sup>3+</sup> content indicates that the fracture of particles becomes progressively difficult with Y<sup>3+</sup> doping. This

leads to diminished values of green density. Thus, even though the SSA increases with Y<sup>3+</sup> doping, a commensurate increase in the sintered density is not observed.

XRD analysis of sintered YSH monoliths revealed that a single phase solid solution is formed only when the Y<sup>3+</sup> concentration is more than 20 mol %, below which the products were only partially stabilized (biphasic) (Fig. 7.21).

In order to optimize the process parameters for obtaining a final product with a desirable density, the variation of  $\alpha$  (shrinkage anisotropy factor) [35, 49] and relative pore fraction with  $\rho_s$  are compared (Fig. 7.22a). It is observed that  $\alpha$  is linearly correlated with the  $\rho_s$  (0.75 - 0.95). Rahmann [35] had reported that  $\alpha$  is inevitable but its magnitude needs to be kept optimum. Additionally, Exner and Giess [49] have shown that  $\alpha$  increases (0.3 – 0.7) with the  $\rho_s$  (60 – 99 % T.D) and it is independent of the size and shape of the particles. These studies [49] were conducted on jagged and spherical powders of dimension 6  $\mu\text{m}$  and 13  $\mu\text{m}$ . The results obtained in this study do follow a linear variation and are in line with the results obtained by Exner and Giess [49]. However, the values of  $\alpha$  are quite high compared to that pertaining to micron sized particles. Thus, it could be concluded that the nc-YSH sinters with uniform AS and RS. Relative pore fraction plot (Fig. 7.22b) reveals that the open pore fraction decreases while the closed pore fraction increases (marginally) with the CP. Fig. 7.22b also reveals that the critical CP is about 353 MPa wherein both closed and open pore fraction were nearly equal (at around 96 % T.D) and are at their minimum.

**Table 7.9 Sintering parameters and  $\rho_s$  of YSH monoliths (317 MPa; CS and TSS method)**

Sample	$\rho_G$	$\rho_s$				
		CS <sub>1</sub>	CS <sub>2</sub>	CS <sub>3</sub>	TSS <sub>1</sub>	TSS <sub>2</sub>
		xxYSH <sub>CS1</sub>	xxYSH <sub>CS2</sub>	xxYSH <sub>CS3</sub>	xxYSHS <sub>1</sub>	xxYSHS <sub>2</sub>
% T. D						
10YSH	44.9 ± 0.2	75.4 ± 0.4	90.8 ± 0.1	92.3 ± 0.1	92.2 ± 0.3	97.0 ± 0.6
20YSH	45.8 ± 0.2	71.8 ± 0.8	82.9 ± 0.7	84.6 ± 0.1	85.1 ± 0.3	93.5 ± 0.4

xx - mole fraction of yttrium (in %)

CP - 317 MPa	CS <sub>1</sub> - 1673 K 4 h	CS <sub>2</sub> - 1773 K 4 h	CS <sub>3</sub> - 1873 K 4 h	<b>TSS<sub>1</sub></b>	Step 1 - 1873 K 1 h Step 2 - 1673 K 4 h	<b>TSS<sub>2</sub></b>	Step 1 - 1873 K 1 h Step 2 - 1773 K 4 h
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**Table 7.10  $\rho_s$  of YSH monoliths which were sintered by using the TSS<sub>2</sub> method**

CP (MPa)	6YSH	10YSH	14YSH % T. D	20YSH	30YSH
<b>60</b>	82.1 ± 0.3	83.7 ± 0.2	84.5 ± 0.5	82.5 ± 0.5	79.8 ± 0.7
<b>120</b>	88.9 ± 1.1	89.4 ± 0.5	89.1 ± 0.3	87.5 ± 0.4	83.6 ± 0.5
<b>180</b>	91.6 ± 0.1	92.5 ± 0.2	92.2 ± 0.6	90.7 ± 0.1	88.2 ± 0.3
<b>244</b>	95.6 ± 0.2	96.3 ± 0.2	94.9 ± 0.1	93.7 ± 0.4	91.6 ± 0.9
<b>317</b>	95.7 ± 0.4	97.0 ± 0.6	94.4 ± 0.8	93.5 ± 0.4	92.7 ± 0.5
<b>353</b>	95.9 ± 0.2	98.2 ± 0.3	96.0 ± 0.2	95.2 ± 0.1	94.4 ± 0.2

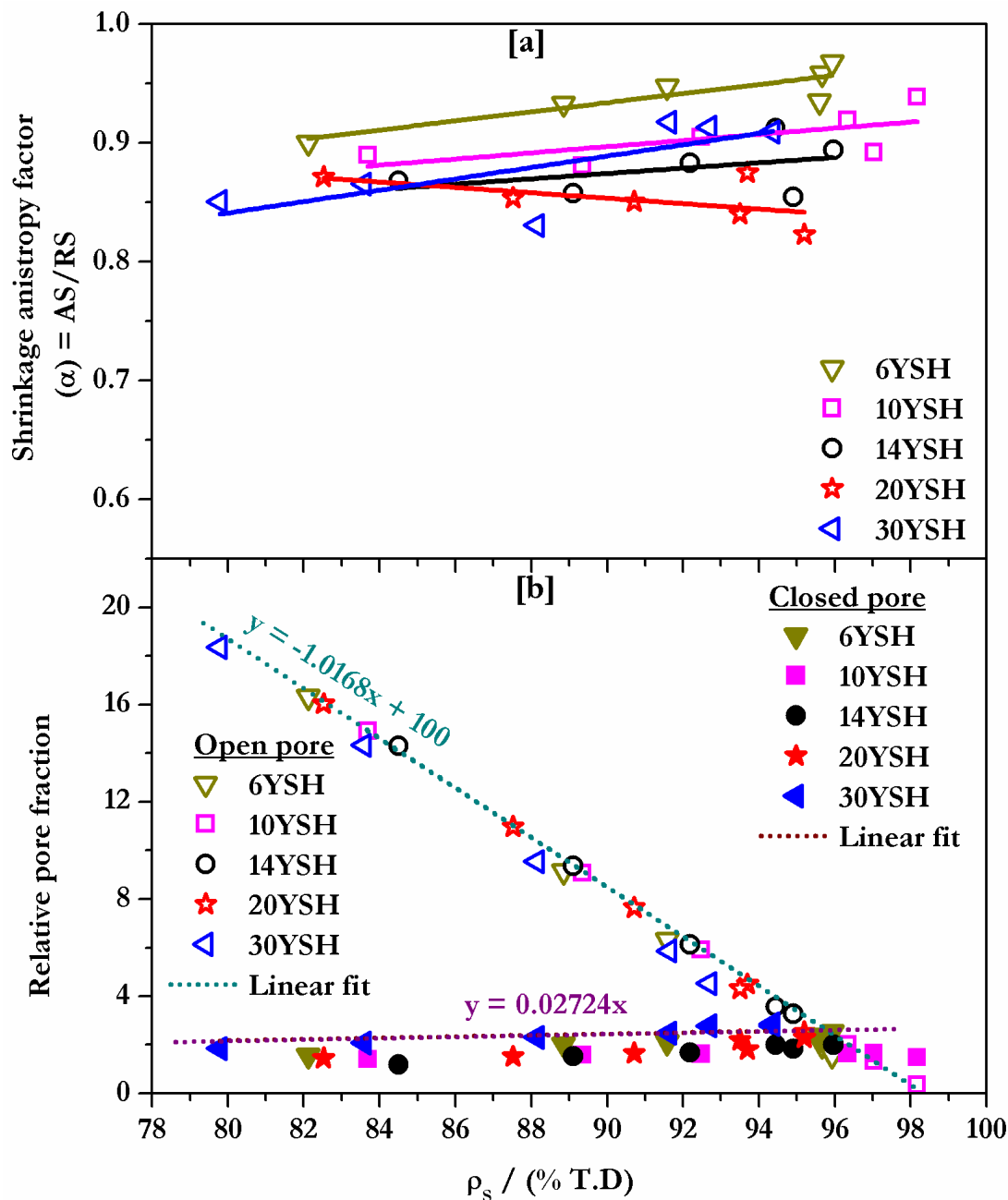
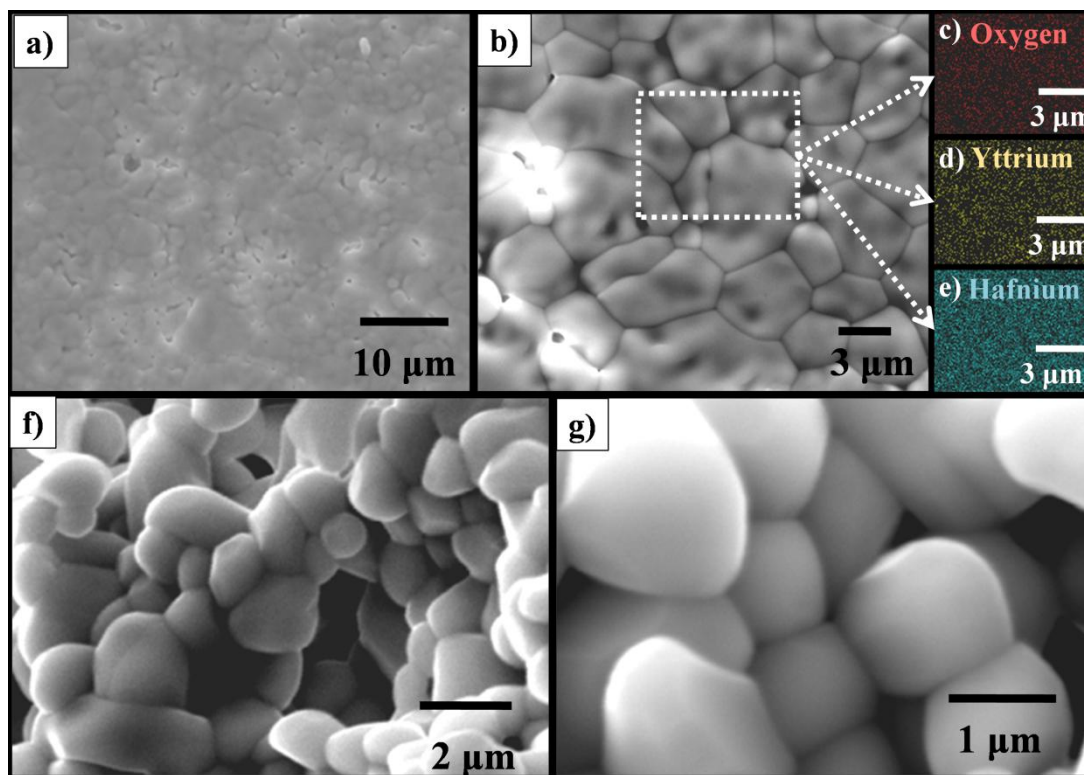


Figure 7.22 (a) Variation in the shrinkage anisotropy factor ( $\alpha$ ) with the sintered density [TSS<sub>2</sub>] and (b) Interdependence of the volume fractions of open and closed pore with sintered density [TSS<sub>2</sub>]

Microstructural investigation of the sintered 30YSH pellets are shown in Figs. 7.23 – 7.24. The images (Figs. 7.23 – 7.24) reveal that the  $\text{Y}^{3+}$  and  $\text{Hf}^{4+}$  are uniformly distributed in the sintered 30YSH monolith. SEM of sintered 30YSH monolith (60 MPa) show the presence of both inter and intergranular pores at the surface as well as in the fractured surface. The SEM

image of 30YSH monoliths (compacted at 353 MPa) reveals many interesting features such as faceted grains with well defined grain boundaries, presence of pentagonal grains with a dihedral angle of  $121 - 127^\circ$  and uniform distribution of yttrium and hafnium on the surface. Additionally, it also reveals that the grain size varies from  $5 - 12 \mu\text{m}$  (YSH derived by using  $\text{TSS}_2$ ).



*Figure 7.23 SEM images obtained with sintered 30YSH pellets (60 MPa) (a-b) porous sintered surfaces, (c-e) elemental mapping/distribution of oxygen, yttrium and hafnium on the selected sintered surface of YSH and (f-g) image of the fractured sintered surface revealing intra and intergranular pores*

#### 7.15.4 YSH crucibles

In general it was observed that the nc-YSH powders compacted at 353 MPa and sintered by the  $\text{TSS}_2$  method had yielded monoliths with the highest  $\rho_s$ . Among the YSH powders, 10YSH had yielded a final sintered density of  $98.2 \pm 0.3 \%$  T.D which is the highest among the values obtained in this study. The XRD studies revealed that the 20YSH and 30YSH powders had yielded monoliths comprising complete solid solution. Hence, among the nc-YSH powders,



30YSH was selected for making crucibles. In addition crucibles were also made out of 10YSH powders in order to understand the effect of phase segregation on the integrity (cracks, chipping and shape distortion) [15] of the sintered YSH crucibles (Fig. 7.25). It was observed that the  $\rho_s$  of 10YSH and 30YSH crucibles were  $97.8 \pm 0.1$  % T.D and  $94.1 \pm 0.3$  % T.D respectively. Further, the sintered crucibles (10YSH and 30YSH) were devoid of cracks and physical defects (layering, cracks, end-capping and hour glassing) (Fig. 7.25). Even though 10YSH powders yielded a marginally higher  $\rho_s$ , the crucibles made from 30YSH were preferred for they would be more suitable for applications that involve thermal cycling.

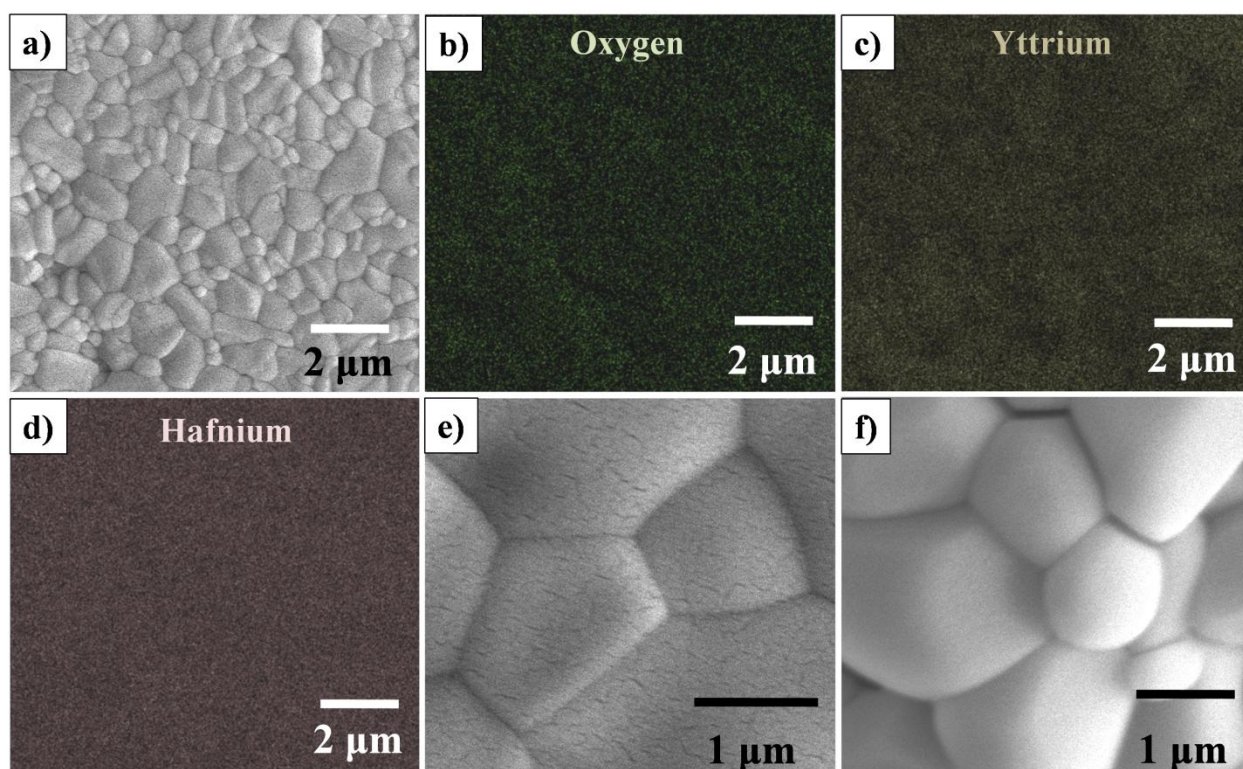


Figure 7.24 SEM images obtained with sintered 30YSH pellets (353 MPa) (a & e) sintered surfaces, (b-d) elemental mapping/distribution of oxygen, yttrium and hafnium on the sintered YSH and (e) typical pentagonal grains revealing  $\approx 121 - 127^\circ$  dihedral angle and (f) image of fractured surface revealing grain coarsening

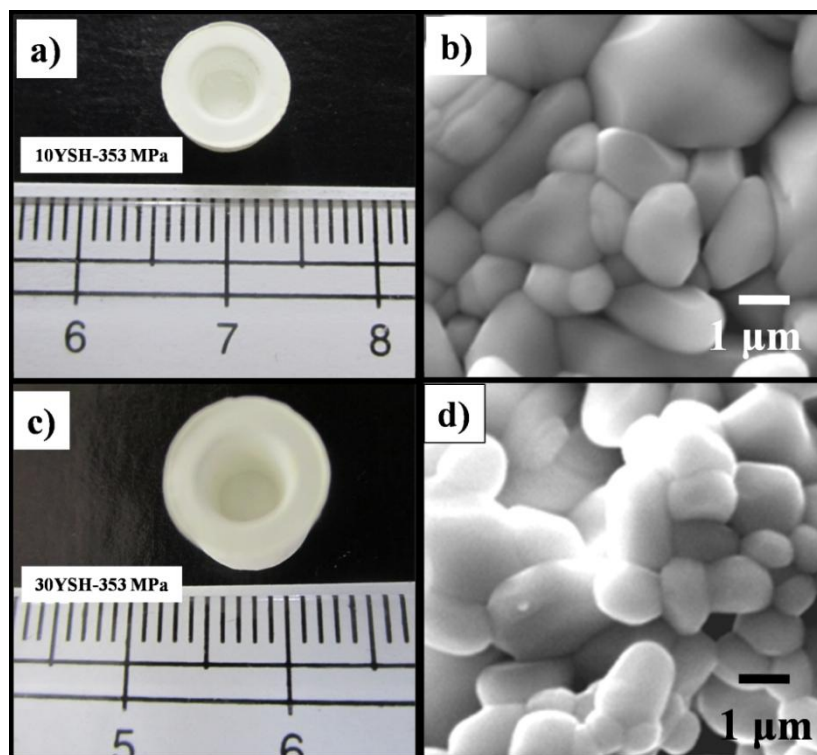


Figure 7.25 (a-b) 10YSH sintered cup derived with 353 MPa pressure and (c-d) 30YSH derived with 353 MPa pressure; (a and c) photograph of sintered YSH cup and (b and d) SEM image fractured surfaces of sintered YSH cups

### 7.16 Conclusions drawn from the synthesis and sintering of nc-YSH

For the first time fine grained nc-YSH powders were prepared by using SMS. It was observed that the yttrium content significantly influences the powder characteristics. Size distribution analysis revealed that the YSH powders exhibited near unimodal size distribution with maxima at  $10\ \mu\text{m}$ . The SSA, XCS, lattice strain and lattice parameter increased with yttrium addition while their  $\rho_B$  showed the reverse trend. TEM investigations reaffirmed the presence of nanograins with unimodal size distribution of grains and SAED further ascertained the presence of a fluorite solid solution. All powders exhibited monotonic increase in  $\rho_G$  with the CP. A compaction pressure of 353 MPa was found optimum in order to sinter YSH compacts containing 10 mol % of yttrium to a sintered density of  $98.2 \pm 0.3\%$  T.D by using the “two-step” sintering (TSS<sub>2</sub>). Point scan and area mapping for constituent elements in the YSH powders and

sintered monoliths confirmed the presence of uniform distribution of yttrium and hafnium. Morphological analysis of polished and thermally etched sintered monoliths revealed the presence of uniform grains with well-defined grain boundaries. The dihedral angle in sintered YSH monoliths was found to be varying between 121-127<sup>0</sup>. Shrinkage anisotropic factor ( $\alpha$ ) revealed that the YSH compacts had undergone near isotropic shrinkage. Small crucibles made out of both 10YSH and 30YSH were devoid of visual cracks and physical defects.

### **7.17 SPS studies on nc-HfO<sub>2</sub> and nc-yttria stabilized hafnia (YSH) powders**

Nc-HfO<sub>2</sub> and nc-YSH powders prepared via SMS were used as such in the SPS studies. Nc-HfO<sub>2</sub> powders were indexed as Hf0D (m-HfO<sub>2</sub>) and Hf82D (c-HfO<sub>2</sub>) while YSH powders were indexed as YSH bearing a prefix that indicated the yttrium content in mole %. The detailed experimental procedure employed in the preparation of nc m-HfO<sub>2</sub> and c-HfO<sub>2</sub> powders and YSH are described in Chapter 2. Hf0D were prepared without the use of sodium nitrite ( $\Phi = 0$ ) while the c-HfO<sub>2</sub> powders were prepared with  $\Phi$  value of 0.82.

#### **7.17.1 SPS of nc-hafnia powders**

XRD patterns (Fig. 7.26) reveal that the metastable c-HfO<sub>2</sub> powders had reverted back to the monoclinic phase upon SPS. The carbon residue in the sintered monoliths was found to vary between 500 to 734 ppm.

The characteristics of the spark plasma sintered pellets are presented in Table 7.11.  $\rho_s$  of these monoliths reveal that both the monoclinic and cubic hafnia powders could be sintered to a density of about 98 % T.D. Further, visual examination of these monoliths revealed that these monoliths were intact with no visible physical defects viz., cracks, hour glassing or deformation. However, pellets made out of nc c-HfO<sub>2</sub> powder when sintered by using the TSS or CS methods had undergone warping and some pellets were found to be cracked. These could be attributed to

the phase reversal during sintering. Comparison of the  $\rho_s$  of  $\text{HfO}_2$  monoliths obtained by using different heating routines reveal that the rate of heating does not strongly influence the  $\rho_s$  of the final product. Nc- $\text{HfO}_2$  undergoes better densification than nc-YSH. The heating rate does not affect the  $\rho_s$ . SPS is energy and cost efficient, as expected, for obtaining the monoliths with about 98 % T.D,  $\rho_s$ .

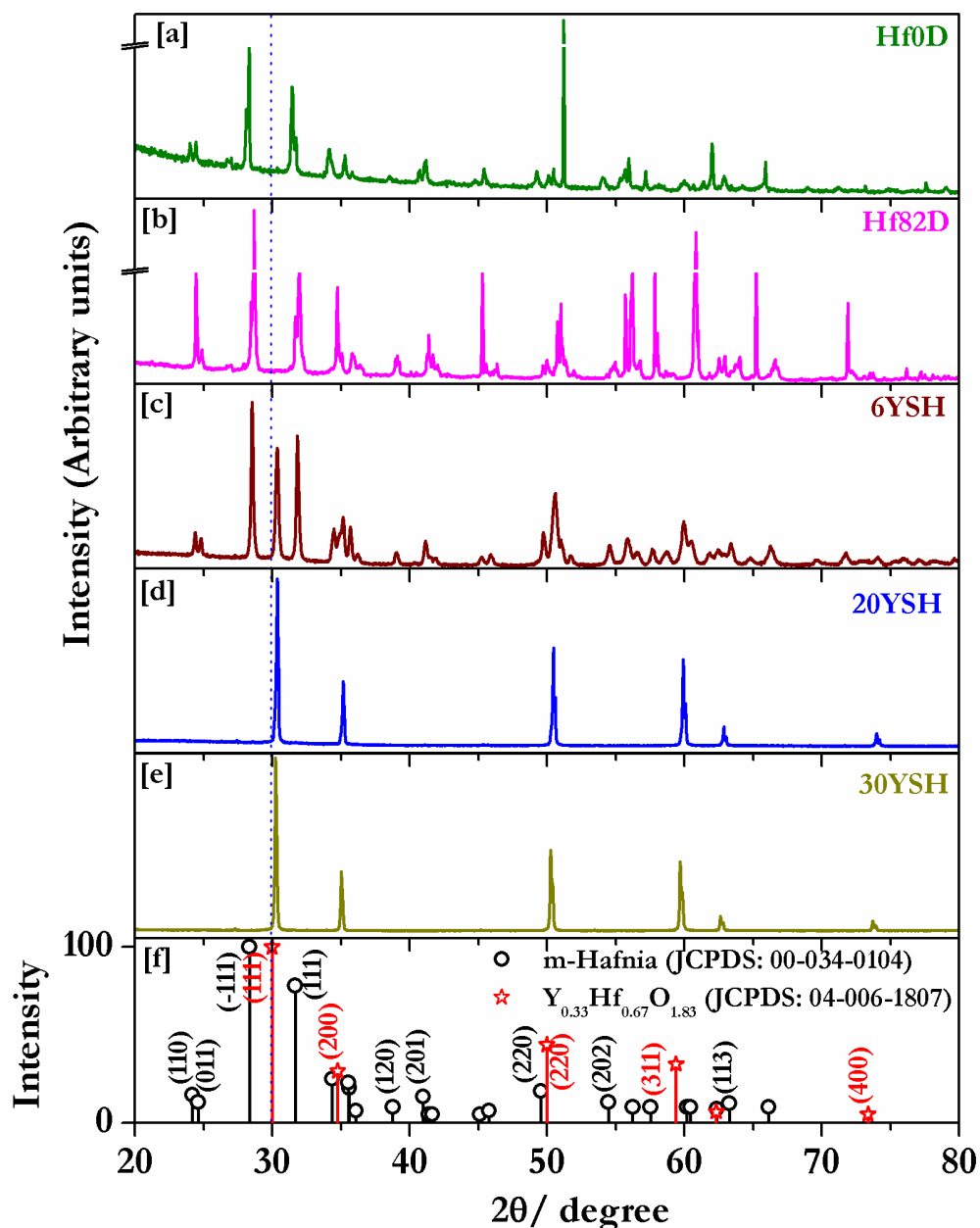


Figure 7.26 XRD patterns pertaining to spark plasma sintered monoliths (a-b) Hafnia (c-e) YSH and their (f) JCPDS pattern

Table 7.11 Characteristics of SPS sintered pellets

Material	Sample Index	Initial phase composition	Heating rate ( $\text{K min}^{-1}$ )	$\rho_s$ (% T. D.)	RC (ppm)	$T_s$
<b>HfO<sub>2</sub></b>	Hf0D	m	50	$98.6 \pm 0.2$	503	1873 K 7 min
	Hf0D	m	100	$98.8 \pm 0.1$	515	
	Hf82D	c (63 %) & m (37 %)	50	$98.5 \pm 0.2$	719	
	Hf82D		100	$97.9 \pm 0.2$	734	
<b>YSH</b>	6YSH	c (79 %) & m (21 %)	100	$97.1 \pm 0.2$	502	
	20YSH		100	$97.3 \pm 0.6$	613	
			100			
	30YSH	c		$96.2 \pm 0.3$	455	

*m*- monoclinic, *c* - cubic, *RC* - carbon residue;  $T_s$  - Sintering schedule

The data pertaining to the synthesis and sintering of nc-hafnia powders are rather scant. Further, no reports have been published so far on the SPS of nc-HfO<sub>2</sub> powders. Our study is the “first of its kind”, on the SPS of pure nc-HfO<sub>2</sub> powders. Recently Dusan et al. [50] had sintered commercial hafnia powders in air (compacted at 440 MPa) without the addition of any sintering aid to a density of 66.1 % T.D (1573 K 3h 30 min) and 90.9 % T.D (1773 K 3 h 30 min). Piluso et al. [15, 34] had compacted hafnia powders by using semi-isostatic pressing in the presence of binder and plastizier and sintered to a density of 95.1 % T.D (1973 K 30 min). However, these compacts cracked during sintering due to phase transformation. Matovic et al. [51] had prepared hafnia powders by the solid state route, compacted at 150 MPa with no sintering additives and sintered these green compacts at different temperatures and obtained the following  $\rho_s$  viz., 88 % T.D (1573 K 2h), 94 % T.D (1673 K 2h) and 97 % T.D (1773 K 2h). Lakhliifi et al. [52] had sintered hafnia powders derived through precipitation method, compacted at 200 MPa and sintered the green pellets in air at different temperatures



ranging between 1973 K to 2173 K to obtain final products with densities 89.6 T.D.% to 95.4 % T.D. (1973 K 2 h), 93.1 % T.D and 87.7 % T.D (2073 2h). Thus, it could be concluded that SPS had led to better densification than conventional method.

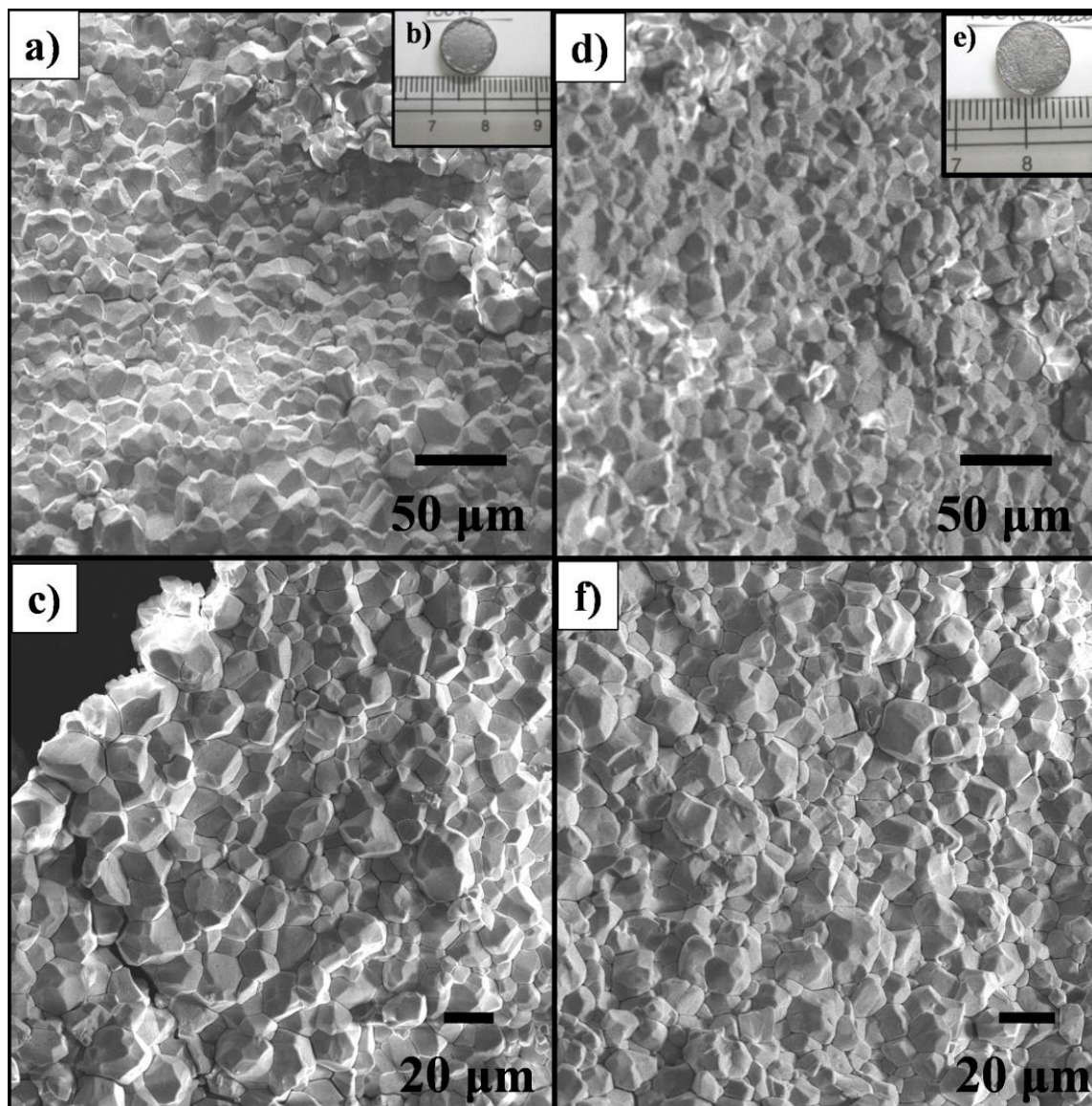


Figure 7.27 SEM images of (a-c) Hafnia ( $\text{HfO}_2$ ); (d-f) Hafnia ( $\text{HfO}_2$ ); (b & e) image showing “as prepared” hafnia pellets covered with graphite layer; (a & d) low magnification images of fractured pellet surface and (c & f) high magnification images showing faceted grains

**Table 7.12 Comparison of the  $\rho_s$  of HfO<sub>2</sub> and YSH monoliths reported in the Literature**

Reference	Sample	Method	CP (MPa)	$\rho_G$ (% T.D)	$S_m$	$T_s$	$\rho_s$ (% T.D)
[50]	HfO <sub>2</sub>	Comm	440	51.7	C (air)	1573 K 3 h 30 min	66.1
						1773 K 3 h 30 min	90.9
					C (Ar)	1573 K 3 h 30 min	66.1
						1773 K 3 h 30 min	90.9
[15]	HfO <sub>2</sub>	Comm	-	-	C (air)	1873 K 30 min	95.1*
	HfO <sub>2</sub> + P 40						72.0
	HfO <sub>2</sub> + P 70						48.0
	HfO <sub>2</sub> + 5 X						88.3
	HfO <sub>2</sub> + 8 X						91.2
[34]	HfO <sub>2</sub>	Comm	0.1 to 30	-	C (air)	1873 K 1h	<b>98.5*</b>
	HfO <sub>2</sub> + 1 X						96.6
	HfO <sub>2</sub> + 3 X						92.5
	HfO <sub>2</sub> + 5 X						91.6
	HfO <sub>2</sub> + 8 X						88.8
[51]	HfO <sub>2</sub>	Re-Ox	150	-	C (air)	1573 K 2 h	88.0
						1673 K 2h	94.0
						1773 K 2 h	<b>97.0</b>
[52]	HfO <sub>2</sub>	Flash reaction		45.6	C (air)	1973 K 2h	89.6
						1973 K 4h	95.4
						2023 K 2h	93.1
						2073 K 2h	87.7
						1973 K 2h	67.4
	HfO <sub>2</sub> + 3 X	Thde	200	45.2	C (air)	1973 K 4h	63.4
						2073 K 2h	65.2
						2173 K 2h	67.4
						1973 K 2h	62.3
						1973 K 4h	59.2
[53]	HfO <sub>2</sub> + 10 X	Thde		43.4	C (air)	2073 K 2h	62.1
						2173 K 2h	63.9
[54]	HfO <sub>2</sub>	Comm	57	-	SPS	1873 K 5 min	95.3
						1473 K 1h	45.0
						1673 K 1h	75.0
						1823 K 1h	90.0
						1873 K 1h	94.0
	HfO <sub>2</sub> + 5 X		160 (IP)	-	C (air)	1923 K 1h	95.0
							88.5
						1873 K 1h	86.5
[55]	HfO <sub>2</sub> + 8 X	Thde	345	-	C (air)	2273 K 1h	92.0
	HfO <sub>2</sub> + 10 X						94.5
	HfO <sub>2</sub> + 12 X						93.4
	HfO <sub>2</sub> + 14 X						90.8
	HfO <sub>2</sub> + 16 X						91.5
	HfO <sub>2</sub> + 18 X						90.7
	HfO <sub>2</sub> + 20 X						89.4
[48]	Hf <sub>0.7</sub> Y <sub>0.3</sub> O <sub>2-<math>\delta</math></sub>	Ball milled	100	-	C (air)	1923 K 10h	74.6
			200				80.7
			400				96.3
			500				97.5
			100		SPS	1923 K 3min	96.0
This study	HfO <sub>2</sub> (Hf11D)	SMS	353	50.2	TSS <sub>2</sub>	Step 1: 1873 K 30min	<b>97.2</b>
	30YSH			45.2		Step 2: 1773 K 4h	94.4
	HfO <sub>2</sub>		50	-	SPS	1873 K 7 min	<b>98.8</b>
	30YSH						<b>97.3</b>

*P* - porous agent (vol%); *X* - mol% Y<sub>2</sub>O<sub>3</sub>; *Thde* - thermal decomposition; *Comm* – commercial powder; *C* - conventional method; *IP* - Isostatic pressing; *CP* - compaction pressure; *T<sub>s</sub>* - Soaking temperature/duration; *S<sub>m</sub>* - sintering method; *S* - external gelation sol-gel technique; *Re-Ox* - Reduction-oxidation and \* - cracked

### **7.17.2 Microstructural and compositional analyses of hafnia monoliths (SPS)**

Microstructures of the hafnia consolidated through SPS is presented in Fig. 7.27 and Fig. 7.28. Both Hf0D and Hf82D show dense grains with no visible pores. Thus, it is evident that crucibles obtained through SPS would be ideal for melting applications. Low magnification and high magnification images of fractured pellet surfaces of Hf0D and Hf82D show uniform distribution of grains with faceted morphology. EDS investigation (point scan) revealed that no major impurities were present within the detection limits. The grain size of SPS was found to be in the range 5 – 25  $\mu\text{m}$  while the CS and TSS<sub>2</sub> derived compacts had grain size varying between 5 – 12  $\mu\text{m}$  and 1 – 4  $\mu\text{m}$  respectively.

### **7.17.3 SPS of nc-YSH powders**

XRD analysis of spark plasma sintered pellets revealed that all the compacts except 6YSH comprised only the cubic phase while the latter consisted of both cubic and monoclinic phases. The carbon residue was found to vary between 455 to 613 ppm.

All YSH pellets were sintered at 1873 K at a heating rate of 100 K min<sup>-1</sup>. Their  $\rho_s$  was in the range of 96 to 97 % T.D. Bu et al. [48] had sintered ball milled YSH powders by using both the conventional and SPS techniques. These authors [48] had reported that the  $\rho_s$  of Hf<sub>0.70</sub>Y<sub>0.30</sub>O<sub>2-x</sub> monoliths were 97.5 % T.D (1923 K 10 h) and 96 % T.D (1873 K 3 min) respectively. In addition, they had also reported that Hf<sub>0.70</sub>Y<sub>0.30</sub>O<sub>2-x</sub> had undergone better densification when sintered by CS as compared to SPS. However, these authors had employed a CP of 500 MPa and had sintered at 1923 K for 10 h to obtain a  $\rho_s$  of 97.5 % T.D. The powder obtained in this study 30YSH had undergone better densification (marginally higher) than those reported by Bu et al. [48] (both in the SPS and conventional method). Tyrpekl et al. [53] had prepared YSH (Hf<sub>0.85</sub>Y<sub>0.15</sub>O<sub>2-x</sub>) by employing the external gelation method and the derived beads



that were sintered by using SPS at 1873 K for 5 min. The sintered density of these monoliths were found to be  $95.3 \pm 0.6$  % T.D which is lower than the values reported in the present study. Zhao et al. [54] had prepared YSH by milling hafnia powders along with 5 mol% and 8 mol% of yttria. These ball milled powders were sintered in air by using the conventional method and were found to yield final products with  $\rho_s$  of 88.5 % T.D and 86.5 % T.D (1873 K 1 h). However, it was observed that these monoliths comprised both the monoclinic and cubic phases and had undergone poor densification. Piluso et al. [34] had published a patent on the preparation and sintering of dense YSH monoliths to be used in nuclear core melting simulation experiment. These authors had varied the yttria content from 0.50 mol% to 8 mol% and had sintered the compacts in air by using CS (1873 K 1 h). The  $\rho_s$  of these monoliths were found to vary between 96.6 % T.D (1 mol% Y<sub>2</sub>O<sub>3</sub>) and 88.8 % T.D (8 mol% Y<sub>2</sub>O<sub>3</sub>). The  $\rho_s$  of YSH monoliths (96.2 % T.D to 97.3 % T.D) reported in this study is the highest among the values reported so far for nc-YSH. Further, a CP as low as 50 MPa and sintering temperature of 1873 K with 7 min holding time was sufficient to sinter it to the above mentioned  $\rho_s$ . Thus, from the foregoing it is evident that the YSH powders derived in this study had undergone better densification when the SPS technique was used, rather than the CS and TSS method.

#### **7.17.4 Microstructural and compositional analyses of YSH monoliths**

SEM image of spark plasma sintered 30YSH monoliths is presented in Fig. 7.28. The fractured pellet surface shows that these pellets are highly dense with no visible pores. However, at higher magnification dents with size ranging between 0.10 to 0.40  $\mu\text{m}$  were observed within the grains. These dents could have been formed due to the closure of pores. High and low magnification images of fractured pellet surface revealed the presence of uniform distribution of grains with their size ranging between 10  $\mu\text{m}$  and 30  $\mu\text{m}$ . Further, the grains were highly faceted

suggesting that the sintering had proceeded up to the final stage. EDS (point scan and elemental mapping) revealed that the mean atom fraction of Hf (in the cation sublattice) was about 0.69 and that Y was distributed uniformly in the YSH matrix.

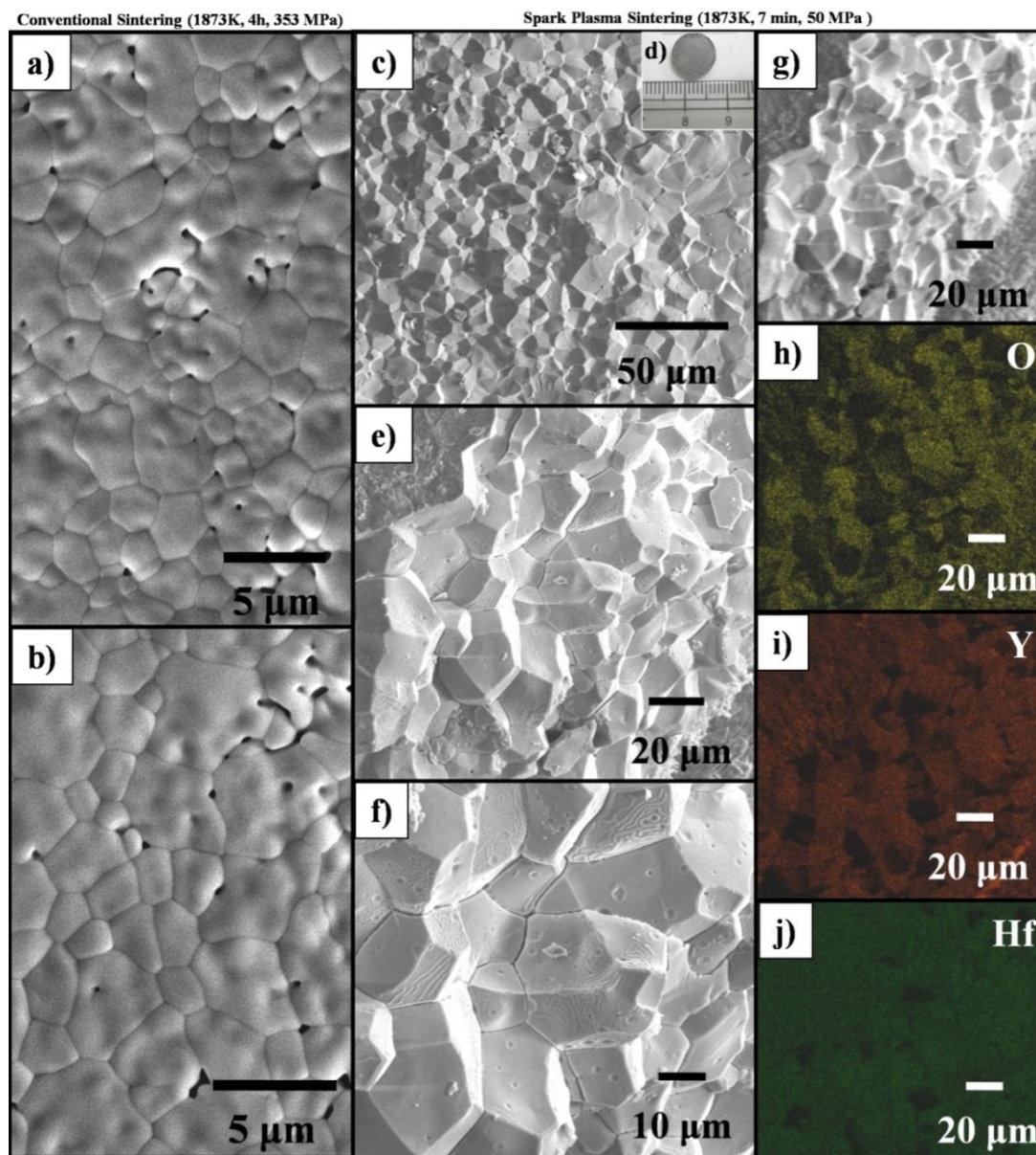


Figure 7.28 SEM images of sintered 30YSH monoliths: (a-b) Conventional sintering (1873 K; 4h; air; 353 MPa) and (c-j) SPS (1873 K; 7 min; 50 MPa) c) low magnification images of fractured pellet surface; (d) image showing “as prepared” pellets covered with graphite layer; (e-f) low magnification image showing well defined grain boundaries and faceted grains; (g) a typical fractured pellet surface showing faceted grains and (h-j) elemental mapping pertaining to image (g) which shows the uniform distribution of respective elements in the YSH matrix

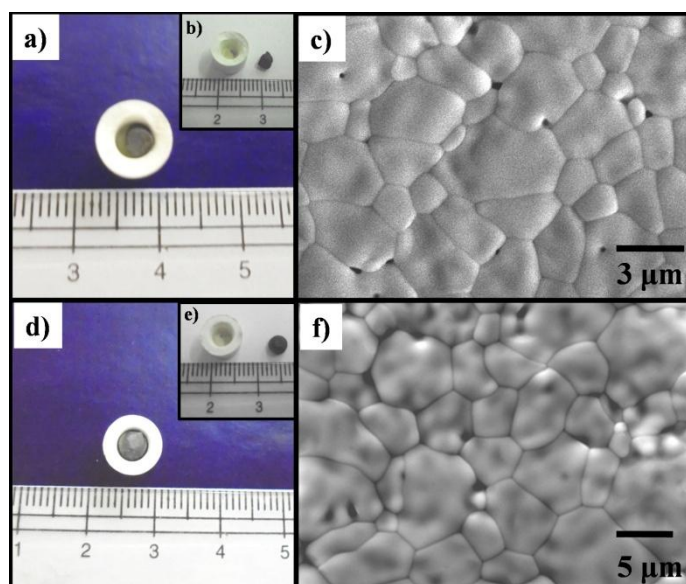
### **7.18 Conclusions drawn from spark plasma sintering studies**

Spark plasma sintering studies of nc-hafnia and nc-YSH powders derived through SMS revealed that a CP as low as 50 MPa and sintering temperature of 1873 K for 7 min is sufficient to obtain dense monoliths of about 99 % T.D (HfO<sub>2</sub> - 98.8 % T.D and YSH - 97.3 % T.D respectively. Both visual and microscopic examinations of sintered monoliths did not reveal any cracks or defects. EDS analysis and area mapping for constituent elements in the sintered monoliths (YSH) confirmed the presence of uniform distribution of yttrium and hafnium. SEM investigations of polished and thermally etched sintered monoliths revealed the presence of uniform distribution of grains with well-defined grain boundaries with their grain sizes varying between 5 - 25  $\mu\text{m}$  (HfO<sub>2</sub>) and 10 - 30  $\mu\text{m}$  (YSH). Higher magnification images of fractured surface of YSH monoliths revealed the presence of dents with their size ranging between 0.30  $\mu\text{m}$  to 0.40  $\mu\text{m}$ . Further investigations are required to optimize the sintering parameters to obtain submicron sized grains.

### **7.19 Compatibility test with molten uranium**

Compatibility test was carried out in the sintered crucibles of hafnia (Hf11D; 353 MPa; TSS<sub>2</sub>) and YSH (10YSH; 353 MPa; TSS<sub>2</sub>) by using the “spot technique” [56-58]. These investigations had revealed that the molten uranium was non-reactive with the crucible surface and the globule of molten uranium could be removed easily (non-wetting) even after repeating the experiments for three times in the same crucible. The fusion temperature of uranium was measured by using two color pyrometer and it was found to be  $1403 \pm 5$  K. Visual examination of both sample and interior of the crucible surface after first two trial experiment did not show any blackening of either crucible or sample surface, however, blackening of sample surface was observed on the third trial.

These crucibles (Hf11D and 10YSH) were subjected to microstructural examination after fracturing and polishing (Fig. 7.29). The microstructure of the inner surface of the crucibles did not reveal adherence of uranium metal or contamination of the crucible surface with uranium. Further, to ascertain this fact, EDS investigation (point scan) was also conducted. All these investigations reaffirmed the absence of the uranium in the interior surface of the crucible. Thus, from the preliminary investigation, it could be concluded that both hafnia and YSH sintered crucibles are compatible with molten uranium. Further experiments are required to reaffirm the utility of these crucibles with more reactive uranium bearing alloys.



*Figure 7.29 (a-c) Hf11D sintered crucible (353 MPa) and (d-f) 10YSH sintered crucible (353 MPa); (a & d) photograph of Hf11D and 10YSH crucibles holding molten uranium respectively; (b & e) photograph showing non-wetting molten uranium separated from Hf11D and 10YSH crucibles respectively; (c-f) SEM images of fractured and polished interior surface Hf11D and 10YSH crucibles (images were taken after compatibility test)*

## 7.20 Conclusions drawn from the compatibility test

Preliminary investigations carried out on the sintered crucibles of hafnia and YSH had revealed that these crucibles could be used for holding uranium bearing alloys. Visual examination of both the sample and interior surface of the crucible did not show the presence of

uranium. Further, these crucibles were non-wetting and could be reused. Microstructural investigations also revealed the absence of uranium in the interior surface of the crucible.

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## Chapter 8

### Conclusions

#### 8.1 Synthesis, Characterization and Sintering of Nanocrystalline Urania

Nc-urania powders were synthesized by using citrate gel-combustion in bulk quantities for the first time. The systematic dependence of the reaction as well as the properties of these nanocrystalline powders on the composition of the combustion mixture (R) was investigated. The course of the combustion reaction in these mixtures was measured with the help of DSC for the first time. These results showed that the rate of this reaction is strongly influenced by the composition of the combustion mixture (R). Mixtures with an R value of 0.25 showed a markedly different behavior compared to the rest and underwent “volume combustion”.

Upon storage the oxygen stoichiometry of the  $\text{UO}_2$  powders was found to change with time, plausibly due to the facile oxidation of these nc powders. All the powders possessed a flaky morphology and comprised agglomerates of nanocrystallites of  $\alpha\text{-U}_3\text{O}_8$  or  $\text{UO}_2$ . The morphology and microstructure of the powders derived from the mixture with the R value of 0.25 were very different from the rest. HRTEM investigations reaffirmed the nanocrystallinity and revealed the presence of faceted nano crystallites and nano pores. The EELS study confirmed the covalency as expected.

It was observed that the  $\rho_B$ , XCS, size distribution of pores and particles, morphology of the powders and their microstructure showed a strong dependence on the value of R. The variation in the bulk density with R and its correlation with the size distribution of particles were investigated. For the first time an attempt was made to de-convolute the particle size distribution data. The contributions from the different size fractions were found to correlate well with the  $\rho_B$ .

The variation in lattice strain in nc-UO<sub>2</sub> derived through citrate gel-combustion and its dependence on size is being reported for the first time. Two distinct regimes viz., nc regime and the microcrystalline regime could be delineated by analyzing the variation in the lattice strain with the XCS. Further analytical models are required, in order to understand the relation between the lattice strain and the distribution of sizes. It appears that the combustion mixtures with R values ranging from 0.25 to 0.50 would yield powders that are most suitable further processing.

Elucidation of a reaction mechanism for the combustion synthesis of uranium oxide was carried out for the first time. The sample gels were analyzed by using TG-DTA-MS and DSC. Three exothermic peaks were observed in both the DTA and DSC analyses. The proposed reaction mechanism was supported by the mass spectrometric analysis of the evolved gases. The  $E_a$  estimated for the first two thermal events were  $152 \pm 6$  and  $179 \pm 8$  kJ mol<sup>-1</sup> respectively. The  $E_a$  for the third thermal event (crystallization of U<sub>3</sub>O<sub>8</sub>) was found to be  $166 \pm 7$  kJ mol<sup>-1</sup>. In this study gels with a fuel to oxidant ratio of 0.25 were investigated. However, the reaction mechanisms and the activation energies will depend on the fuel (citric acid) to oxidant (nitrate) ratio of the gels. Further investigations are required to study the systematic variation of citrate gel-combustion of urania with different fuel to nitrate ratio (R).

Systematic investigation on sintering of nc-UO<sub>2</sub> powders derived through citrate gel-combustion method was carried out for the first time. Sintering was carried out by using three different methods, viz., i) conventional method, ii) low temperature two-step sintering (LTTSS<sub>1</sub>) and iii) low temperature two-step sintering (LTTSS<sub>2</sub>). Among these two-step sintering LTTSS<sub>2</sub> was found most suitable. Powders derived from starting mixtures with an R value of 0.10 and 0.25 were found to be highly sinterable and yielded a maximum sintered density of  $\approx 98$  % T.D with uniform grains. Through optimization trials, 180 MPa and LTTSS<sub>2</sub> were found to be the

ideal conditions to obtain high density  $\text{UO}_2$  pellets. Shrinkage anisotropy factor ( $\alpha$ ) of sintered  $\text{UO}_2$  monoliths were investigated for the first time. Relative size fraction of open and closed pore fraction of sintered  $\text{UO}_2$  monoliths were also investigated. The method employed in this study has led to a new fabrication procedure which would be energy and cost efficient for obtaining  $\text{UO}_2$  pellets with a uniform grain size of about 1-10  $\mu\text{m}$ .

## **8.2 Preparation of $\text{UO}_2$ foam and porous $\text{UO}_2$ pellets**

$\text{UO}_2$  foam was successfully prepared for the first time by using a sucrose-gel precursor. This comprised both meso and macro pores and possessed good handling strength. However, the presence of large amounts of carbon residue would limit their utility for the intended application, viz., DOR, owing to the electronic conductivity brought about by carbon. Typically 30 to 40% porosity would be ideal for the DOR process. However, the densities of these foams are far lower than the optimum value suitable for the end use.

A fuel to oxidant ratio (R) of 0.25, a CP of 180 MPa and a  $\text{TSS}_3$  with a maximum temperature of 1473 K were found to be the optimum conditions for obtaining a product with a desirable density of about 60 to 70 % T. D.

## **8.3 Synthesis, Characterization and Sintering of Nanocrystalline Thoria**

Nc- $\text{ThO}_2$  powders were prepared by using citrate gel-combustion method in bulk quantities by varying the fuel to nitrate mole ratio ( $R = 0$  to 0.50). The systematic dependence of the properties of nc- $\text{ThO}_2$  powders on R was investigated. It was observed that the  $\rho_B$ , SSA, PSD, XCS and lattice strain showed a systematic dependence on the R value. The combustion reaction in the mixture with an R value of 0.50 was investigated with DTA, DSC and mass spectrometry. Direct evidence for the consumption of oxygen during combustion is being reported for the first time. It was observed that the mixture with R values 0.13 and 0.17 exhibited

vigorous and moderate volume combustion respectively. Microstructural investigations revealed that the volume combustion derived thorium powders were porous and comprised aggregates of nanograins. TEM investigation reaffirmed their nanocrystallinity. For the first time, EELS investigation was carried out on the nc-ThO<sub>2</sub> powders and the branching ratio (B) was calculated for both the “as prepared” and “calcined” powders. No evidence could be obtained for the existence of thorium in multiple oxidation states. TEM investigations also revealed that the nc-ThO<sub>2</sub> comprised unimodal grain size distribution with their size ranging between 6 - 16 nm with maxima at 10 nm.

It was observed that the volume combustion derived nc-ThO<sub>2</sub> powders were highly sinterable. A compaction pressure of 243 MPa and TSS with a final sintering temperature of 1773 K were found suitable to sinter the compacts prepared from T<sub>C</sub>13C powders to a  $\rho_s$  of  $98.8 \pm 0.3$  % T.D. Microstructural analysis of polished and thermally etched sintered thorium monoliths revealed that they comprised uniform faceted grains with well-defined grain boundaries. For the first time, sintering anisotropy factor ( $\alpha$ ) was estimated and it revealed that the ThO<sub>2</sub> compacts had undergone near isotropic shrinkage during sintering. This work describes a cost and energy efficient method for the production of high density pellets and small crucibles from nc-ThO<sub>2</sub>.

#### **8.4 Synthesis, Conventional Sintering and SPS of Nanocrystalline Yttria**

It was demonstrated for the first time that VCR takes place in mixtures containing yttrium nitrate with citric acid with an R value of 0.17. The powders derived through VCR were found to be nanocrystalline, fine grained and highly porous.

All the powders comprised nc aggregates. It was demonstrated that the  $\rho_B$ , SSA, PSD, XCS and the morphology of these powders were unique as compared to the powders derived through other methods reported in the literature [1-13]. Microstructural analysis of the “A”

powders carried out by using TEM confirmed the presence of nc c-Y<sub>2</sub>O<sub>3</sub>. Both TEM and SEM investigations revealed that these powders possessed nano pores.

The calcined products were found to be highly sinterable. It was demonstrated that Y<sub>2</sub>O<sub>3</sub> pellets with a density as high as  $98.9 \pm 0.1$  % T. D. could be produced by using the “two-step sintering” method (TSS<sub>1</sub><sup>Y</sup>) at a final temperature as low as 1673 K. Shrinkage anisotropy factor ( $\alpha$ ) and relative pore fraction of sintered Y<sub>2</sub>O<sub>3</sub> were linearly correlated with the compaction pressure. Similarly, it was observed that citrate gel-combustion derived nc-Y<sub>2</sub>O<sub>3</sub> could be sintered to a density of  $99.3 \pm 0.2$  % T. D by using SPS (1873 K 7 min; 50 MPa and grain size: 6-12  $\mu$ m).

### **8.5 Salient features of the results obtained from citrate gel-combustion synthesis of nc-urania, nc-thoria and nc-yttria**

Nc-urania nc-thoria and nc-yttria powders were synthesized by using citrate gel-combustion in bulk quantities (about 30 - 60 g) for the first time. The systematic dependence of the reaction as well as the properties of these nc powders on the composition of the combustion mixture (R) was investigated. Thermal analysis of citrate gels containing thorium nitrate or uranyl nitrate were carried out with the help of DSC for the first time (nc-urania and nc-thoria). These results showed that the rate of this reaction is strongly influenced by the composition of the combustion mixture (R). It was demonstrated for the first time that “volume combustion reaction” takes place in citrate gels containing thorium nitrate, yttrium nitrate and uranyl nitrate with citric acid at an R value of 0.125, 0.17 and 0.25 respectively.

It was observed that the  $\rho_B$ , XCS, size distribution of pores and particles, morphology of the powders and their microstructure showed a strong dependence on the value of R. The morphology and microstructure of the powders through volume combustion were very different

from the rest. HRTEM investigations reaffirmed the nanocrystallinity of the final products and revealed the presence of faceted nano crystallites and nano pores in them. The variation in the  $\rho_B$  with R and its correlation with the size distribution of particles were investigated. For the first time an attempt was made to de-convolute the particle size distribution data. It was observed that the number of modes in size distribution of particles had a correlation with the  $\rho_B$  value. The  $\rho_B$  of the powders with tetra modal and trimodal distributions was higher than that of the bimodal powders. Variation in the lattice strain in these nc-powders and their correlation with the XCS is being reported for the first time. Two regimes could be delineated (nc-urania) viz., nc regime and microcrystalline regime wherein the former exhibited a higher lattice strain even after annealing at higher temperature while the latter exhibited the conventional microcrystalline powder property.

Systematic investigation on sintering of nc powders derived through citrate gel-combustion method was carried out by using three different methods, viz., i) conventional method - CS, ii) two-step sintering - TSS<sub>1</sub> and iii) TSS<sub>2</sub>. For the first time, shrinkage anisotropy factor ( $\alpha$ ) pertaining to the sintering of compacts made out of nc UO<sub>2</sub>, ThO<sub>2</sub> and Y<sub>2</sub>O<sub>3</sub> was estimated. It was established that these compacts had undergone near isotropic shrinkage. The method employed in this study has led to a new fabrication procedure which would be energy and cost efficient for obtaining highly sintered pellets (UO<sub>2</sub>, ThO<sub>2</sub> and Y<sub>2</sub>O<sub>3</sub>) with uniform grain size.

## 8.6 Salt melt synthesis and sintering of nc-HfO<sub>2</sub> and nc-YSH

A procedure based on the salt melt synthesis that employed molten mixtures of KNO<sub>3</sub> and NaNO<sub>3</sub> along with different amounts of NaNO<sub>2</sub> was optimized to obtain nc m-HfO<sub>2</sub>, c-HfO<sub>2</sub> and YSH powders in bulk, with fine grain size and uni-modal size distribution of particles. It was

also demonstrated that either the metastable cubic form or the thermodynamically stable monoclinic form could be derived at room temperature by tailoring the composition of the melt. It was also observed that the yttrium content (for YSH preparation) and nitrite content (for HfO<sub>2</sub> preparation) significantly influence the powder characteristics. The SSA and lattice strain of nc-HfO<sub>2</sub> decreased with the nitrite content while the XCS showed a reverse trend. Microstructural analysis of m-HfO<sub>2</sub> and c-HfO<sub>2</sub> powders by using TEM reaffirmed their nanocrystallinity as well as their crystallite size estimated from XRD (20–40 nm). Further, XRD, TEM and Raman spectra ascertained that the starting mixtures with  $\Phi$  values of 0–0.32 and 0.82 yielded m-HfO<sub>2</sub> and c-HfO<sub>2</sub> respectively. Comparison of the Raman spectra pertaining to both microcrystalline and nc samples (HfO<sub>2</sub>) revealed that the latter exhibited broader peaks due to quantum confinement. EELS of m-HfO<sub>2</sub> ( $\Phi = 0$ ) and c-HfO<sub>2</sub> ( $\Phi = 0.82$ ) were consistent with the observations reported in earlier investigations [14–17]. Direct evidence in support of the presence of Hf in an oxidation state lower than 4+ could not be obtained.

In the nc-YSH derived through SMS, SSA, XCS, lattice strain and lattice parameter increased with the yttrium content while the BD showed a reverse trend. TEM investigations reaffirmed the presence of nanograins with unimodal size distribution and SAED further ascertained the presence of fluorite solid solution.

All nc HfO<sub>2</sub> and YSH powders exhibited monotonic increase in  $\rho_G$  with the CP. A CP of 353 MPa was required to compact and sinter hafnia to a  $\rho_S$  of about  $\approx 97$ –98 % T.D by using TSS<sub>2</sub> method. Point scan and area mapping for constituent elements in the YSH powders and sintered monoliths confirmed the presence of uniform distribution of yttrium and hafnium. Morphological analysis of polished and thermally etched sintered monoliths of HfO<sub>2</sub> and YSH revealed the presence of uniform grains with well-defined grain boundaries. The dihedral angle

in sintered hafnia YSH monoliths was found to be varying between  $121\text{-}127^\circ$  and  $109\text{-}130^\circ$ . Shrinkage anisotropic factor revealed that the both hafnia and YSH compacts had undergone near isotropic shrinkage.

Small crucibles could be made out of both 10YSH and 30YSH by die casting and could be sintered to high densities and were devoid of cracks and physical defects. Selected powders of  $\text{HfO}_2$  and YSH were used in the fabrication of cups and the compatibility of these cups with molten U at 1405 K was tested. These investigations revealed that these could be used for U metal melting since the cups were compatible with molten U at 1420 K.

### **8.7 Spark Plasma Sintering of nc- $\text{HfO}_2$ and nc-YSH**

SPS of nc- $\text{HfO}_2$  (SMS) and nc-YSH (SMS) was carried out for the first time to prepare dense pellets. Nc-  $\text{HfO}_2$  and nc-YSH revealed a maximum sintered density of 98.8% and 97.3% T.D. respectively. SEM investigation revealed that the grain sizes were varying from 9 - 25  $\mu\text{m}$  (both  $\text{HfO}_2$  and YSH). However, further optimization of experimental parameters is required in order to obtain nanograined monoliths ( $\text{HfO}_2$  and YSH) by using SPS.

### **8.8 Scope for future work**

These investigations suggest that the following studies could be taken up in future:

- Further experiments need to be carried out with the porous pellets prepared by the method reported here. This warrants further optimization trails for the preparation of porous  $\text{ThO}_2$  and  $\text{UO}_2$  pellets.
- The kinetics of gel-combustion reaction of  $\text{Th}^{4+}$  containing gels had not been investigated so far. This needs to be taken up.



- In order to understand the coarsening and densification in nc powders vis-à-vis their microcrystalline counterparts, further dilatometry experiments need to be taken up on the sintering of nc powders.
- Only preliminary trials have been carried out on the SPS of nc-HfO<sub>2</sub> and nc-YSH. Even though substantial reduction in grain growth has been achieved, nanograined (< 100 nm) monoliths could not be prepared. Further optimization trials need to be undertaken, in order to accomplish the same.
- Effect of nitrite to nitrate mole ratio and the influence of yttrium content on the stability of nanocrystalline YSH structures could be investigated.
- The effect and the influence of salt mixtures containing chlorides, nitrate and/or nitrite of lithium, sodium and/or potassium on the formation of nanocrystalline metastable hafnia and YSH powders could be investigated.
- Experiments pertaining to the utility of sintered hafnia and YSH crucibles with more reactive uranium bearing alloys could be taken up.
- Mechanical properties of sintered compacts viz., ductility, hardness, impact resistance, and fracture toughness could be compared with their respective microstructures.
- Further, the mechanical properties of sintered monoliths derived by using different processing techniques could also be compared.

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